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# Boosting the acidic electrocatalytic nitrogen reduction performance of MoS<sub>2</sub> by strain engineering

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It is widely confirmed that expanding the layer spacing of layered-structural  $MoS_2$  can boost the hydrogen evolution reaction (HER) activity of  $MoS_2$ . Inspired by this, strain engineering strategy is applied on defect-rich  $MoS_2$  nanosheets by facilely F substitution to compress the interlayer space of  $MoS_2$  owing to the smaller size and higher electronegativity of F than S and catalytic HER was remarkably surpressed. By considering the strongly reduced uphill energy for the hydrogenation of adsorbed  $N_2$  on  $MoS_2$  due to the introduction of F ions revealed by the first-principle calculation, electrochemical nitrogen reduction reaction (NRR) activity and selectivity on the F doped  $MoS_2$  (F- $MoS_2$ ) catalyst in acidic condition can be significantly boosted. Faradic efficiency toward NRR on F- $MoS_2$  is therefore enhanced to 20.6% with the NH<sub>3</sub> yield high to 35.7 µg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> at the -0.2 V vs. RHE during the long-term operation.

#### Introduction

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NH<sub>3</sub> is one of the most essential chemicals for the industrial producing of fertilizers, dyes and resins.<sup>1, 2</sup> Although both elements (N and H) in NH<sub>3</sub> are abundant on earth, the intrinsic inert property of N<sub>2</sub>, which is the most abundant molecule in air, makes the producing of NH<sub>3</sub> from N<sub>2</sub> very difficult. Haber-Bosch process, which is the primary artificial NH<sub>3</sub> producing strategy nowadays, undergoes with metal catalyst under high temperatures (400-500 °C) and pressures (15-25 MPa). <sup>3, 4</sup> Around 1-2% of the world's energy supply is therefore consumed by the Haber-Bosch process. Energy-efficient strategies, represented by electrochemical nitrogen reduction widely studied.5-10 reaction (NRR). were therefore Encouragingly, NRR using protons as hydrogen source can be efficiently powered by electricity under ambient condition. However, the most severe challenge for aqueous NRR is the poor efficiency ascribed to the competition between hydrogen evolution reaction (HER) and NRR.11 HER is supposed to be one of the kinetically fastest electrochemical reactions due to that only two electrons are required to accomplish the reduction reaction and the standard redox potentials of  $H^+/H_2$  ( $E^0(H^+/H_2)$ H<sub>2</sub>)) and N<sub>2</sub>/NH<sub>3</sub> ( $E^0$ (N<sub>2</sub>/NH<sub>3</sub>)) couples are very close. As a result, even using noble metals as catalyst, the activity and selectivity of NRR under ambient condition in aqueous

electrolyte is much lower than expected due to the existence of competitive HER. 12 Actually, numerous noble-metal free catalysts have been developed for HER catalysis and highly efficient noble-metal-free hydrogen generation has been achieved.<sup>13-15</sup> Among which, MoS<sub>2</sub> has been considered as one of the most promising noble-metal-free HER catalysts due to the Pt-like property and proper Mo(III)/Mo(IV) redox potential (0.04 V)<sup>16</sup> and was also widely researched for NRR due to that requirements of NRR and HER on active sites are similar.<sup>17-20</sup> Density functional theory (DFT) calculations revealed that the edge of MoS<sub>2</sub> is the electrocatalytically active site for both NRR and HER <sup>19</sup> while the basal plane is inert for NRR. Great NRR activity in neutral condition was detected for  $MoS_2$  with Faradic efficiency (FE) of 8.34% and NH<sub>3</sub> yield of 29.28 µg h<sup>-1</sup> mg<sup>-1</sup>cat in 0.1 M Na<sub>2</sub>SO<sub>4</sub>. Unfortunately, NRR catalytic activity of  $MoS_2$  in acidic condition, which is preferred for NRR due to that 6 H atoms are required for the fixation of every N<sub>2</sub> molecule <sup>5, 20-24</sup>, is much poorer than the recently reported cost-effective NRR catalysts 25-29 ascribed to the great H+ reduction activity of MoS<sub>2</sub>. Strategies were applied to enhance the selectivity as well as NH<sub>3</sub> yield of MoS<sub>2</sub> based catalysts in acidic condition.  $^{\rm 30\text{-}33}$  Ru/2H-MoS\_2 interfaces were hence engineered with the acidic NRR FE enhanced to 17.6%. <sup>31</sup> Other than the noble-metal Ru, employing cost-effective active centers, including reduced graphene oxide <sup>32</sup> and single transition metal atom<sup>33</sup>, can also boost the NRR activity and selectivity in acidic condition.

Here in this work, a facile strain engineering strategy was proposed to boost the acidic NRR activity and selectivity of defect-rich MoS<sub>2</sub> nano-sheets since strain engineering has been widely applied for electrocatalytic activity adjustment of both metallic <sup>34-39</sup> and transition metal complex catalysts <sup>40-43</sup>. Especially for the layered-structural MoS<sub>2</sub>, interlayer space was expanded *via* different methods for HER catalytic activity improving.<sup>44-46</sup> Inspired by this, we proposed a facile strategy

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to compress the interlayer space of MoS<sub>2</sub> *via* F doping as demonstrated in **Scheme 1** to reduce the HER activity and therefore enhance the NRR selectivity by considering the small size of F ion and great electronegativity of F. Moreover, first-principle calculation reveals that the introduction of F ions would also significantly lower the uphill energy for the hydrogenation of adsorbed N<sub>2</sub>, leading to the formation of highly active NRR catalytic centers. Due to the simultaneously enhanced NRR selectivity and activity, FE toward NRR of the F doped Mo<sub>2</sub>S (F-Mo<sub>2</sub>S) catalyst can be therefore strongly boosted 20.6% with the NH<sub>3</sub> yield high to 35.7  $\mu$ g h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> at -0.2 V vs. RHE.



 $\mbox{Scheme 1}.$  Schematic diagram of strain engineering via F doping on the edge site of  $\mbox{MoS}_2$  nanosheet.

#### **Results and discussion**

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In order to confirm the successful synthesis of  $\mathsf{MoS}_2$  and the successful doping of F ions in F-MoS<sub>2</sub>, X-ray diffraction (XRD) analysis was carried out (Figure 1a). All the diffraction peaks of F-MoS<sub>2</sub> agree well with the standard pattern of hexagonal MoS<sub>2</sub> (JCPDS card No. 73-1508), revealing the high purity of the product, while all the characteristic peaks of F-MoS<sub>2</sub> are negatively shifted as desired due to the smaller size and higher electronegativity of F than S. Especially, this negatively shifted (002) peak indicates that the layer spacing of the F-MoS<sub>2</sub> catalyst was slightly compressed since (002) facet is related to the interlayer of hexagonal MoS2.47, 48 Scanning electron microscope (SEM) image of the F-MoS<sub>2</sub> catalyst in Figure 1b reveals that the layered structure of the pristine MoS<sub>2</sub> (SEM image in Figure S1) was remained in F-Mo<sub>2</sub>S. Meanwhile, the corresponding energy dispersive spectrum (EDS) reveals that atomic ratio of F in the F-MoS<sub>2</sub> catalyst is 1.12%, slightly higher than designed due to the better retention ability of F during the hyrothermal synthesis. By increasing the atomic ratio of S to F to 2:100 during the synthesis process, the  $F-MoS_2-2$ sample was prepared. It can be found that the morphology of F-MoS<sub>2</sub>-2 is remarkably changed compared with F-MoS<sub>2</sub> according to the SEM image of F-MoS<sub>2</sub>-2 (Figure S2). The  $MoS_2$ layers are accumulated for F-MoS<sub>2</sub>-2 and the specific surface area would be strongly decreased due to the higher F content. Specific surface areas were therefore characterized using the Brumauer-Emmett-Teller (BET) method with N2 adsorptiondesorption isotherms displayed in Figure S3. The BET surface area of F-MoS<sub>2</sub>-2 was decreased from 18 m<sup>2</sup>/g of F-MoS<sub>2</sub> to 12 m<sup>2</sup>/g as expected although more F ions would lead to extra defects. The observed wrinkled structure with crumpled edge and high transparency shown in both the transmission

electron microscope (TEM) image (Figure S4) and the bighe angle annular dark field scanning transmission electron microscope (HAADF-STEM) image of F-MoS<sub>2</sub> (Figure 1c) illustrates the ultrathin feature of the F doped  $MoS_2$ nanoflakes of F-MoS<sub>2</sub>. The corresponding EDS elemental mappings displayed in Figure 1d-f reveal that the F-MoS<sub>2</sub> catalyst is predominantly composed of Mo and S with F atoms doped uniformly.



**Figure 1**. (a) XRD patterns of the pristine MoS<sub>2</sub> and F-MoS<sub>2</sub> catalysts; (b) SEM image, (c) HAADF-STEM image and (d-f) corresponding EDS elemental mapping images of the F-MoS<sub>2</sub> catalyst.

High-resolution transmission electron microscopy (HR-TEM) images are displayed in Figure 2 to in-detail reveal the micromorphology and strain effect of the F-MoS<sub>2</sub> flake. It can be detected from the HR-TEM images on edge of the F-MoS<sub>2</sub> flakes (Figure 2a-b) that the F-MoS<sub>2</sub> flakes mainly consist of 3-6 S-Mo-S layers with numerous defects engineered. By measuring the thickness of a typical 5-layer nanosheet in Figure 2b, distance of a single S-Mo-S layer can be calculated to be 0.58 nm, which is decreased by 8% compared with the pristine defect-rich MoS<sub>2</sub> nanosheet prepared from the same strategy <sup>48</sup>. For the purpose of further confirming the effect of F doping on compression of the MoS<sub>2</sub> interlayer distance, Raman analysis was carried out on both F-MoS<sub>2</sub> and pristine  $MoS_2$  (Figure S5). Note that both the  $E^{1}_{2g}$  and  $A_{1g}$  bands of the F-MoS<sub>2</sub> Raman spectrum shift to a lower wavenumber compared with the pristine MoS<sub>2</sub>, indicating that layeredstructural MoS<sub>2</sub> sheets were compressed by the doped F ions <sup>49, 50</sup>. HR-TEM image on F-MoS<sub>2</sub> surface (Figure 2c) shows that defects are exsited. Note that numerous crystal fringes are discontinuous in Figure 2c, indicating the existence of 1T/2H phase interfaces, which is further manifested by the selected area electron diffraction (SAED) pattern (insert of Figure 2c) in the form of six independent diffraction arcs, a representative quasiperiodic structure with rich defects.

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Figure 2. HR-TEM images on (a-b) edge and (c) surface of the F-MoS<sub>2</sub> catalyst.

Sub-angstrom resolution HAADF-STEM image on surface of the F-MoS<sub>2</sub> were taken to clearly identify the defects and phase interfaces of the F-MoS<sub>2</sub> catalyst (Figure 3a). A trigonal lattice structure corresponding to the  $1T\text{--}\mathsf{MoS}_2$  and the common honeycomb lattice area of the 2H–MoS<sub>2</sub> are both clearly visible with interphase lined. At the same time, the uniformly dark regions as marked in red circles confirm the existence of defects on the F-MoS<sub>2</sub> surface. As a supplementary evidence for the extra surface defects, which are not as effective on electrochemical catalysis as the edge defects, formed by F doping. The F-MoS<sub>2</sub> catalyst possesses higher BET surface area (18 m<sup>2</sup>/g) compared with the pristine  $MoS_2$  (10 m<sup>2</sup>/g) due to the remained edge defects and additionally generated surface defects. X-ray photoelectron spectroscopy (XPS) analysis was subsequently executed to in detail study the elemental composition and surface chemical state of the F-MoS<sub>2</sub> catalyst. The survey XPS spectrum of the F-MoS<sub>2</sub> catalyst (Figure S6) confirms the existence of F in the F-MoS<sub>2</sub> catalyst and the F content in the F-MoS2 is 1.04 atom.%, very close to the SEM-EDS result. The Mo 3d high resolution XPS spectrum of the F-MoS<sub>2</sub> catalyst (Figure 3b) reveals a doublet of predominantly characteristic 1T phase peaks of Mo  $3d_{3/2}$  and Mo  $3d_{5/2}$  located at 231.4 eV and 228.2 eV, which are much lower than that of their 2H phase counterparts (232.1 eV and 229.0 eV). Negatively shifted S 2p peak (Figure S7) can confirm the transfer of  $MoS_2$  from 2H to 1T phase in the F-MoS<sub>2</sub> catalyst. Interestingly, further quantitative analysis based on the deconvoluted Mo 3d resonances exhibited that content of 1T phase in the F-MoS<sub>2</sub> catalyst is increased compared with the pristine MoS<sub>2</sub> although the interlayer distance was compressed.

Although the additional defects and the enhanced 1T phase content in F-MoS<sub>2</sub> should be benificial for HER catalysis in common sence, HER activity of MoS<sub>2</sub> was strongly suppressed by the doped F ions due to the strain effect according to the linear sweep voltammogramm (LSV) curves (Figure 3c). The HER current density at -0.3 V vs. RHE was strongly decreased by 43.5% for the F-MoS<sub>2</sub> catalyst compared with the pristine MoS<sub>2</sub> atalyst. It can be therefore indicated that HER activity of surface defects as well as phase interfaces of MoS<sub>2</sub> is much lower than that of the edge-defects. In the case of F-MoS<sub>2</sub>, activity of edge-defects was strongly reduced due to the compression effect of F ions. As a result, it is reasonable to imply that F-MoS<sub>2</sub> may possess greater acidic NRR selectivity. With the saturated gas in electrolyte changed to Nawacidic LSV of both MoS<sub>2</sub> and F-MoS<sub>2</sub> are positively shifted tompared with those collected in Ar-saturated electrolyte due to the widely approved NRR activity of MoS<sub>2</sub> (Figure S8). Especially at 1 mA/cm<sup>2</sup>, overpotential of  $MoS_2$  was decreased by 11 mV, attributed to reduction of N2, while this value is increased to 23 mV for the F-MoS<sub>2</sub> catalyst. This significant difference between the LSV curves of  $F-MoS_2$  in Ar and  $N_2$  condition indicates the great selectivity of F-MoS<sub>2</sub> on NRR. Similary, LSV current density difference of F-MoS<sub>2</sub>-2 with higher F content measured in Ar and N<sub>2</sub> condition is also remarkable (Figure S9) although the activity in both Ar and N<sub>2</sub> conditions was decayed due to the reduction of defects. By directly comparing the LSV curves of the two catalysts collected in N<sub>2</sub> saturated 0.05 M H<sub>2</sub>SO<sub>4</sub> solution (Figure 3d), current density decrement at -0.3 V vs. RHE ascribed to F doping is significantly reduced to 28.4%, ca. half of that in Ar saturated electrolyte. More importantly, current density of F-MoS<sub>2</sub> is high to 2.36 mA/cm<sup>2</sup>, which is even 22.6% higher than that of the pristine MoS<sub>2</sub> catalyst at -0.25 V vs. RHE. The strongly changed electrochemical catalytic property caused by the ambient adjustment can confirm the great selectivity of active sites in F-MoS<sub>2</sub> toward NRR.



Figure 3. (a) Sub-angstrom resolution HAADF-STEM image on surface of the F–MoS<sub>2</sub> flake. (b) Mo 3d high resolution XPS spectra and the pristine MoS<sub>2</sub> and F-MoS<sub>2</sub> catalysts. LSV curves of MoS<sub>2</sub> and F-MoS<sub>2</sub> measured in (c) Ar and (d) N<sub>2</sub> saturated 0.05 M H<sub>2</sub>SO<sub>4</sub> solutions.

Since great NRR selectivity of F-Mo<sub>2</sub>S in acidic condition was experimentally confirmed, first-principle calculation was subsquently deployed to theoretically evaluate the effect of F doping on the catalytic NRR activity of MoS<sub>2</sub>. The distal pathway in the association mechanism is more feasible than other pathways since it allows stabilizing the intermediates:

\*+N₂(g)→\*N₂→\*NNH→\*NNH₂→\*N+NH₃(g)→\*NH→\*NH₂→\*N H₃→\*+ NH₃(g)

Mo sites on the edge of  $MoS_2$  layers were chosen as the primary active sites of the NRR process since the Mo atom has both empty d orbitals which can accept the long-pair electrons

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from  $N_2$  molecules and the occupied d orbitals which are capable of reducing the N2 triple bond significantly. The free energy changes and the structures of each step of both MoS<sub>2</sub> and F-MoS<sub>2</sub> in NRR process are displayed in Figure 4. It can be noted that free energy change of nitrogen adsorption on F- $MoS_2$  edge (-0.85 eV) is significantly lower than  $MoS_2$  (-0.38 eV), which suggested that the introduction of F atom can enhance the  $N_2$  absorption ability on F-MoS<sub>2</sub>. The Gibbs free energy diagram for  $MoS_2$  (Figure 4a) showed that the first hydrogenation step of the adsorbed N<sub>2</sub> molecule occurs difficultly with an uphill free energy change of 0.64 eV. For the subsequent elementary reaction steps of the distal mechanism, the hydrogenation of \*N-NH<sub>2</sub> was followed by the release of first  $NH_3$  and then the \*N intermediate was formed. It can be therefore considered that the formation of \*N-NH, which bears the highest uphill free energy of 0.64 eV, is the ratedetermining step of NRR on MoS<sub>2</sub>. For F-MoS<sub>2</sub>, the Gibbs free energy change of the same rate-determining step is only 0.36 eV, which is 44% lower than that of MoS<sub>2</sub> (Figure 4b), aggreeing well with the significantly reduced NRR onset potential of F-MoS<sub>2</sub> comapred with the pristine MoS<sub>2</sub>.



Figure 4. Gibbs free energy diagrams of distal pathways for NRR on (a)  $F-MoS_2$  and (b)  $F-MoS_2$  at different applied potentials. (White, yellow, red, cyan and blue balls represent the H, S, F, Mo and N atoms, respectively.)

Since the effect of F doping on promotion of NRR selectivity and activity of F-MoS<sub>2</sub> are confirmed, chronoamperometry (CA) measurements were therefore carried out in N<sub>2</sub> saturated 0.05  $M H_2SO_4$  electrolyte (Figure S10) to quantitatively analyze the NRR performance of F-MoS<sub>2</sub> by utilizing the traditional indophenol blue method <sup>51</sup>. Typical double-cell three-electrode electrochemical setup with catalyst coated glassy carbon electrode as working electrode were used for the CA measurements and the calibration curves are displayed in Figure S11. UV-vis absorption spectra of the electrolyte stained with indophenol indicator after 2 h electrolysis at a series of potentials for MoS<sub>2</sub> and F-MoS<sub>2</sub> are displayed in Figure S12. It is suggested that both  $\mathsf{MoS}_2$  and  $\mathsf{F}\text{-}\mathsf{MoS}_2$  can catalyze NRR at -0.15 V vs. RHE and potentials ranging from -0.30 V to -0.15 V vs. RHE are selected to study the NRR electrocatalysis performance.

NH<sub>3</sub> yield calculated from the partial current densities for NH<sub>3</sub> production at various applied potential On MdS2 Shart AND S2 are compared in Figure 5a. Although overall current densities on these two catalysts are increased with the applied potential during the CA test (Figure S10), NH<sub>3</sub> yield is undependent on the applied potential. By considering the catalyst loading on the electrode, average NH<sub>3</sub> yield at -0.20 V vs. RHE of the F-MoS<sub>2</sub> catalyst is high to 35.7  $\mu$ g h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup>, which is among the best reported cost-effective NRR catalysts (Table S1). At the same time, this value is also higher than those measured at -0.15 V and -0.25 V vs. RHE. In contrast, NH<sub>3</sub> yield catalyzed by MoS<sub>2</sub> at -0.2 V vs. RHE is ca. 50% lower compared with that catalyzed by F-MoS<sub>2</sub> as desired although NH<sub>3</sub> yield of MoS<sub>2</sub> at -0.15 V vs. RHE is much higher than that of F-MoS<sub>2</sub>. As another important descriptor of NRR performance, FE of the catalysts was calculated (detail in Supporting Information) to evaluate the selectivity of NRR catalysts (Figure 5b). As expected, NRR FE of the F-MoS<sub>2</sub> catalyst is much greater than that of the pristine MoS<sub>2</sub> catalyst at applied potentials ranging from -0.20 V to -0.30 V vs. RHE. Especially at -0.2 V vs. RHE, NRR FE of the F-MoS<sub>2</sub> catalyst can reach 20.6%, which is among those of the best reported noble-metal-free catalysts (Table S1) and is also much greater than that of the pristine MoS<sub>2</sub>. In order to confirm the superior NRR catalytic activity of F-MoS<sub>2</sub>, we also carried out the Nuclear Magnetic Resonance (NMR) tests to quantitatively analyze the ammonia concentration from the established standard curve (Figure S13).<sup>52</sup> An intensive <sup>14</sup>NH<sub>4</sub>+ NMR signal was detected for F-Mo<sub>2</sub>S and the calculated Faradaic efficiency and NH<sub>3</sub> yield rate was similar to the UV-vis method shown in Figure 5c. Also, only <sup>15</sup>NH<sub>4</sub><sup>+</sup> signal was recorded with <sup>15</sup>N<sub>2</sub> as feeding gas depicting that and the N<sub>2</sub> gas, other than the residual contaminants from the catalyst synthesis, was the nitrogen source for the formation of NH<sub>3</sub>. Durability of NRR on F-MoS<sub>2</sub> was subsequently investigated by repeatedly performing the CA tests with NH<sub>3</sub> yield (Figure 5d) and NRR FE (Figure S14) collected. Both great activity and selectivity can be retained during the durability test. NH<sub>3</sub> yield is higher than 30  $\mu g$   $h^{\text{-1}}\,mg_{\text{cat}}^{-1}$  and FE is higher than 20% for all the five repeated tests. After 10 h continuously testing, NRR FE of NH<sub>3</sub> production on the F-MoS<sub>2</sub> catalyst is calculated to be

26%, which is even higher than that of the first two hours.

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Figure 5. (a) Average yield rate of NH<sub>3</sub> production and (b) NRR FE at different applied potentials on MoS<sub>2</sub> and F-MoS<sub>2</sub>; (c) NMR spectra of electrolyte after NRR catalysis by F-MoS<sub>2</sub> (insert: comparison of Faradaic efficiency and NH<sub>3</sub> yield rate of F-MoS<sub>2</sub> between UV-vis and NMR methods); (d) 10 h durability test for F-MoS<sub>2</sub> toward N<sub>2</sub> electrochemical reduction at -0.2 V vs. RHE.

#### Methods

**Catalyst synthesis.** The F-MoS<sub>2</sub> catalyst was prepared by a conventional hydrothermal method <sup>45, 48</sup>. 2.2836 g sulfocarbamide as S source and 11.1 mg NH<sub>4</sub>F as F source (atomic ratio of S to F is set to be 100:1) were dissolved in 40 mL deionized water under stirring for 30 min. Subsequently, 0.2358 g ammonium molybdate was added to form a homogeneous solution. The mixed solution was then transferred into a 50 mL Teflon-lined stainless steel autoclave and kept at 220 °C for 18 h. After cooled to room temperature, the product was washed with deionized water and ethanol for three times to remove any residual reactants. Same procedures were used for the pristine  $MoS_2$  preparation without NH<sub>4</sub>F.

**First-principle calculation.** The calculations were performed with the Vienna Ab-initio Simulation Package (VASP). <sup>53-55</sup> The Perdew-Burke-Ernzerhof (PBE) approximation <sup>56</sup> of density functional theory (DFT) was used to describe the exchange-correlation interactions and the projector augmented wave (PAW) method <sup>57</sup> to account for core-valence interactions. The energy cutoff for plane wave expansions was set to 400 eV, and the reciprocal space was sampled by a 2×2×1 grid which is generated by VASPKIT <sup>58</sup>. At least 15 Å vacuum layer was applied in the z-direction of the slab models to prevent the vertical interactions between slabs. All structures were fully relaxed to the ground state and spin-polarization was considered in all calculations. The convergence thresholds for structural optimization was set at 0.02 eV/Å in force and the convergence criterion for energy is  $1\times10^{-5}$  eV.

The reaction Gibbs free energy changes ( $\Delta$ G) for each step were based on the computational hydrogen electrode model proposed by Nørskov *et al* <sup>59, 60</sup>, and can be calculated using the following equation:

 $\Delta \mathbf{G} = \Delta \mathbf{E} + \Delta \mathbf{Z} \mathbf{P} \mathbf{E} - \mathbf{T} \Delta \mathbf{S} + \Delta \mathbf{G}_{U} + \Delta \mathbf{G}_{pH}$ 

where  $\Delta E$  is obtained directly from DFT calculations<sub>rt</sub> $\Delta Z B_{Hirls}$  the change in zero-point energies (ZPE), DOIs the 300 Mperature (298.15 K), and  $\Delta S$  is the change in entropy of products and reactants.

Details on material characterizations, electrochemical measurements and quantification of ammonia are provided in Supporting Information.

#### Conclusions

In summary, F ions were employed into the lattice of layeredstructural MoS<sub>2</sub> to compress the interlayer space to simultaneously improve the NRR selectivity and activity in acidic condition. HER activity of the F-MoS<sub>2</sub> catalyst is strongly reduced due to the strain effect and the NRR selectivity of the F-MoS<sub>2</sub> catalyst is therefore strongly enhanced. Since NRR activity of Mo<sub>2</sub>S can also be significantly boosted by the doped F ions according to the first-principle calculation, F-Mo<sub>2</sub>S was therefore considered as a superior NRR catalyst with relatively low cost. At relatively low overpotential (-0.2 V vs. RHE), NH<sub>3</sub> yield resulted from NRR is high to 35.7 µg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> with a great NRR FE of 20.6%. By considering the great durability of F-MoS<sub>2</sub>, this work provides a facile strategy for the destination of efficient N<sub>2</sub> fixation catalysts.

#### Conflicts of interest

There are no conflicts to declare.

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Interlayer space of  $MoS_2$  was compressed by the substituted F ions for the purpose of rationally boosting the NRR activity and selectivity.

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