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Ambient-Temperature Synthesis of Primary Amines *via* Reductive Amination of Carbonyl Compounds

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KEYWORDS: Reductive amination, Ambient temperature, Primary amines, Carbonyl compounds, Supported metal catalysts

ABSTRACT: Efficient synthesis of primary amines *via* low-temperature reductive amination of carbonyl compounds using NH₃ and H₂ as the nitrogen and hydrogen resources is highly desired and challenging in chemistry community. Herein, we employed naturally occurring phytic acid as a renewable precursor to fabricate titanium phosphate (TiP)-supported Ru nanocatalysts with

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3 different reduction degrees of RuO₂ (Ru/TiP-x, x represents the reduction temperature) by
4 combining ball milling and molten-salt processes. Very interestingly, the obtained Ru/TiP-100
5 had good catalytic performance for the reductive amination of carbonyl compounds at ambient
6 temperature, resulting from the synergistic cooperation of the support (TiP) and the Ru/RuO₂
7 with suitable proportion of Ru⁰ (52%). Various carbonyl compounds could be efficiently
8 converted into the corresponding primary amines with high yields. More importantly, the
9 conversion of other substrates with reducible groups could also be achieved at ambient
10 temperature. Detail investigations indicated that the partially reduced Ru and the support (TiP)
11 were indispensable. The high activity and selectivity of Ru/TiP-100 catalyst is originated from
12 the relative high acidity and the suitable electron density of metallic Ru⁰.
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31 1. INTRODUCTION

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34 Primary amines are very important compounds and are widely applied to produce fine chemicals,
35 agrochemicals, pharmaceuticals, and functionalized materials, *etc.*¹⁻³ Synthesis of primary
36 amines is of central importance,⁴⁻⁸ and several synthetic methods have been developed, including
37 reductive amination of carbonyl compounds,⁹⁻¹² *N*-alkylation of ammonia with haloalkanes¹³ or
38 alcohols,¹⁴⁻¹⁶ and reduction of specific nitrogen sources (*e.g.*, oxime ethers,¹⁷ amides,¹⁸ nitriles,¹⁹
39 and nitro compounds²⁰). Among these methods, reductive amination of carbonyl compounds
40 employing ammonia (NH₃) and H₂ as the nitrogen resource and reductant is the most attractive
41 route because carbonyl compounds, NH₃ and H₂ are all inexpensive and widely available raw
42 materials. Moreover, the reductive amination of carbonyl compounds can proceed at relatively
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3 mild conditions and water is the main byproduct. This makes reductive amination of carbonyl
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5 compounds an atom-effective and environmental-friendly approach to produce primary amines.
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8 Various catalysts, especially supported metals, have been developed for the synthesis of
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10 primary amines *via* reductive amination of carbonyl compounds.²¹⁻²⁸ For example, Ni@SiO₂
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12 (using NH₃ and 2 MPa H₂)²¹ and Ni/Al₂O₃ (using aqueous ammonia and 1 MPa H₂)²² can
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14 catalyze reductive amination of carbonyl compounds at 120 and 80 °C, respectively. MOF-
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16 derived cobalt nanoparticles could efficiently catalyze the formation of primary amines *via*
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18 reductive amination using NH₃ and 4 MPa H₂ at 120 °C.²³ Moreover, reductive amination of
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20 aldehydes/ketones could be carried out with aqueous NH₃ and 2 MPa H₂ over partially reduced
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22 Ru/ZrO₂ at 65-125 °C,²⁴ and Ru/Nb₂O₅ could promote the reductive amination of carbonyl
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24 compounds using NH₃ at 90 °C and 4 MPa H₂.²⁵ It was also found that Pd⁰/enzymatic multiple
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26 relay catalytic system showed good performance for the reductive amination of carbonyl
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28 compounds using HCO₂NH₄ at 80 °C.²⁶ Additionally, primary amines could be generated from
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30 reductive amination of carbonyl compounds over Cu/ZrO₂ at 250 °C,²⁷ Pt-MoO_x/TiO₂ at 100
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32 °C,²⁸ and Rh/Al₂O₃ at 80 °C,²⁹ *etc.* However, most of these processes require high reaction
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34 temperature, and one great challenge in this area is to develop robust and efficient catalytic
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36 systems that can perform reductive amination of carbonyl compounds at ambient temperature.
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43 Herein, we developed a series of titanium phosphate-supported Ru nanocatalysts (denoted
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45 as Ru/TiP-x, and x represents the reduction temperature), which employed naturally occurring
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47 phytic acid as a renewable precursor. These Ru catalysts with different reduction degree of RuO₂
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49 were then systematically investigated for the reductive amination of carbonyl compounds to
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51 produce primary amines using NH₃ and H₂ as the nitrogen and hydrogen resources. It was found
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53 that the Ru/TiP-100 with a reduction degree of RuO₂ of around 52% showed the highest activity
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3 and selectivity at ambient temperature, resulting from the desirable electron density of the
4 metallic Ru and the strong acidity of the titanium phosphate. The fact that this catalytic reaction
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8 can be performed at ambient temperature with Ru-TiP-100 represents a major breakthrough in
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10 this area. The synergistic cooperation between the active metal species and the support resulted
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12 in its high activity; and the wide applicability of this catalyst to other substrates with other
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14 reducible groups further confirms its great potential.
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21. METHODS

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24 **2.1. Materials.** Ruthenium(III) chloride (99%), titanium(IV) *n*-butoxide (99%),
25 cyclohexanone (99%), cycloheptanone (99%), 2-pentanone (99%), 4-methyl-2-pentanone (99%),
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27 3-pentanone (99%), 2-octanone (99%), 2-nonanone (99%), 4-phenyl-2-butanone (99%),
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29 valeraldehyde (98.5%), *n*-octanal (98%), 3-phenylpropionaldehyde (95%), furfural (98%),
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31 benzaldehyde (98%), 4-fluorobenzaldehyde (99%), 4-chlorobenzaldehyde (98%), 4-
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33 bromobenzaldehyde (99%), *p*-anisaldehyde (99%), 3,4-dimethoxybenzaldehyde (99%), 4-*tert*-
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35 butylbenzaldehyde (96%), 4-acetamidobenzaldehyde (98%) and methyl 4-formylbenzoate (99%)
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37 were provided by J&K Scientific Ltd. Potassium nitrate (99+%), androsterone (97%) and
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39 titanium(IV) oxide (98%) were obtained from Acros. Phytic acid (70+% aqueous solution),
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41 methanol and acetone were purchased from Sinopharm Chemical Reagent Beijing Co. Ltd.
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43 Cyclopentanone (99.5%), acetophenone (99%) and zirconium dioxide (99%) were purchased
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45 from Alfa Aesar. Butyraldehyde (99%), citronellal (96%), 3-pyridinecarboxaldehyde (98%), 5-
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47 hydroxymethylfurfural (98%) and Ru/C (5 wt%) were purchased from Innochem. 4-Formyl-
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49 *trans*-stilbene (98%) was purchased from TCI.
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3 **2.2. Preparation of RuO₂/TiP and TiP.** In a typical procedure for preparing RuO₂/TiP,
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5 phytic acid (1 mmol) and tetrabutyl titanate (3 mmol) were completely mixed with potassium
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7 nitrate (15 g) by ball milling in a polyurethane tank (50 ml) with zirconia balls (3 mm×10 g and
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9 8 mm×50 g) for 10 h, and the milling speed was 300 r min⁻¹. After the above process, the milling
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11 tank was placed into an oven (80 °C) for 12 h to evaporate the generated *n*-butyl alcohol. Then,
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13 ruthenium trichloride (RuCl₃, 1 mmol) was added, and the mixture was milled for another 24 h.
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15 After the mixture was further dried at 80 °C in a vacuum oven to remove the small amount of
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17 water and *n*-butyl alcohol, it was further milled for 6 h to ensure that RuCl₃ was dispersed
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19 uniformly. After that, the obtained solid was calcined in air at 400 °C for 2 h (5 °C min⁻¹).
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21 Finally, the product was thoroughly washed with hot deionized water to remove KNO₃. The only
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23 difference for the preparation of TiP was that the step for the addition of RuCl₃ was omitted.
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29 **2.3. Preparation of Ru/TiP-x.** RuO₂/TiP was loaded into the reactor with methanol. After
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31 sealing, 2 MPa H₂ was charged and the reactor was put into a constant temperature air bath at
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33 desired temperature for 2 h. Finally, Ru/TiP-x, where x represented the reduction temperature,
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35 was recovered by centrifugation, and washed with methanol and ethyl ether (5 × 10 mL), then
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37 finally dried at 60 °C under vacuum.
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41 **2.4. Preparation of Ru/TiO₂, and Ru/ZrO₂.** The synthesis of Ru/ZrO₂ and Ru/TiO₂ are of
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43 similar procedures and here we use Ru/ZrO₂ as an example. In a typical procedure for preparing
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45 Ru/ZrO₂ (Ru 5 wt%), ZrO₂ (0.5 g) was initially dispersed into an aqueous solution of RuCl₃
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47 under stirring and kept overnight. The solvent was slowly evaporated at 60 °C by the rotary
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49 evaporation. Then, the solid was further dried at 80 °C for 12 h under vacuum, and subsequently
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51 calcined at 300 °C for 2 h (5 °C min⁻¹). Finally, the obtained sample was reduced at 150 °C under
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3 hydrogen flow for 2 h. Ru/TiO₂ was also prepared according to this route by changing the
4 support from ZrO₂ to TiO₂.
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8 **2.5. Typical procedures for the reductive amination of carbonyl compounds.** In a
9 typical experiment, the desired carbonyl compound and catalyst were charged into a stainless
10 steel reactor with Teflon coating (14 mL inner volume). After the reactor was sealed, it was
11 purged with 0.2 MPa NH₃ for three times to remove air residual. After that, the NH₃ was charged
12 into the reactor to reach a desired pressure. Then, the reactor was further pressurized with H₂.
13 Then the reactor was put into a constant temperature air bath at desired temperature, and the
14 magnetic stirrer was started. After a certain reaction time, the reactor was placed into ice water
15 and the gases in the reactor was released slowly through a cold trap containing methanol to
16 absorb the trace amounts of reactant and product. After depressurization, methanol in the cold
17 trap and internal standard *n*-butanol (cyclohexanol for the case with butyraldehyde as the
18 substrate) were added into the reactor. The reaction mixture was then analyzed quantitatively by
19 GC (Agilent 6820) equipped with a flame-ionized detector, and identification of the products
20 was done by GC-MS (Shimadzu QP2010).
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38 **2.6. Reusability of the Ru/TiP-100.** To examine the reusability of Ru/TiP-100, the catalyst
39 was recovered by centrifugation and washed with methanol and ethyl ether (5 × 10 mL). After
40 drying under vacuum at 60 °C for 12 h, the recovered catalyst was reused for the next cycle.
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45 **2.7. Characterization.** The scanning electron microscopy (SEM) measurements were
46 performed on a Hitachi S-4800 scanning electron microscope operated at 15 kV. The
47 transmission electron microscopy (TEM) images were obtained using a TEM JEOL-1011 and
48 TEM JEOL-2100. Powder X-ray diffraction (XRD) patterns were collected on a Rigaku D/max-
49 2500 X-ray diffractometer using Cu K α radiation (λ = 0.154 nm). Fourier transform infrared
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3 (FT-IR) spectra were recorded using a Bruker Tensor 27 spectrometer and the samples were
4 prepared by the KBr pellet method. The N₂ adsorption-desorption isotherm was determined using
5 the Micromeritics ASAP 2020 msystem. X-ray photoelectron spectroscopy (XPS) measurements
6 were carried out on a ESCAL Lab 220i-XL specrometer. The content of Ru in the RuO₂/TiP was
7 determined by inductively coupled plasma atomic emission spectroscopy (ICP-AES VISTA-
8 MPX). ³¹P MAS NMR measurements were carried out on Bruker AVIII 500WB. H₂-TPR, NH₃-
9 TPD and CO₂-TPD were performed on Micromeritics' AutoChem 2950 HP Chemisorption
10 Analyzer. AFM was performed on Dimension FASTSCANBIO. CO-DRIFT spectra were
11 collected on Bruker Tensor II spectroscope equipped with a MCT detector. The sample was
12 degassed at 300 °C for 2 h and then cooled to 25 °C in a Ar flow (10 mL min⁻¹). Taking this as
13 the background, the sample was exposed to a 0.4% CO/Ar flow, and then purged in an Ar flow
14 (10 mL min⁻¹) to remove physically adsorbed CO. IR spectra of chemisorbed CO were recorded
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37 **3. RESULTS AND DISCUSSION**

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40 **3.1. Preparation and Characterization of the RuO₂/TiP.** Titanium phosphate supported
41 RuO₂ material (RuO₂/TiP) was synthesized using naturally occurring phytic acid as the
42 renewable precursor through the combination of ball milling and molten-salt processes (Figure
43 S1), which were widely employed in the synthesis of nanomaterials.³⁰⁻³² Power X-ray diffraction
44 (XRD) patterns (Figure 1A) showed that the prepared RuO₂/TiP had low crystallinity with no
45 characteristic peaks of RuO₂ species, indicating that the RuO₂ species were highly dispersed
46 without aggregation. In the ³¹P MAS NMR spectra, ³¹P signal for RuO₂/TiP became broadened
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with a slight shift compared with that of phytic acid (Figure 1B), indicating the presence of strong interaction between Ti^{4+} and the phosphate groups. Moreover, in FT-IR spectrum of RuO_2/TiP (Figure S2A), a sharp band around 1050 cm^{-1} corresponding to Ti-O-P stretching vibrations was found, while this band was absent for TiO_2 , suggesting the presence of Ti-O-P networks in RuO_2/TiP .^{33,34} Additionally, Brunauer-Emmett-Teller (BET) surface area of RuO_2/TiP was $225.3\text{ m}^2/\text{g}$ as calculated from the N_2 adsorption-desorption isotherm (Figure S2B).

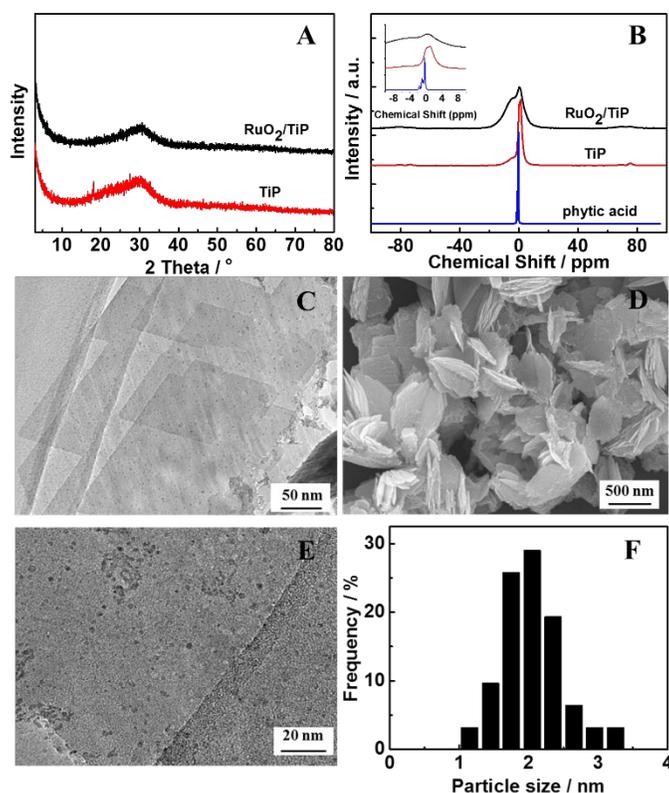


Figure 1. Characterization of the synthesized RuO_2/TiP . (A) Powder XRD pattern, (B) ^{31}P MAS NMR spectra, (C,E) TEM image, (D) SEM images and (F) the size distribution of RuO_2 particles in the prepared RuO_2/TiP .

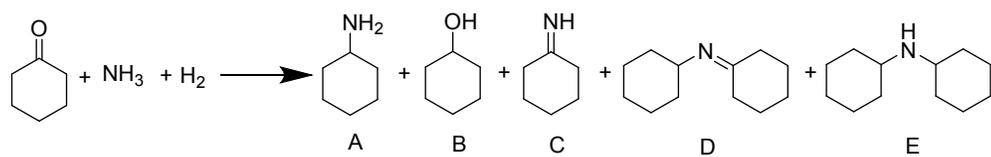
Transmission electron microscopy (TEM) and scanning electron microscopy (SEM) images clearly showed that the synthesized RuO_2/TiP had a two-dimensional structure (Figures 1C and

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3 1D), and the thickness of RuO₂/TiP nanosheets was around 2 nm as measured by AFM (Figure
4 S3). Meanwhile, RuO₂ nanoparticles dispersed uniformly in the RuO₂/TiP (Figure 1E) with the
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6 particle sizes centered at 2 nm (Figure 1F), which was consistent with the results of XRD (Figure
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8 1A). Elemental distribution mappings (Figure S4) indicated that Ti, O, P and Ru were dispersed
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10 uniformly in RuO₂/TiP. Additionally, H₂-TPR (Figure S5) demonstrated that the RuO₂/TiP could
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12 be reduced from 60 °C, and the advantage of such low temperatures is that the reduction degree
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14 of RuO₂ can be easily controlled, and the reduction process does not affect the size distribution
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16 of Ru species or the structure of the catalysts.
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23 **3.2. Activity of various catalysts.** Ru-based catalysts are generally known to favor the
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25 formation of primary amines by the reductive amination of carbonyl compounds, thus various
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27 Ru-based catalysts were initially screened for the reductive amination of cyclohexanone to
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29 cyclohexylamine as a model reaction at 30 °C (Table 1). In the absence of any catalysts, no
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31 cyclohexylamine was detected (Table 1, entry 1). The synthesized RuO₂/TiP with 3.35 wt% Ru
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33 (from ICP-AES) was found inactive for the formation of cyclohexylamine (Table 1, entry 2). In
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35 contrast, cyclohexylamine was generated over Ru/TiP-80 (Table 1, entry 3), indicating the key
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37 role of metallic Ru in this catalytic reaction. It has been reported that the reduction degree of
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39 RuO₂ in the Ru/ZrO₂ catalysts could greatly affect their activity and selectivity of reductive
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41 amination.²⁴ Therefore, we carried out the reduction of the obtained RuO₂/TiP at different
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43 temperature and time to control the reduction degree of RuO₂, which shows key influences to the
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45 catalytic activity (Figures 2A and 2B) as discussed in the following section. At 30 °C, the
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47 Ru/TiP-100 with a RuO₂ reduction degree of 52% (Table 1, entry 4) showed better performance
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49 than Ru/TiP-80 (44% reduction degree, Table 1, entry 3), and the yield of cyclohexylamine
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51 could reach 97% over the Ru/TiP-100 with a complete conversion of cyclohexanone. When the
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3 reaction was conducted at 30 °C over Ru/TiP-150 (55% reduction degree), the cyclohexylamine
4 yield slightly decreased with more cyclohexanol generated (Table 1, entry 5). Negligible
5 cyclohexylamine was detected when the reaction was carried out at 30 °C with Ru/TiP-150-30h
6 (67% reduction degree, Table 1, entry 6), and higher reaction temperature (80 °C) was needed to
7 achieve a good yield of cyclohexylamine (91%) with a reaction time of 6 h (Table 1, entry 7). In
8 comparison, we examined the activity of Ru/TiO₂ (with a RuO₂ reduction degree of 53%) and
9 the reported Ru/ZrO₂-150 (with a RuO₂ reduction degree of 49%) under our reaction conditions
10 (Table 1, entries 8 and 9), but poor performance was achieved. Ru/ZrO₂-150 was efficient but
11 only at higher reaction temperature (95 °C),²⁴ suggesting that the support material was also a key
12 factor for the performance of the catalysts. Additionally, commercial Ru/C catalyst (Table 1,
13 entries 10 and 11) also required high temperature (80 °C) and longer reaction time (24 h) to
14 achieve a relative high yield of cyclohexylamine (82%) with the formation of more cyclohexanol
15 (about 16%). The above results indicated that the Ru/TiP-100 was the only efficient catalyst at
16 ambient temperature for the conversion of cyclohexanone to cyclohexylamine.
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Table 1. Activity of various catalysts for reductive amination of cyclohexanone.^a



C1CCCCC1=O + NH₃ + H₂ →
 C1CCCCC1N (A) +
 C1CCCCC1O (B) +
 C1CCCCC1=NO (C) +
 C1CCCCC1=N(C2CCCCC2) (D) +
 C1CCCCC1NC2CCCCC2 (E)

Entry	Catalyst	Conversion (%)	Yield (%)				
			A	B	C	D	E
1	Blank	85	0	0	81	0	0
2	RuO ₂ /TiP	83	0	0	80	0	0
3	Ru/TiP-80	>99	10	2	0	83	0
4	Ru/TiP-100	>99	97	2	0	<1	0
5	Ru/TiP-150	>99	96	4	0	0	0
6 ^b	Ru/TiP-150-30h	71	<1	1	33	34	0
7 ^c	Ru/TiP-150-30h	>99	91	9	0	0	0
8 ^d	Ru/TiO ₂	93	<1	0	54	36	0
9 ^e	Ru/ZrO ₂	90	<1	0	58	27	0
10	Ru/C	90	0	0	73	14	0
11 ^f	Ru/C	>99	82	16	0	2	0

^aReaction conditions: cyclohexanone, 1 mmol; methanol, 2 mL; H₂, 1.4 MPa; NH₃, 0.6 MPa; catalyst, 0.2 mol%; 30 °C; 6 h. The Ru loading in RuO₂/TiP-x, Ru/TiO₂, Ru/ZrO₂, and Ru/C was 3.35, 4.86, 5.04, and 5 wt%, respectively. ^bThe reduction time for RuO₂/TiP was 30 h. ^cThe reaction was conducted at 80 °C. ^dThe reduction degree of RuO₂ in Ru/TiO₂ was controlled at 53%. ^eThe catalyst was prepared based on reference 24. ^fThe reaction was conducted at 80 °C for 24 h.

3.3. Effect of H₂/NH₃ Ratio on the Reaction Activity and Selectivity. H₂/NH₃ ratio is another key factor in determining the selectivity of cyclohexylamine over Ru/TiP-100 catalyst (Figure 2C), and the best H₂/NH₃ ratio was found to be 7/3. Lowering or rising H₂/NH₃ ratio was found to suppress the subsequent conversion of the formed Schiff base to the desired primary amine. In another aspect, more cyclohexanol would be generated from the direct hydrogenation of cyclohexanone with excess H₂.

3.4. Reusability of Ru/TiP-100. As important properties of a heterogeneous catalyst, the reusability and the heterogeneous nature of Ru/TiP-100 were evaluated as these are the crucial.

Ru/TiP-100 could be recycled for at least 5 times without decline of the catalytic activity and product selectivity (Figure 2B). Moreover, no obvious change was observed between the virgin and recovered Ru/TiP-100 as characterized by SEM, TEM and XPS (Figure S6), further confirms the high stability of Ru/TiP-100. Additionally, the yield of cyclohexylamine plateaued after Ru/TiP-100 was removed from the reaction system after 3 h (Figure S7), and no Ru species were detected by ICP examination. These results firmly verified the heterogeneous nature of Ru/TiP-100.

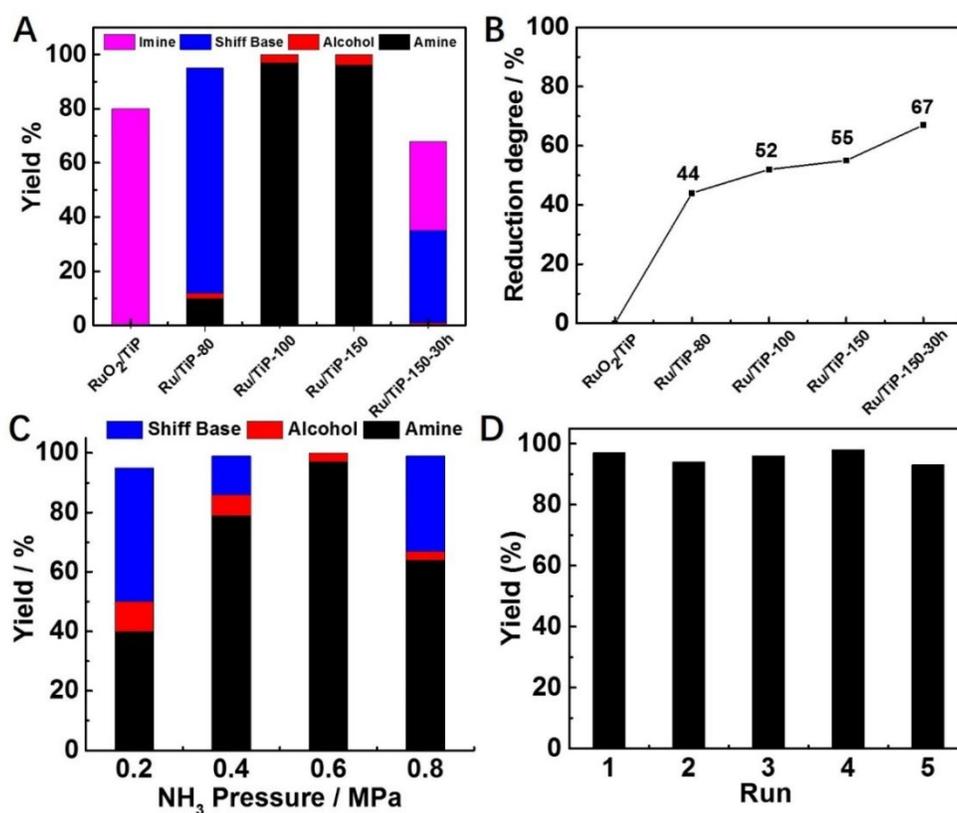
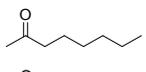
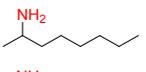
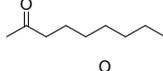
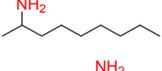
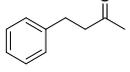
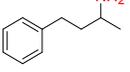


Figure 2. (A) Effect of reduction temperature for RuO₂/TiP, (B) Reduction degree of RuO₂/TiP in Ru/TiP-x detected by XPS, (C) Effect of NH₃ pressure, and (D) Reusability of Ru/TiP-100. Reaction conditions: cyclohexanone, 1 mmol; methanol, 2 mL; 30 °C; 6 h; Ru/TiP-100, 0.2 mol%; Total pressure of NH₃ and H₂ was 2 MPa, and 1.4 MPa H₂ and 0.6 MPa NH₃ in D.

3.5. Scope of the substrates. Encouraged by the good performance of Ru/TiP-100 for the reductive amination of cyclohexanone, the reductive amination of other ketones was explored

over Ru/TiP-100 (Table 2). In our catalytic system, all examined alkyl ketones (Table 2, entries 1-8) could be efficiently converted into the corresponding primary amines with good yields at 30 °C. Although the reactivity of aryl ketone (acetophenone) was very poor at 30 °C because of the electronic and steric effect of phenyl group (Table 2, entry 9), a satisfactory yield (93%) of the desired product could be achieved (Table 2, entry 10) by increasing the temperature (80 °C) and lowering the H₂ pressure (0.4 MPa H₂ in a total pressure of 1 MPa).

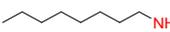
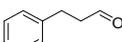
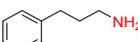
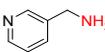
Table 2. Reductive amination of various ketones over Ru/TiP-100.^a

Entry	Ketone	Product	Time (h)	Yield (%)
1			10	92
2			6	97
3			10	95
4			10	96
5			15	97
6			10	95
7			10	94
8			15	98
9			24	<1
10 ^b			24	93

^aReaction conditions: ketone, 1 mmol; methanol, 2 mL; H₂, 1.4 MPa; NH₃, 0.6 MPa; Ru/TiP-100 (the Ru loading was 3.35 wt% Ru), 0.2 mol%; 30 °C. ^b80 °C; NH₃, 0.6 MPa; H₂, 0.4 MPa.

In comparison with ketones, the reductive amination of aldehydes to primary amines with high selectivity is more challenging because of their higher reactivity. To our delight, Ru/TiP-100 even showed high activity and selectivity for reductive amination of various aldehydes with a suitable NH₃/H₂ ratio (1.7 MPa H₂ and 0.3 MPa NH₃ at a total pressure of 2 MPa) at 30 °C (Table 3), and the corresponding primary amines could be generated with high selectivity. In addition, it was demonstrated that Ru/TiP-100 showed much better performance under lower reaction temperature (30 °C) and H₂ pressure (< 2 MPa) than the typical reported catalysts (Table S1). These results further indicated the good performance of Ru/TiP-100 for the reductive amination of various carbonyl compounds.

Table 3. Reductive amination of various aldehydes over Ru/TiP-100.^a

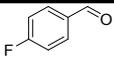
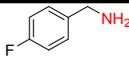
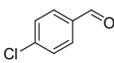
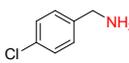
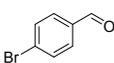
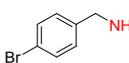
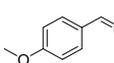
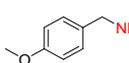
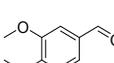
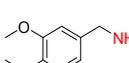
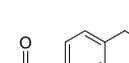
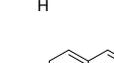
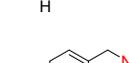
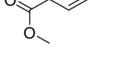
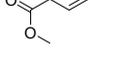
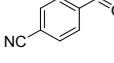
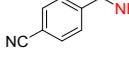
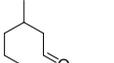
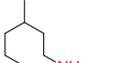
Entry	Aldehyde	Product	Time (h)	Yield (%)
1			15	96
2			15	94
3			15	96
4			24	92
5			24	91
6			15	96
7			20	97

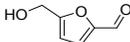
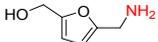
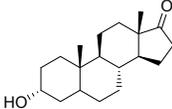
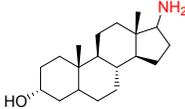
^aReaction conditions: aldehyde, 1 mmol; methanol, 2 mL; H₂, 1.7 MPa; NH₃, 0.3 MPa; Ru/TiP-100 (the Ru loading was 3.35 wt% Ru), 0.2 mol%; 30 °C.

More importantly, the aryl aldehydes with reduction-sensitive substituents, including halogen (Table 4, entries 1-3), methoxy (Table 4, entries 4-5), acetamido (Table 4, entry 6), ester (Table 4, entry 7), nitrile (Table 4, entry 8), and ethylene (Table 4, entries 9-10) groups, could all be converted into the desired primary amines at high yields, and those reducible groups remained

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3 intact. In addition, 5-hydroxymethylfurfural (a biomass platform molecule) and androsterone (a
4 bio-active molecule) could also be transformed into the corresponding primary amines with high
5 yields of 93% and 92%, respectively (Table 4, entries 11 and 12). These results further
6 highlighted the unique advantage of applying ambient temperature reaction condition with those
7 substrates that possess h reduction-sensitive substituents.
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20 **Table 4.** Reductive Amination of Various Challenging Substrates over Ru/TiP-100.^a
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Entry	Aldehyde	Product	Time (h)	Yield (%)
1			24	92
2			24	90
3			24	86
4			15	92
5			15	91
6			24	84
7			24	83
8			24	93
9			15	89
10			24	87 ^c

11			24	93
12 ^b			24	92 ^c

^aReaction conditions: ketone, 1 mmol; methanol, 2 mL; H₂, 1.4 MPa; NH₃, 0.6 MPa; Ru/TiP-100 (the Ru loading was 3.35 wt% Ru), 0.2 mol%; 30 °C. ^bH₂, 1.4 MPa; NH₃, 0.6 MPa. ^cIsolated yields, and the isolation method was based on reference 21.

3.6. Reasons for the High Activity of the Ru/TiP-100. As discussed above, Ru/TiP-100 showed much better activity and selectivity than Ru/C and Ru/TiO₂ (Table 1). As examined by XPS, the binding energy of Ru 3d (for Ru⁰, 280.94 eV) in Ru/TiP-100 was much lower than those in Ru/TiO₂ and Ru/C (Figure S8), indicating that the Ru⁰ in Ru/TiP-100 was more negatively charged, which favors the formation of active H on the metallic Ru for the hydrogenation steps (Figure S9). Furthermore, *in situ* CO-DRIFT measurements were performed to determine the electronic property of the Ru species in Ru/TiP-100 and Ru/TiO₂. As shown in Figure 3, the band of the CO that was adsorbed on the metallic Ru (Ru-CO) of Ru/TiP-100 showed an obvious red shift in comparison to the one that was adsorbed on the metallic Ru in Ru/TiO₂. The red shift of the CO adsorption band strongly suggested the increased electron density of the metallic Ru in Ru/TiP-100 compared with that in Ru/TiO₂, which was consistent with the XPS results (Figure S8). These results indicated that TiP was a better electron-donating support than TiO₂, which was probably caused by the higher basicity of TiP than TiO₂ as the basic support was generally recognized to favor the transfer of electron from support to the supported metals.^{25,35,36} Based on the results of CO₂-TPD (Figure S10), Ru/TiP-100 indeed possesses much larger amount of basic sites with higher strength than Ru/TiO₂. Therefore, it could be concluded that the metallic Ru mainly interacted with the basic sites in the Ru/TiP-100,

and thus, the electron density of metallic Ru in Ru/TiP-100 was higher than that in Ru/TiO₂. This phenomenon was probably caused by the electronic metal-support interaction (EMSI) between the Ru species and basic sites of the TiP support in the Ru/TiP-100.³⁷⁻⁴¹ The results above elucidated the key role of the TiP support as the electron donor to significantly increase the electron density of Ru species (both metallic Ru and RuO₂), which facilitates the activation of H₂ in the hydrogenation steps (Figure S9).

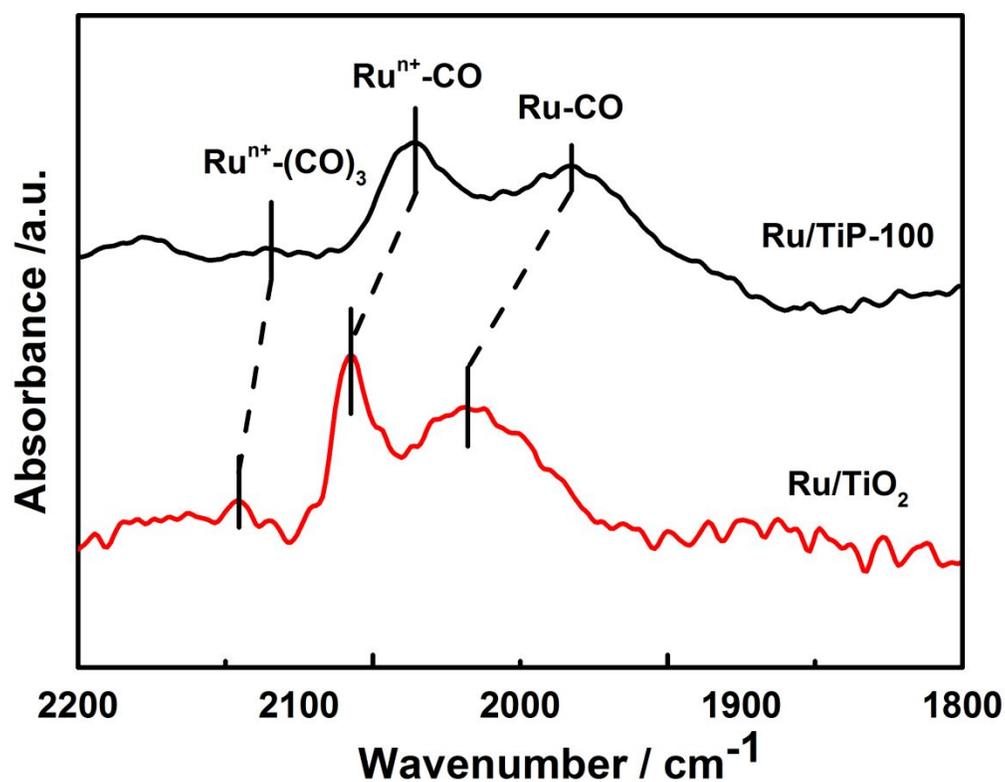


Figure 3. *In situ* DRIFT spectra of CO adsorbed on Ru/TiP-100 and Ru/TiO₂.

In another aspect, the reduction temperature of RuO₂/TiP showed strong impact on the reaction activity and product distribution (Figure 2A). Clearly, higher reduction temperature would lead to an increased reduction degree of RuO₂ to metallic Ru⁰ in RuO₂/TiP, as confirmed by XPS (Figure 2B and Figure 4). It is widely acknowledged that the metallic Ru sites can

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3 facilitate the hydrogenation steps (Figure S9), and thus, Ru/TiP-100 showed much better
4 performance than RuO₂/TiP (without metallic Ru⁰) and Ru/TiP-80. However, with excess
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6 metallic Ru⁰ in the catalyst (*e.g.*, Ru/TiP-150), the selectivity of the desired primary amines
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8 would decrease, and with extended reduction time, the desired product is not even formed (*e.g.*,
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10 Ru/TiP-150-30h). It is commonly accepted that the different electronic state of the Ru species
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12 plays a crucial role on the catalytic behaviour of the Ru/TiP-x. As determined by XPS (Figure 4),
13
14 the binding energy of Ru 3d became lower with the increasing reduction temperature, suggesting
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16 the formation of more negatively charged Ru⁰ (higher electron density) at higher reduction
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18 temperature.^{42,43} The higher electron density of Ru⁰ was beneficial for the formation of the active
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20 H on Ru for hydrogenation of imines and Schiff bases (Figure S9). However, when the electron
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22 density of Ru⁰ is overly high, strong adsorption of imines and Schiff bases occurs, especially at
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24 30 °C, owing to the strong electrophilicity of imines and Schiff base.⁴⁴⁻⁴⁷ This results in the lower
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26 ability of their subsequent hydrogenation to form the desired primary amines, which could be the
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28 main reason that Ru/TiP-150-30h needed higher reaction temperature (80 °C, Table 1, entry 7) to
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30 desorb the imines and Schiff bases and to release the active hydrogenation sites, so that a good
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32 yield of primary amines can be achieved at 80 °C. The above results imply that the catalytic
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34 performance of Ru/TiP-x was significantly affected by its proportion of metallic Ru and RuO₂, to
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36 reach an optimised electron density of Ru⁰ for activation of H₂ and desorption of intermediates
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38 (imines and Schiff bases). Therefore, Ru/TiP-100 showed the best performance among the
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40 Ru/TiP-x owing to its suitable amount of Ru⁰ (around 52%).
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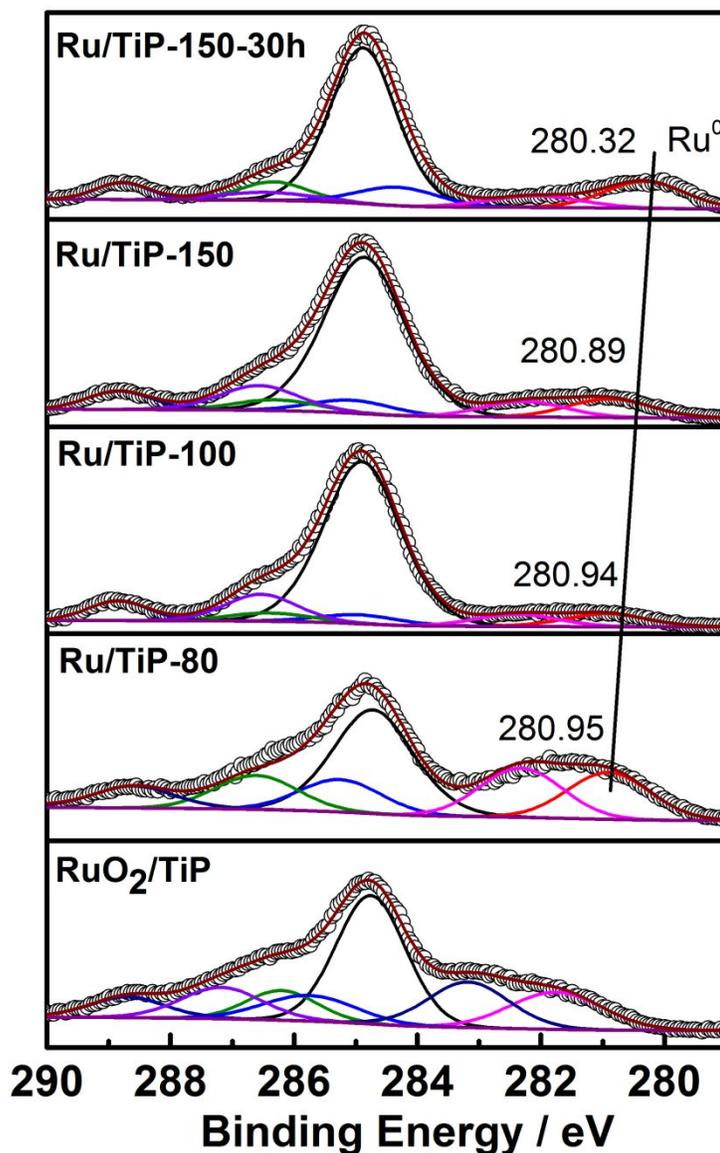


Figure 4. XPS spectra of Ru 3d in RuO₂/TiP and Ru/TiP-x.

Additionally, it should be pointed out that the acidity of Ru/TiP-100 (from the NH₃-TPD results in Figure S11) was much higher than those of Ru/TiO₂ and the reported Ru/ZrO₂.²⁴ Higher acidity was beneficial to the activation of the C=N groups in the *in situ* generated imines and Schiff bases *via* the interaction between the acidic sites and the N atom of the corresponding C=N bonds (Figure S12),^{48,49} thus aided the reaction to occur at low temperature.

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3 The results above indicated that the combination of the support TiP and the Ru species
4 (Ru⁰/RuO₂) with suitable Ru⁰ proportion contributed to the good performance of Ru/TiP-100.
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6 First, TiP could significantly increase the electron density of Ru⁰ in Ru/TiP-100 *via* EMSI effect
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8 (Figure 3), which was beneficial to the activation of H₂ in the hydrogenation step (Figure S9) in
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10 the catalytic cycle. Meanwhile, the strong acidic property of TiP results in the high acidity of
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12 Ru/TiP-100 (Figure S11), and higher acidity could activate the C=N bonds in the *in situ*
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14 generated imines and Schiff bases for their subsequent conversion to the desired products.⁴⁹
15
16 Therefore, TiP was a better support than TiO₂ and ZrO₂. Secondly, the suitable reduction degree
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18 of RuO₂ could ensure the ample Ru⁰ for H₂ activation and control the electron density of Ru⁰ to a
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20 suitable degree for the desorption of intermediates (imines and Schiff bases), which both affected
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22 the catalytic performance. Therefore, RuO₂ of suitable amount played a key role in tuning the
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24 electron density of Ru⁰. On the basis of the above discussion, both the support material and the
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26 Ru species affected the catalytic activity significantly, and in Ru/TiP-100, TiP (strong acidity
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28 and EMSI effect) and Ru⁰/RuO₂ with suitable Ru⁰ proportion cooperated nicely to promote the
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30 reductive amination at ambient temperature.
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38 **3.7 Mechanism Discussion.** To investigate the mechanism of the catalytic reaction
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40 mechanism, the dependence of product distribution on time was studied in detail by employing
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42 reductive amination of cyclohexanone as an example. As shown in Figure 5, most of
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44 cyclohexanone were rapidly consumed in 1 h to form imine and Schiff base. No
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46 cyclohexylamine (the desired product) was detected in the first hour because the formed
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48 cyclohexylamine from imine hydrogenation could easily react with cyclohexanone to generate
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50 Schiff base. Cyclohexylamine began to form when most of cyclohexanone was converted after
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52 1.5 h. Finally, cyclohexylamine was generated from the conversion of both imine and Schiff
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base. In the reaction process, nearly no cyclohexanol was detected because the imine formed much more quickly, which resulted in the rapid conversion of cyclohexanone with NH_3 , and thus decreased the direct hydrogenation of cyclohexanone to a large extent. Moreover, control experiments using Schiff base as the reactant over Ru/TiP-100 (Figure S13) indicated that the primary amine was yielded in the presence of NH_3 , while the secondary amine was formed without NH_3 . These results further clearly explained the absence of secondary amine in the entire reaction process. Additionally, when using aldehydes as the substrates, the formed imines would be converted into imidazolines (a potential by-product, Figure S14) at a very low yield.

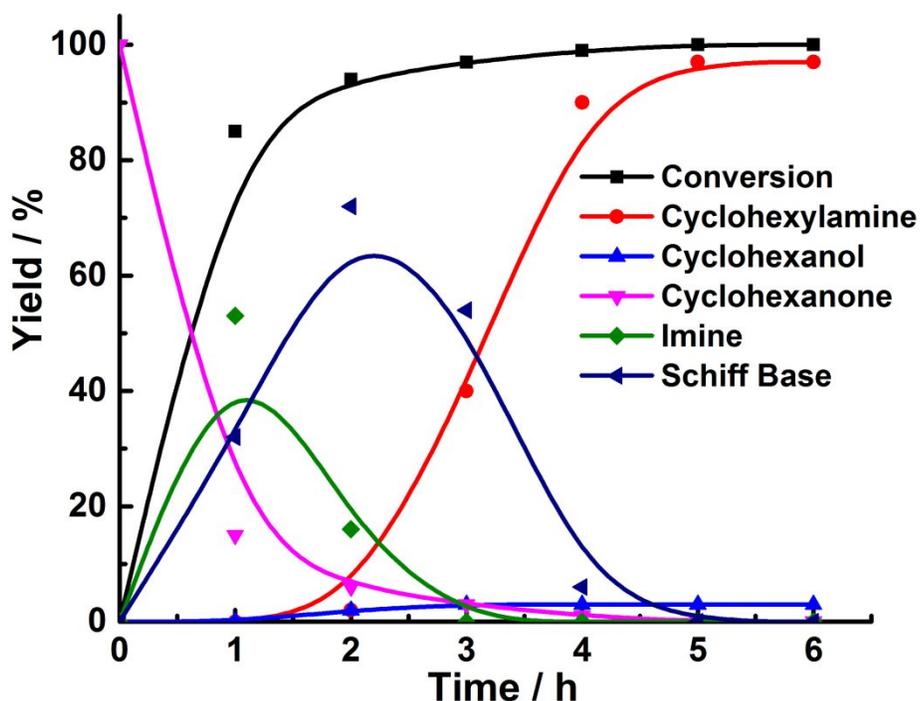


Figure 5. Time-Yield plots. Reaction conditions: cyclohexanone, 1 mmol; methanol, 2 mL; 30 °C; Ru/TiP-100 (the Ru loading was 3.35 wt% Ru), 0.2 mol%; 1.4 MPa H_2 and 0.6 MPa NH_3 .

On the basis of the above discussion and some reported knowledges,^{23-25,50} a reasonable mechanism was proposed for the reductive amination of carbonyl compounds to primary amines

using NH_3 and H_2 over Ru/TiP-100 (Figure 6). Initially, imines were rapidly generated from the condensation of carbonyl group and NH_3 even in the absence of any catalysts. Subsequently, the formed imines were hydrogenated over Ru/TiP-100 to produce primary amines (desired products), which could rapidly react with the unreacted carbonyl compounds to form Schiff bases. Finally, in the presence of NH_3 , the generated Schiff bases were further converted into the desired primary amines over Ru/TiP-100.

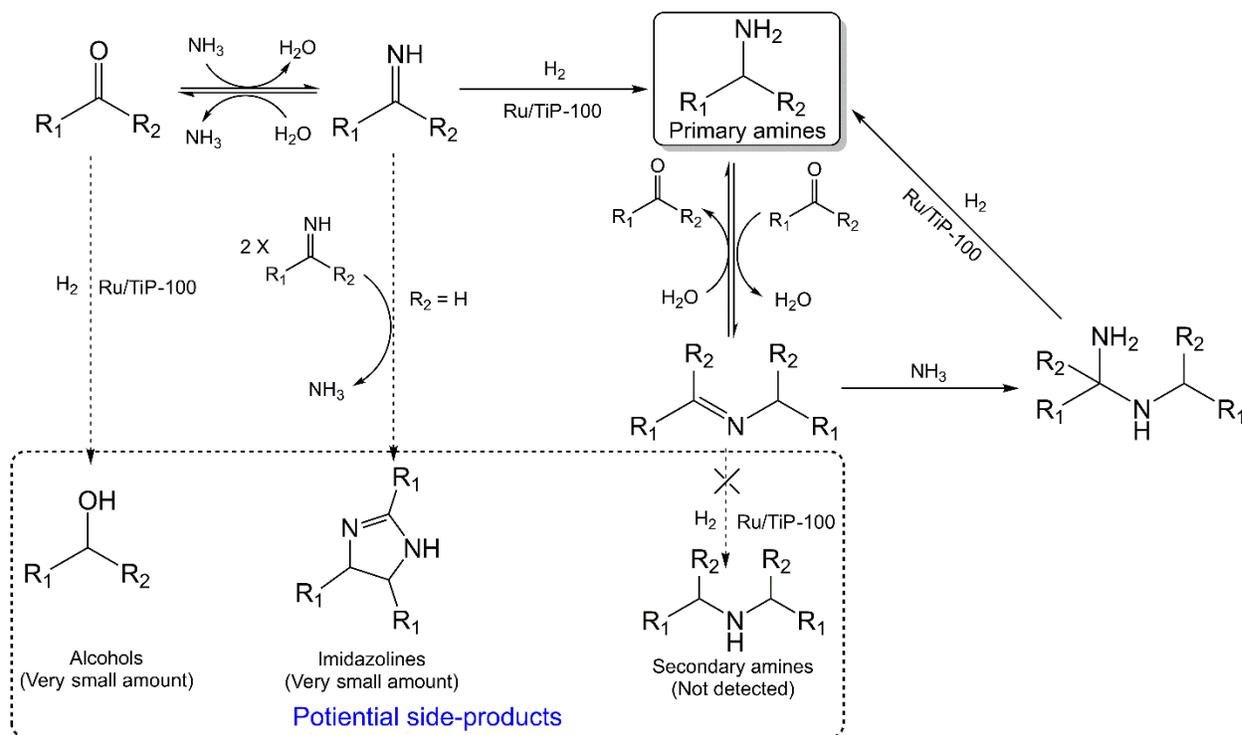


Figure 6. A proposed mechanism for the reductive amination of carbonyl compounds to primary amines using NH_3 and H_2 over Ru/TiP-100.

4. CONCLUSIONS

In conclusion, various primary amines were successfully synthesized from the reductive amination of carbonyl compounds using NH_3 and H_2 as the nitrogen and hydrogen resources

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3 over Ru nanocatalysts on titanium phosphate at ambient temperature. The properties of both Ru
4 species (Ru/RuO₂) and the support materials had strong impacts on the reaction activity and
5 selectivity, and Ru/TiP-100 provided the best performance owing to the combination of TiP and
6 Ru/RuO₂ with suitable proportion of Ru⁰ (52%). Detailed study indicated that the moderating
7 effect of RuO₂ and the electronic metal-support interaction resulted in the suitable electron
8 density of Ru species, which could balance the activation of H₂ for the hydrogenation steps and
9 the desorption of intermediates (imines and Schiff bases). Meanwhile, the relative higher acidity
10 of Ru/TiP-100 could promote the conversion of C=N group in the *in situ* generated imines and
11 Schiff bases into the desired primary amines. We believe that the prepared Ru/TiP-100 has the
12 great potential for the production of primary amines *via* ambient-temperature reductive
13 amination of carbonyl compounds.
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32 ASSOCIATED CONTENT

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45 46 47 48 **Notes** 49

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51 The authors declare no competing financial interest.
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3 **Supporting Information.** The Supporting Information is available free of charge on the ACS
4 Publications website.
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8 The process for the preparation of RuO₂/TiP, characterization of the synthesized RuO₂/TiP
9 employing various techniques (*i.e.*, FT-IR spectrum, and N₂ adsorption-desorption isotherms),
10 AFM and EDS mapping images of the prepared RuO₂/TiP, H₂-TPR profiles of RuO₂/TiP, TEM
11 image, SEM image and XPS spectra of Ru 3d for the recovered Ru/TiP-100, time-yield plots for
12 reductive amination of cyclohexanone, XPS spectra of Ru 3d in Ru/C, Ru/TiO₂ and Ru/TiP-100,
13 the hydrogenation steps in the reaction process, CO₂-TPD profile and basic sites quantity of
14 Ru/TiP-100 and Ru/TiO₂, NH₃-TPD profile and acidic sites quantity of RuO₂/TiP, Ru/TiP-100
15 and Ru/TiO₂, comparison of Ru/TiP-100 with state-of-the-art catalysts, the activation of C=N
16 groups in the *in situ* generated imines and Schiff bases, control experiments using Schiff base as
17 the reactant, and GC-MS spectra of imidazoline, and the GC chromatograms.
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31 32 33 **ACKNOWLEDGMENT**

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