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This manuscript has been accepted after peer review and appears as an Accepted Article online prior to editing, proofing, and formal publication of the final Version of Record (VoR). This work is currently citable by using the Digital Object Identifier (DOI) given below. The VoR will be published online in Early View as soon as possible and may be different to this Accepted Article as a result of editing. Readers should obtain the VoR from the journal website shown below when it is published to ensure accuracy of information. The authors are responsible for the content of this Accepted Article.

To be cited as: ChemSusChem 10.1002/cssc.201601364

Link to VoR: http://dx.doi.org/10.1002/cssc.201601364



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## Selective Aerobic Oxidation of Alcohols over Atomicallydispersed Non-Precious Metal Catalysts

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Abstract: Catalytic oxidation of alcohols often requires the presence of expensive transition metals. Herein, we show that earth-abundant Fe atoms dispersed throughout a nitrogen-containing carbon matrix catalyze the oxidation of benzyl alcohol and 5-hydroxymethylfurfural by O<sub>2</sub> in the aqueous phase. The activity of the catalyst can be regenerated by a mild treatment in H<sub>2</sub>. An observed kinetic isotope effect indicates  $\beta$ -H elimination from the alcohol is the kinetically-relevant step in the mechanism, which can be accelerated by substituting Fe with Cu. Dispersed Cr, Co and Ni also convert alcohols, demonstrating the general utility of metal-nitrogen-carbon materials for alcohol oxidation catalysis. Oxidation of aliphatic alcohols was substantially slower than that of aromatic alcohols, but addition of 2,2,6,6-tetramethyl-1-piperidinyloxy as a co-catalyst with Fe can significantly improve the reaction rate.

Precious metal catalysts are widely used in petrochemical and refineries, pharmaceutical production facilities environmental remediation devices.<sup>[1]</sup> In particular, the aerobic oxidation of biomass-derived alcohols to corresponding aldehydes and acids in the aqueous phase using heterogeneous precious metal catalysts, such as Au, Pt, Pd and Ru, has received growing attention because it offers a green and sustainable route to value-added chemicals.<sup>[2]</sup> The limited annual production and very high price of the metals, however, can be a significant barrier to commercialization of new processes.<sup>[3]</sup> Therefore, replacement of precious metals with more earth-abundant metals would be quite advantageous.

Recently, non-precious metal catalysts confined in a nitrogen-containing carbon matrix, which were prepared by pyrolysis or a ball milling method, exhibited decent activity in electrochemical reactions<sup>[4]</sup> and organic synthesis.<sup>[6]</sup> For example, the efficient activation of dioxygen has been reported with Fe-containing, nitrogen-doped carbon (Fe-N-C) in the electrochemical O<sub>2</sub> reduction reaction (ORR), with a comparable activity to the well-known Pt ORR catalysts.<sup>[6]</sup> Alcohol oxidation reactions can also be catalyzed by the Fe-based catalysts, such as Fe-containing polyoxometalates,<sup>[7]</sup> nano-Fe<sub>2</sub>O<sub>3</sub> particles<sup>[8]</sup> and

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encapsulated or supported Fe complexes,<sup>[9]</sup> but these catalysts often require the addition of peroxides, which is likely the consequence of the poor ability of the catalyst to activate dioxygen. As an Fe-N-C catalyst has previously demonstrated excellent ORR performance, we hypothesized that it might also be a promising catalyst for the aerobic oxidation of alcohols. In fact, Jagadeesh et al. have reported the aerobic oxidative nitrification of various alcohols over Fe-N-C and identified aldehydes as intermediates.<sup>[10]</sup> To the best of our knowledge, however, the exploration of Fe-N-C and other platinum group metal-free analogues as potential catalysts for alcohol oxidation in water to produce aldehyde or acid products has not been reported and the mechanism of alcohol oxidation remains unclear. The current study relates extensive materials characterization results to catalytic performance, explores the kinetics of alcohol oxidation in liquid water, examines the regenerability of the catalysts and compares a variety of nonprecious metal, atomically-dispersed M-N-C catalysts.



Figure 1. Aberration-corrected STEM images of a) fresh and b) used Fe-N-C; c) fresh and d) used Cu-N-C. Used catalysts were recovered after 8 h of benzyl alcohol oxidation reaction, washed and dried.

An Fe-N-C catalyst synthesized by pyrolysis of  $Fe(NO_3)_3$ and nicarbazin (details provided in the supplementary information) was investigated in the aqueous-phase aerobic alcohol oxidation reaction. Although the catalyst has been leached with acid to remove Fe or Fe<sub>3</sub>C nanoparticles, some nanoparticles (5 – 30 nm) were still observed (Figure S1a), which has also been observed by others using similar synthesis methods and shown to be covered by a graphitic carbon shell.<sup>[5e,11]</sup> Extensive prior characterization of our Fe-N-C catalyst by X-ray photoelectron spectroscopy (XPS), Mössbauer spectroscopy and *in-situ* X-ray absorption spectroscopy indicates that ~90% of the iron is atomically-dispersed as nitrogen-coordinated Fe (Fe-N<sub>x</sub>) species and are proposed to be

the ORR active sites.<sup>[12]</sup> The predominant existence of atomically-dispersed Fe in the sample used here was confirmed by aberration-corrected scanning transmission electron microscopy (AC-STEM) (Figure 1a). The weight loading of Fe was determined to be 1.2 wt% from XPS (Table S1) and 1.5 wt% from inductively coupled plasma atomic emission spectroscopy (ICP-AES) (Table S2), respectively. A similar metal loading from XPS (surface-sensitive) and ICP-AES (bulk) is consistent with the atomically-dispersed iron species composing a large fraction of the total iron on the catalyst.

Table 1. Rates of benzyl alcohol oxidation over fresh, used and regenerated M-N-C catalysts  $^{\rm [a]}$ 

Entry	Catalyst	Treatment <sup>[b]</sup>	Rate (10 <sup>-8</sup> mol s <sup>-1</sup> g <sub>cat</sub> <sup>-1</sup> )	TOF (10 <sup>-3</sup> s <sup>-1</sup> ) <sup>[c]</sup>	
1	Cr-N-C	Fresh	84	6.5	
2	Fe-N-C	Fresh	17	0.78	
3	Co-N-C	Fresh	180	15	
4	Ni-N-C	Fresh	64	3.1	
5	Cu-N-C	Fresh	204	34	
6	Cr-N-C	Used	46	3.6	
7	Fe-N-C	Used	11	0.52	
8	Co-N-C	Used	21	1.7	
9	Ni-N-C	Used	7.3	0.36	
10	Cu-N-C	Used	21	3.5	
11	Cr-N-C	Regenerated	67	5.2	
12	Fe-N-C	Regenerated	19	0.90	
13	Co-N-C	Regenerated	133	11	
14	Ni-N-C	Regenerated	14	0.70	
15	Cu-N-C	Regenerated	31	5.0	

[a] Reaction conditions: 353 K, 10 mL 0.05 M benzyl alcohol aqueous solution, 0.0400 g Fe-N-C or 0.0130 g M-N-C (M = Cr, Co, Ni, Cu), 1 MPa O<sub>2</sub>. Reaction profiles are shown in Figure S2. [b] The used catalysts were recovered after 8 h of benzyl alcohol oxidation reaction, washed and dried; The regenerated catalysts were recovered after 8 h of oxidation reaction, washed, dried and treated in dihydrogen flow at 573 K for 3 h. [c] The turnover frequency (TOF) [mol alcohol converted (mol metal)<sup>-1</sup> s<sup>-1</sup>] was derived from the initial rate calculated from conversion after 30 min of reaction, which was below 10% in all cases (Figure S2).

The rate of benzyl alcohol oxidation over Fe-N-C under mild conditions (353 K, 1 MPa O<sub>2</sub>, aqueous solution) was measured to be  $1.7 \times 10^{-7}$  mol s<sup>-1</sup> g<sub>cat</sub><sup>-1</sup> (Table 1, Entry 2), which is equivalent to a turnover frequency (TOF) of 0.00078 s<sup>-1</sup> based on total Fe atoms. As control experiments, the conversion of benzyl alcohol was evaluated under identical conditions in the presence of Norit activated carbon and activated-carbon-supported Fe (Fe/C) with similar Fe loading and nanoparticle size compared to Fe-N-C (Figures S1). In addition, metal-free nitrogen-containing carbon (N-C) was evaluated for benzyl alcohol oxidation in the absence and presence of soluble Fe<sup>3+</sup> (Fe(NO<sub>3</sub>)<sub>3</sub>) (Table S3). The conversion of benzyl alcohol over activated carbon and supported Fe nanoparticles was negligible whereas the reaction rate over N-C (with or without the presence of Fe<sup>3+</sup> ion) is ~20 % of that observed with the equivalent

amount of Fe-N-C. The low observed catalytic activity of N-C, compared with Fe-N-C, is likely related to the nitrogen sites on the carbon, which have been reported to participate in the partial reduction of O<sub>2</sub>.<sup>[13]</sup> Considering the loading of nitrogen in the carbon matrix is much larger than that of Fe ( $n_{\rm N}$ : $n_{\rm Fe} \sim 21^{[12]}$ ) and Fe-N-C is about 500% more active than N-C, we propose that the Fe-N<sub>x</sub> sites are the primary active sites for benzyl alcohol oxidation.

The reaction orders with respect to O<sub>2</sub> and benzyl alcohol were evaluated over the range of 0.3 - 1 MPa O<sub>2</sub> and 0.025 - 10.1 M benzyl alcohol. As illustrated in Figures S2a,b and summarized in Table 2, the reaction orders were close to zero, indicating the saturated adsorption of O<sub>2</sub> and benzyl alcohol. To further explore the reaction mechanism, the kinetic isotope effect utilizing deuterated alcohol (C<sub>6</sub>H<sub>5</sub>CD<sub>2</sub>OH) was evaluated. As summarized in Table 2, a significant kinetic isotope effect of 4.8 was observed, indicating  $\beta$ -H elimination is a kinetically-relevant step during benzyl alcohol oxidation over Fe-N-C. For comparison, the KIE was measured to be 1.8 over commercial carbon-supported Pt catalyst (Pt/C), which is a well-studied material for alcohol oxidation.<sup>[14]</sup> Moreover, the influence of tertbutanol and 1,4-benzoquinone, known scavengers for hydroxyl and superoxide radicals,<sup>[15]</sup> on the rate of benzyl alcohol oxidation was examined over Fe-N-C and Pt/C. As revealed in Table S4, the introduction of the radical scavengers did not substantially change the rate of alcohol oxidation over either Fe-N-C or Pt/C. These results suggest that hydroxyl and superoxide radicals are not involved in the benzyl alcohol oxidation over Fe-N-C.

Table 2. Kinetic isotope effect and orders of reaction for benzyl alcohol oxidation

TOFD	$TOF_{H}$	n <sub>dioxygen</sub>		n <sup>[c]</sup>
(10 <sup>-3</sup> s <sup>-1</sup> ) <sup>[a]</sup>	$/TOF_{D}$	0.3 – 1 MPa	1 – 2 MPa	Palcohol
0.16	4.9	0	0	0
16	2.2	0.7	0	0
	TOF <sub>D</sub> (10 <sup>-3</sup> s <sup>-1</sup> ) <sup>[a]</sup> 0.16 16	$\begin{array}{c c} TOF_D & TOF_H \\ (10^{\cdot 3} \ s^{\cdot 1})^{[a]} & /TOF_D \\ \hline 0.16 & 4.9 \\ 16 & 2.2 \\ \end{array}$	$\begin{array}{c c} {\sf TOF}_{\sf D} & {\sf TOF}_{\sf H} & {\it n_{dioxy}} \\ (10^{-3}  {\sf s}^{-1})^{[a]} & /{\sf TOF}_{\sf D} & 0.3 - 1  {\sf MPa} \\ \hline 0.16 & 4.9 & 0 \\ 16 & 2.2 & 0.7 \end{array}$	$\begin{array}{c c} {\sf TOF}_{\sf D} & {\sf TOF}_{\sf H} & {\it n_{dioxygen}}^{[{\sf D}]} \\ (10^{\cdot3}  {\rm s}^{\cdot1})^{[a]} & /{\sf TOF}_{\sf D} & 0.3 - 1  {\sf MPa} & 1 - 2  {\sf MPa} \\ \hline 0.16 & 4.9 & 0 & 0 \\ 16 & 2.2 & 0.7 & 0 \end{array}$

[a] The turnover frequency (TOF) [mol alcohol converted (mol metal)<sup>-1</sup> s<sup>-1</sup>] was derived from the initial rate calculated from conversion after 30 min of reaction, which was below 10% in all cases. Reaction conditions: 353 K, 10 mL 0.05 M deuterated benzyl alcohol ( $C_6H_5CD_2OH$ ) aqueous solution, 0.0400 g Fe-N-C or 0.0130 g Cu-N-C, 1 MPa O<sub>2</sub>. b: Reaction conditions: 353 K, 10 mL 0.05 M benzyl alcohol aqueous solution,

b: Reaction conditions: 353 K, 10 mL 0.05 M benzyl alcohol aqueous solution, 0.0400 g Fe-N-C or 0.0130 g Cu-N-C, 0.3 - 2 MPa  $O_2$ . The dependence of TOF on  $O_2$  pressure was shown in Figure S3.

c: Reaction conditions: 353 K, 10 mL benzyl alcohol aqueous solution (0.025 – 0.1 M), 0.0400 g Fe-N-C or 0.0130 g Cu-N-C, 1 MPa  $O_2.$ 

Slight deactivation was observed after 8 h of reaction. As shown in Table 1, Entries 2 and 7, ~35% of the initial activity of Fe-N-C was lost after recovery from the reactor compared to the fresh catalyst. To investigate the cause of deactivation, the used catalyst was characterized by AC-STEM and ICP-AES. High-resolution electron microscopy (Figure 1b) revealed atomically-dispersed Fe-N<sub>x</sub> sites remained on the used catalyst and elemental analysis of the fresh and recovered catalysts confirmed that the Fe loading was unaffected by reaction (Table S2). Moreover, the concentration of Fe in the reaction medium after 8 h was less than 0.03 mM, consistent with less than 2% of available iron being leached into the solution. Indeed, the

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catalytic activity can be almost fully regenerated by a reductive treatment in H<sub>2</sub> (Table 1, Entries 2, 7, 12). These results suggest that the Fe-N<sub>x</sub> sites are stable under the reaction conditions and the deactivation is likely the result of strongly adsorbed species on active sites, which were removed during the  $H_2$  treatment. This was also supported by an extra peak at around 573 K observed during H<sub>2</sub>-temperature-programmed reduction of a used Fe-N-C catalyst (Figure S4). A similar deactivation behavior was also observed during alcohol oxidation over a Pt catalyst.<sup>[16]</sup> The oxidation of other alcohols, including 5hydroxymethylfurfural (HMF), ethanol, 1,6-hexanediol and glycerol, was also investigated over the Fe-N-C catalyst. As shown in Figure 2, benzyl alcohol and HMF were efficiently and selectively converted to benzyl aldehyde and 2,5-diformylfuran (DFF), respectively. The selectivity to benzyl aldehyde and DFF was 92% and 82% at the conversion of 79% and 49%, respectively. Less than 3% conversion of ethanol, 1,6hexanediol and glycerol was observed under the same conditions, which is likely the result of either more difficult activation of β-H in the aliphatic alcohols or severe catalyst deactivation.



Figure 2. Conversion and product distribution from oxidation of benzyl alcohol, 5-hydroxymethylfurfural (HMF), glycerol, ethanol and 1,6-hexanediol (HDO) over Fe-N-C. Reaction conditions: 353 K, 10 mL 0.05 M benzyl alcohol aqueous solution, 0.167 g Fe-N-C, 1 MPa  $O_2$ , 8 h reaction time.

In an attempt to improve the rate of alcohol oxidation over our heterogeneous catalytic system, 2,2,6,6-tetramethyl-1piperidinyloxy (TEMPO) was added to the reaction medium, which has been reported as a co-catalyst when combined with first-row transition metal complexes for homogeneous or electrochemical oxidation of alcohols.<sup>[17]</sup> As shown in Table S5, the catalytic amount of additive TEMPO (1 mM) significantly increased the rate of benzyl alcohol oxidation. The conversion of benzyl alcohol after 30 min increased from 2.4 % to 12.2% with the addition of TEMPO. More importantly, the oxidation of 1,6hexanediol, an aliphatic diol, was significantly promoted by TEMPO, with 6.3% conversion after 30 min, compared to 0.5% conversion without the addition of TEMPO.

A series of M-N-C catalysts containing other metals (M = Cr, Co, Ni, Cu) was also prepared by the same method used to synthesize Fe-N-C and evaluated in the benzyl alcohol oxidation.

A related study on the oxidative nitrification of alcohols by Jagadeesh et al. revealed Fe and Co catalysts exhibited the best activity and selectivity.<sup>[18]</sup> As shown in Table 1, Entries 1-5, benzyl alcohol was also efficiently converted over all of the M-N-C catalysts in this work. The activity of these M-N-C (M = Cr, Co, Ni, Cu) catalysts was much greater than that of Fe-N-C, among which Cu-N-C was the most active catalyst with a TOF of 0.034 s<sup>-1</sup> (~50 times greater than that of Fe-N-C and only about one order of magnitude lower than Pt). As shown in Figure 1c, the high-resolution STEM image confirmed the atomic dispersion of Cu, which likely resides in nitrogen-coordinated sites. Similar to Fe-N-C, the reaction order with respect of O<sub>2</sub> and benzyl alcohol was close to 0 in the range of 1 - 2 MPa O<sub>2</sub> and 0.025 - 0.1 M benzyl alcohol over Cu-N-C (Figures S2c and S2d). However, at lower  $O_2$  pressure (0.3 – 1 MPa), the  $O_2$  reaction order was ~0.7 The higher O2 reaction order over Cu-N-C versus Fe-N-C is possibly correlated to the observed lower activity of Cu-N-C in ORR as reported by Serov et al.[18] Interestingly, a much weaker kinetic isotope effect was observed during oxidation of deuterated benzyl alcohol over Cu-N-C compared to Fe-N-C (2.2 versus 4.9) (Table 2), which might be related to a more facile  $\beta$ -H elimination on the Cu catalyst.

The stability of M-N-C catalysts was also investigated. Similar to the behavior of Fe-N-C, loss of activity was observed over M-N-C (M = Cr, Co, Ni, Cu) after 8 h of benzyl alcohol oxidation (Table 1, Entries 1-10). More specifically, only ~10% of the initial activity was observed with recycled Co-N-C, Ni-N-C and Cu-N-C catalysts. Microscopy revealed that Cu remained atomically dispersed throughout the reaction (Figure 1d) and negligible Cu leaching was observed by ICP-AES (Table S2). In an attempt to regenerate the activity of used M-N-C, H<sub>2</sub> treatment at 573 K was performed on the recovered catalysts. Whereas the majority of catalytic activity was recovered from Cr-N-C, Fe-N-C and Co-N-C, the Ni-N-C and Cu-N-C samples were not efficiently regenerated (Table 1).

This work provides a systematic evaluation of the aqueous-phase aerobic alcohol oxidation at mild temperature over a series of non-precious-metal M-N-C catalysts. Benzyl alcohol and HMF were efficiently and selectively converted to the aldehyde products over the earth-abundant Fe-N-C catalyst with a slight loss of activity that could be fully regenerated by simple H<sub>2</sub> treatment. The rate of aliphatic alcohol oxidation was quite slow over Fe-N-C but can be significantly promoted by adding a catalytic amount of TEMPO. The highest activity for benzyl alcohol oxidation was obtained over Cu-N-C, which is tentatively attributed to a faster  $\beta$ -H elimination step. Mechanistic studies of these systems are currently underway.

#### **Experimental Section**

See the Supporting Information for Experimental Details, which include Materials and Methods; Element loadings from XPS and ICP-AES; Reaction rates over different materials; Influence of radical trap and TEMPO addition on reaction rate; STEM images of Fe-N-C and supported Fe catalysts; Influence of dioxygen pressure on TOF; reaction profiles of benzyl alcohol oxidation over M-N-C; and H<sub>2</sub> TPR results from fresh and used Fe-N-C.

### Acknowledgements

This work is supported by the US NSF under grant numbers EEC-0813570 (Center for Biorenewable Chemicals,CBiRC) and CBET-1157829, and in part by the US DOE-EERE Fuel Cell Technology Program (subcontract to Northeastern University, with PI Sanjeev Mukerjee). A portion of the microscopy research was conducted at the Center for Nanophase Materials Sciences in Oak Ridge National Lab, which is a DOE Office of Science User Facility.

**Keywords:** Heterogeneous catalyst • Oxidation • Reaction mechanism • N-doped carbon • Non-precious metal

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## COMMUNICATION

Iron atoms dispersed throughout a nitrogen-containing carbon matrix catalyze alcohol oxidation by O<sub>2</sub> in the aqueous phase. The used catalyst can be regenerated by a mild treatment in H<sub>2</sub>. An observed kinetic isotope effect indicates  $\beta$ -H elimination is a kinetically-relevant step in the mechanism, which can be accelerated by substituting Fe with Cu.



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10.1002/cssc.201601364