

Letter

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Design of Core-Pd/Shell-Ag Nanocomposite Catalyst for Selective Semihydrogenation of Alkynes

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Abstract

We designed core-Pd/shell-Ag nanocomposite catalyst (Pd@Ag) for highly selective semihydrogenation of alkynes. The construction of the core-shell nanocomposite enables a significant improvement in the low activity of Ag NPs for the selective semihydrogenation of alkynes because hydrogen is supplied from the core-Pd NPs to the shell-Ag NPs in a synergistic manner. Simultaneously, coating the core-Pd NPs with shell-Ag NPs results in efficient suppression of overhydrogenation of alkenes by the Pd NPs. This complementary action of core-Pd and shell-Ag provides high chemoselectivity toward a wide range of alkenes with high *Z*-selectivity under mild reaction conditions (room temperature and 1 atm H₂). Moreover, Pd@Ag can be easily separated from the reaction mixture and is reusable without loss of catalytic activity or selectivity.

<u>Keyword</u>

core-shell, silver, palladium, semihydrogenation, alkyne

Text

Nano-structured composites with a core (inner material) and shell (outer layer) structure, so-called core-shell materials, have attracted enormous attention as highly

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functionalized nanoarchitectures in diverse areas such as sensors¹, quantum dots², photonic crystals³, and catalysts⁴. The extensive study on design of core-shell materials stems from their own intriguing characteristics, including optical, electronic, and chemical properties. In the field of the catalyst design, core-shell nanoparticles have exhibited unique and promising properties, such as high stability against sintering^{4d}, high activity through maximization of core-shell interfacial interaction^{4b}, and multi-functionalized catalysis for one-pot tandem reaction through accumulation of different active species in the core and shell^{4c}. Fine-tuning the composition and morphology of such composites will enable rational design of novel core-shell nanoparticle catalysts with fascinating tailored activities.

The semihydrogenation reaction, which converts alkynes to alkenes, is one of the most important and fundamental reactions in manufacturing processes of bulk and fine chemicals⁵. In this context, Lindlar catalyst (Pd/CaCO₃ treated by Pb salts) has been a good first port of call in the synthesis of diverse alkenes⁶. However, the Lindlar catalyst has serious drawbacks such as high toxicity of Pb species and the low alkene selectivity when employing terminal alkynes due to the rapid overhydrogenation of terminal alkenes to alkanes. Therefore, the development of the alternative Pb-free catalysts using Pd⁷, Ni⁸, Cu⁹, Ru¹⁰ and Au¹¹ have been extensively studied.

It is well known that unmodified Pd NPs inherently shows high catalytic activity for hydrogenation of alkynes, but low selectivity for alkenes due to overhydrogenation. In contrast, Ag NPs has extremely low catalytic activity for semihydrogenation, requiring high temperature or high H₂ pressure, despite intrinsically showing high alkene-selectivity due to the rather weak complexation of Ag with alkenes¹². In consideration of beneficial properties of Pd and Ag NPs, we anticipated that the construction of a bimetallic core-shell nanocomposite catalyst consisting of Pd NPs in the core and Ag NPs in the shell (Pd@Ag) would address the trade-off between activity and selectivity for Pd and Ag NPs in semihydrogenation. Our design concept of Pd@Ag represents the building of a compatible relationship between Pd, with its high activity, and Ag, with its high alkene-selectivity, by construction of a core-shell structure. Pd NPs in the core store hydrogen to form palladium-hydride (PdH)¹³ through the H₂-permeable Ag shell nano-layer¹⁴. The inner PdH serves hydrogen to the outer Ag shell, providing the Pb-free and selective semihydrogenation of alkynes occurring on the Ag surface. Simultaneously, coating the Pd NPs by a Ag layer results in efficient suppression of the overhydrogenation of alkenes at the Pd surface. This complementary action of Pd and Ag, in which the advantages of Pd and Ag are integrated while their

disadvantages are remedied in a synergistic manner, allows selective semihydrogenation under mild reaction conditions (Figure 1).

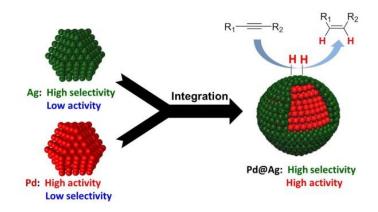


Figure 1 Design concept of complementary bimetalic core-Pd/shell-Ag catalyst for selective semihydrogenation of alkynes

Pd@Ag was synthesized by the seeding method (for details, see Supporting Information). Pd NPs with a mean diameter of 24.1 ± 5.7 nm were synthesized by reduction of Pd(acac)₂ in the presence of polyvinyl alcohol (PVA), with ethylene glycol as a solvent and reducing reagent. Next, the resulting Pd NPs were used as seeds for the formation of Pd@Ag by reduction of AgNO₃, with different Ag/Pd ratios (Ag/Pd = 0.10, 0.15, 0.20, 0.25, 0.50), using ascorbic acid in water. Hereafter, the resulting Pd@Ag catalysts are denoted Pd@Ag-X, where X is the Ag/Pd ratio.

Representative images of Pd@Ag-0.20 observed by transmission electron microscopy (TEM) and high-angle annular dark-field STEM (HAADF-STEM) are depicted in Figure 2. It can be seen that the NPs had a mean diameter of 26.2 ± 5.7 nm (Figure 2a). In the HAADF-STEM image of Pd@Ag, well-defined lattice fringes were observed (Figure 2b). The detected lattice fringes had d-spacing attributed to Ag {111} (2.36 Å) and Ag {200} (2.04 Å). This fact indicates that crystalline Ag grows on the surface of Pd NP seed. The elemental distribution of Ag on the Pd NPs in Pd@Ag (Figure 2c) was examined by scanning TEM (STEM) coupled with energy-dispersive X-ray spectroscopy (EDX) (Figures 2d, e, and f). Elemental mapping of Pd@Ag based on quantification analysis of EDX spectra clearly revealed that it comprised Pd NPs in the core and a nano-layer of Ag with a thickness of ca. 1 nm in the shell. The formation of a thin shell of Ag manoparticles or an alloy of Ag and Pd was observed around 35–50°



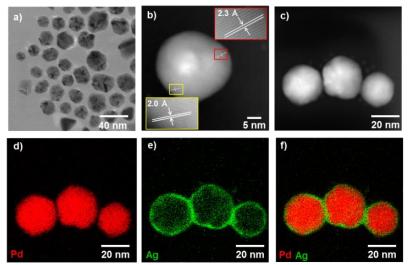


Figure 2 Composition and structural analysis of Pd@Ag-0.20. a) TEM image. b) and c) HAADF-STEM images. Elemental mapping images of d) Pd and e) Ag. f) Composite overlay image formed from d) and e).

After loading onto hydroxyapatite (HAP) which was chosen due to easy handling and to ensure high dispersion, the Pd@Ag-X composites were used as catalysts in the batchwise semihydrogenation of 1-octyne (1) at room temperature under atmospheric pressure of H_2^{15} . In order to compare catalytic activity, both single Pd NPs (Pd seed for Pd@Ag) and Ag NPs loaded on HAP were prepared. The results are shown in Table 1. Pd NPs promoted rapid overhydrogenation, quantitatively giving the undesired product *n*-octane (3) (Table 1, Entry 1). Ag NPs did not show any catalytic activity under the conditions used (Table 1, Entry 2). As previously reported^{12b}, highly alkene-selective catalysis of Ag NPs was confirmed under high pressure of H_2 (50 atm), although with extremely low activity (turnover frequency = 0.035 h^{-1}) (Table 1, Entry 3). In contrast, the various Pd@Ag-X composites showed differing activity and selectivity toward 2 depending on the value of X. When the Ag/Pd ratio X was increased from 0.10 to 0.20, alkene-selectivity steadily increased (Table 1, Entries 4-6), with Pd@Ag-0.20 exhibiting the highest catalytic activity, affording 2 in quantitative yield (Table 1, Entry 6). Upon a further increase in the Ag/Pd ratio to 0.50, complete alkene-selectivity was retained but the activity of the catalyst gradually decreased (Table 1, Entries 8 and 9). Interestingly, the excellent alkene-selectivity of Pd@Ag-0.20 was maintained even when the reaction time was prolonged after full conversion of 1 (Figure S16). Notably, the C=C bond of 2 remained almost intact up to a H_2 pressure of 50 atm (Table 1, Entry 7). This high performance of Pd@Ag-0.20 arising from the core-shell structure is in sharp contrast with many previous catalysts, including the Lindlar catalyst and Pd-Ag alloys, which easily causes overhydrogenation of terminal alkenes to alkanes¹⁶.

Hex $ Hex Hex Hex H_2$ (1 atm), r.t.		Hex 🔦 2	Hex $\widehat{}_3$		
Entry	Catalyst	Time [h]	Conv. [%]ª	2 [%] ^a	3 [%] ^a
1	Pd NPs	0.5	>99	0	>99
2 ^b	Ag NPs	2.5	0	-	-
3 ^c	Ag NPs	20	36	36	0
4	Pd@Ag-0.10	2.5	>99	23	76
5	Pd@Ag-0.15	2.5	>99	80	19
6	Pd@Ag-0.20	2.5	>99	>99	0
7 ^d	Pd@Ag-0.20	1.0	>99	>99	0
8	Pd@Ag-0.25	2.5	65	65	0
9	Pd@Ag-0.50	2.5	22	22	0

Table 1 Semihydrogenation of **1** using various Pd-Ag catalysts

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Reaction conditions: Catalyst (0.10 g, Pd: 0.33 mol%, Ag: 0.033 mol%-0.17 mol%), **1** (0.3 mmol), EtOH (2 ml). ^aDetermined by GC using internal standard technique. ^bAg/HAP (Ag: 0.33 mol%). ^cAg/HAP (Ag: 50 mol%), H₂ (50 atm). ^dH₂ (50 atm).

The catalytic potential of Pd@Ag-0.20, which exhibited the best performance, was investigated using various alkynes in a batch reactor. A wide range of terminal and internal alkynes containing functional groups such as hydroxyl, carboxylic acid, ester, amine, cyano, and halogen groups were smoothly converted to the corresponding alkenes with >99% selectivity (Table 2). After the reaction, the Pd@Ag catalyst loaded onto HAP was easily recovered by filtration, and proved to be reusable, retaining its high activity and selectivity during five recycling experiments, which demonstrates its high durability (Table 2, Entry 2). We also examined the practical utility of Pd@Ag by using a plug flow reactor for gram-scale synthesis. When **1** (10 mmol, 1.10 g) in ethanol (0.10 M) was passed through a Pd@Ag-0.20-packed column reactor at a flow rate of 4.2 mL h⁻¹ along with H₂ at atmospheric pressure, **2** was successively obtained in over 99% yield (96% isolated yield; 1.07 g).

Entry	Product	Time	Conv.	Yield	E/Z
		[h]	[%] ^a	[%] ^a	[%] ^a
1		2.5	>99	>99 (95)	-
2 ^b	Hex ́	2.5	>99	>99	-
3	HO()2	1.0	>99	>99 (93)	-
4	$CI \left(\frac{1}{3} \right)$	1.5	>99	>99 (91)	-
5	HO ₂ C	3.0	>99	>99 (92)	-
6	NC	3.0	>99	>99 (93)	-
7 ^c		14	>99	>99 (92)	-
8	Ph	3.0	>99	>99 (96)	-
9	Ph	3.0	>99	>99 (95)	-
10	Pr	4.0	>99	>99 (94)	0/100
11	Ph	4.0	>99	>99 (98)	0/100
12	Et	5.0	>99	>99 (94)	0/100
13	Pr OH	5.5	>99	>99 (94)	0/100
14	CO ₂ Et	5.0	>99	>99 (91)	4/96
15 ^d	EtO ₂ C CO ₂ Et	12	>99	>99 (92)	16/84
16	Hex NEt2	15	>99	>99 (93)	0/100

 Table 2 Semihydrogenation of various alkynes

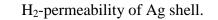
Reaction conditions: Pd@Ag-0.20 (0.10 g, Pd: 0.33 mol%, Ag: 0.066 mol%), alkyne (0.3 mmol), EtOH (2 mL). ^aDetermined by GC using internal standard technique. Values in parentheses are isolated yields. ^b5th reuse. ^cHexane (2 mL). ^d50 ^oC.

To elucidate the reasons for the significant differences in the performance of Pd@Ag-X depending on X, the shell effect of Ag was investigated by CO adsorption FTIR spectroscopy (Figure S13). It is well known that CO is not adsorbed onto the Ag NP surface but is strongly adsorbed on Pd NPs¹⁷. In fact, when single Ag NPs and Pd NPs were treated with CO, no CO adsorption peaks were observed for Ag NPs, while

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two CO adsorption peaks derived from CO stretching at 1930 cm⁻¹ and 2060 cm⁻¹ were observed for Pd NPs. IR spectra of Pd@Ag-0.10 and Pd@Ag-0.15 treated with CO showed two peaks in the same position as for single Pd NPs. On the other hand, it is notable that Pd@Ag-0.20, Pd@Ag-0.25, and Pd@Ag-0.50 showed no CO adsorption peaks, demonstrating that the Pd NPs were entirely covered by Ag in a core-shell structure. These results showed that the low alkene-selectivity of Pd@Ag-0.10 and Pd@Ag-0.15 was strongly associated with the presence of the exposed Pd NPs, causing overhydrogenation. The steadily decreasing activity of Pd@Ag-X as X increased from 0.20 to 0.50 was explained by the increase in thickness of the Ag shell, which hinders the supply of hydrogen from the core-Pd NPs to the surface Ag sites. TEM images of Pd@Ag supported the contention that the thickness of the Ag shell could be controlled by changing the amount of Ag used. The mean diameters of Pd@Ag-X, where X was 0.10, 0.15, 0.20, 0.25, and 0.50, were 25.2 ± 4.0, 25.9 ± 4.9, 26.2 ± 5.7, 26.6 ± 5.9, and 27.0 ± 4.5 (Figure S1–S4, S6, and S7).

Among noble metals, Ag nanocrystals have uniquely bifunctional properties with not only the alkene-selective catalysis but also the high activity for surface-enhanced Raman spectroscopy (SERS), allowing in-situ monitoring of Ag-catalyzed surface reaction. Therefore, we investigated the Pd@Ag-catalyzed semihydrogenation by SERS. Figure 3(A) shows SERS spectra from ethanol suspension of Pd NPs and Pd@Ag in the presence of phenylacetylene (PA) as a Raman probe. No peaks of PA (0.12 mM) without nanoparticles or with Pd NPs were confirmed (Figure 3A (a) and (b)). Interestingly, when the colloidal Pd@Ag was dropped into the ethanol solution of PA, new peaks at 1980 cm⁻¹ (C=C stretching mode) and 1590 cm⁻¹ (benzene ring mode) appeared, demonstrating the SERS activity of Pd@Ag (Figure 3A (c)). The shift in the peak at 2111 cm⁻¹ for the C=C stretching of free PA to 1980 cm⁻¹ is assigned to surface adsorption of PA on Ag (Figure 3A (c) vs. (d)), in agreement with previous finding¹⁸. Moreover, the SERS activity of Pd@Ag enabled the in-situ monitoring of the Pd@Ag-catalyzed semihydrogenation of PA. After adding Pd@Ag to the PA solution under atmospheric H₂ conditions, the SERS spectrum was recorded (Figure 3B). The peaks attributed to the PA adsorbed on the surface of Ag gradually decreased during the semihydrogenation of PA, supporting that the semihydrogenation undergoes on the surface of Ag shell of Pd@Ag where the Pd core serves as a hydrogen source due to the formation of a PdH species. The formation of the PdH was confirmed by XRD analysis (Figure S12) where the XRD peaks attributed to Pd core of Pd@Ag shifted to low-angle side under H₂ atmosphere. Furthermore, the H₂-D₂ exchange experiment using Ag NPs catalyst (Scheme S2) revealed the formation of HD, indicating the possibility for



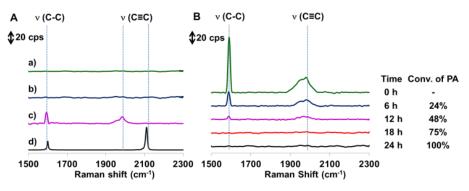


Figure 3 (A) Raman spectra recorded from ethanol suspension of nanoparticles in the presence of PA: a) 0.12 mM PA, b) 0.12 mM PA with Pd NPs, c) 0.12 mM PA with Pd@Ag-0.20 and d) reference PA (intensity: 1/500). (B) SERS spectra recorded during the semihydrogenation of PA catalyzed by Pd@Ag-0.20 at r. t. under 1 atm of H₂.

In conclusion, we designed core-Pd/shell-Ag nanocomposite catalysts (Pd@Ag) whose components acted in complementary fashion to achieve Pb-free and highly selective semihydrogenation of alkynes under mild reaction conditions. The Pd@Ag catalyst (loaded on HAP) was reusable and applicable to use in a plug flow reactor. It was found that the core-Pd enhanced the activity of the shell-Ag by serving as a hydrogen source, while, at the same time, the shell Ag reduced the intrinsically low alkene-selectivity of Pd by inhibiting contact between Pd and alkenes. As a whole, the complementary relationship between Pd and Ag derived from the core-shell arrangement resulted in highly active and selective catalysis in the semihydrogenation of alkynes.

Supporting Information

Experimental details and characterization of catalysts. This material is available free of charge via the Internet at http://pubs.acs.org.

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[15] We chose hydroxyapatite as support which results in highest efficiency among the tested supports. See, Section 5 in the supporting information for details.

[16] It is reported that Pd-Ag alloy showed high selectivity for the semihydrogenation of acetylene in excess ethylene where small ensemble sites of the Pd-Ag alloy are effective. We prepared the Pd-Ag alloys with small ensemble sites and tested them in the hydrgeneation of 2 under the same reaction condition. The comparison between

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Pd@Ag and the Pd-Ag alloys was discussed, see the section 6 comparison between Pd@Ag and conventional catalysts in the Supporting Information. For Pd-Ag alloy in semihydrogenation, see: (a) Johnson, M. M.; Walker, D. W.; Nowack, G. P. (Phillips Petroleum Company), US 4404124, **1983**. (b) Thanh, C. N.; Didillon, B.; Sarrazin, P.; Cameron, C. (Institut Francais du Petrole), US 5648578, 1997. (c) Zhang, Q.; Li, J.; Liu, X.; Zhu, Q. Appl. Catal. A: Gen. 2000, 197, 221-228. (d) Lamb, R. N.; Ngamson, B.; Trimm, D. L.; Gong, B.; Silveston, P. L.; Praserthdam, P. Appl. Catal. A: Gen. 2004, 268, 43-50. (e) Zea, H.; Lester, K.; Datye, A. K.; Rightor, E.; Gulotty, R.; Waterman, W.; Smith, M. Appl. Catal. A: Gen. 2005, 282, 237-245. (f) Huang, W.; Pyrz, W.; Lobo, R. F.; Chen, J. G. Appl. Catal. A: Gen. 2007, 333, 254-263. (g) Lamberov, A. A.; Il'yasov, S. R.; Gil'manov, Kh.; Trifonov, S. V.; Shatilov, V. M.; Ziyatdinov, A. Sh. Kinet. Catal. 2007, 48, 136-142. (h) Ahn, I. Y.; Lee, J. H.; Kim, S. K.; Moon, S. H. Appl. Catal. A: Gen. 2009, 360, 38-42. (i) Lee, J. H.; Kim, S. K.; Ahn, I. Y.; Kim, W.-J.; Moon, S. H. Catal. Commun. 2011, 12, 1251-1254. (j) Pachulski, A.; Schödel, R.; Claus, P. Appl. Catal. A: Gen. 2011, 400, 14-24. (k) Zhang, Y.; Diao, W.; Williams, C. T.; Monnier, J. R. Appl. Catal. A: Gen. 2014, 469, 419-426. (1) Pei, G. X.; Liu, X. Y.; Wang, A.; Lee, A. F.; Isaacs, M. A.; Li, L.; Pan, X.; Yang, X.; Wang, X.; Tai, Z.; Wilson, K.; Zhang, T. ACS Catal. 2015, 5, 3717-3725.

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Graphic Abstract

