## Iridium Catalysis

## Selective Catalytic Transfer Dehydrogenation of Alkanes and Heterocycles by an Iridium Pincer Complex\*\*

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**Abstract:** Catalytic alkane dehydrogenation is a reaction with tremendous potential for application. We describe a highly active PSCOP-pincer iridium catalyst for transfer dehydrogenation of cyclic and linear alkanes. The dehydrogenation of linear alkanes occurs under relatively mild conditions with high regioselectivity for  $\alpha$ -olefin formation. In addition, the catalyst system is very effective in the dehydrogenation of heterocycles to form heteroarenes and olefinic products.

he selective functionalization of abundant alkanes to form value-added products is an attractive, but highly challenging, task. Among the few reported transformations of alkanes, catalytic alkane dehydrogenation (AD) has received significant attention, because it converts low-value hydrocarbon feedstocks into olefins and arenes, which are important intermediates in organic synthesis and widely used as raw materials in many industrial processes. Heterogeneous AD is carried out on a large-scale in the petrochemical industry; however, such processes typically operate at very high temperatures (>500 °C) and afford low product selectivities.<sup>[1]</sup>

Pioneered by Crabtree and Felkin,<sup>[2]</sup> numerous homogenous AD catalysts, mainly the group 9 metal complexes, have been developed in the past three decades.<sup>[3]</sup> A major breakthrough in homogenous AD was the report of bis(phosphine) (PCP)Ir pincer catalysts for dehydrogenation of cyclic and linear alkanes by Kaska, Jensen, and Goldman.<sup>[4]</sup> Following that, the Brookhart group reported the isostructural bis(phosphinite) (POCOP)Ir pincer complexes (Figure 1).<sup>[5]</sup> The subtle change of the linker from CH<sub>2</sub> group to an O atom leads to Ir catalysts that are somewhat more efficient than the PCP analogues in transfer dehydrogenation of cyclooctane. More recently, related (PCP)Ir complexes with metallocene backbones,<sup>[6]</sup> (PCP)Ir and (PCP)Ru complexes containing fluorinated phosphino substitutes,<sup>[7]</sup> and CCC pincer carbene-Ir complexes<sup>[8]</sup> have been developed for homogenous AD. In addition, Goldman and Brookhart have developed several Ir-pincer AD-based tandem reactions, such as alkane

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Figure 1. Structures of PCP, POCOP, and PSCOP iridium complexes.

metathesis,<sup>[3a,9]</sup> alkane dehydroaromatization,<sup>[10]</sup> and the synthesis of p-xylene from ethylene.<sup>[11]</sup>

Despite tremendous progress in the field of homogenous AD, the reported catalytic systems suffer from harsh reaction conditions (150-250 °C) and the lack of regioselectivity in the dehydrogenation of acyclic alkanes.<sup>[3b]</sup> Furthermore, poor functional-group compatibility of these homogenous catalysts restricts the application of catalytic dehydrogenation in the synthesis of fine chemicals. Herein, we report the preparation of a PSCOP-type Ir pincer complex supported by a hybrid phosphinothious/phosphinite pincer ligand (Figure 1). The (*i*Pr<sub>4</sub>PSCOP)Ir complex exhibits very high catalytic activity for transfer dehydrogenation of cyclic alkanes.<sup>[12]</sup> It effects dehydrogenation of linear alkanes under mild conditions and affords excellent regioselectivity for a-olefin formation. This new system can be applied to the selective dehydrogenation of a variety of heterocycles to access heteroatom-containing aromatic or olefinic compounds.

The synthesis of (*i*Pr<sub>4</sub>PSCOP)IrHCl complex **3** is outlined in Scheme 1. Deprotonation of *meta*-mercaptophenol with NaH, followed by diphosphorylation with chlorodiisopropyl-



Scheme 1. Synthesis of (iPr<sub>4</sub>PSCOP)IrHCl 3.

phosphine afforded the PSCOP ligand **4** in 66% yield. The iridium complex **3** was obtained in 50% yield through cyclometalation of the ligand with [{Ir(cod)Cl}<sub>2</sub>] (cod = 1,5-cyclooctadiene) in toluene under reflux. The <sup>31</sup>P{<sup>1</sup>H} NMR spectrum of complex **3** exhibits an AB splitting pattern, which is consistent with two nonequivalent metal-bridged P nuclei. The characteristic hydridic (IrH) resonance appears at -37.06 ppm in the <sup>1</sup>H NMR spectra, which is close to that expected for a five-coordinate Ir<sup>111</sup> hydrido chloride species with the hydride *trans* to a vacant coordination site.

Complex **3** was first tested as a precatalyst for transfer dehydrogenation of cyclooctane (COA) with *tert*-butylethy-

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lene (TBE) as the hydrogen acceptor. The COA/TBE transfer dehydrogenation is a benchmark reaction. A system containing Ir precatalyst **3** (1.3 mM), NaOtBu (1.95 mM), COA (3.9M), and TBE (3.9M, 3000 equiv relative to Ir), was heated at 200 °C under argon in a sealed vessel. The results are summarized in Table 1. Upon activation with NaOtBu, **3** 

**Table 1:** TONs for transfer dehydrogenation of COA and TBE catalyzed by complexes **3** and **2** upon activation with NaOtBu.<sup>[a]</sup>

	+ 7	[Ir]/NaC 200 °	DtBu C ►	) + 🗡	~
	COA TBE		COE	TBA	
Entry	t [min]	<b>3</b> <sup>[b]</sup>	<b>2</b> <sup>[b]</sup>	<b>3</b> <sup>[c]</sup>	<b>3</b> <sup>[d]</sup>
1	10	485	1186	937	-
2	30	1399	1423	999	-
3	60	2649	1514	_	1401
4	240	2905	1794	-	3805
5	480	2985	1876	_	5728
6	900	-	-	-	5901

[a] Average of three runs. TONs were calculated based on conversion of TBE determined by GC analysis. [b] Using a 3000:3000:1 ratio of COA/ TBE/catalyst with 3.9 m TBE. [c] Using a 4840:1000:1 ratio of COA/TBE/**3** with 1.3 m TBE. [d] Using a 6000:6000:1 ratio of COA/TBE/**3**.

was highly active for the COA/TBE transfer dehydrogenation. Catalysis with **3** gave 2649 turnovers after 1 h, and 2905 turnovers after 4 h. The process converted > 99% of TBE to TBA (2985 turnovers) after 8 h. Analysis of the dehydrogenation products by NMR spectroscopy revealed the formation of 1,3-cyclooctadiene (1,3-COD) besides the major product COE (COE/1,3-COD = 5.4:1).<sup>[13]</sup>

For comparison, we carried out catalysis in parallel with the Brookhart complex ( $tBu_4POCOP$ )IrHCl **2**, which has been reported for effective COA/TBE transfer dehydrogenation.<sup>[5b]</sup> Although the initial rate with **3** was lower than catalysis with **2** (485 turnovers with **3** in 10 min vs. 1186 turnovers with **2**), the productivity of the former is significantly higher than the latter (2985 turnovers with **3** in 8 h vs. 1876 turnovers with **2**). The initial lower turnover frequencies (TOFs) for the reaction with **3** compared to that with **2** is likely due to catalysis inhibition by TBE at high concentrations, as found for the PCP-Ir system.<sup>[4a]</sup> Indeed, we found that the concentration of the hydrogen acceptor affects the reaction rate. A run using TBE (1.3 m, 1000 equiv relative to **3**) gave 937 turnovers after 10 min, compared to 485 turnovers in the reaction with TBE (3.9 m; Table 1).

To further evaluate the catalytic efficiency of **3**, we decreased the loading of the catalyst in the COA/TBE transfer dehydrogenation. A ferrocene-based iridium pincer catalyst has been previously reported to be most active for the transfer dehydrogenation of COA; a TON of up to 3300 was obtained after 8 h at 180 °C with a COA/TBE/catalyst ratio of 21420:21420:1.<sup>[6,14]</sup> When a 6000:6000:1 molar ratio of COA/TBE/**3** was used, the reaction gave 5728 turnovers after 8 h and 5901 turnovers after 15 h at 200 °C (Table 1); more than 98% of TBE was converted to TBA in 15 h.

Next, we investigated the catalytic activity of  $\mathbf{3}$  in the transfer dehydrogenation of a linear alkane. A system

containing 3 (1.0 mм), NaOtBu (1.5 mм), TBE (0.5 м, 500 equiv relative to Ir) in an n-octane solution was heated at 200°C under argon. The reaction gave 495 turnovers after 30 min at 200°C, and TBE was fully converted into TBA within 60 min (500 turnovers) (Table 2, entry 1). As a comparison, performing the catalysis with  $(tBu_4PCP)IrH_2$  1 and (tBu<sub>4</sub>POCOP)IrHCl 2 under identical reaction conditions gave only 135 and 143 turnovers after 60 min, respectively (entries 2 and 3). The initial rate of the n-octane/TBE transfer dehydrogenation using 3 is also greater than that obtained using complexes 1 and 2 (114 turnovers with 3 in 5 min vs. 69 with 1 and 19 turnovers with 2). Additionally, the reaction conducted with a higher concentration of TBE (3.0 M, 3000 equiv relative to 3) gave 930 after 1 h and 1211 turnovers after 4 h (entry 4). On the basis of comparison with precedents,<sup>[4j]</sup> we conclude that 3/NaOtBu is among the most active systems for transfer dehydrogenation of linear alkanes.

The selective formation of valuable  $\alpha$ -olefins by alkane dehydrogenation is of fundamental interest. Goldman et al. have shown that the  $(tBu_4PCP)Ir$  complex 1 exhibits high kinetic regioselectivity for  $\alpha$ -olefin formation, but the terminal olefin can be rapidly converted into internal olefins through olefin isomerization.<sup>[4e]</sup> As shown in Table 2, after 5 min of thermolysis at 200 °C, 1-octene constitutes 33%, 51%, and 26% of the total octenes for the run with complexes 3, 1, and 2, respectively (entries 1–3). At first glance, the regioselectivity for  $\alpha$ -olefin formation with **3** appears to be significantly lower than that with 1. However, a comparison of the product distributions after the same turnovers reveals a similar regioselectivity between complexes 3 and 1. The reaction with 3 afforded 33% of 1-octene after 114 turnovers in 5 min; and the run with 1 gave 31% of 1-octene after 120 turnovers in 30 min.

Homogeneous catalysis under mild conditions is important for broad synthetic applications of alkane dehydrogenation. Given the high activity of 3 in transfer dehydrogenation of alkanes at 200 °C, we assessed its catalytic performance at lower temperatures. To our delight, complex 3 exhibits appreciable activity for the *n*-octane/TBE transfer dehydrogenation at 100°C. Significantly, it shows exceptionally high regioselectivity for  $\alpha$ -olefin formation under these conditions at low turnover numbers. As shown in Table 2, entry 5, 1octene is the sole dehydrogenation product within the first hour at 100°C (14 turnovers). After heating for 8 h (35 turnovers), 1-octene still accounts for 48% of the total octenes, and the combined percentage of 1-octene and 2octenes accounts for 100% of the total. The data imply that the 3-catalyzed isomerization of 2-octenes to 3- or 4-octenes is much slower relative to the isomerization of 1-octene to 2octenes.

The high activity and mild reaction conditions in AD encouraged us to examine the viability of the new Ir complex **3** in the dehydrogenation of heterocycles. Compared to well-documented catalytic dehydrogenation reactions of alkanes,<sup>[3b, 15]</sup> alcohols,<sup>[15]</sup> and amines,<sup>[15]</sup> examples of homogeneous catalytic dehydrogenation of heterocycles are rare. In 1997, Jensen and Kaska reported the complex **1**-catalyzed transfer dehydrogenation of tetrahydrofuan (THF) with TBE to give a mixture of dihydrofurans and furan at 200 or 150 °C.<sup>[4c]</sup> In

## Angewandte mmunications

Table 2:	Ir-catalyzed	transfer	dehydrogenation	of <i>n</i> -octane	and	TBE	at 2	200	or	100	°C. <sup>[a</sup>
				[lr] (1.0 mm)							

Table 2:	Ir-cataly	alyzed transfer dehydrogenation of <i>n</i> -octane ar <i>n</i> -octane + TBE (0.5 or 3.0 m) NaOtBu (1.5 mM) 200 or 100 °C				t 200 or 100°C. <sup>[a]</sup> s + TBA		<ul> <li>(1 mol%) gave 2-methylbenzo</li> <li>furan 5c in 67% yield after 24 h</li> <li>Transfer dehydrogenation of 1,4</li> <li>dioxane with 3 (1 mol%) select</li> </ul>	
Entry	Cat.	t [min]	TON	1-Octene	1-Octene	trans-2-Octene	cis-2-Octene	tively formed 1,4-dioxene 5d i	
				[IIIM]		[mm]	[пм]	84 % yield after 12 h; no 1,4-dioxi	
1 <sup>[c,d]</sup>	3	5	114	38	33	44	20		
		10	192	37	19	77	37	observed, even in the presence of	
		30	495	13	3	137	65	2 equiv of TBE. Dehydrogenatio	
		60	500	10	2	110	50	of THF with TBE (2 equiv) usin	
2 <sup>[c,d]</sup> 1	1	5	69	35	51	20	10	a higher catalyst loading (5 mol%	
		10	92	39	42	32	16	viold often 24 h Only a tree	
		30	120	37	31	48	23	yield after 24 h. Only a trac	
		60 135	27	27 20	64	27	2%) was observed under th		
3 <sup>[c,d]</sup> 2	2	5	19	5	26	9	4	conditions. <sup>[20]</sup> Similarly, the reactio	
		10	26	5	19	12	5	of 2-methyltetrahydrofuan selec	
		30	84	6	7	31	14	tively vielded the fully dehydroger	
		60	143	7	5	47	21	ated product 2-methylfuran (57%	
4 <sup>[c,e]</sup> 3	3	3	10	154	43	28	64	25	<b>5</b> f) after 12 h at 150 °C. In contrast
		30	539	50	9	169	85	to the good conversion observed i	
		60	930	47	5	211	109	reactions with O-heterocycle	
		240	1211	39	3	220	107	transfer dehydrogenation of tetra	
5 <sup>[f,d]</sup>	3	30	10	10	100	0	0	hydrothiophene $(4g)$ resulted i a low conversion. Because the neu	
		60	14	14	100	0	0	tral S donors are softer and mor	
		240	26	17	68	9	0	nolarizable than the neutral O do	
		480	35	17	48	11	7	polarizable than the neutral Odd	
[a] Aver	age of th	ree runs; T	ONs were	e calculated ba	ased on conversion	n of TBE, as detern	nined by GC	nois, we tentatively attribute th	

analysis. [b] The fraction of 1-octene relative to the total octenes. [c] At 200°C. [d] Ir (1.0 mm), TBE (0.5 м). [e] Ir (1.0 mм), ТВЕ (3.0 м). [f] At 100°С.

2009, Fujita and Yamaguchi reported the first example of Ircatalyzed dehydrogenation of tetrahydroquinolines.<sup>[16]</sup> Very recently, Xiao et al. demonstrated that a cyclometalated Ir<sup>III</sup> imino complex is highly efficient for acceptorless dehydrogenation of N-heterocycles.<sup>[17]</sup> To date, however, the scope of heterocycles in dehydrogenation reactions is mainly limited to benzofused N-heterocycles bearing NH functional groups.<sup>[18]</sup> Catalytic dehydrogenation of O- and S-heterocycles, and Nheterocycles without benzofusion remains to be explored.

Our preliminary results show that the (*i*Pr<sub>4</sub>PSCOP)Ir complex is capable of catalyzing dehydrogenation of a variety of O- and N-containing heterocycles (Table 3). The reactions were carried out at 120 °C, unless otherwise noted.<sup>[19]</sup> In the presence of only 0.1 mol% of 3, isochroman (4a) was readily dehydrogenated to form benzopyran (5a) in 91% yield. The dehydrogenation of 2,3-dihydrobenzofuran with TBE (1 equiv) gave benzofuran (5b) in 80% yield after 12 h. Notably, a minimal amount of 2,2'-bibenzofuran (5b'; 2%) was also detected in this reaction. This biaryl product was likely formed through dehydrogenative dimerization of 5b. When TBE (2 equiv) and 3 (5 mol %) were used, the yield of 5b' was increased to 37% and benzofuran 5b was obtained as the minor product (11%). As expected, the introduction of a methyl substituent at the 2-position of 2,3-dihydrobenzofuran prevented dimerization. However, the dehydrogenation of 2,3-dihydro-2-methylbenzofuran 4c is slower than the reaction with 4b. Treatment of 4c with TBE (2 equiv) using Ir

polarizable than the neutral O donors, we tentatively attribute the low reactivity of S-heterocycles to the high binding affinity of S atom to the Ir center, which inhibits the dehydrogenation process. (iPr<sub>4</sub>PSCOP)Ir-catalyzed transfer dehydrogenation of Nheterocycles occurred efficiently, although such substrates require a relatively high catalyst loading (1-5 mol %). Reactions of indolines, tetrahydroquinoline, and tetrahydroisoquinoline with TBE gave indoles 5h (80%) and 5I (96%), quinoline (5i; 76%), and isoquinoline (5k; 50%) in moderate to high yields. Dehydrogenations of N-heterocycles without benzofusion also occurred, albeit at relatively high temperatures (150-200°C). The conversion of piperidines to pyridines 51 (47%) and 5m (63%) is remarkable, given the fact that the products are good ligands and the build-up of pyridines may result in catalyst inhibition. N-methylpyrrole (5n) was obtained in 83% yield from *N*-methylpyrrolidine.<sup>[18]</sup> The reaction of N-(1-cyclohexenyl)pyrrolidine with TBE (4 equiv) gave N-(1-cyclohexenyl)pyrrole **50** (54%) and 1phenylpyrrole 50' (16%) after 24 h at 150°C. The results indicate Ir-catalyzed dehydrogenation of the pyrrolidine ring is more efficient than the dehydrogenation of the cyclohexenyl ring under these reaction conditions. Finally, the reaction of N-methylmorpholine with TBE (2 equiv) catalyzed by 3 (0.5 mol%) selectively formed 2,3-dehydro-Nmethylmorpholine (5p) in 82% yield; the synthesis of 5p is very challenging by other means.<sup>[21]</sup>

In conclusion, we have prepared a new phosphinothious/ phosphinite (*i*Pr<sub>4</sub>PSCOP)Ir pincer complex. Upon activation with NaOtBu, this complex exhibits exceptionally high activity for transfer dehydrogenation of alkanes with tert**Table 3:** Transfer dehydrogenation of heterocycles with TBE. The product yield was determined by <sup>1</sup>H NMR spectroscopy with 1,3,5-trimethoxybenzene as an internal standard, unless otherwise noted.



[a] With **3** (0.1 mol%) and TBE (1 equiv). [b] With **3** (5 mol%) and TBE (2 equiv). [c] With **3** (1 mol%) and TBE (2 equiv). [d] With **3** (5 mol%) and TBE (4 equiv). [e] With **3** (0.5 mol%) and TBE (2 equiv). [f] The yield of product was determined by GC analysis with mesitylene as an internal standard.

butylethylene as the hydrogen acceptor. In addition, the  $(iPr_4PSCOP)Ir$  complex gives high kinetic selectivity for dehydrogenation of linear alkanes to  $\alpha$ -olefins under relatively mild reactions conditions. The new catalytic system can be applied to the selective dehydrogenation of a wide variety of heterocycles to produce heteroarenes and olefinic products by transfer dehydrogenation.

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- [13] Determined by <sup>13</sup>C NMR spectroscopy, the sum of COE and COD double bonds equals TON of TBE within 10% difference. Trance amount of ethylbenzene (<2%) and *o*-xylene (<2%) were detected by GC/MS.
- [14] During the preparation of this manuscript, Yamamoto et al. reported Ir pincer complexes containing a "7-6-7" fused-ring backbone, which gave a maxium TON of 4100 after 24 h at

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