

## Full Paper

## Decoration of an #-Resorcyate Nucleus as part of the Manufacture of a Glucokinase Activator

Phillip Hopes, Thomas Langer, Kirsty Millard, and Alan Steven

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5 **Decoration of an  $\alpha$ -Resorcylate Nucleus as part of the Manufacture of a**  
6 **Glucokinase Activator**  
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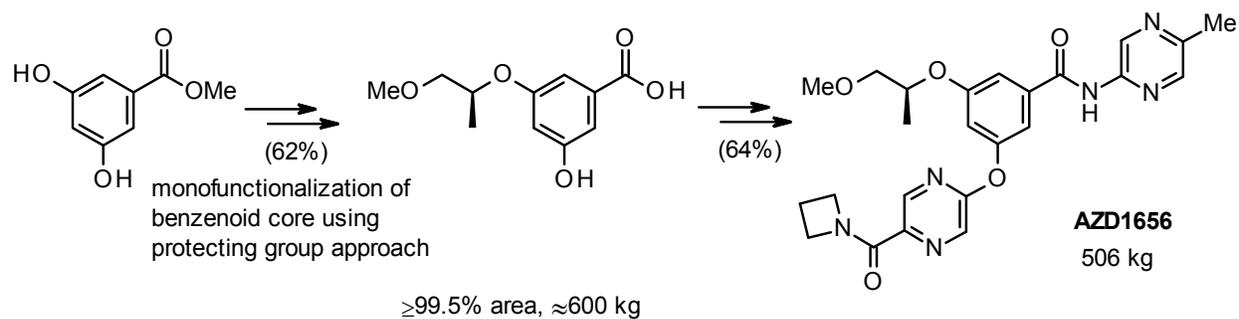
8 Phillip Hopes,<sup>†</sup> Thomas Langer,<sup>‡</sup> Kirsty Millard,<sup>‡</sup> and Alan Steven<sup>\*‡</sup>  
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10 <sup>†</sup> Cyton Biosciences Ltd, 68 Macrae Road, Bristol, BS20 0DD, United Kingdom  
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12 <sup>‡</sup> Pharmaceutical Technology & Development, AstraZeneca, Charter Way, Macclesfield, SK10 2NA,  
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17 [Alan.Steven@astrazeneca.com](mailto:Alan.Steven@astrazeneca.com)  
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## ABSTRACT

The need to define a set of processes for the manufacture of a glucokinase activator called for an evaluation of different strategies to differentiate the hydroxyls of an  $\alpha$ -resorcylic acid derivative. Whilst direct functionalization proved possible, it did not allow access to crystalline intermediates that offered control over the rejection of process impurities. The strategy taken forward involved the installation of a benzoyl protecting group using careful control of pH in order to achieve useful levels of selectivity. This allowed the remaining  $\alpha$ -resorcylic hydroxyl to be functionalized using a Mitsunobu reaction, with liquid-liquid partitioning being used to separate downstream intermediates of interest away from the redox byproducts of this reaction. Downstream challenges that were overcome in order to deliver a commercially viable means of manufacturing the API included developing an amidation reaction with a poorly reactive aminopyrazine coupling partner.

## KEY WORDS

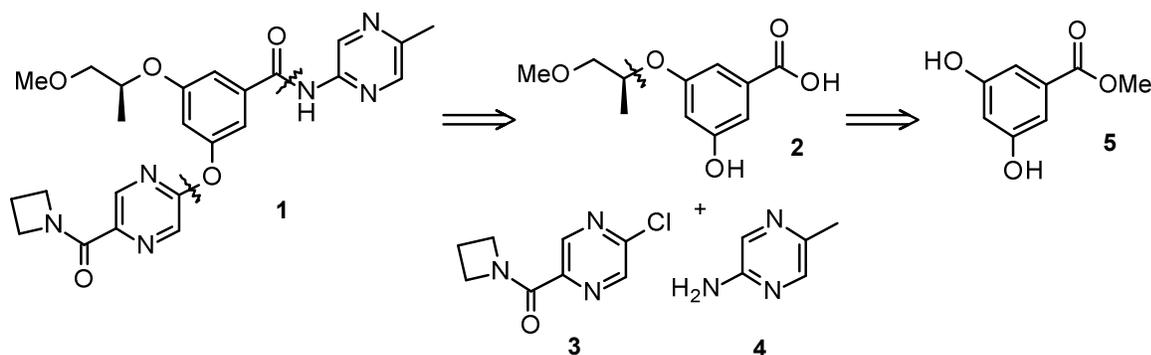
resorcylic, monobenzoylation, Mitsunobu, glucokinase activator,  $S_NAr$ , amidation

## INTRODUCTION

**AZD1656 (1)**, a compound containing two pyrazine units, has been under development by AstraZeneca as a glucokinase activator for the treatment of type 2 diabetes.<sup>1-4</sup> Investigations around synthetic route design for **AZD1656 (1)** led to the decision to route via acid **2**, and to elaborate it to the API through couplings with chloropyrazine **3**<sup>5</sup> and aminopyrazine **4** (Scheme 1),<sup>6</sup> compounds whose development activities have been disclosed recently. Access to acid **2**, an  $\alpha$ -resorcylic derivative bearing a side-chain with a stereogenic center, required a means of differentiating between the hydroxyl groups of methyl  $\alpha$ -resorcylic (**5**), our starting material of choice. This article will discuss how this challenge was overcome, as part of a wider discussion around the selection of the synthetic route, the development

of manufacturable processes and learning gained from the commercial-scale manufacture of **AZD1656** (1).

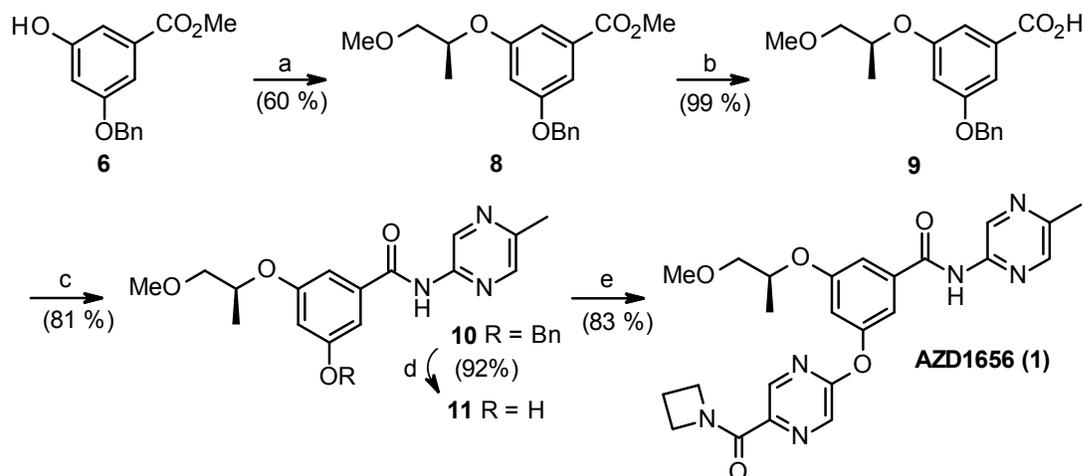
**Scheme 1.** Disconnections of **AZD1656** (1)



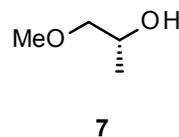
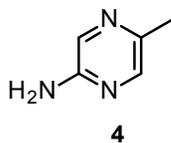
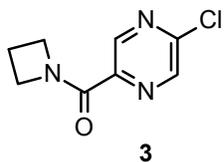
**MEDICINAL CHEMISTRY APPROACH**

The chemistry utilized in order to achieve the selection of a candidate drug by the project is outlined in Scheme 2. It differentiated the hydroxyl groups of the  $\alpha$ -resorcyate core by dibenzylating methyl  $\alpha$ -resorcyate (**5**) before hydrogenolyzing this material using exactly one equivalent of hydrogen gas. This protocol produced ether **6** contaminated by methyl  $\alpha$ -resorcyate (**5**) and residual dibenzylated material, both of which were removed by chromatographic purification. The chiral side-chain was incorporated by engaging phenol **6** in a Mitsunobu etherification with (*R*)-1-methoxypropan-2-ol (**7**) so as to afford ether **8**. The API was duly accessed, after the required protecting group removals, through the sequential appendage of aminopyrazine **4** to acid **9** so as to afford amide **10**, and chloropyrazine **3** to phenol **11**. As well as being step-heavy, a consequence of the use of protecting groups to differentiate between the  $\alpha$ -resorcyate hydroxyls, the intermediates associated with the medicinal chemistry route included a number of oils and low-melting solids whose purification required chromatography.

**Scheme 2** Medicinal Chemistry Approach to **AZD1656** (1)

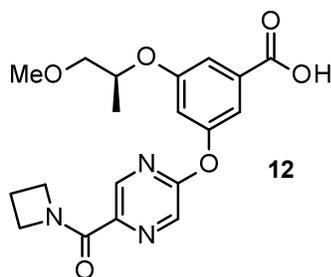


a) **7**, PPh<sub>3</sub>, DIAD, THF; b) 2 M NaOH, MeOH; c) (COCl)<sub>2</sub>, DMF, CH<sub>2</sub>Cl<sub>2</sub> then **4**, C<sub>5</sub>H<sub>5</sub>N, 0 °C to RT; d) H<sub>2</sub>, 10 %wt/wt, Pd-C, ethanol, THF; e) **3**, Cs<sub>2</sub>CO<sub>3</sub>, MeCN, 120 °C (microwave)



## SYNTHESIS STRATEGY

When the project entered development, the retention of the  $\alpha$ -resorcyate core, two pyrazines and a chiral side-chain as the building blocks of the synthesis was appealing. The use of acid **12** (Figure 1) as the synthetic precursor to the API held attraction on the grounds that it was known to be a highly crystalline material whose isolation could be used as a late-stage control point. Regardless, in the spirit of building up knowledge around alternative route options in early chemical development, exploratory studies that involved the early introduction of aminopyrazine **4** were undertaken. Its amidation with an  $\alpha$ -resorcyate unit with at least one unprotected hydroxyl quickly floundered. The activated carbonyl functionality of the  $\alpha$ -resorcyate preferred to react with another such unit to form ester impurities, rather than with the poorly nucleophilic amine of aminopyrazine **4**.

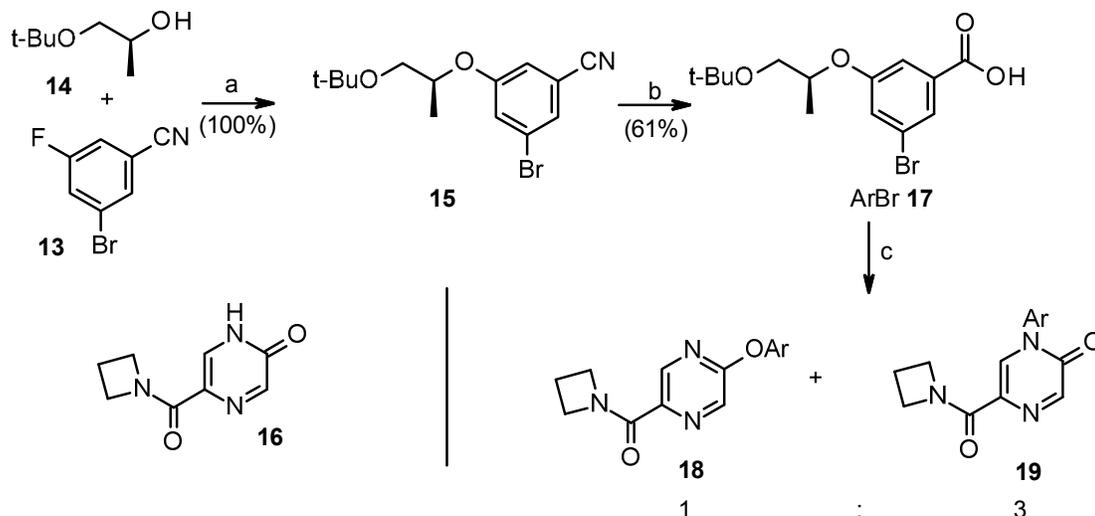


14 **Figure 1** Synthetic precursor to API

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18 **INITIAL  $\alpha$ -RESORCYLATE FUNCTIONALIZATION STUDIES**

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20 Given the intent to use the amidation of aminopyrazine **4** with acid **12** for the API bond-forming step,  
21 efforts turned to the identification of an efficient synthesis of the latter. The use of a 3,5-  
22 dihalobenzonitrile starting material, as an alternative to methyl  $\alpha$ -resorcyate (**5**), was briefly considered.  
23 Successive nucleophilic displacements on a compound such as **13** should differ greatly in their  
24 respective rates, allowing the 3- and 5- positions to be successfully differentiated. This approach was  
25 tested on material that was associated with a structurally-related drug candidate, alcohol **14** (Scheme 3).<sup>7</sup>  
26  
27 Whilst the initial  $S_NAr$  to give ether **15** was successful, the attempted union of pyrazinone **16** and aryl  
28 bromide **17** afforded a mixture of ethers **18** and **19** in which the ambidentate nucleophile had  
29 preferentially reacted through nitrogen, rather than the pyrazinone oxygen atom.  
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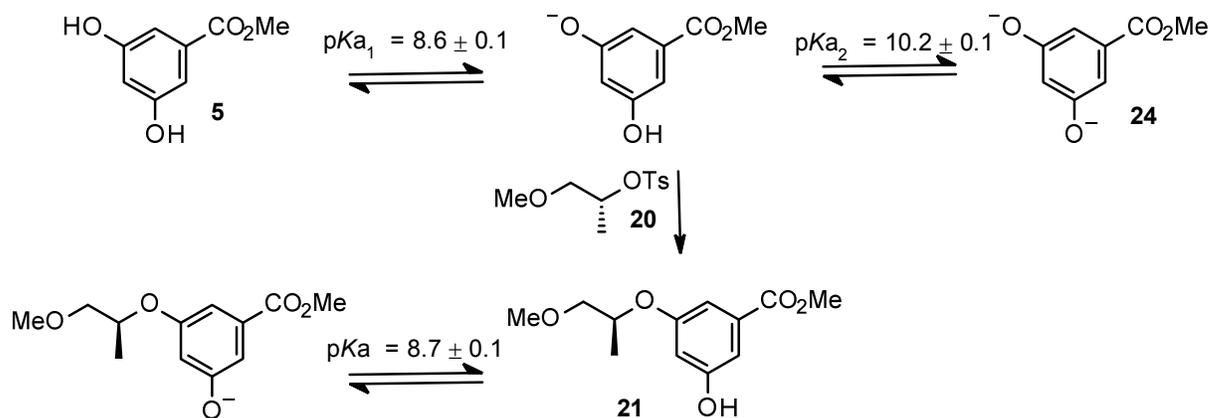
40 **Scheme 3** Attempted derivatization of a 3,5-dihalobenzonitrile **13**



a) NaHMDS, DMF, 23 °C; b) NaOH (aq.), EtOH,  $\Delta$  then HCl (aq.); c) **16**, Cs<sub>2</sub>CO<sub>3</sub>, CuI, 2,2,6,6-tetramethylheptane-3,5-dione, NMP, 125 °C then HCl (aq.)

Attention returned to methyl  $\alpha$ -resorcyate (**5**) as a starting material and the search for a selective monoalkylation that would allow the chiral side-chain to be introduced.<sup>8-9</sup> In spite of the screening of different bases and solvents, alkylations with tosylate **20** (prepared from alcohol **7**<sup>3a,10</sup>) suffered from poor conversions or selectivity (monoalkylation vs bisalkylation).<sup>11</sup> The same problem was observed with an assessment of a Mitsunobu etherification option. The propensity for a monoalkylated derivative like ether **21** to react again, before all of the methyl  $\alpha$ -resorcyate (**5**) has been consumed may be explained by the similarity in the pK<sub>a</sub> values of the latter and ether **21** (Scheme 4).

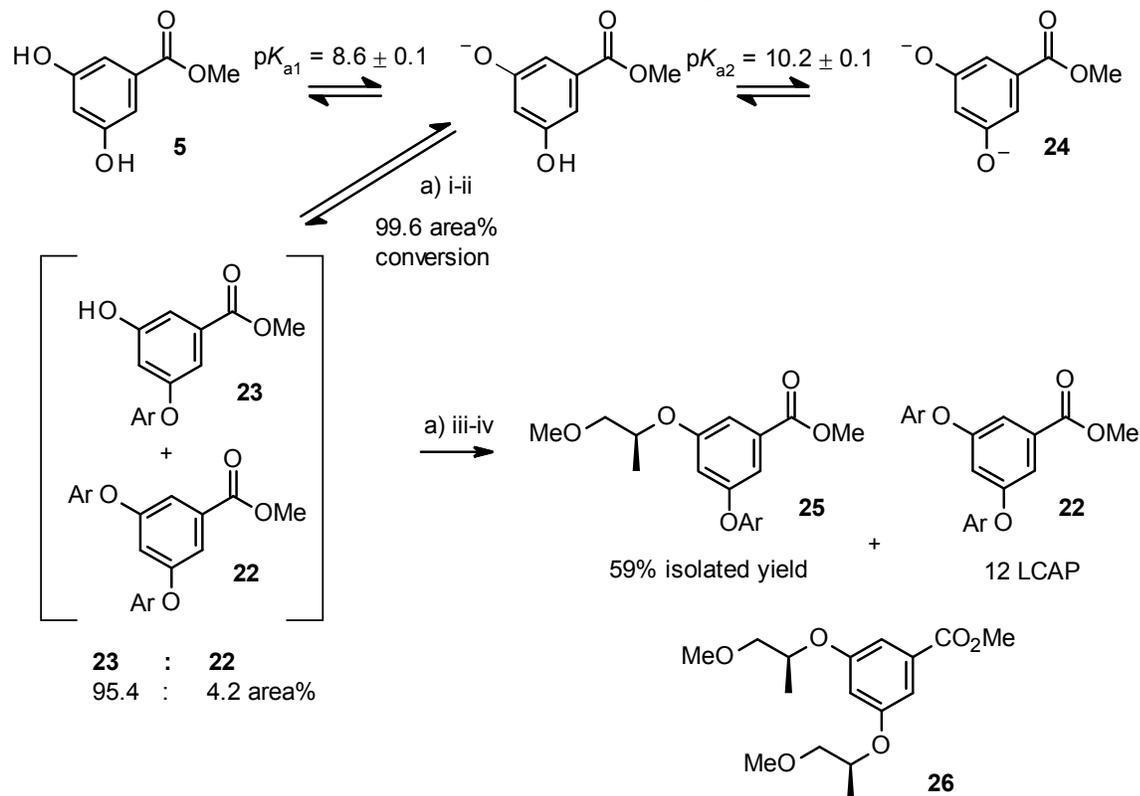
**Scheme 4** Calculated pK<sub>a</sub> values (aqueous, T=25 °C, zero ionic strength)<sup>12</sup> relevant to monoalkylation approach



A monoarylation approach was studied in parallel with the alkylation studies described above, and started with the use of potassium carbonate as base and chloropyrazine **3** as electrophile. In addition to the risk of overarylation to form bisether **22** (Scheme 5), in an analogous fashion to that described above, these efforts were soon found to be complicated by the ability of the newly-installed pyrazine of ether **23** to intermolecularly migrate under the basic conditions of the reaction. This led to the regeneration of a quantity of bisether **22** (now via a mechanism distinct from overreaction) and methyl  $\alpha$ -resorcyate (**5**).<sup>3c</sup> Gratifyingly, prestirring the methyl  $\alpha$ -resorcyate (**5**) with excess carbonate base, prior to the addition of the electrophile led to useful selectivities, by allowing access to the more basic (and presumably more nucleophilic)  $\alpha$ -resorcyate dianion **24** (Scheme 5). After some optimization which included switching to the use of cesium carbonate as base, the dosed addition of a slight excess (0.97 molar equivalents) of chloropyrazine **3** to a solution of methyl  $\alpha$ -resorcyate (**5**) in dimethyl sulfoxide led to a useful level of selectivity for ether **23** versus bisether **22** (Scheme 5). The intention was then to alkylate the remaining  $\alpha$ -resorcyate hydroxyl through a Williamson etherification with tosylate **20**, so as to form ether **25**. The screening of solvents, carbonate bases and strong organic bases led to the selection of the use of cesium carbonate in DMSO for the etherification. A drawback of the telescoped use of these basic conditions was disruption of the equilibrium shown in Scheme 5, resulting in scrambling of the recently installed pyrazine moiety. This migration led to an increase in the amount

of bisether **22** in the mixture (to 12% area by HPLC (LCAP)). The migration also liberated methyl  $\alpha$ -resorcyate (**5**), opening the door to the formation of another bisether **26**.<sup>13</sup>

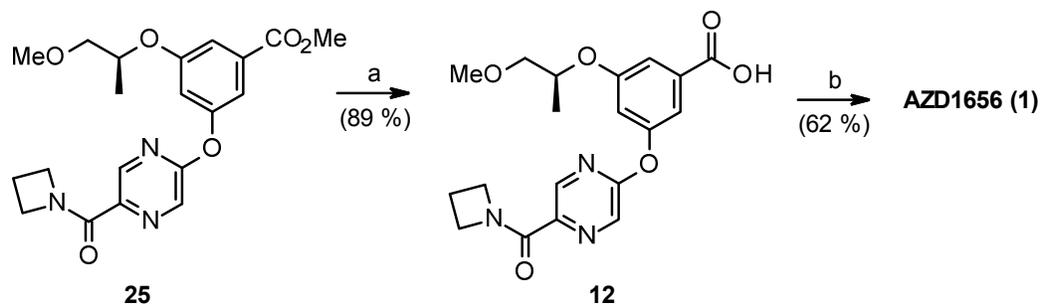
**Scheme 5** Derivatization of methyl  $\alpha$ -resorcyate (**5**) using an initial monoarylation.



a) i)  $\text{Cs}_2\text{CO}_3$  (2.5 eq.), DMSO, 50 °C, ii) **3** (0.97 eq.), dosed addition, iii) **20**, 80 °C, iv) chromatography

Even when pure, ether **25** was an oil preventing its purification through crystallization. After it had been chromatographically purified from the mixture of compounds shown in Scheme 5, ether **25** was successfully hydrolyzed to acid **12**, using careful control of the reaction temperature and time to minimize hydrolysis of the base-labile azetidine amide and pyrazine-ether bonds. The sequences shown in Schemes 5 and 6 were leveraged in order to deliver 3.4 kg of **AZD1656** (**1**).

**Scheme 6** Completion of the first development delivery of **AZD1656** (**1**)



a) i) NaOH (aq), NMP,  $-10\text{ }^{\circ}\text{C}$ , ii) AcOH (aq); b) 4, T3P, *N*-methylmorpholine, 2-MeTHF, reflux

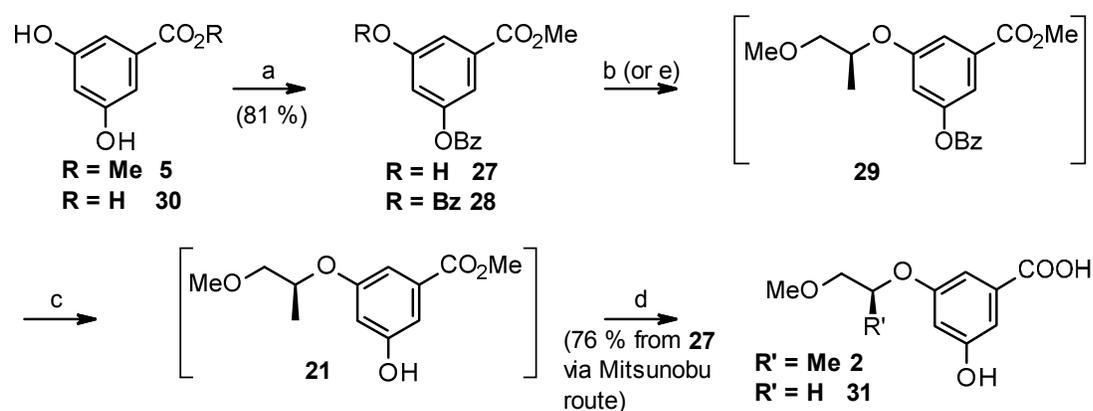
### LATER $\alpha$ -RESORCYLATE FUNCTIONALIZATION STUDIES

The attractiveness of compound **25** as an intermediate for the commercial route used to supply **AZD1656 (1)** was diminished by its being an oil. Thus, our investigation of competing route options was restarted and focused on the identification of possible crystalline intermediates. The  $\alpha$ -resorcyrate studies detailed above were already known to generate materials that were mostly oils and so attention turned to the generation of a crystalline material through the monoprotection of methyl  $\alpha$ -resorcyrate (**5**). Such a material would be primed for the introduction of the chiral side-chain through alkylation before deprotection steps would reveal acid **2** (Scheme 1), a solid that was known to be isolable in spite of its modest melting point ( $42\text{ }^{\circ}\text{C}$ ). Whilst a synthetic strategy which uses protecting groups has inherent inefficiencies associated with it, it was hoped these could be mitigated by using a group that could be removed alongside the hydrolysis of the methyl ester functionality of the  $\alpha$ -resorcyrate ring.

These considerations led to the targeting of the monobenzylation of methyl  $\alpha$ -resorcyrate (**5**),<sup>9,14</sup> a known transformation and one that was reported to generate a solid product,<sup>15</sup> ester **27** (Scheme 7), whose crystallization could further enhance the impurity control strategy for the API. Gratifyingly, the transformation was successful in our hands. The insolubility of ester **27** in the aqueous reaction medium was no doubt responsible for the limited levels of the bisbenzoyl byproduct **28** observed. Maintaining

the pH within a range of 7.8–8.2 was found to be critical. This was initially achieved by codosing benzoyl chloride with a separate addition of sodium hydroxide buffered with sodium dihydrogenphosphate, and restricted bisbenzoylation to ca. 6 LCAP. The use of aqueous solutions of lithium hydroxide or potassium carbonate offered improvements, and their use in combination produced a superior result still. Buffering with this mixture allowed ester **27** to be isolated with levels of methyl  $\alpha$ -resorcylate (**5**) and the overreaction product **28** that were both below 2 LCAP.

**Scheme 7** Synthesis of acid **2** using a benzoyl protecting group strategy



- a) BzCl, PhMe, LiOH (aq),  $\text{K}_2\text{CO}_3$  (aq); b) (*R*)-1-methoxypropan-2-ol (**7**),  $\text{PPh}_3$ , DIAD, PhMe, 0 °C;  
 c) NaOMe, MeOH; d) KOH (aq); e) **20**,  $\text{Cs}_2\text{CO}_3$ , DMSO

With the  $\alpha$ -resorcylate 3- and 5-substituents successfully differentiated, through either monoarylation or monobenzoylation, there was now the need to etherify the remaining hydroxyl with the chiral side-chain. Whilst the retention of the Williamson ether synthesis remained an option, drawbacks included the relative expense of cesium carbonate, concerns over its suspension given its high density, and the negative impact on process mass intensity and throughput of washing out DMSO using multiple water washes. Further caveats included its use of a potential genotoxic impurity, in the form of tosylate **20**, albeit one whose downstream purging meant that it did not affect the API quality, and benzoyl group migration under the basic conditions of the reaction. Attention thus returned to the consideration of a Mitsunobu reaction as a possible means of installing the side-chain. This reaction has found limited

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4 uses in large-scale production due to the challenge of separating the reaction product from its redox  
5 byproducts, a phosphine oxide and dialkyl azodicarboxylate.<sup>16-21</sup> In our case, we were attracted by the  
6 option of telescoping the product of the etherification into a step that would remove the benzoyl  
7 protecting group. In unveiling the  $\alpha$ -resorcylic hydroxyl, it was hoped that liquid-liquid partitioning  
8 could then be used to draw it into an alkaline phase, away from the Mitsunobu byproducts.  
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11 After some experimentation with the solvent and the order of addition of the reagents, it was found the  
12 addition of diisopropyl azodicarboxylate to a toluene solution of the other components led to the rapid  
13 and clean conversion of phenol **27** to ether **29** (Scheme 7). The reaction proved to be a faster and  
14 higher-yielding than the Williamson etherification conditions against which it was being compared  
15 (reaction condition *e* in Scheme 7), and proceeded without any scrambling of the benzoyl group. DSC  
16 analysis showed there were no thermal stability issues with any of the process or waste streams  
17 associated with the Mitsunobu reaction.<sup>22</sup>  
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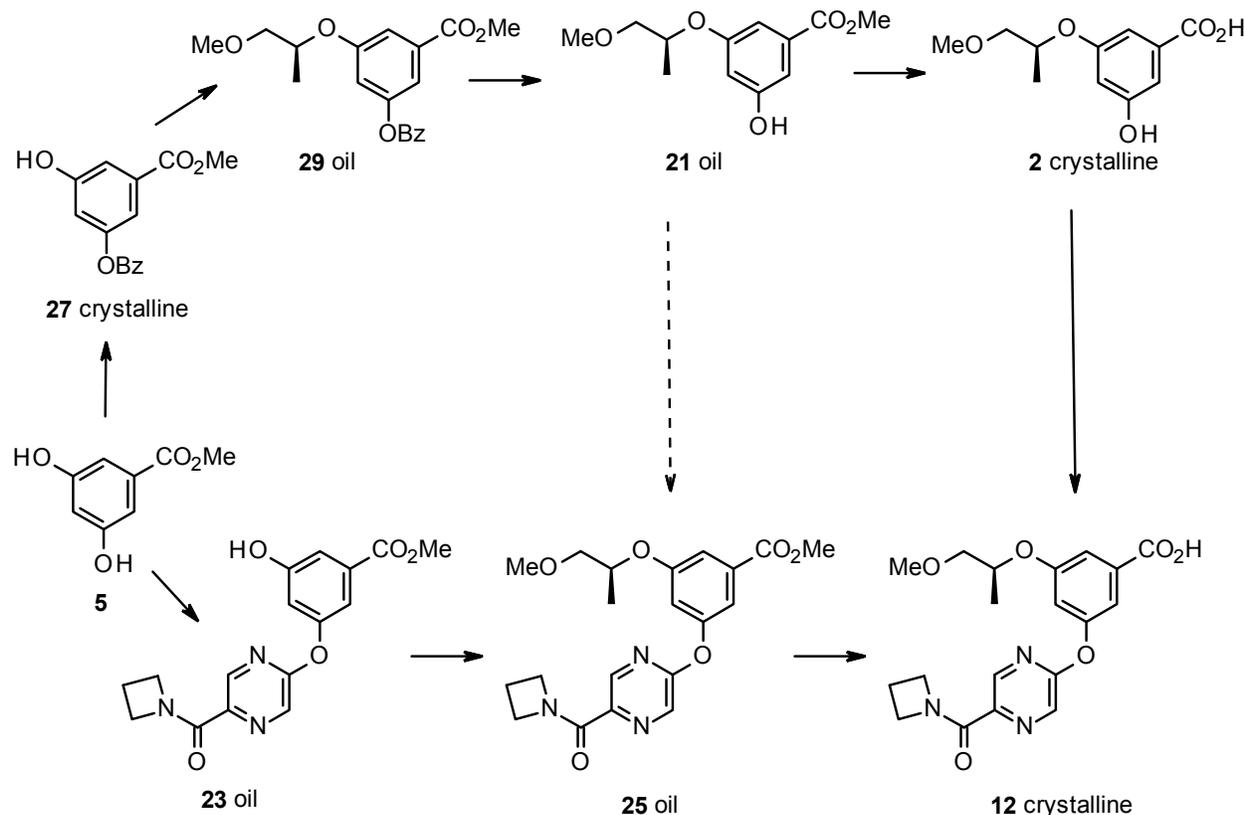
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20 Using a benzoyl protecting group to access acid **2** potentially posed the challenge of cleanly separating  
21 benzoic acid from the compounds of interest arising from the removal of the two ester groupings of  
22 compound **29** using aqueous base. With this in mind, a transesterification approach was instead targeted  
23 for the debenzoylation. Gratifyingly, the addition of methanolic sodium methoxide, once the redox  
24 byproducts of the Mitsunobu reaction had been filtered off, smoothly converted ester **29** to phenol **21**  
25 (Scheme 7). Curiously, any lingering compound **28**, an impurity which would reform  $\alpha$ -resorcylic acid  
26 (**30**) on downstream processing, transesterified at a slower rate than ester **29**. Thus, once the  
27 transesterification was complete, careful extraction with dilute (0.25 M) potassium hydroxide solution  
28 left the methyl esters of the  $\alpha$ -resorcylic components intact, allowing the potassium salt of phenol **21** to  
29 be partitioned away from compound **28**, together with the methyl benzoate coproduct of the  
30 transesterification, residual organic-soluble redox byproducts from the Mitsunobu reaction, and bisether  
31 **26**, a compound which arose from the reaction of the residual methyl  $\alpha$ -resorcylic (**5**) in phenol **27**.  
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4 The addition of more potassium hydroxide basified the phase containing the phenol **21**, allowing the  
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6 hydrolysis of its methyl ester so as to give acid **2** (Scheme 7). Trace levels of upstream impurities were  
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8 still present alongside acid **2**, though they could be purged by pH-controlled liquid-liquid extractions,  
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10 ahead of the crystallization of **2**. Thus, after a pH adjustment to 9.5–10.0, washing the aqueous phase  
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12 with *tert*-butyl methyl ether removed any residual triphenylphosphine oxide and diisopropyl  
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14 azodicarboxylate. After further acidification to pH 1.3–1.5, the extraction of acid **2** with *tert*-butyl  
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16 methyl ether reduced accompanying levels of  $\alpha$ -resorcylic acid **30** (arising from the presence of  
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18 compound **28** in ester **29**) to  $\leq 0.2$  LCAP.

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21 The coupling of acid **2** and chloropyrazine **3** was assessed using a variety of solvents and bases. The  
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23 reaction proved high-yielding using cesium carbonate in DMSO. Whilst this combination of materials  
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25 brought with it the drawbacks outlined above for the Williamson etherification, we were confident that  
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27 these could be overcome with future process design studies. Consequently, the route that had been  
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29 initiated with the monobenzoylation of methyl  $\alpha$ -resorcylic acid (**5**) had yielded a means of accessing acid  
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31 **12**, the precursor to the API.  
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## 36 ROUTE SELECTION

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38 The existence of both the monobenzoylation approach and that which was initiated by the monoarylation  
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40 of methyl  $\alpha$ -resorcylic acid (**5**) meant one option had to be discarded prior to initiating development for  
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42 commercial-scale production of the API. The route options are outlined in Scheme 8. In spite of the  
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44 monobenzoylation approach involving two more transformations (5) than the monoarylation option that  
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46 routed via ether **23**, the selection of the former was straightforward. The monobenzoylation approach  
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48 featured a crystalline precursor (acid **2**) to acid **12**, high-yielding transformations, the ability to partition  
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50 away related substances and reaction byproducts through liquid-liquid extractions and the opportunity to  
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52 telescope the steps associated with the conversion of ester **27** to acid **2**.  
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**Scheme 8** Summary of approaches to acid **2**

Whilst the monoarylation approach featured fewer chemical transformations than the monobenzoylation approach, this came at the expense of routing via oils. Another consideration was that the hydrolysis of the ester functionality of compound **25**, so as to afford acid **12**, was still going to be challenging to achieve whilst avoiding significant levels of hydrolysis of the azetidine amide and C<sub>pyrazine</sub>-O bonds. This also ruled out converting compound **21** of the monobenzoylation approach to acid **12** via ether **25** (dotted arrow in Scheme 8).

**SCALEUP OF MANUFACTURE OF ACID 2**

Not unexpectedly, given the presence of multiple phases, and the potential for bisbenzoylation, the successful scaleup of the monobenzoylation reaction was envisaged as being challenging.<sup>23</sup> Indeed, initial pilot plant batches produced ester **27** with up to 20 LCAP of overreaction product **28**. This was

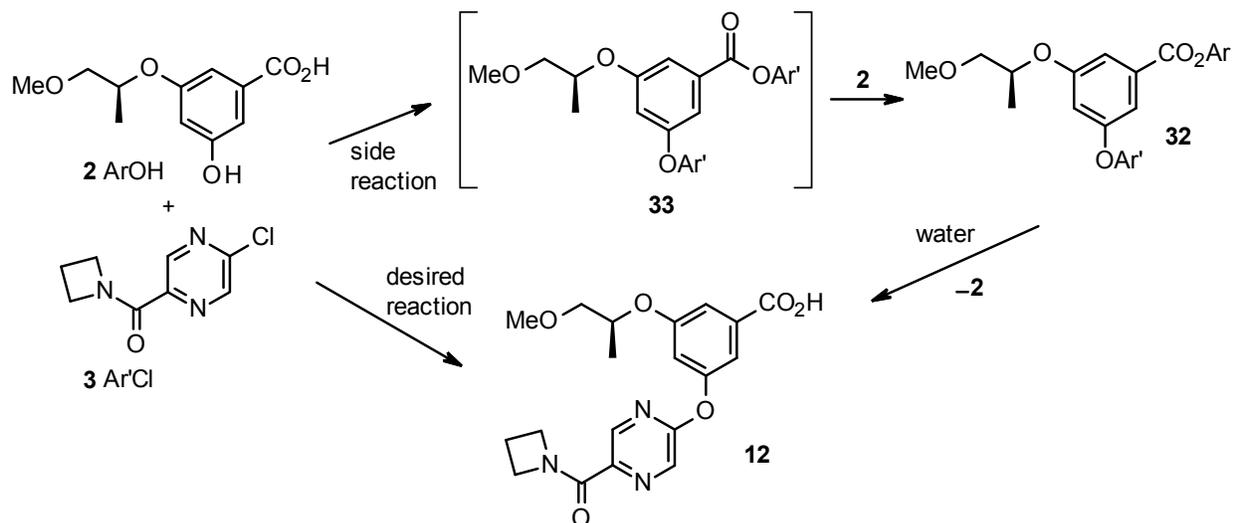
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4 partly attributed to pH measurements used to control the reagent additions, not aligning with the local  
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6 pH at the site of the reaction. After assessing different locations of the reactor pH probe in an attempt to  
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8 achieve a correlation with at line measurements, the attachment of the pH probe to the reactor's  
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10 sampling device was selected and used to control the rate of reagent addition. Dosing the benzoyl  
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12 chloride as a solution in toluene was found to attenuate its background hydrolysis to benzoic acid and to  
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14 make the control of pH easier. This had to be balanced against the increasing tendency of ester **27** to  
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16 coalesce from fine particles into a thick, unstirrable mixture as the amount of toluene used was  
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18 increased. A path forward was achieved by limiting the amount of toluene (54% wt/wt) used to dilute  
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20 the benzoyl chloride and the length of time after the end of the addition before the product was filtered  
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22 off. With these modifications in place, a normalized conversion of methyl  $\alpha$ -resorcyate (**5**) to ester **27**  
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24 of 96 LCAP could be typically achieved whilst restricting the amount of overreaction product **28** to  
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26 about 2 LCAP. Prolonged vacuum drying failed to reduce the water content of the initially isolated ester  
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28 **27** below ~0.5% wt/wt. This level required better control to ensure ester **27** was reproducibly consumed  
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30 in the ensuing Mitsunobu reaction, thus limiting the amount of  $\alpha$ -resorcylic acid equivalent that could  
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32 potentially track through the rest of the synthesis. This control was achieved and the purity improved by  
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34 treating a solution of the initially isolated ester **27** with powdered cellulose before it was crystallized  
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36 from a mixture of toluene and isopropyl acetate. In this way, 1.02 metric tons of ester **27** with a water  
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38 content of <0.1% wt/wt were manufactured over four batches, and in an overall yield of 81%. At the  
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40 end of the Mitsunobu reaction, the addition of 0.07% mol/mol seed induced the crystallization of 75% of  
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42 the theoretical amount of both triphenylphosphine oxide and diisopropyl hydrazine-1,2-dicarboxylate as  
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44 a readily filtered complex (1:1 mol/mol). The further elaboration of the toluene solution of ether **29**  
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46 proved straightforward, using the chemistry shown in Scheme 7. In this way, 619 kg of acid **2** were  
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48 made with an  $\alpha$ -resorcylic acid (**30**) content of only 0.1 LCAP and in an overall yield of 62% from  
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50 methyl  $\alpha$ -resorcyate (**5**). The purity across four batches was 99.5–99.7 LCAP with the largest impurity  
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4 (ca. 0.20 LCAP) being the analog **31** arising from the presence of 2-methoxyethanol in the (*R*)-1-  
5 methoxy-2-propanol (**7**) starting material (Scheme 7). Despite its reputation of generating a lot of waste,  
6 it should be noted that, in spite of development efforts, the sequence that utilized a Williamson  
7 etherification (reaction condition *e* in Scheme 7) had a much less favourable process mass intensity  
8 (207.4 kg/(kg **2**)) at the point where it was supplanted by the Mitsunobu route (69.6 kg/(kg **2**)).  
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### 17 **S<sub>N</sub>Ar REACTION DEVELOPMENT**

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19 A large amount of process development was performed on the stages associated with the conversion of  
20 methyl  $\alpha$ -resorcylate (**5**) to acid **2** in the period leading up to route selection. By contrast, the  
21 development of the conversion of acid **2** to **AZD1656** (**1**) had been developed only enough to derisk the  
22 continual manufacture of clinical supplies. With the route selected, there was the opportunity to  
23 consider more wide-ranging improvements to these latter stages. The assessment of 325 mesh  
24 potassium carbonate as a cheaper and more easily suspended alternative to the cesium carbonate used to  
25 date was initially characterized by excessive reaction times. This was addressed through the addition of  
26 1 relative volume of water which presumably helped to solubilize the base (Scheme 9). More basic  
27 systems, accessed by adding more water or replacing too much of the potassium carbonate charge with  
28 potassium hydroxide liquor, gave rise to byproducts arising from the hydrolysis (not shown) of the  
29 amide or C<sub>pyrazine</sub>-O bonds of ether **12**. As with all heterogeneous reactions, there was the risk of the  
30 offline analysis of the reaction being performed with a sample that was not representative of the whole  
31 batch. With this in mind, a model based on in-line Raman data was built to allow the conversion of acid  
32 **2** to ether **12** to be followed during production.<sup>24</sup> A small amount (0.1-0.2 LCAP) of impurity **32** always  
33 formed in the reaction, presumably through the intermediacy of an activated carbonyl species **33**  
34 (Scheme 9). Impurity **32** could be conveniently degraded to acid **12** by adding more water at the end of  
35 the reaction to basify the system.  
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**Scheme 9** Transformations associated with S<sub>N</sub>Ar reaction



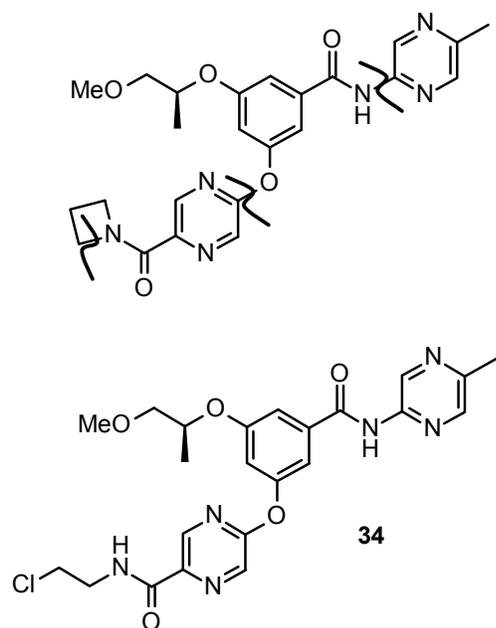
Conditions: DMSO-water (6:1, v/v), K<sub>2</sub>CO<sub>3</sub>, 57 °C then water

The acidification of the batch at the reaction close with dilute aqueous hydrochloric acid resulted in the uncontrolled precipitation of acid **12**. After gathering solubility data for this material as a function of temperature and solvent (DMSO-water mixtures), a final solvent composition of 56% v/v dimethyl sulfoxide was targeted. This was achieved by acidifying with hydrochloric acid, whilst taking care to ensure the final pH was above 2.5 so as to avoid the acid-mediated degradation of acid **12**. The potassium chloride generated by the neutralization of the potassium carbonate base was screened off in order to control the sulfated ash content of the product. After subsequent cooling and seeding, a slurry of acid **12** formed which filtered rapidly and gave low losses to liquors (1.8% yield loss). After drying, the material isolated contained low amounts of dimethyl sulfoxide (<0.05% wt/wt), inorganics (0.35% wt/wt), water (0.16% wt/wt) and related substances (0.56 LCAP). Despite the volumetric efficiency of this processing option, to date there has not been the opportunity to test it in anything other than a laboratory setting. Instead, as part of plant manufactures, the acid **12** content of the slurry arising from the acidification of the batch was dissolved in warm isopropyl acetate by way of liquid-liquid extractions. A water wash rid the extracts of adventitiously extracted dimethyl sulfoxide before

1  
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4 azeodrying and cooling crystallized acid **12** that was readily filtered, washed and dried. This protocol  
5  
6 allowed 742 kg of acid **12** to be produced in an overall yield of 93%.  
7  
8  
9

## 10 **AMIDATION**

11  
12 The elaboration of acid **12** to **AZD1656 (1)** requires its union with aminopyrazine **4**. The poor  
13  
14 nucleophilicity displayed by aminopyrazine **4** led to limited success when a slew of different amidation  
15  
16 conditions were screened. Whilst conversions were in general aided by increasing the reaction  
17  
18 temperature, this was often at the expense of competing S<sub>N</sub>Ar reactions at the pyrazine rings of  
19  
20 **AZD1656** (Figure 2).<sup>25</sup> Activating acid **12** as an acid chloride generated hydrogen chloride which,  
21  
22 without scavenging, was found to open the azetidine ring so as to form alkyl chloride **34** as a byproduct  
23  
24 (Figure 2). The limited delocalization of the azetidine nitrogen lone pair into the amide carbonyl can be  
25  
26 used to rationalize the comparative basicity of the azetidine nitrogen and hence the susceptibility of the  
27  
28 azetidine amide towards this side-reaction. It is notable that this ring-opening of azetidine amides has  
29  
30 found preparative use.<sup>26</sup>  
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**Figure 2** Sites of side reactions when screening conditions for conversion of acid **12** to **AZD1656 (1)** and structure of alkyl chloride **34**

A successful reagent combination used *n*-propylphosphonic anhydride (T3P) and *N*-methylmorpholine in 2-methyltetrahydrofuran. Whilst this enabled early development deliveries of **AZD1656 (1)** (Scheme 6), the continued use of T3P posed a number of drawbacks. These included the need and expense associated with the use of a ~70% mol/mol excess of the reagent to completely consume acid **12**.<sup>27</sup> As a listed chemical weapons precursor,<sup>28</sup> the storage, use and disposal of T3P needs to be fully documented, whilst the *n*-propylphosphonic acid waste generated by its use requires treatment prior to discharge into watercourses. Finally, impurities formed in a process using T3P retarded the rate of crystallization of the desired polymorph (*vide infra*), necessitating its later recrystallization.

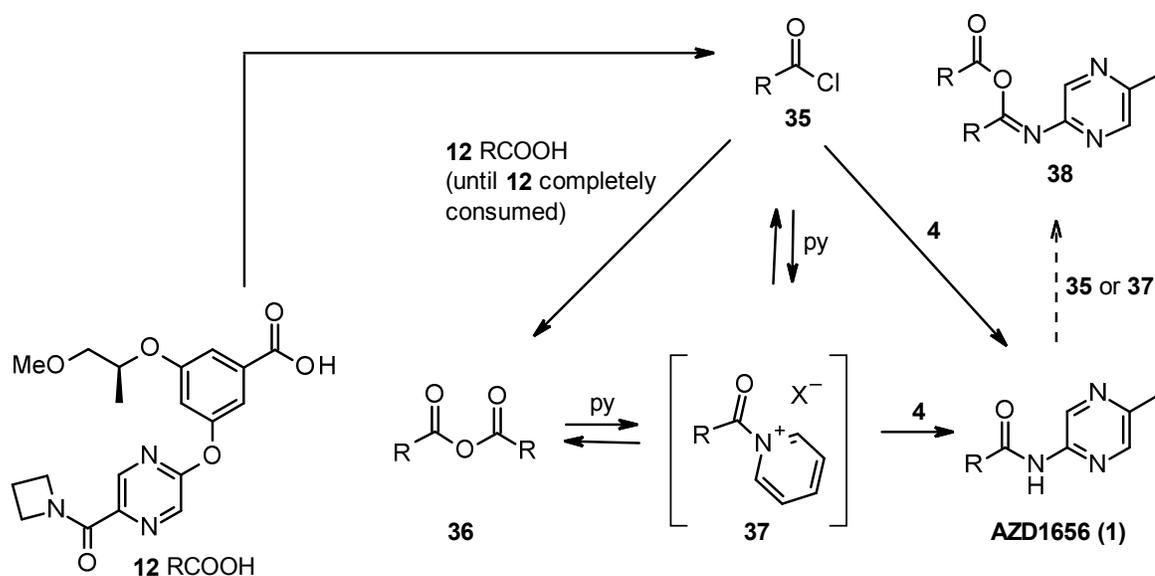
With the need to development a long-term solution for the amidation step, attention turned to the activation of acid **12** as an acid chloride **35** (Scheme 10). Whilst the use of thionyl chloride in this regard was one of the better performers in the initial screen of conditions, the conversion was still only

1  
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4 modest due to the formation of significant quantities of the acid anhydride intermediate **36** (Scheme 10),  
5  
6 a material that showed limited reactivity towards aminopyrazine **4**. The generation of hydrogen chloride  
7  
8 as a byproduct also brought the need to scavenge it adequately so as to avoid the formation of alkyl  
9  
10 chloride **34** (Figure 2).

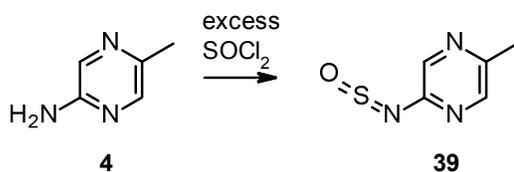
11  
12 In spite of these challenges, the economics of using thionyl chloride as a reagent were persuasive. It was  
13  
14 recognized from the outset that the presence of even small amounts of an acyl pyridinium species **37**  
15  
16 could provide a valuable conduit for improving the conversion of acid **12** to acid chloride **35** (at the  
17  
18 expense of acid anhydride **36**), as shown in Scheme 10, and accelerating the conversion of acid chloride  
19  
20 **35** to **AZD1656 (1)**.<sup>29</sup> It was also appreciated that through the judicious choice of solvent,  
21  
22 (super)stoichiometric amounts of pyridine itself could simultaneously be used to scavenge the hydrogen  
23  
24 chloride generated as a byproduct of the acid chloride formation, limiting its ability to open up the  
25  
26 azetidine ring. The examination of literature  $pK_a$  data immediately drew us to the potential use of  
27  
28 acetonitrile as the reaction solvent ( $pK_{a\text{HCl}} = 10.3$ ,<sup>30</sup>  $pK_{a\text{pyH}^+} = 12.5$ <sup>31</sup>). Gratifyingly, this combination of  
29  
30 pyridine additive (3 eq.) and solvent met with immediate success and a readily stirred reaction mixture.  
31  
32 Raman monitoring revealed the rapid consumption of acid **12** to give an intermediate, presumably  
33  
34 anhydride **36**. Levels of the latter then fell away to low levels at the expense of growth in levels of  
35  
36 another material, presumably acid chloride **35**, which was now able to persist given the ever decreasing  
37  
38 levels of acid **12**. The addition of aminopyrazine **4** at this point led to a high reaction conversion to  
39  
40 **AZD1656 (1)** in under 30 min and the material isolated contained only ca. 200 ppm of alkyl chloride **34**.  
41  
42 Process optimization involved the addition of the activated species to a solution of aminopyrazine **4**.  
43  
44 This controlled overreaction to form *O*-acyl impurity **38** (Scheme 10), and allowed a reaction conversion  
45  
46 of 99 LCAP to be reliably achieved. Interestingly, the reaction conversion was found to be adversely  
47  
48 affected when particularly dry acetonitrile (20 ppm) was used. This water had a role in hydrolysing the  
49  
50 excess thionyl chloride (20% mol/mol) present at the end of the activation stage of the reaction,  
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preventing the excess reagent from transforming aminopyrazine **4** into an *N*-sulfinyl imine **39** (Scheme 10).<sup>32</sup> Gratifyingly, the reactions went to completion with a 10% molar excess of aminopyrazine **4** and plant-grade acetonitrile (water content 100-200 ppm). Workup development included washing out the pyridine at the end of the reaction using sulfuric acid, rather than hydrochloric acid, in order to mitigate the risk of azetidine ring-opening.

**Scheme 10** Working mechanism summarizing key transformations consistent with conversion of acid **12** to AZD1656 (**1**)



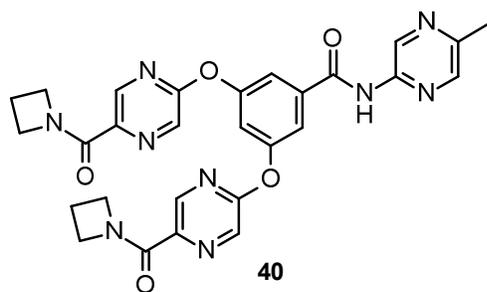
a) i)  $\text{SOCl}_2$ , *py* (3 eq.), MeCN, 20 °C, ii) add to **4** in MeCN, 20 °C



### CRYSTALLIZATION OF AZD1656 (**1**)

Screening had unearthed five polymorphs (including hydrates) on top of Form VI, the thermodynamically most stable polymorph that had been requested by drug product colleagues. Form VI could be accessed by slowly cooling a methyl isobutyl ketone (MIBK) solution of the API in the

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4 presence of micronized Form VI seed ( $>55 \text{ m}^2/\text{kg}$  input) such that the batch was kept supersaturated  
5  
6 with respect to Form VI but undersaturated with respect to a metastable (but kinetically more accessible)  
7  
8 form.<sup>33</sup> When levels of chloropyrazine **3** and compound **40** (Figure 3), the latter arising from the  
9  
10 presence of  $\alpha$ -resorcylic acid (**30**) in acid **2** were below levels that slowed the rate of crystallization of  
11  
12 Form VI, this polymorph could be crystallized in an isolated yield of 86%. Slow cooling was also  
13  
14 important in that it reduced the entrainment of MIBK in the crystals. The enantiomeric excess of the  
15  
16 **AZD1656** (**1**) prepared (97.6 LCAP), prior to the crystallization of Form VI was in accord with that of  
17  
18 the (*R*)-1-methoxy-2-propanol (**7**) input (97.5 LCAP), consistent with a complete inversion of  
19  
20 stereochemistry during the Mitsunobu reaction. The crystallization of Form VI reduced the amount of  
21  
22 the undesired enantiomer to 1.3-1.4 LCAP. As the initial crystallization was performed in a facility that  
23  
24 was not fully certified for the isolation of API destined for clinical trials, it was necessary to redissolve  
25  
26 the material in MIBK, screen it and to crystallize it again in just such a facility. When the amidation  
27  
28 process was not capable of producing Form VI directly (as was the case with the T3P-mediated  
29  
30 amidation), such a recrystallization was required anyway. Whilst it may not be a necessity for any  
31  
32 future manufactures performed in an appropriately certified facility, in this case it allowed the isolation  
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34 of the API in a yield of 86%.  
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**Figure 3** Structure of API impurity **40**

## CONCLUSIONS

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4 Various strategies were investigated in order to differentiate between the hydroxyl groups of an  $\alpha$ -  
5 resorcyate derivative. The option pursued involved the monobenzoylation of methyl  $\alpha$ -resorcyate (**5**),  
6 a slurry-to-slurry reaction that relied on the insolubility of the monobenzoyl ester product **27** in the  
7 reaction medium and maintaining accurate pH control on changing scale and equipment in order to limit  
8 bisbenzoylation. The chiral side-chain was emplaced using the Mitsunobu reaction: the solubility of a  
9 downstream intermediate in alkali allowed it to be partitioned away from the organic-soluble  
10 byproducts. These reaction conditions generated significantly less waste than a Williamson  
11 etherification variant. Thionyl chloride and pyridine in acetonitrile were used to achieve the successful  
12 amidation of an aminopyrazine **4** displaying low reactivity. These conditions offered a substantial cost-  
13 saving over the use of T3P. They also allowed access to the desired polymorph of the drug substance, a  
14 form that was thermodynamically preferred but slow-growing and disfavored by the presence of  
15 impurities, such that the recrystallization of the API was no longer a necessity. The processes described  
16 herein allowed the production of 506 kg of **AZD1656 (1)**.  
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## 34 **Experimental Section**

35  
36 **General.** NMR spectra were recorded on a Bruker instrument with tetramethylsilane (TMS) as internal  
37 reference. Chemical shifts are expressed in ppm ( $\delta$ ) relative to TMS, coupling constants ( $J$ ) are in Hz.  
38 Infrared spectra were recorded with diamond ATR sampling on an FTIR spectrometer using powdered  
39 samples or oils. Melting points were recorded using a Q2000 differential scanning calorimeter from TA  
40 Instruments. High resolution mass spectra were recorded on a Waters Synapt UPLC-MS instrument.  
41 Unless stated otherwise, commercial grade materials were used and stated temperatures refer to the  
42 temperature of the batch.  
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## 53 **Preparation of ester **27****<sup>34</sup>

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4 A solution of benzoyl chloride (479 kg, 3.41 kmol) in toluene (658 L) was added over no more than 2 h  
5  
6 to a slurry of methyl  $\alpha$ -resorcylate (**5**) (259 kg, 1.54 kmol) in water (2,600 L), which was being stirred at  
7  
8 20 °C. The pH was adjusted to 8.0 $\pm$ 0.2 prior to the start of (ca. 55 L) and during (ca. 1525 L) the  
9  
10 addition by dosing a freshly-prepared aqueous solution containing both lithium hydroxide (3.8% wt/wt)  
11  
12 and potassium carbonate (4.8% wt/wt). At the end of the addition of the benzoyl chloride solution, the  
13  
14 batch was maintained for a further 30 min using the addition of the alkali (ca. 65 L) to maintain the same  
15  
16 pH. The slurry was then filtered and the cake was washed with water (640 L). The material was  
17  
18 dissolved in isopropyl acetate (1755 L) and stirred at 55 °C with Vitacel FAC 200 (21 kg) and activated  
19  
20 charcoal (8 kg of 2CW CECA). After 15 min., the slurry was filtered and washed through with  
21  
22 isopropyl acetate (275 L). The batch volume was then reduced by vacuum distillation (275 mBarA).  
23  
24 Once 800 kg of distillate had been collected, toluene was added continuously (1155 L) whilst a further  
25  
26 800 kg of distillate were collected. The batch was cooled to 12 °C over at least 2 h. After a further 1 h,  
27  
28 the slurry was isolated by filtration and the cake washed with toluene (555 L). Vacuum drying (50  
29  
30 mBarA) at 60 °C afforded ester **27** as a white solid (340 kg, 81%). Mp 139 °C. IR 3431, 1706, 1599,  
31  
32 1331, 1272, 1246, 1144, 1106, 1086, 1071, 1009, 998, 764, 706 cm<sup>-1</sup>. <sup>1</sup>H NMR (DMSO-d<sub>6</sub>, 500 MHz)  $\delta$   
33  
34 (ppm) 10.26 (1H, s), 8.12 (2H, dd,  $J=8.2$ , 1.3 Hz), 7.74 (1H, tt,  $J=7.5$ , 1.3 Hz), 7.60 (2H, dd,  $J=8.2$ , 7.5  
35  
36 Hz), 7.32 (1H, dd,  $J=2.2$ , 1.4 Hz), 7.28 (1H, dd,  $J=2.2$ , 1.4 Hz), 6.98 (1H, dd,  $J=2.2$ , 2.2 Hz), 3.84 (3H,  
37  
38 s). <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, 126 MHz)  $\delta$  (ppm) 165.5, 164.4, 158.6, 151.6, 134.1, 131.6, 129.9 (2C), 129.0  
39  
40 (2C), 128.8, 114.0, 113.6, 113.2, 52.3. HRMS elemental calculated for C<sub>15</sub>H<sub>11</sub>O<sub>5</sub> (M-H)<sup>-</sup>: 271.0606;  
41  
42 found: 271.0615.  
43  
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47  
48 **Preparation of phenol 2.** (*R*)-1-Methoxy-2-propanol (**7**) (102 kg, 1.13 kmol) was added to a solution  
49  
50 of phenol **27** (245 kg, 900 mol) and triphenylphosphine (295 kg, 1.12 kmol) in toluene (2087 kg), and  
51  
52 washed through with toluene (20 kg). Diisopropyl azodicarboxylate (228 kg, 1.13 kmol) was added  
53  
54 over at least 1 h whilst maintaining the batch temperature at 2 °C. After stirring for 30 min at this  
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4 temperature, and warming to 20 °C, the batch was seeded with the 1:1 mol/mol complex of  
5  
6 triphenylphosphine oxide and diisopropyl hydrazinedicarboxylate (0.6 kg, 0.2% wt/wt). After stirring  
7  
8 for 2 h, the slurry was filtered and the cake washed with toluene (210 kg). A chromatographically-  
9  
10 purified sample of the filtrate gave ether **29** as a colorless oil. IR 1721, 1589, 1446, 1300, 1242, 1136,  
11  
12 1101, 1079, 1060, 1022, 996, 765, 705 cm<sup>-1</sup>. <sup>1</sup>H NMR (DMSO-d<sub>6</sub>, 500 MHz) δ (ppm) 8.13 (2H, dd,  
13  
14 *J*=8.3, 1.3 Hz), 7.71 (1H, tt, *J*=7.1, 1.3 Hz), 7.58 (2H, dd, *J*=8.3, 7.1 Hz), 7.40 (1H, app d, *J*=2.3 Hz),  
15  
16 7.40 (1H, app d, *J*=2.2 Hz), 7.22 (1H, dd, *J*=2.3, 2.2 Hz), 4.68 (1H, qdd, *J*=6.3, 6.1, 4.0 Hz), 3.84 (3H,  
17  
18 s), 3.49 (1H, dd, *J*=10.6, 6.1 Hz), 3.45 (1H, dd, *J*=10.6, 4.0 Hz), 3.29 (3H, s), 1.24 (3H, d, *J*=6.3 Hz).  
19  
20 <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, 126 MHz) δ (ppm) 165.4, 164.4, 158.7, 151.7, 134.1, 131.7, 129.9 (2C), 128.9  
21  
22 (2C), 128.7, 114.8, 114.4, 113.8, 74.9, 73.3, 58.5, 52.4, 16.3. HRMS elemental calculated for C<sub>19</sub>H<sub>19</sub>O<sub>6</sub>  
23  
24 (M-H)<sup>-</sup>: 343.1182; found: 343.1202.  
25  
26  
27  
28  
29

30 The filtrate was treated with methanolic sodium methylate (130 kg of 30.0% wt/wt, 722 mol) and stirred  
31  
32 at 25 °C for 60 min. After cooling to 2 °C, the solution was extracted with dilute potassium hydroxide  
33  
34 solution (1547 kg of 0.25 M, 387 mol, split over two extractions). A chromatographically-purified  
35  
36 sample of the extracts gave phenol **21** as a colorless oil. IR (cm<sup>-1</sup>) 3353, 1721, 1593, 1236, 1148, 1096,  
37  
38 1025, 1001, 765. <sup>1</sup>H NMR (DMSO-d<sub>6</sub>, 500 MHz) δ (ppm) 9.82 (1H, s), 6.99 (1H, dd, *J*=2.2, 1.5 Hz),  
39  
40 6.94 (1H, dd, *J*=2.4, 1.5 Hz), 6.61 (1H, dd, *J*=2.4, 2.2 Hz), 4.55 (1H, qdd, *J*=6.3, 6.0, 4.1 Hz), 3.80 (3H,  
41  
42 s), 3.45 (1H, dd, *J*=10.5, 6.0 Hz), 3.38 (1H, dd, *J*=10.5, 4.1 Hz), 3.26 (3H, s), 1.18 (3H, d, *J*=6.3 Hz).  
43  
44 <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, 126 MHz) δ (ppm) 166.2, 159.0, 158.9, 131.6, 108.9, 107.8, 107.1, 75.1, 72.8,  
45  
46 58.5, 52.1, 16.5. HRMS elemental calculated for C<sub>12</sub>H<sub>15</sub>O<sub>5</sub> (M-H)<sup>-</sup>: 239.0919; found: 239.0926.  
47  
48  
49  
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52 The extracts were combined and diluted with potassium hydroxide liquor (100 kg of 50% wt/wt, 891  
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54 mol). The solution was stirred at 24 °C for 60 min. The pH was adjusted to 9.5–10.0 using hydrochloric  
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4 acid solution (approximately 57 kg of 33% wt/wt, 516 mol), before it was washed at 23 °C with *tert*-  
5  
6 butyl methyl ether (927 kg, split over 2 washes). The pH was then adjusted to 1.5 at 23 °C using  
7  
8 concentrated hydrochloric acid (approximately 160 kg of 33% wt/wt, 1.45 kmol) before extractions were  
9  
10 performed with *tert*-butyl methyl ether (927 kg, split over two extractions). The organic extracts were  
11  
12 combined and stirred for 30 min with activated charcoal (17 kg, 25W CECA). The slurry was filtered  
13  
14 and the charcoal washed with *tert*-butyl methyl ether (89 kg). The batch volume was reduced by 670 kg  
15  
16 using vacuum distillation at 300 mBarA, before it was diluted with toluene (632 kg). The solution was  
17  
18 washed with water (735 kg) at 50 °C before being diluted with toluene (253 kg) and heptane (300 kg).  
19  
20 Solvent (315 kg) was removed by vacuum distillation at 350 mBarA. The batch was cooled to 38 °C  
21  
22 and seeded with acid **2** (0.2 kg). It was then cooled to 2 °C over at least 1 h and left to desupersaturate  
23  
24 for a further 30 min. The slurry was filtered and the cake washed with toluene (211 kg). The cake was  
25  
26 vacuum dried below 50 °C and 100 mBarA. This afforded acid **2** as a white solid (155 kg, 76%). Mp 42  
27  
28 °C. IR (cm<sup>-1</sup>) 2933, 1687, 1592, 1448, 1296, 1203, 1147, 1082, 1022, 846, 770, 730, 704, 674. <sup>1</sup>H  
29  
30 NMR (500 MHz, DMSO-d<sub>6</sub>) δ (ppm) 6.94 (1H, dd, *J*=2.2, 1.4 Hz), 6.91 (1H, dd, *J*=2.4, 1.4 Hz), 6.55  
31  
32 (1H, dd, *J*=2.4, 2.2 Hz), 4.54 (1H, qdd, *J*=6.3, 6.0, 4.1 Hz), 3.46 (1H, dd, *J*=10.5, 6.0 Hz), 3.44 (1H, br  
33  
34 s), 3.44 (1H, br s), 3.41 (1H, dd, *J*=10.5, 4.1 Hz), 3.27 (3H, s), 1.19 (3H, d, *J*=6.3 Hz). <sup>13</sup>C NMR (126  
35  
36 MHz, DMSO-d<sub>6</sub>) δ (ppm) 167.2, 158.7, 158.6, 132.8, 108.9, 107.4, 107.0, 74.9, 72.6, 58.5, 16.5. HRMS  
37  
38 elemental calculated for C<sub>11</sub>H<sub>13</sub>O<sub>5</sub> (M-H)<sup>-</sup>: 225.0763; found: 225.0759.

39  
40  
41 **Preparation of ether 12.** A slurry of acid **2** (150.0 kg at 98.5% wt/wt, 653.1 mol), chloropyrazine **3**  
42  
43 (136.4 kg at 98.4% wt/wt, 679.2 mol) and potassium carbonate (226 kg, 1.63 kmol) in dimethyl  
44  
45 sulfoxide (886 L) and water (148 L) was stirred with a jacket temperature of 57 °C overnight (16 h).  
46  
47 Water (1240 L) was added and the batch maintained with the same jacket temperature for a further 60  
48  
49 min before being cooled to 21 °C.<sup>35</sup> Concentrated hydrochloric acid (203 L of 11.60 M, 2.35 kmol) was  
50  
51 added over 60 min. Dilute hydrochloric acid (approx. 261 L of 1 M, 261 kmol, CARE: offgassing of  
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1  
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4 carbon dioxide) was then added so that the final measured pH was in the range of 3.0–4.5. The batch  
5  
6 was then warmed and isopropyl acetate (1480 L) charged so that the batch temperature did not drop  
7  
8 below 40 °C. The batch was allowed to equilibrate with a 75 °C jacket and the phases cut. The aqueous  
9  
10 phase was extracted once again at 75 °C with more isopropyl acetate (1480 L) before being discarded.  
11  
12 The two isopropyl acetate extracts were combined and washed at 63 °C with water (739 L), seeded (738  
13  
14 g of acid **12**). The jacket temperature was linearly ramped to 60 °C over 6 h. The batch was then  
15  
16 distilled to 900–1200 L using a –450 mbarG vacuum. The jacket temperature was then ramped to 21 °C  
17  
18 at –12 °C/h. After stirring out at this temperature for a further 6 h, the slurry was filtered and the damp  
19  
20 cake washed with isopropyl acetate (591 L). Vacuum oven drying (–250 mBarG) at 50 °C afforded acid  
21  
22 **12** as a white solid (227.2 kg, 89.8%). Mp 157 °C. IR (cm<sup>-1</sup>) 1701, 1609, 1565, 1438, 1274, 1112,  
23  
24 1028, 771, 704. <sup>1</sup>H NMR (DMSO-d<sub>6</sub>, 500 MHz) δ (ppm) 8.65 (1H, d, *J*=1.3 Hz), 8.50 (1H, d, *J*=1.3  
25  
26 Hz), 7.36 (1H, dd, *J*=2.3, 1.3 Hz), 7.31 (1H, dd, *J*=2.1, 1.3 Hz), 7.14 (1H, dd, *J*=2.3, 2.1 Hz), 4.66 (1H,  
27  
28 qdd, *J*=6.3, 6.1, 3.9 Hz), 4.53 (2H, t, *J*=7.7 Hz), 4.07 (2H, t, *J*=7.8 Hz), 3.49 (1H, dd, *J*=10.6, 6.1 Hz),  
29  
30 3.44 (1H, br s), 3.44 (1H, dd, *J*=10.6, 3.9 Hz), 3.27 (3H, s), 2.27 (2H, tt, *J*=7.8, 7.7 Hz), 1.21 (3H, d,  
31  
32 *J*=6.3 Hz). <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, 126 MHz) δ (ppm) 166.4, 162.7, 159.9, 158.9, 153.6, 142.1, 141.4,  
33  
34 133.6, 133.4, 114.4, 113.5, 113.4, 74.9, 73.2, 58.5, 54.2, 48.8, 16.3, 16.2. HRMS elemental calculated  
35  
36 for C<sub>19</sub>H<sub>22</sub>N<sub>3</sub>O<sub>6</sub> (M+H<sup>+</sup>): 388.1509; found: 388.1511.  
37  
38  
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40  
41 **Preparation of Form VI of AZD1656 (1).** A mixture of acid **12** (100 kg, 258 mol) and pyridine (61.3  
42  
43 kg, 774 mol) in dry acetonitrile (500 L) was prepared. Thionyl chloride (36.9 kg, 310 mol) was added  
44  
45 rapidly (CARE: exotherm, off-gassing of sulfur dioxide) and washed through with dry acetonitrile (100  
46  
47 L), whilst maintaining the batch temperature below 20 °C. The yellow solution so formed was added  
48  
49 without undue delays to a pre-prepared solution of aminopyrazine **4** (31.0 kg, 284 mol) in dry  
50  
51 acetonitrile (500 L),<sup>36</sup> whilst maintaining the batch temperatures of both solutions below 20 °C. After  
52  
53 washing through with dry acetonitrile (100 L) and a further 1 h at 20 °C, the batch was washed (CARE:  
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4 off-gassing) twice with sodium bicarbonate solution (150 L total of 7% wt/wt, split over 2 washes). The  
5  
6 organic phase (solution A) was retained, whilst the aqueous washes were back-extracted at 20 °C with  
7  
8 MIBK (250 L). The back-extract and solution A were combined and distilled to 450 L at 250 mBarA.  
9  
10 MIBK (1000 L) was charged and the batch redistilled to 400 L at 300 mBarA. MIBK (600 L) was  
11  
12 added and the solution washed at 45 °C with dilute sulfuric acid solution (1000 L of 1 M). The organic  
13  
14 phase (solution B) was retained, whilst the aqueous washes were back-extracted at 45 °C with MIBK  
15  
16 (250 L).<sup>37</sup> The back-extract and solution B were combined and washed at 45 °C with sodium  
17  
18 bicarbonate solution (500 L, 7% wt/wt) then water (500 L). The organic phase was distilled to 400 L  
19  
20 before being diluted with more MIBK (420 L). Seeding at 45 °C with **AZD1656 (1)** (Form VI, 4.0 kg,  
21  
22 4.0% wt/wt) was followed by aging at this temperature for 4 h. The batch was cooled at 6 °C/h to 20 °C  
23  
24 where it was held for a further 4 h before heptane (1200 L) was added in 6 equal portions at 1 h  
25  
26 intervals. The batch was isolated by filtration and the cake washed with a mixture of heptane and MIBK  
27  
28 (500 L of 2:1 v/v) before being vacuum dried at 45 °C. This yielded **AZD1656 (1)** as a white solid (107  
29  
30 kg, 85% corrected for 98% wt/wt). Mp 108 °C. IR (cm<sup>-1</sup>) 3249, 1632, 1549, 1435, 1344, 1307, 1291,  
31  
32 1273, 1264, 1248, 1225, 1175, 1132, 1113, 1090, 1027, 843, 752, 699. <sup>1</sup>H NMR (DMSO-d<sub>6</sub>, 500 MHz)  
33  
34 δ (ppm) 11.03 (1H, s), 9.26 (1H, d, *J*=1.4 Hz), 8.67 (1H, d, *J*=1.3 Hz), 8.55 (1H, d, *J*=1.3 Hz), 8.34 (1H,  
35  
36 d, *J*=1.4 Hz), 7.57 (1H, dd, *J*=2.2, 1.6 Hz), 7.47 (1H, dd, *J*=2.1, 1.6 Hz), 7.12 (1H, dd, *J*=2.2, 2.1 Hz),  
37  
38 4.78 (1H, qdd, *J*=6.3, 6.0, 3.9 Hz), 4.55 (2H, t, *J*=7.4 Hz), 4.08 (2H, t, *J*=7.8 Hz), 3.52 (1H, dd, *J*=10.7,  
39  
40 6.0 Hz), 3.47 (1H, dd, *J*=10.7, 3.9 Hz), 3.29 (1H, s), 3.26-3.31 (2H, m), 2.47 (3H, s), 2.28 (2H, tt, *J*=7.8,  
41  
42 7.4 Hz), 1.25 (3H, d, *J*=6.3 Hz). <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, 126 MHz) δ (ppm) 164.6, 162.7, 159.9, 158.8,  
43  
44 153.6, 148.7, 146.5, 142.2, 141.7, 141.4, 136.3, 135.9, 133.5, 113.3, 113.0, 111.9, 74.9, 73.0, 58.5, 54.1,  
45  
46 48.7, 20.4, 16.4, 16.1. HRMS elemental calculated for C<sub>24</sub>H<sub>27</sub>N<sub>6</sub>O<sub>5</sub> (M+H<sup>+</sup>): 479.2043; found:  
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48 479.2051.  
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4 **Recrystallization of AZD1656 (1).** A supersaturated solution of **AZD1656 (1)** (100 kg, 1 eq.) and  
5 MIBK (670 L), that had been pre-screened at 70 °C, was seeded at 45 °C with a micronized (surface  
6 area = 3.3 m<sup>2</sup>/g) sample of **AZD1656 (1)** (Form VI, 1.75 kg, 1.75% wt/wt). After being aged for 3 h, the  
7 batch was cooled at 0.1 °C/min to 0 °C,<sup>38</sup> where it was isolated by filtration after being held for a further  
8 3 h.<sup>39</sup> The cake was sequentially washed with a chilled (0 °C) mixture of MIBK and heptane (200 L of  
9 1:2 v/v) and then heptane (200 L), before being dried under vacuum at 60 °C. This yielded **AZD1656**  
10 **(1)** (Form VI, 83.3 kg, 83.3%) as a white solid.  
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## 21 ASSOCIATED CONTENT

22  
23 Supporting information available: <sup>1</sup>H NMR spectra, <sup>13</sup>C NMR spectra, infrared spectra and DSC traces  
24 for ester **27**, ether **29**, phenol **21**, acid **12** and **AZD1656 (1)**.  
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## 30 AUTHOR INFORMATION

### 31 Corresponding Author

32 E-mail: Alan.Steven@astrazeneca.com

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34 ORCID Alan Steven: 0000-0002-0134-0918  
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### 38 Notes

39 The authors declare no competing financial interest.  
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44 We are grateful to Dottikon Exclusive Synthesis for performing the manufacture of acid **2**.  
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18 soluble derivative, which could be partitioned away from **20** in an aqueous workup.  
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21 11. A two step tosylation-etherification sequence proceeded with complete inversion of  
22  
23 stereochemistry with a variety of  $\alpha$ -resorcylate derivatives over the course of the project, with no  
24  
25 detectable erosion in the integrity of the stereogenic center.  
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29 12.  $pK_a$  DB in ACD/Spectrus software, ACD Labs, 2015 Pack 2.  
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31  
32 13. Whilst the amount of bisether **26** present in the batch generated as part of the first development  
33  
34 manufacture was not recorded, a laboratory run where it was present at 6.5 LCAP at the end of the  
35  
36 reaction provides some idea of the level likely to have been present.  
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38  
39 14. Brief attempts to monofunctionalize using a biotransformation were also made. A range of  
40  
41 hydrolases were screened using vinyl acetate, butanoate, laurate, stearate and benzoate as acyl donors  
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45 to completion.  
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24 33. A low equilibrium concentration of molecules displaying the conformation of Form VI was  
25  
26 provisionally used to explain why its crystals grew much more slowly than the metastable polymorph  
27  
28 ('Form I').  
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30  
31 34. In order to afford a homogeneous solution and to mitigate the risk of precipitation of insoluble  
32  
33 lithium carbonate, the alkaline solutions used in this benzylation reaction were prepared by mixing  
34  
35 separate aqueous solutions of lithium hydroxide and potassium carbonate, shortly before their use, in  
36  
37 order to give a solution with the solute concentrations indicated.  
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40  
41 35. This step serves to hydrolyse an ester impurity **32**.  
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43  
44 36. This reverse addition limits the formation of impurity **38** formed by the *O*-acylation of the  
45  
46 newly-installed amide of **AZD1656 (1)**.  
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48  
49 37. Unnecessary delay should be avoided during the preceding wash and this back-extraction in  
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51 order to avoid the acid-mediated degradation of **AZD1656 (1)**.  
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4 38. The entrainment of MIBK in occlusions was a problem with this crystallization. Although  
5  
6 temperature cycling could be used such that the MIBK content could be reduced to below 0.5% wt/wt  
7  
8 after drying, it damaged the agglomerates of API and hindered their filtration and was superceded by  
9  
10 carefully controlled cooling.

11  
12  
13 39. The polymorph was checked by XRPD prior to isolation. In the event that the undesired Form I  
14  
15 was present, the slurry was recrystallized after heating to 50 °C.  
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