

# Catalytic hydrogenation of amino acids to amino alcohols with complete retention of configuration†

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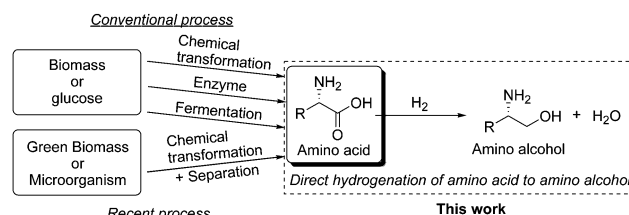
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**Rh-MoO<sub>x</sub>/SiO<sub>2</sub> is an effective heterogeneous catalyst for selective hydrogenation of amino acids to amino alcohols in a water solvent. MoO<sub>x</sub> modification of Rh drastically enhanced the activity and improved the selectivity and ee. Various amino alcohols were obtained in high yields (90–94%) with complete retention of configuration.**

Amino acids are important organic compounds because they are intermediates in metabolism as well as essential building blocks of proteins, and furthermore, they are also used as versatile chemicals such as animal feed additives, catalysts, flavour enhancers and intermediates for medicines. Amino acids can be readily prepared by fermentation, enzymatic transformation, chemical transformation and extraction.<sup>1</sup> Particularly, in fermentation, amino acids are produced in high volume from glucose that is one of the important platform chemicals for biorefinery. In addition, recently, amino acid synthesis from green biomass (grass or leaf)<sup>2</sup> or microorganisms (microalgae or cyanobacteria)<sup>3</sup> has attracted much attention because these materials are potential renewable biomass resources (Scheme 1). Therefore, amino acids can be regarded as important key chemicals for biorefinery, and the development of transformation methods of amino acids will become more and more significant.<sup>4</sup>

Aminoalcohols are important components included in many synthetic and natural products, and are especially used as intermediates for synthesis of pharmaceuticals, insecticidal reagents and chiral auxiliaries.<sup>5</sup> In addition, amino alcohols can be easily converted with CO<sub>2</sub> to cyclic carbamates including oxazolidinones,<sup>6</sup> which have many applications like chiral auxiliaries, solvents and pharmaceutical agents.<sup>6</sup> Therefore, development of efficient synthetic methods for chiral aminoalcohols is an intriguing target for chemists. Conventionally, amino alcohols have been synthesized by hydrogenation of amino acids with metal hydrides<sup>7</sup> or reaction of epoxides with amines.<sup>8</sup> However, these methodologies suffer from production of



Scheme 1 Process for preparation of amino alcohols via amino acids from biomass resources.

a large amount of salts, use of expensive reagents and/or use of large excessive reagents. To overcome these problems, improved methods<sup>9</sup> and new methodologies such as aminohydroxylation of terminal C=C bonds,<sup>10</sup> hydrogenation of amino acids or esters by H<sub>2</sub>,<sup>11</sup> hydroxymethylation of imines<sup>12</sup> and addition of acyloxymethyl to imine and hydrolysis<sup>13</sup> have been intensively developed. Among these methodologies, direct hydrogenation of amino acids<sup>11a-e</sup> by hydrogen is the most ideal from the viewpoint of green chemistry because the by-product is only water (Scheme 1) and amino acid is a potential feedstock as mentioned above. Ru/C<sup>11a-d</sup> and Ru-Re<sup>11e</sup> were reported to be effective catalysts, however catalysis of Ru/C has serious drawbacks such as high temperature, low activity and loss of optical purity, and that of Ru-Re has drawbacks such as high pressure, low yield and low activity (Table S1, ESI†). In particular, maintaining the optical purity of the substrate is important because aminoalcohol forms a main structure of medicines and chiral auxiliaries. Therefore, the effective catalysts that can realize both high activity and complete chirality retainment under mild reaction conditions ( $T < 363$  K,  $H_2 < 10$  MPa) in hydrogenation of amino acids are desired to be developed.

Up to now, our group<sup>14</sup> and other groups<sup>15</sup> have reported that the reducible metal oxide (M'O<sub>x</sub>: ReO<sub>x</sub>, WO<sub>x</sub>, MoO<sub>x</sub>) modified noble metal (M) catalyst (M-M'O<sub>x</sub> catalyst) is effective for the selective hydrogenolysis of polyols or cyclic ethers and selective hydrogenation of carboxylic acids, amides or  $\alpha,\beta$ -unsaturated aldehydes. Expanding the potential of the M-M'O<sub>x</sub> catalyst will provide a new synthetic method and a new direction in the design of heterogeneous catalysts.

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In this communication, we report that Rh-MoO<sub>x</sub>/SiO<sub>2</sub> acts as a highly efficient heterogeneous catalyst for direct hydrogenation of amino acids to amino alcohols with complete retention of substrate configuration in a water solvent at low temperatures (313–323 K).

Initially, catalyst screening in the hydrogenation of L-alanine (**1**) to L-alaninol (**2**) at 353 K and 8 MPa H<sub>2</sub> with H<sub>3</sub>PO<sub>4</sub>aq as a model reaction was carried out using various carbon supported M-M'O<sub>x</sub> catalysts (M-M'O<sub>x</sub>/C: M = Rh, Ru, Pd and Pt, M'O<sub>x</sub> = MoO<sub>x</sub>, WO<sub>x</sub> and ReO<sub>x</sub>) and SiO<sub>2</sub> supported Rh-M'O<sub>x</sub> catalysts (Rh-M'O<sub>x</sub>/SiO<sub>2</sub>) (Table 1). The loading amount of noble metals was 5 wt% for M/C and M-M'O<sub>x</sub>/C, and 4 wt% for Rh-M'O<sub>x</sub>/SiO<sub>2</sub>. The molar ratio of M' to M was 1/8. Among the M/C catalysts, Ru/C showed higher activity than the other M/C catalysts, followed by Rh/C (entries 1, 9, 13 and 17). As for carbon supported M-M'O<sub>x</sub> catalysts, addition of M'O<sub>x</sub> to Rh/C and Pt/C drastically changed the catalytic performance, leading to high yield and/or high selectivity (entries 1–4 and 17–20), although the changes of yield and selectivity were hardly observed in the other carbon supported M-M'O<sub>x</sub> catalysts (entries 9–16). Particularly, MoO<sub>x</sub> and WO<sub>x</sub> modified Rh/C catalysts showed excellent catalytic performance. Then, Rh-M'O<sub>x</sub>/SiO<sub>2</sub> catalysts were examined in the same reaction (entries 5–8). Compared with Rh-M'O<sub>x</sub>/C catalysts, Rh-M'O<sub>x</sub>/SiO<sub>2</sub> catalysts showed higher activities, and Rh-MoO<sub>x</sub>/SiO<sub>2</sub> provided the highest yield and selectivity among Rh-M'O<sub>x</sub>/SiO<sub>2</sub> catalysts. It should be noted that the activity and selectivity of Rh-MoO<sub>x</sub>/SiO<sub>2</sub> (entry 6) are much higher than those of Rh/SiO<sub>2</sub> (entry 5) and MoO<sub>x</sub>/SiO<sub>2</sub> (entry 21). These results indicate that the high activity and high selectivity are generated by the synergy between Rh and MoO<sub>x</sub>. In terms of activity and selectivity, Rh-MoO<sub>x</sub>/SiO<sub>2</sub> is regarded as the best catalyst for the reaction.

Table 1 Hydrogenation of **1** over various catalysts

Entry	Catalyst	Conv./ %	Yield ( <b>2</b> )/%	Select./%			
				<b>2</b>	<b>3</b>	<b>4</b>	<b>5</b>
1	Rh/C	2.0	1.8	87.6	12.4	0.0	0.0
2	Rh-MoO <sub>x</sub> /C	23.8	21.8	91.5	8.5	0.0	0.0
3	Rh-WO <sub>x</sub> /C	29.6	26.1	88.2	11.8	0.0	0.0
4	Rh-ReO <sub>x</sub> /C	16.1	13.4	83.2	16.8	0.0	0.0
5	Rh/SiO <sub>2</sub>	3.7	3.1	84.4	15.6	0.0	0.0
6	Rh-MoO <sub>x</sub> /SiO <sub>2</sub>	46.8	42.2	90.2	11.0	0.0	0.0
7	Rh-WO <sub>x</sub> /SiO <sub>2</sub>	41.7	36.2	86.9	13.1	0.0	0.0
8	Rh-ReO <sub>x</sub> /SiO <sub>2</sub>	25.3	21.4	84.5	15.5	0.0	0.0
9	Ru/C	7.5	7.0	94.2	5.8	0.0	0.0
10	Ru-MoO <sub>x</sub> /C	6.9	6.2	90.1	9.9	0.0	0.0
11	Ru-WO <sub>x</sub> /C	7.4	6.7	90.8	9.2	0.0	0.0
12	Ru-ReO <sub>x</sub> /C	9.1	8.0	87.5	12.5	0.0	0.0
13	Pd/C	0.0	0.0	—	—	—	—
14	Pd-MoO <sub>x</sub> /C	0.0	0.0	—	—	—	—
15	Pd-WO <sub>x</sub> /C	0.0	0.0	—	—	—	—
16	Pd-ReO <sub>x</sub> /C	1.3	1.2	95.2	4.8	0.0	0.0
17	Pt/C	0.3	0.3	0.3	0.0	0.0	0.0
18	Pt-MoO <sub>x</sub> /C	11.4	9.4	82.5	17.5	0.0	0.0
19	Pt-WO <sub>x</sub> /C	15.4	13.8	89.4	10.6	0.0	0.0
20	Pt-ReO <sub>x</sub> /C	3.8	3.2	83.9	16.1	0.0	0.0
21	MoO <sub>x</sub> /SiO <sub>2</sub>	0.0	0.0	—	—	—	—

Reaction conditions: catalyst (M'/M = 1/8) 50 mg, L-alanine 0.4 g, H<sub>3</sub>PO<sub>4</sub>aq (0.29 M) 20 g, H<sub>2</sub> 8 MPa, 353 K, 4 h.

In order to determine the optimized amount of MoO<sub>x</sub> in Rh-MoO<sub>x</sub>/SiO<sub>2</sub> catalysts, the effect of MoO<sub>x</sub> amount was studied by changing the molar ratio of MoO<sub>x</sub> to Rh from 0 to 1 (Table S2, ESI<sup>†</sup>). The activity showed volcano-type tendency and the highest activity was obtained with a Mo/Rh molar ratio of 1/8. On the other hand, the selectivity is gradually increased with increasing Mo/Rh molar ratio. From the viewpoints of selectivity and activity, Rh-MoO<sub>x</sub>/SiO<sub>2</sub> with a Mo/Rh molar ratio of 1/8 is an optimal catalyst for the reaction.

The effect of added acids was examined using mineral acids like H<sub>2</sub>SO<sub>4</sub> and H<sub>3</sub>PO<sub>4</sub>, and solid acids like ZSM-5 and SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> (Table S3, ESI<sup>†</sup>). Without any acids, the yield was very low (4.1%), while the selectivity was high. The same result was obtained using solid acids, which indicates that solid acids did not act as an acid. On the other hand, mineral acids such as H<sub>2</sub>SO<sub>4</sub> and H<sub>3</sub>PO<sub>4</sub> promoted the reaction to afford **2** in more than five times higher yields than solid acids and no additive. H<sub>2</sub>SO<sub>4</sub> provided a twice higher yield than H<sub>3</sub>PO<sub>4</sub>, indicating that H<sub>2</sub>SO<sub>4</sub> is the most suitable in this reaction system.

The reusability of Rh-MoO<sub>x</sub>/SiO<sub>2</sub> was examined (Fig. S1, ESI<sup>†</sup>). The catalyst can be easily retrieved from the reaction mixture by centrifugation. The recovered catalyst was washed by water and used for the reusability test. The catalyst can be reused at least two times without loss of activity and selectivity.

The time-course in the hydrogenation of **1** over Rh-MoO<sub>x</sub>/SiO<sub>2</sub> is shown in Fig. 1. The reaction proceeds smoothly to reach full conversion of **1**. The selectivity of **2** hardly changed during the course of the reaction and even after the full conversion of **1**, which suggests that no over-reaction of **2** takes place. In addition, no racemization of **1** and **2** was observed, resulting in high enantio excess (ee) of **2** (>99.9%). On the other hand, isopropylamine (**3**) was produced at the initial stage, and the selectivity was unchanged during the reaction, suggesting that **3** was produced simultaneously with **2**. Therefore, the Rh-MoO<sub>x</sub>/SiO<sub>2</sub> catalyst is quite suitable for selective synthesis of amino alcohol without loss of optical purity of the starting material.

The performance of Rh-MoO<sub>x</sub>/SiO<sub>2</sub> was compared with that of Rh/SiO<sub>2</sub> (Scheme 2). The selectivity and ee of Rh-MoO<sub>x</sub>/SiO<sub>2</sub> were

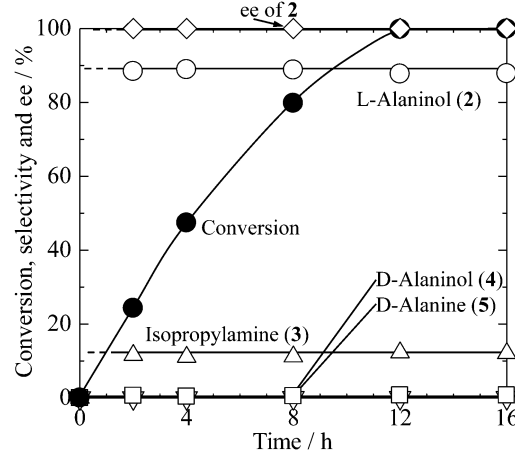


Fig. 1 Time-course of hydrogenation of L-alanine over Rh-MoO<sub>x</sub>/SiO<sub>2</sub>. Reaction conditions: Rh-MoO<sub>x</sub>/SiO<sub>2</sub> (Mo/Rh = 1/8) 100 mg, L-alanine 2 g, H<sub>2</sub>SO<sub>4</sub> 22 mmol, H<sub>2</sub>O 19.3 g, H<sub>2</sub> 8 MPa, 353 K.

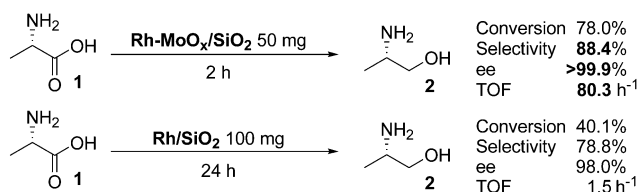
Table 2 Hydrogenation of various amino acids over Rh-MoO<sub>x</sub>/SiO<sub>2</sub>

Entry	Substrate	Product	Conv./%	Yield/%	ee/%
1 2 <sup>a</sup>			>99.9 99.1	92.8 93.7	>99.9 >99.9
3			>99.9	92.3	—
4 <sup>b</sup>			>99.9	92.8	—
5 <sup>c</sup>			>99.9	92.5	n.d. <sup>d</sup>
6 <sup>c</sup>			>99.9	90.5	>99.9
7 <sup>c</sup>			>99.9	90.6	n.d. <sup>d</sup>
8 <sup>c</sup>			99.8	90.0	—
9 <sup>c</sup>			>99.9	91.1	—

Reaction conditions: Rh-MoO<sub>x</sub>/SiO<sub>2</sub> (Mo/Rh = 1/8) 100 mg (<sup>b</sup>200 mg <sup>c</sup>500 mg), amino acid (4.5 mmol), H<sub>2</sub>SO<sub>4</sub> 5 mmol, H<sub>2</sub>O 20.0 g, H<sub>2</sub> 8 MPa 323 K (<sup>a</sup>313 K). <sup>d</sup> The configuration was not determined.

much higher than those of Rh/SiO<sub>2</sub>. TOF was calculated using the following equation: TOF = L-alaninol (mmol)/total Rh (mmol)/time (h). Rh-MoO<sub>x</sub>/SiO<sub>2</sub> provided fifty times higher TOF than Rh/SiO<sub>2</sub>. These results indicate that MoO<sub>x</sub> modification of Rh/SiO<sub>2</sub> brings about not only high TOF and high selectivity but also high ee.

The scope of amino acids was examined over Rh-MoO<sub>x</sub>/SiO<sub>2</sub> at a lower reaction temperature of 323 K (Table 2). **1** reacted to afford **2** with a high yield of 92.8% and high selectivity and ee (entry 1). Moreover, at 313 K, **2** was obtained with a higher yield of 93.7% (entry 2). Other α-amino acids (entries 3–7) were also converted to the corresponding amino alcohols in high yields (90.5–92.8%) and ee. In addition, the reactions of β-amino acid and γ-amino acid provided the β-amino alcohol and γ-amino alcohol in high yields (entries 8 and 9). It should be noted that Rh-MoO<sub>x</sub>/SiO<sub>2</sub> enables high yield synthesis of serinol



Scheme 2 Comparison of performance between Rh-MoO<sub>x</sub>/SiO<sub>2</sub> and Rh/SiO<sub>2</sub>. Reaction conditions: catalyst (Mo/Rh = 1/8), L-alanine 0.4 g, H<sub>2</sub>SO<sub>4</sub> 5 mmol, H<sub>2</sub>O 20.0 g, H<sub>2</sub> 8 MPa, 353 K. TOF = L-alaninol (mmol)/total Rh (mmol)/time (h).

(entry 4), which is an important intermediate for various useful chemicals such as medicines<sup>16</sup> and X-ray contrast agents.<sup>17</sup> Therefore, Rh-MoO<sub>x</sub>/SiO<sub>2</sub> can be applied to various amino acids without loss of the optical purity and is very useful from the practical viewpoint.

In conclusion, Rh-MoO<sub>x</sub>/SiO<sub>2</sub> acts as an efficient heterogeneous catalyst for hydrogenation of amino acids to amino alcohols in water. The synergy between MoO<sub>x</sub> and Rh drastically improved the activity, selectivity and ee of the produced amino alcohols. This catalyst can be applied to versatile amino acids to afford the corresponding amino alcohols in high yields (90–94%) without loss of the optical purity of the amino acids.

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