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# Direct formation of $H_2O_2$ from $H_2$ and $O_2$ over a Pd/SiO<sub>2</sub> catalyst: the roles of the acid and the liquid phase

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#### Abstract

The direct formation of  $H_2O_2$  from  $H_2$  and  $O_2$  was carried out over a Pd/SiO<sub>2</sub> catalyst in a medium of ethanol or water acidified with either  $H_2SO_4$  or HCl. The  $H_2SO_4$ /ethanol system is the most favorable for peroxide formation. Both the proton and the anion, in the case of Cl<sup>-</sup>, promote the net formation of the peroxide. Protons inhibit the reduction of  $H_2O_2$  by  $H_2$ , and chloride ions limit the direct reduction of  $O_2$  to water, presumably by blocking Pd ensembles. Sulfate ions, being noncoordinating ligands, do not serve this function; therefore the  $H_2SO_4$ /water system is a poor medium for producing the peroxide. By contrast, the  $H_2SO_4$ /ethanol system is believed to be effective because in the presence of  $O_2$ , acetate ions are formed from ethanol, and these ions block Pd ensembles in the same manner as chloride ions. © 2004 Elsevier Inc. All rights reserved.

Keywords: Hydrogen peroxide; Palladium/silica; Supported palladium catalysts

# 1. Introduction

Since the early work of Pospelova and coworkers [1-3], there has been considerable effort dedicated to understanding the details of the direct reaction of H<sub>2</sub> and O<sub>2</sub> to form H<sub>2</sub>O<sub>2</sub> [4–10]. The reaction is complicated because it involves a three-phase system that includes a solid catalyst (usually including Pd), a liquid phase, and the reagent gases. Research has focused on the state of the catalyst and the role of the liquid, which includes an acid. Other modifiers, such as Br<sup>-</sup>, may be included to improve the selectivity for H<sub>2</sub>O<sub>2</sub> formation. Work in our laboratory has shown that when the reaction is carried out in an aqueous HCl solution, Pd is lost from its support as PdCl<sub>4</sub><sup>2-</sup>, which, in turn, may be reduced to colloidal Pd [4–7]. The latter form of Pd is believed to be the active component in this case. By contrast, in ethanol the Pd largely remains on the silica support during the reaction. In this communication HCl and  $H_2SO_4$ , with either water or ethanol as the liquid phase, are compared. It is shown that with Pd/SiO<sub>2</sub>, the  $H_2SO_4$ /ethanol system is the most favorable liquid phase for  $H_2O_2$  formation, whereas in the  $H_2SO_4$ /water system almost no peroxide is formed. This surprising result has been reported previously by Thompson and coworkers [11], but the origin of the phenomenon was uncertain. In a comparison of the several systems, it is important to recognize that the solubility of  $H_2$  is five-fold larger in ethanol than in water and the solubility of  $O_2$  is eight-fold larger in ethanol than in water [11]. Moreover, because of surface tension and viscosity differences, the bubble size in ethanol is considerably smaller than that in water. These factors are important because at some level the reaction is transport limited.

# 2. Experimental

# 2.1. Preparation of the catalyst

A detailed description of the catalyst preparation, reactivity measurement, and analytical methods has been published

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elsewhere [6,7]. Briefly, the catalyst was 5 wt% Pd supported on Cab–O–Sil M5 silica, which has a surface area of ca. 200 m<sup>2</sup> g<sup>-1</sup>. The material was prepared by an incipient wetness method with an aqueous solution of  $PdCl_4^{2-}$ . The catalyst precursor was pretreated in flowing O<sub>2</sub> at 400 °C and reduced for 30 min under H<sub>2</sub> flowing at 20 ml min<sup>-1</sup>. The average particle size was estimated by TEM to be 6 nm before reaction, and the particle size was distributed in a range of 5–40 nm after reaction in the H<sub>2</sub>SO<sub>4</sub>/ethanol system, and most of these particles were about 10 nm in diameter. As demonstrated by XPS, most of the supported Pd was in the metallic state.

#### 2.2. Reactivity measurement

The reactions were carried out at atmospheric pressure and at 10 °C in glass reactors described in Ref. [6]. Hydrogen and oxygen were added via a glass frit to the stirred slurry containing the catalyst. The gases were introduced as a  $4:1 \text{ O}_2/\text{H}_2$  mixture at a flow rate of 50 ml min<sup>-1</sup>. At this ratio the  $\text{O}_2/\text{H}_2$  gas mixture is explosive, and appropriate precautions should be taken. For example, the catalyst should be introduced as a slurry rather than in the dry state. The liquid phase consisted of 60 ml of ethanol or water acidified with HCl or H<sub>2</sub>SO<sub>4</sub>. Unless stated otherwise, the solutions were either 0.17 N in HCl or 0.24 N in H<sub>2</sub>SO<sub>4</sub>, and the amount of catalyst was 50 mg. The "ethanol solution" contained a small amount of water that was introduced with the acid.

#### 3. Results and discussion

## 3.1. Synthesis of $H_2O_2$ in $H_2SO_4$ -acidified solutions

The increase in the concentration of  $H_2O_2$  as a function of time for the reaction carried out at two different normalities of  $H_2SO_4$  in ethanol is shown in Fig. 1A. Over



Fig. 1. Catalytic formation of  $H_2O_2$  in the ethanol solution acidified to ( $\blacktriangle$ ) 0.12 N and ( $\blacktriangledown$ ) 0.24 N in  $H_2SO_4$ , and ( $\blacksquare$ ) 0.24 N  $H_2SO_4$ /water: (A) concentration of  $H_2O_2$ , (B) conversion of  $H_2$ , and (C) selectivity for  $H_2O_2$ .

a period of 7 h in 0.24 N H<sub>2</sub>SO<sub>4</sub>, the concentration of H<sub>2</sub>O<sub>2</sub> reached 2.4 wt%, which corresponds to a net rate of 32 mmol<sub>H<sub>2</sub>O<sub>2</sub>  $g_{Pd}^{-1}$  min<sup>-1</sup>. This is about 30% larger than the rate reported for the HCl/ethanol system [7] under the same reaction conditions (see below). At 0.12 N H<sub>2</sub>SO<sub>4</sub> the rate was slightly smaller than that found in the 0.24 N H<sub>2</sub>SO<sub>4</sub>/ethanol solution. But when the liquid phase was water, acidified to 0.24 N in H<sub>2</sub>SO<sub>4</sub>, only a very small amount of H<sub>2</sub>O<sub>2</sub> was formed during the first 2 h, and thereafter no additional peroxide was produced.</sub>

The hydrogen conversion levels and the selectivities are shown in panels B and C, respectively, for the  $H_2SO_4$ /ethanol system. Here the selectivity is defined as the percentage of  $H_2$  that reacts to  $H_2O_2$ . With increasing acid strength in ethanol, the conversion of  $H_2$  increases somewhat more than the rate of peroxide formation; hence, the selectivity decreases slightly. Surprisingly, in the aqueous phase the  $H_2$ conversion remained constant at about 20%, even when no  $H_2O_2$  was being formed, which means that all of the reacted  $H_2$  was being converted to water.

The amount of Pd lost from the catalyst in the  $H_2SO_4/$  ethanol system was significantly less than that in the HCl/ ethanol system. After 5 h of reaction the concentration of Pd in the liquid phase was  $2.6 \times 10^{-5}$  M in the former case and  $6.5 \times 10^{-5}$  M in the latter, as determined from inductively coupled plasma (ICP) analysis. Had all of the Pd entered the liquid phase, the concentration would have been  $4.0 \times 10^{-4}$  M.

## 3.2. Synthesis of $H_2O_2$ in HCl-acidified solutions

For purposes of comparison, previously reported results [7] obtained with the HCl/ethanol and HCl/water systems are shown in Fig. 2. Most notable is the fact that  $H_2O_2$ formation continued over a 7-h period in the aqueous phase at a rate that was only about half of that found in ethanol.



Fig. 2. Catalytic formation of  $H_2O_2$  in ( $\checkmark$ ) 0.17 N HCl/ethanol and ( $\blacksquare$ ) 0.17 N HCl/water solutions: (A) concentration of  $H_2O_2$ , (B) conversion of  $H_2$ , and (C) selectivity for  $H_2O_2$ .

The selectivity decreased from 51 to 36% over 5 h. The latter selectivity is almost the same as that obtained with the HCl/ethanol system and is comparable to those obtained in the H<sub>2</sub>SO<sub>4</sub>/ethanol systems. The similarities between the ethanol and aqueous systems are somewhat fortuitous, however, since the state of the Pd varies between the two cases as noted above. The variation of rate with time, as observed for the aqueous system, is typical of the colloid, which is intrinsically unstable.

#### 3.3. Combinations of HCl, H<sub>2</sub>SO<sub>4</sub>, water, and ethanol

In an effort to elucidate the roles of each component, several combinations of the two acids and the two liquids were studied; the results are presented in Fig. 3. In all cases 50 mg of Pd/SiO<sub>2</sub> was present. First, the reaction was carried out in an equal volume mixture of ethanol and water with H<sub>2</sub>SO<sub>4</sub> as the acid. After 7 h, 0.8 wt% H<sub>2</sub>O<sub>2</sub> was formed, which is about one-third of that produced in pure ethanol (Fig. 1A). The H<sub>2</sub> consumption was less than that in pure ethanol but more than that in pure water. Here water seems to have a dilution effect, but it does not completely inhibit the reactions when H<sub>2</sub>SO<sub>4</sub> is the acid.

A second experiment involved the addition of HCl to the  $H_2SO_4$ /water system after the reaction had proceeded for 2 h. During the first 2 h the formation rate of  $H_2O_2$  was very small, as expected, but when 0.17 N HCl was added the rate increased to about the level observed for the HCl/water system (Fig. 2A). From this result one can conclude that sulfate ions do not poison the catalyst when water is the liquid phase.



Fig. 3. Catalytic formation of  $H_2O_2$  in 0.24 N  $H_2SO_4$ /water (30 ml)– ethanol (30 ml): ( $\bullet$ ) concentration of  $H_2O_2$  and ( $\bigcirc$ ) conversion of  $H_2$ . Catalytic formation of  $H_2O_2$  in 0.24 N  $H_2SO_4$ /water solution: ( $\blacksquare$ ) concentration of  $H_2O_2$  and ( $\square$ )  $H_2$  conversion. After 2 h, 0.24 N  $H_2SO_4$ /water solution was made 0.17 N in HCl: ( $\blacktriangle$ ) concentration of  $H_2O_2$ .

In the previous study [7] it was found that in pure ethanol (no acid added) a small amount of H<sub>2</sub>O<sub>2</sub> appeared during the first hour, but thereafter there was no net formation of the peroxide. Similar results were also reported for an aqueous system [5]. Meanwhile, in ethanol the  $H_2$  conversion was 45%, and when H<sub>2</sub>O<sub>2</sub> was added to the system, it decomposed over a period of 4 h, even in the presence of the reagents. These results confirm that one of the roles of the acid (protons) is to inhibit the subsequent reduction of H<sub>2</sub>O<sub>2</sub> by hydrogen, as has been pointed out previously [6,7]. Other investigators have suggested that the role of the acid is to prevent the base-catalyzed *decomposition* of H<sub>2</sub>O<sub>2</sub> [1,8,10]; however, with ethanol as the liquid phase, this seems unlikely. In a separate experiment H<sub>2</sub>O<sub>2</sub> was added to nonacidified ethanol that contained the catalyst and O<sub>2</sub>. Before the addition of H<sub>2</sub>O<sub>2</sub>, the system had been exposed to both reagents. The  $H_2O_2$  concentration (0.8 wt%) decreased slightly at first and then remained constant for a period of 4 h; that is, in the absence of an acid the H<sub>2</sub>O<sub>2</sub> did not decompose.

#### 3.4. Secondary reactions in the $H_2SO_4$ /ethanol system

Even in the presence of the acid, secondary reactions do occur, and these result in the loss of selectivity. This effect is illustrated by the results summarized in Table 1 and Fig. 4. The amount of catalyst was increased from 20 to 120 mg, and the concentration of  $H_2O_2$ , the conversion of  $H_2$ , and the selectivity were determined after 5 h on stream. Whereas the  $H_2$  conversion continued to increase with catalyst loading, the concentration of  $H_2O_2$  reached a maximum at a loading of 40 mg and decreased such that with 120 mg of catalyst almost no  $H_2O_2$  was detected. The peroxide selectivity reached a maximum at a loading of 30 mg of catalyst.

The role of secondary reactions in these phenomena is confirmed by the results in Fig. 4. In these experiments the reaction was allowed to proceed for 2 h, and then ca. 0.8 wt%  $H_2O_2$  was added to the system. When 30 mg of catalyst was present, the subsequent formation rate of  $H_2O_2$  formation remained the same; however, when 90 mg of catalyst was added, the amount of  $H_2O_2$  actually decreased with time.

These results may be understood in terms of consecutive reactions in which  $H_2O_2$  is first formed and then is subse-

Effect of catalyst amount on $H_2O_2$ concentration,	H2 conversion and selec-
tivity for H <sub>2</sub> O <sub>2</sub> <sup>a</sup>	

Table 1

Amount of catalyst (mg)	H <sub>2</sub> O <sub>2</sub> concentration (%)	H <sub>2</sub> conversion (%)	Selectivity for H <sub>2</sub> O <sub>2</sub> (%)
20	1.3	35	32
30	1.5	37	45
40	1.9	49	40
50	1.7	55	34
70	0.5	65	10
90	0.1	68	1.9
120	Trace	75	Trace

<sup>a</sup> 5 wt% Pd/SiO<sub>2</sub>, 0.24 N H<sub>2</sub>SO<sub>4</sub>/ethanol, after 5 h reaction.



Fig. 4. Catalytic formation of  $H_2O_2$  in 0.24 N  $H_2SO_4$ /ethanol solutions before and after the addition of  $H_2O_2$ : 30 mg catalyst, ( $\blacktriangle$ )  $H_2O_2$  concentration, ( $\triangle$ )  $H_2$  conversion; 90 mg catalyst, ( $\blacksquare$ )  $H_2O_2$  concentration, ( $\square$ )  $H_2$  conversion.

quently reduced by H<sub>2</sub>. But there is a question as to why the rates of the primary and secondary reactions do not both increase proportionally with catalyst loading. In the case of H<sub>2</sub> the conversion levels clearly exceed differential conditions; therefore, it is expected that the extent of conversion would not remain linear. The variation in the net rate of H<sub>2</sub>O<sub>2</sub> formation may be related to diffusional effects; that is, the contact of H<sub>2</sub>O<sub>2</sub> with Pd probably is not transport limited since the peroxide is completely dissolved in the ethanol, but the availability of both H<sub>2</sub> and O<sub>2</sub> at the catalyst is probably transport limited. One would expect the rate of H<sub>2</sub>O<sub>2</sub> formation to remain constant, whereas the rate of H<sub>2</sub>O<sub>2</sub> reduction would continue to increase with the addition of more catalyst. The fact that  $H_2O_2$  is reduced more rapidly than it is formed is evident from the results of Fig. 4 when 90 mg of catalyst was present.

#### 4. Conclusions

The results of this study further establish that the anion in an acid, as well as the proton, plays a role in the selective formation of  $H_2O_2$ . Moreover, the liquid phase also becomes involved in several ways. As noted above, with the HCl/water system, the strongly coordinating chloride ligands give rise  $PdCl_4^{2-}$  complexes, which are intermediates in the formation of colloidal Pd when  $H_2$  is present. Chloride ions in sufficiently high concentrations may also block Pd ensembles that promote the dissociation of O<sub>2</sub>, which results in the direct formation of water. The positive role of bromide in improving the selectivity has been attributed to this effect, but much lower concentrations of bromide are need to achieve higher selectivities [10]. The sulfate ion is a noncoordinating ligand and would not be expected to block Pd ensembles. Finally, ethanol, but not water, may result in surface species that block the ensembles that are responsible for the direct formation of water. There is evidence from surface science that under mild conditions ethanol reacts with oxygen on the Pd(110) surface, forming surface acetate ions [12]. We have added acetic acid (0.01 N) to an almost inactive Pd/SiO2-H2SO4/water system and have found that H<sub>2</sub>O<sub>2</sub> is indeed formed at about the same rate as in the conventional HCl/water system (Fig. 2A). Taken together, these observations seem to provide a rational explanation for the behaviors of the several acid-liquid phase combinations that have been described here. One is able to understand, for example, why the H<sub>2</sub>SO<sub>4</sub>/ethanol phase is active and selective for the direct formation of H<sub>2</sub>O<sub>2</sub>, whereas the H<sub>2</sub>SO<sub>4</sub>/water phase results only in the formation of water. The secondary reduction of H<sub>2</sub>O<sub>2</sub> may also play a role, but this does not appear to be a dominant reaction at the lower catalyst loadings.

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