Cite this: Chem. Commun., 2012, 48, 9465–9467

COMMUNICATION

In situ generated "lanthanum(III) nitrate alkoxide" as a highly active and nearly neutral transesterification catalyst[†]

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Received 12th July 2012, Accepted 30th July 2012 DOI: 10.1039/c2cc34987f

In situ generated lanthanum(III) nitrate alkoxide is a highly active and nearly neutral transesterification catalyst, which can promote non-epimerized transesterification of α -substituted chiral carboxylic esters under reflux conditions.

The transesterification of carboxylic esters with alcohols is one of the most valuable methods for ester synthesis.¹ In particular, harmless and colorless La(III) complexes, unlike conventional Al(III),² Ti(IV),³ Sb(III),⁴ Sn(IV),⁵ Zr(IV),^{3a,6} Hf(IV),^{3a,6} B(III),⁷ Zn(II),⁸ etc., have been proved to be one of the most effective catalysts by Okano, Brown, and Li et al.9 We also recently reported that lanthanum(III) isopropoxide (1)-2-(2-methoxyethoxy)ethanol (2) as an acid-base combined catalyst¹⁰ promoted the transesterification of carboxylic esters, less-reactive dimethyl carbonate (8), and much less-reactive methyl carbamates with an equivalent amount of 1°-, 2°-, and less-reactive 3°-alcohols.¹¹ In this catalysis, however, 1 is highly Brønsted basic and cannot be used for non-epimerized transesterification of chiral α -substituted esters under the practical azeotropic reflux conditions (>50 °C) (eqn (1)). Also, 1 is expensive for industrial application, not available in bulk quantities, and unstable under moist conditions to decompose into inactive lanthanum(III) oxide. Therefore, alternative low-priced and much more stable La(III) precursors are desired.12

$$R_{+}^{1} \xrightarrow{O} OMe + R^{3}OH \xrightarrow{Cat. La(O/Pr)_{3} (1)}{OMe + R^{3}OH \xrightarrow{Cat. HO(CH_{2}CH_{2}O)_{2}Me (2)}{\frac{hexane or heptane}{50 °C to azeotropic reflux}} \xrightarrow{R^{2}}_{High yield, low ee} (1)$$

To overcome these subjects, we envisioned that inexpensive lanthanum(III) nitrate, which is much more stable than 1 due to the coordinative NO_3^- moieties and less hygroscopic than La(OTf)₃, can be one of the most promising compounds.¹³ Moreover, we here selected to use highly Brønsted basic [PMe(octyl)₃](OCO₂Me) (4) as a key additive in the presence of alcohol (ROH). Compound 4 would react with ROH

besides irreversible decomposition to MeOH and CO₂ under mild azeotropic reflux conditions, and give an uncertain mixture of La(OR)_m(NO₃)_{3-m} (m = 1-3) (5) *in situ* without removal of [PMe(octyl)₃](NO₃) (6) (Fig. 1). Pentacoordinated 6 with soft character would unlikely ligate to the Lewis acidic lanthanum center, and thus high catalytic activity will be maintained. Moreover, the preparation technique according to the amount of starting **4** might control the ratio of these active catalysts in the equilibrium. In particular, we assumed that more neutral and thus less basic La(OR)₂(NO₃) (**5a**) and LaOR(NO₃)₂ (**5b**) rather than strongly basic La(OR)₃ (**5c**) should be of great advantage for undeveloped non-epimerized transesterification of chiral α -substituted esters.

At the outset of our study, by taking advantage of the low price and high polarity of dimethyl carbonate (8) (bp 90 °C) for La(III) catalysts, we examined the probe transesterification of 8 with 1-ethynyl-1-cyclohexanol (9a) (2 mmol scale) as a less-reactive 3°-alcohol (Table 1). In the presence of 3 mol% of La(NO₃)₃·H₂O (3) from La(NO₃)₃·6H₂O,¹⁴ the reaction was conducted under azeotropic reflux conditions with the removal of methanol using MS 5 Å in a Soxhlet thimble. However, 3 was hardly soluble in 8, and the product (10a) was obtained in only 38% yield after 12 h (entry 1). In sharp contrast, addition of [PMe(octyl)₃](OCO₂Me) (4) (6 mol%) to 3 (3 mol%) was expectedly effective to promote the reaction (98% yield within 10 h) under homogeneous reaction conditions (entry 2).



Remarkably, the use of much less expensive La(NO₃)₃·xH₂O (x = 3-5) showed almost the same catalytic activity after desiccation to **3** under <3 Torr at 170 °C for 12 h¹⁴ (entry 2, parentheses). The yield slightly decreased (86%) when 3 mol% of **4** was used, while 9 mol% of **4** exhibited a comparable result

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[†] Electronic supplementary information (ESI) available: Experimental details and product characterization. See DOI: 10.1039/c2cc34987f



Fig. 1 "Lanthanum(III) nitrate alkoxide" in situ.

 Table 1
 Optimization of La(III) catalysts

MeO´ 8 (4	O └ OMe I mL)	+ OH 9a (2 mmol) Handlive (3–9 mol%) La(NO ₃) ₃ ·H ₂ O (3) (3 mol%) additive (3–9 mol%) (bath temperature 110	5Å) °C) 10	OCO ₂ Me
Entry	La(III)	Additive	Time [h]	Yield [%]
1	3	_	12	38
2	3	[PMe(octyl) ₃](OCO ₂ Me) (4) (6 mol%)	10	98 (> 99) ^a
3	3	4 (3 mol%)	10	86
4	3	4 (9 mol%)	10	98
5		4 (6 mol%)	10	<1
6		$[PMe(octyl)_3](NO_3)$ (6) (6 mol%)	10	0
7		HNO ₃ (6 mol%)	10	<1
8	3	KOt-Bu (9 mol%)	10	24
9	3	$P(octyl)_3$ (7) (6 mol%)	10	> 99
^{<i>a</i>} Catalyst 3 was prepared from $La(NO_3)_3 \cdot xH_2O(x = 3-5)$.				

(98%) to that obtained using 6 mol% of 4 (entries 2-4). As other active candidates in situ, compound 4, [PMe(octyl)₃](NO₃) (6),¹⁵ and HNO₃ were much less effective (<1% yields for 10 h) (entries 5-7), and these results strongly suggest that 3 and 4 are critical precursors for the active La(III) catalysts in situ. Additionally, it is noted that highly basic "La(OR)₃", which was prepared in situ from 3 (3 mol%) and KOt-Bu (9 mol%), showed low catalytic activity (24% yield), since much less active La(III) at species such as K[La(OR)_m(NO₃)_{4-m}] might be involved under basic conditions (entry 8). It is noted that, according to Perosa's report,¹⁵ compound 4 can be synthesized from $P(octyl)_3$ (7) and 8 in methanol at 0 °C in the presence of 3. As expected, the perfect yield was established when 6 mol% of technical-grade 7 was used in the presence of 3 mol% of 3 (entry 9). We observed, in the resulting crude mixture, a sole ³¹P NMR (CDCl₃) signal at 32.35 ppm and m/z =385.39 in ESI-MS analysis, which can be attributed to the $[PMe(octyl)_3]^+$ moiety (Fig. 1). Moreover, when the reaction was conducted on the 200 mmol scale (24.8 g) of 9a, catalyst 3- 7_2 showed high catalytic activity, and 10a was obtained in 95% yield (34.6 g) (eqn (2)). On the other hand, moisture-sensitive 1.2^{11a} was much less effective (40% yield), even on the 40 mmol scale with prolonged reaction time (92 h) (eqn (2)). Moreover, the catalyst 5 in situ from 3.7_2 was active after removal of products and volatiles in vacuo, and could be recycled three times on the 40 mmol scale (4.97 g of 9a each time, 99->99% yields) (eqn (3)).

With the optimal homogeneous reaction conditions in hand, we next examined other alcohols (Table 2).¹⁶ Due to the minimal steric hindrance of **8**, not only 2°-alcohols but also 3°-alcohols were used, and the desired products (**10b–d**) were





Product (10), isolated yield, and reaction time



^{*a*} Unless otherwise noted, 3 mol% of **3**·**4**₂, **3**·**7**₂, or **1**·**2**₂ was used. ^{*b*} 1 mol% of **3**·**4**₂, **3**·**7**₂, or **1**·**2**₂ was used. ^{*c*} Diethyl carbonate was used in place of **8**. Bath temperature was 145 °C.

obtained in 96–>99% yields. Compared with the previous catalyst 1.2₂, 3.4₂ or 3.7₂ provided much higher catalytic activity. Moreover, less-reactive diethyl carbonate in place of 8 could be used, and the corresponding cyclohexyl ethyl carbonate (10e) was obtained in 98–99% yield after 1 h in the presence of 1 mol% of 3.4₂ or 3.7₂. Totally, the transesterification of much harmless dialkyl carbonates with various alcohols is highly useful in industry, since phosgene as a traditional reactant is deadly toxic.

In transesterification, epimerization of the substrate and/or the product is a serious problem. In particular, synthesis of chiral *a*-substituted ester under harsh basic conditions at azeotropic reflux temperature is one of the challenging issues in really practical transesterification. As expected, our previous basic catalyst 1.2_2 caused racemization under reflux conditions (bath temperature, 90 °C), and the corresponding product (12a) was obtained in 87% yield as a complete racemate from (R)-mandelate (11a) (>99% ee) and benzyl alcohol (9b) (eqn (4)). In sharp contrast, the use of much more neutral 3.4 and 3.4_2 provided 12a in 61% and 91% yield, respectively, without a loss of optical purity (>99% ee), although we observed the decrease in optical purity (87% ee) when 3.4_3 was used. These results strongly suggest that the actual catalysts in situ should be $LaOR(NO_3)_2$ (5a) and/or $La(OR)_2NO_3$ (5b) rather than $La(OR)_3$ (5c), which would be in equilibrium in the reaction mixture as shown in Fig. 2.



Furthermore, the non-epimerized transesterification of other unstable chiral substrates (11) was demonstrated (Table 3).¹⁶ Some substrates were applicable under the optimized reaction conditions at 90 °C in the presence of 3.4₂ without serious loss of optical purity (96–>99% ee in 12d, 12e, and 12h). However, other substrates showed the decrease in optical purity (87–94% ee in 12b, 12c, 12f, and 12g) even if the reaction temperature was



Fig. 2 Catalysts in situ, ee, and the yield of the products.

 Table 3
 Non-epimerized transesterification



5 Å was used in situ.

70 °C. According to the hypothesis of the equilibrium among the catalysts (**5a–c**) as shown in Fig. 2, the reactions proceeded smoothly without a loss of optical purity or with almost intact optical purity (96–>99% ee) when 3.4 was used in place of 3.4₂. Totally, not only α -oxy-substituted esters (**12b** and **12h**), but also α -amino esters (**12c–e**), α -chloro ester (**12f**), and naproxen derivative (**12g**) could be used in 3.4₂- or 3.4-catalyzed transesterification.

In summary, we have developed highly useful and homogeneous acid–base combined catalysts for transesterification, nearly neutral lanthanum(III) nitrate alkoxide, which can be readily prepared *in situ* from inexpensive La(NO₃)₃·H₂O and [PMe(octyl)₃](OCO₂Me). The most privilege of these active La(III) catalysts is highly practical non-epimerized transesterification of chiral α -substituted esters under azeotropic reflux conditions (96–>99% ee). Since really practical catalysts for transesterification are still strongly desired in both laboratory and industry, we believe that this new methodology without a complicated procedure can help problems for further improvements in transesterification.

Financial support was partially provided by MEXT, KAKENHI (21200033), the Yazaki Memorial Foundation for Science and Technology. MH is grateful to the Nippon Shokubai Award in Synthetic Organic Chemistry, Japan.

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