

PdZn/ α -Al₂O₃ catalyst for liquid-phase alkyne hydrogenation: effect of the solid-state alloy transformation into intermetallics

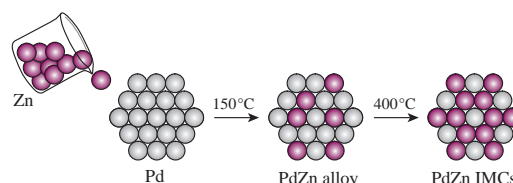
Igor S. Mashkovsky,^{*a} Pavel V. Markov,^a Galina O. Bragina,^a Galina N. Baeva,^a Aleksandr V. Rassolov,^a Andrey V. Bukhtiyarov,^b Igor P. Prosvirin,^b Valery I. Bukhtiyarov^b and Aleksandr Yu. Stakheev^a

^a N. D. Zelinsky Institute of Organic Chemistry, Russian Academy of Sciences, 119991 Moscow, Russian Federation. Fax: +7 499 135 5328; e-mail: im@ioc.ac.ru

^b G. K. Boreskov Institute of Catalysis, Siberian Branch of the Russian Academy of Sciences, 630090 Novosibirsk, Russian Federation

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The complex characterization of a PdZn/Al₂O₃ catalyst by XPS, XRD, TEM and H₂-TPD techniques revealed the route of solid-state alloy \rightarrow intermetallics transformation. The influence of this transformation on the performance of PdZn/Al₂O₃ in the liquid-phase hydrogenation of diphenylacetylene was estimated.



Nowadays, mono- and bimetallic clusters with controlled catalytic properties are extensively used as catalysts for a number of chemical processes due to the possibility of tuning their activity, selectivity and stability under reaction conditions.^{1–6} Intermetallic compounds (IMCs) are of growing interest as highly selective heterogeneous catalysts.^{7–9} In contrast to substituted alloys, IMCs are stable against segregation having ordered crystal structure different from the structure of the constituting metals. The intermetallic PdZn system is a promising catalytic composition, which is successfully used in industry for selective alkyne hydrogenation, methanol steam reforming, biomass conversion, *etc.*¹⁰ Several reviews have been focused on the general properties of IMCs and on the properties of PdZn compositions in particular.^{6,7,11} It is important that the PdZn system can form either substituted solid-state alloy or IMCs.¹² However, the effect of PdZn solid-state alloy–PdZn IMCs transformation on the catalytic performance was not studied in details. Here, to trace this effect, the PdZn/Al₂O₃ catalyst was reduced stepwise at 150, 200, 250, 300, 350 and 400 °C; after each reduction stage, a sample of the catalyst was taken for characterization and catalytic study. Details of catalyst preparation and characterization by XPS, XRD, TEM and H₂-TPD techniques can be found in Online Supplementary Materials.

The XPS study of the formation of Pd–Zn bimetallic particles was carried out by monitoring the Pd 3d and Zn 2p regions (Figure 1) after each step of catalyst reduction. Before reduction, Pd 3d_{5/2} and Zn 2p_{3/2} peaks were observed at 337.2 and 1022.3 eV for PdO and ZnO, respectively.^{13,14} After reduction at 200–250 °C, the Pd 3d_{5/2} peak shifted to 335.8 eV indicating Pd²⁺ \rightarrow Pd⁰ reduction and characteristic of Pd⁰ in PdZn alloy.^{7,15,16} In the Zn 2p region, an additional signal appeared at 1020.5 eV characteristic of Zn⁰. This observation suggests that the reduction of Zn is facilitated in the presence of Pd *via* hydrogen activated on Pd. Note that the Zn 2p_{3/2} binding energy is lower than that of metallic Zn (~1021.5 eV) denoting the formation of PdZn alloy.¹² XPS analysis also demonstrates that the Zn⁰/Pd⁰ ratio is about 1.0, and this value is achieved after reduction at 200 °C.

After reduction at 300 and 400 °C, Zn⁰ 2p_{3/2} predominates indicating further reduction of Zn. Simultaneously, we can

observe a minor shift of Pd 3d_{5/2} toward a lower binding energy by 0.3–0.4 eV. This shift can be tentatively ascribed to the formation of PdZn intermetallics (see XRD data below). Alternatively, it may be caused by Zn evaporation and partial depletion of the PdZn particle surface in zinc¹⁷ since the Zn⁰/Pd⁰ ratio decreases from ~1.0 to ~0.5 after reduction at 400 °C.

Figure 2 shows XRD patterns for the PdZn/ α -Al₂O₃ supported catalysts reduced at different temperatures. Profiles of Pd/ α -Al₂O₃ and unreduced PdZn/ α -Al₂O₃ are also displayed for comparison. For the reference monometallic Pd/Al₂O₃ catalyst, two XRD reflexes were observed at ~40.0° and ~46.7°, corresponding to Pd(111) and Pd(200), respectively.¹⁸ The XRD pattern of the unreduced PdZn catalyst displays a group of signals at 31.0–35.0°. A wide and asymmetrical peak at ~34.0° can be attributed to PdO,¹⁹ and low-intensity peaks at ~31.8°, ~34.3° and ~36.3° are assigned to (100), (002) and (101) of ZnO with a polycrystalline wurtzite structure, respectively.^{20–22} No typical Zn⁰ signals at 38.9°, 43.1° or 54.2° were observed.^{14,23}

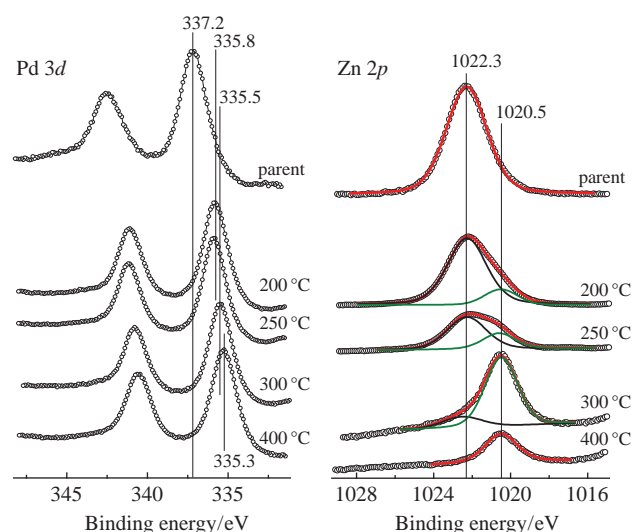


Figure 1 Pd 3d and Zn 2p XPS spectra of parent PdZn/ α -Al₂O₃ catalysts and those reduced (H₂, 250 mbar, 1 h) at different temperatures.

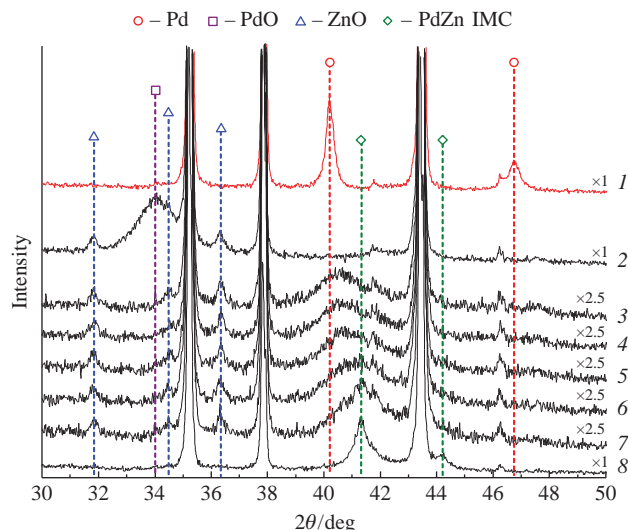


Figure 2 Comparison of XRD patterns for (1) Pd/ α -Al₂O₃ and (2) PdZn/ α -Al₂O₃ catalysts, parent and (3)–(8) reduced at (3) 150, (4) 200, (5) 250, (6) 300, (7) 350 and (8) 400 °C.

After PdZn/ α -Al₂O₃ reduction at 150 °C, the intensities of PdO and ZnO signals diminished and a wide reflex appeared at \sim 39.0–41.5°. Note that the position of its maximum does coincide with the position of Pd(111) \sim 40.0° in Pd/Al₂O₃ and is shifted toward higher 2θ with a maximum at 40.6°, which suggests the formation of PdZn substituted alloy even at a temperature of 150 °C. Low intensity of a signal, its asymmetry and the absence of the Pd(200) reflex at 46.7° indicate that the structure of the alloyed particles is largely disordered and the formed particles are small. These results are consistent with published data²⁴ and TEM data (Figure 3). The following H₂ treatment at 200 and 250 °C results in a gradual shift of the peak at 40.6° toward higher angles indicating the enrichment of PdZn solid solution in Zn.²⁵ Simultaneously, the intensity of ZnO reflex notably decreases.

The transformation of PdZn solid-state alloy to the intermetallic structure begins as the temperature is raised above 300 °C. A wide Bragg peak appears at \sim 41.4° ascribed to PdZn intermetallic compound.^{9,22,26} However, the most part of PdZn particles is still as a solid-state alloy, as evidenced by the broadening and low intensity of a peak at \sim 41.4°. With a further increase in H₂ reduction temperature to 400 °C, the intensity of this signal grows, and it becomes more symmetrical and intense. Moreover, an additional reflex appears at 44.0° giving distinct

evidence for the formation of PdZn IMCs.^{9,14} The asymmetry of this reflex indicates some irregularity of IMCs structure.^{10,15,27}

Since our XPS and XRD data suggest the formation of PdZn alloy after reduction at 150–200 °C, we additionally verify its formation by an H₂-TPD method. A specific characteristic of Pd is its ability to absorb a considerable amount of H₂ to form α - and/or β -PdH_x hydride phases.^{28,29} The hydrogen of this hydride structure is capable to migrate to Pd surface under reaction conditions enhancing the complete alkyne hydrogenation. However, upon the formation of a bimetallic PdM (M = Cu, Ag, In, Pb, *etc.*) alloy, the solubility of hydrogen significantly decreases; this makes it possible to avoid or minimize the PdH phase formation.^{30,31} Thus, the higher selectivity of bimetallic or intermetallic hydrogenation catalysts can be attributed to the inhibition of palladium hydride phase formation.^{8,32}

An H₂-TPD study was performed to compare Pd hydride formation ability in PdZn/Al₂O₃ and Pd/Al₂O₃ (Figure S1, Online Supplementary Materials). The H₂-TPD profile of Pd/Al₂O₃ displays a desorption peak at 75–90 °C with a maximum at 83 °C characteristic of PdH_x decomposition.^{26,28,33} In contrast, no signal was observed in the TPD pattern of the PdZn/Al₂O₃ catalyst reduced at 150 and 400 °C. This observation provides evidence of PdZn solid-state alloy formation even after reduction at 150 °C, in agreement with XPS and XRD data.

Thus, XPS, XRD and H₂-TPD results clearly indicate the formation of solid-state PdZn alloy after reduction at 150–300 °C and its transformation to IMCs as the reduction temperature increases to 350–400 °C. To reveal the effect of this transformation on the catalytic performance in alkyne hydrogenation, the synthesized catalysts were studied in the liquid-phase hydrogenation of diphenylacetylene. Figure 4 shows the kinetic profiles of hydrogen uptake for Pd/Al₂O₃ and PdZn/Al₂O₃ samples reduced at different temperatures. The PdZn/Al₂O₃ catalyst reduced at 200 °C exhibited a distinctly different kinetic behavior, as compared to that of the parent Pd sample. The kinetic profile of PdZn/Al₂O₃ catalyst exhibits pronounced downward bending after the uptake of 1 equiv. of H₂. A comparison of TOF₁ (alkyne to alkene hydrogenation) and TOF₂ (alkene to alkane hydrogenation) values shows that TOF₁ for PdZn/Al₂O₃ decreases by a factor of 4, while TOF₂ decreases by a factor of \sim 17 in comparison with that of the monometallic Pd/Al₂O₃ (see Table S1 in Online Supplementary Materials). As a result, the TOF₁/TOF₂ ratio (so-called kinetic selectivity) increases by a factor of 4: from 9.61 for Pd/Al₂O₃ to \sim 38 for PdZn/Al₂O₃. Taking into account H₂-TPD data, we can suggest that the lower TOF₂ value for PdZn/Al₂O₃ catalysts originates from the disappearance of a PdH_x hydride

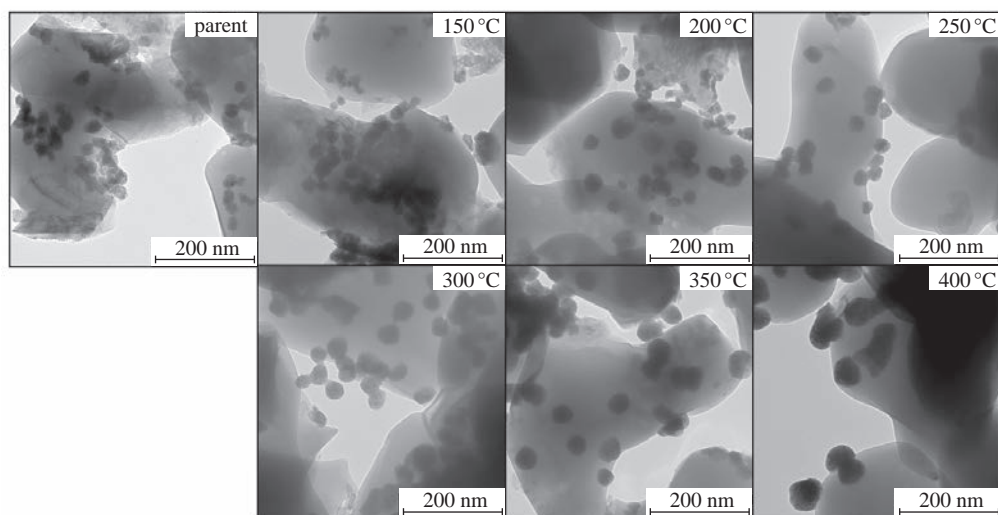


Figure 3 TEM images of parent PdZn/ α -Al₂O₃ catalysts and the catalysts reduced at 150–400 °C.

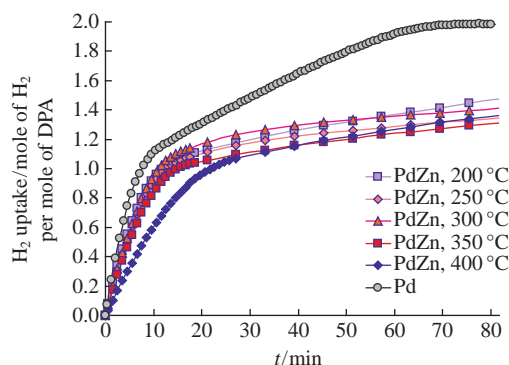


Figure 4 Effect of reduction temperature on the hydrogen uptake for Pd/Al₂O₃ and PdZn/Al₂O₃ catalysts in the liquid-phase hydrogenation of diphenylacetylene.

phase due to PdZn alloy formation. The observed change of the general reaction kinetics on the PdZn/Al₂O₃ catalyst is of considerable practical interest since it allows one to effectively control the course of the reaction and to stop the hydrogenation after the complete alkyne conversion into olefin.

It is important to note the identity of catalytic performances of PdZn/Al₂O₃ samples reduced at 200–400 °C. Only a slight decrease in the overall catalytic activity was observed, which is probably attributed to the enlargement and agglomeration of bimetallic nanoparticles under reduction conditions in accordance with TEM data (Figure 3). The particle size of PdZn IMCs increases from 17 (for PdZn sample reduced at 150 °C) to ~57 nm (after 400 °C treatment). An increase in the reduction temperature also does not lead to appreciable changes in the selectivity of the process. At a 90% alkyne conversion, selectivity of alkene formation for Pd/Al₂O₃ is about 91% while for PdZn/Al₂O₃ this parameter is ~92–94% (Table S1). This result clearly indicates that the PdZn solid-state alloy–PdZn intermetallic compound transformation does not exert a significant effect on the catalytic performance.

Thus, a comparison of the catalytic data with XRD, XPS, and H₂ TPD results suggests that the main reason for the change in the overall kinetics of hydrogenation on PdZn catalysts compared to monometallic Pd results mostly from the suppression of a PdH phase due to PdZn substitutional alloy formation, whereas the PdZn solid-state alloy–PdZn IMCs transformation only slightly affects catalytic characteristics.

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Online Supplementary Materials

Supplementary data associated with this article can be found in the online version at doi: 10.1016/j.mencom.2018.03.014.

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