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Title: Characterization and reactivity of γ -Al₂O₃ supported Pd-Cu bimetallic nanocatalysts for the selective oxygenization of cyclopentene



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Author: Wei-Wei Liu Yi-Si Feng Guang-Yu Wang Wei-Wei Jiang Hua-Jian Xu

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Graphical Abstract

Characterization and reactivity of γ-Al₂O₃ supported Pd-Cu bimetallic nanocatalysts for the selective oxygenization of cyclopentene

Wei-Wei Liu^a, Yi-Si Feng^{a,b,c*}, Guang-Yu Wang^a, Wei-Wei Jiang^a, Hua-Jian Xu^{a*}

^a School of Chemistry and Chemical Engineering, School of Medical Engineering, Hefei University of Technology, Hefei 230009, China

^b Anhui Key Laboratory of Controllable Chemical Reaction & Material Chemical Engineering, Hefei 230009, China

^c Anhui Provincial Laboratory of Heterocyclic Chemistry, Maanshan 243110, China

$$+ O_2 (1 \text{ MPa}) \xrightarrow{\text{Pd-Cu}(5:1)/\gamma - \text{Al}_2O_3} O Conv. > 85\%, \text{Sele.} > 95\%$$

A series of γ -Al₂O₃ supported Pd-Cu bimetallic nanocatalysts are investigated for the selective oxygenization of cyclopentene to cyclopentanone.

Original article **Characterization and reactivity of** γ-Al₂O₃ supported Pd-Cu bimetallic nanocatalysts for the selective oxygenization of cyclopentene

Wei-Wei Liu^a, Yi-Si Feng^{a,b,c*}, Guang-Yu Wang^a, Wei-Wei Jiang^a, Hua-Jian Xu^{a*}

^aSchool of Chemistry and Chemical Engineering, School of Medical Engineering, Hefei University of Technology, Hefei 230009, China ^bAnhui Key Laboratory of Controllable Chemical Reaction & Material Chemical Engineering, Hefei 230009, China ^cAnhui Provincial Laboratory of Heterocyclic Chemistry, Maanshan 243110, China

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ABSTRACT

Article history: Received 16 December 2015 Received in revised form 29 January 2016 Accepted 25 February 2016 Available online	In this work, $Pd-Cu/\gamma-Al_2O_3$ is prepared by the impregnation method and investigated for selective oxygenization of cyclopentene to cyclopentanone. A series of bimetallic $Pd-Cu/\gamma-Al_2O_3$ nanocatalysts were prepared and the structures characterized by XRD, XPS and TEM. We determined that the					
Keywords: Impregnation method, Oxygenization, Cyclopentanone, Cyclopentene, Pd-Cu /y-Al ₂ O ₃ .	obtained Pd-Cu/ γ -Al ₂ O ₃ (molar ratio Pd:Cu = 5:1) was an efficient catalyst for the oxygenization of cyclopentene to cyclopentanone with >95% selectivity and >85% conversion (100° C, 1 MPa initial O ₂ pressure, 7 h).					

1. Introduction

Cyclopentanone is an important fine chemical intermediate for the preparation of new spices, a variety of antiinflammatory, anti-cancer drugs, pesticides and herbicides [1]. Currently, the main method of preparation of cyclopentanone in industrialized production is by intramolecular decarboxylation of adipic acid at high temperature with barium hydroxide as catalyst. But this method has disadvantages due to the shortage and high cost of raw materials, and is not in conformity with green chemistry principles. With the rapid development of the petrochemical industry, cyclopentene is abundant and the method to synthesize cyclopentanone *via* cyclopentene has received wide attention. The early literature reported that cyclopentene was oxidized by N₂O with high yield and the absence of a catalyst. But there were shortcomings, for example, the reaction pressure and temperature were high, N₂O damaged the equipment and caused environmental pollution [2]. Takehira and others used homogeneous catalyst PdCl₂-CuCl₂, PdCl₂-FeCl₃ to catalyze the oxygenization of cyclopentene to generate cyclopentanone, however, this method had a low conversion rate and the reusability of catalyst was unsatisfactory [3, 4].

According to the mechanism of oxygenization of cyclopentene to cyclopentanone, a solid catalyst consisting of metal would be useful for this reaction. Due to good mechanical strength and thermal stability, γ -Al₂O₃ has been widely applied as the carrier in industry. According to literature, Pd is active to the fracture of C=C and shows good selectivity in the catalytic oxygenization of cyclopentene, but has relatively low catalytic efficiency. Nickel and copper are non-noble metals with great catalytic ability. In the study of the Wacker method to synthesize cyclopentanone, PdCl₂/CuCl₂ performed good catalytic activity [3, 4], consequently we speculated that Cu may be beneficial in the synthesis of C=O. Mao used Pd-Cu bimetallic catalysts for the oxygenization of styrene, showed good catalytic ability and selectivity [5]. Therefore, in our study, Pd-Cu/ γ -Al₂O₃ was chosen as the catalyst to oxidize cyclopentene.

The aim of this paper is to report the preparation, characterization and catalytic performance of $Pd-Cu/\gamma-Al_2O_3$ (with difference mole ratios of Pd:Cu). Moreover, the parameters influencing the reaction of cyclopentene to cyclopentanone are intensely studied.

2. Experimental

Preparation of Pd-Cu/ γ -Al₂O₃ catalysts: The Pd-Cu/ γ -Al₂O₃ catalysts were prepared by the impregnation method [6-10]. In a typical Pd-Cu (5:1)/ γ -Al₂O₃ catalyst synthesis process, PdCl₂ (131.9 mg, 0.75 mmol) and CuCl₂·2H₂O (25.1 mg, 0.15 mmol) were dissolved in 10 mL acetic acid solutions (0.0225 mol/L) with constant agitation (500 rpm/min) at r.t. To this clear solution, then was slowly added γ -Al₂O₃ (1.5 g) and uniformly stirred at 300 rpm/min for 5 h. After impregnated, the solution was heated at 100 °C for removal of the redundant H₂O, forming a sticky substance which was dried in vacuum oven at 80 °C for 12 h. Subsequently, the resulting catalytic forerunners were ground to powders and calcined in nitrogen (0.3 L/min) heating from

* Corresponding author.

E-mail address: hjxu@hfut.edu.cn

r.t.to 500 °C at a rate of 5 °C/min, then kept at 500 °C for 4 h. Subsequently, the sample precursors were reduced by hydrogen (0.15 L/min) in the nitrogen at 500 °C for 2 h. Finally, the Pd-Cu $(5:1)/\gamma$ -Al₂O₃ catalyst was obtained. In order to research the effect of the loading of metals, different catalysts of Pd/Cu mole ratios were synthesized for use in the oxygenization reaction.

Characterization: The XRD of different samples were recorded on a Rigaku D/MAX 2500 (V) Diffractometer with Cu K α radiation and scanned at a rate of 10°/min over the range 20°~90°. The XPS analysis was confirmed on Thermo Fisher Scientific ESCALAB 250 using a monochromatic Al K $_{\alpha}$ gun with photonic energy of 1486.6 eV as the X-ray source under reduced vacuum conditions. The binding energies (B.E.) acquired in the XPS analysis were compensated by using the adventitious C 1s 284.6 eV signal for any charging effects. The TEM images of catalysts were obtained on a JEOL JEM-2100F Electron Microscope equipped with EDS at an accelerating voltage of 120 kV. Samples were prepared by ultrasonic dispersion in ethanol and deposited on a copper grid for analysis.

Catalytic reaction: In a typical procedure, 15 mL cyclopentene (0.17 mol), 60 mL ethyl alcohol (1.03 mol) and Pd-Cu $(5:1)/\gamma$ -Al₂O₃ catalyst (0.24 g, 2.0 wt% of cyclopentene) were added into 0.1 L closed autoclave. The mixture was stirred (400 rpm/min) under 1.0 MPa oxygen pressure at 100 °C for 7 h. Specific parameters are provided in Supporting Information.

3. Results and discussion

3.1. Characterization of catalysts

3.1.1. X-ray diffraction

The XRD patterns of Pd/ γ -Al₂O₃, Cu/ γ -Al₂O₃ and diverse Pd-Cu/ γ -Al₂O₃ catalysts are exhibited in Fig. 1. The results show a low intensity level for all characteristic diffraction planes, except for the planes associated with the γ -Al₂O₃ support [10]. For γ -Al₂O₃, four apparent signals (Fig. 1A) at $2\theta = 19.6^{\circ}$, 21.2°, 27.5°, 57.2° were detected, corresponding to the (110), (102), (211) and (305) facets (JCPDS 50-1496), respectively [11]. Shown in Fig. 1B is the XRD patterns of Cu/ γ -Al₂O₃ catalysts with apparent signals at $2\theta = 43.3^{\circ}$ and 74.1° corresponding to the (111) and (220) facets (JCPDS 04-0836). In Fig. 1C, there are four signals at $2\theta = 27.3^{\circ}$ (PdO, JCPDS 50-1496) and 40.1°, 46.7°, 68.2° (Pd, JCPDS 46-1043) and the Cu peak found at $2\theta = 43.3^{\circ}$ facets (JCPDS 04-0836). Three apparent signals at $2\theta = 30.580^{\circ}$, 35.121° and 63.106° facets (JCPDS 48-0587) are due to Pd-Cu bimetallic alloys peaks (Fig. 1C, D, E). The XRD spectra of Pd-Cu/ γ -Al₂O₃ with different mole ratios of Pd/Cu show that the diffraction peaks became wider and the positions of the diffraction peaks were shifted to lower angle with the addition of Pd content. Shifting to lower angle is probably due to the formation of a nano-alloy and the wider diffraction signal indicated that the crystal grain became smaller and the Pd content would be helpful into the reduction of Cu. No signals of the Pd species could be observed in the XRD spectra of Pd-Cu/ γ -Al₂O₃, which may be attributed to the good dispersion of Pd [12]. In addition, the calculative results indicated that the size of Pd-Cu crystalline grain was around 13.4, 15.1 and 16.3 nm by the Scherrer formula. In conclusion, we need further data to confirm the presence of hypothetical Pd-Cu bimetallic nanoparticles in catalysts by XPS and TEM analysis.

3.1.2. X-ray photoelectron spectroscopy

The Pd-Cu/ γ -Al₂O₃ XPS spectra of different Pd-Cu molar ratios are shown in Fig. 2. The results show that there were two oxygenization states in XPS Cu 2p spectra. The binding energies in Fig. 2. centered at 953.1 eV (2p_{1/2}) and 932.7 eV (2p_{3/2}) were attributed to Cu⁰ and Cu¹ [13]. The differences of Cu⁰ and Cu¹ were not obvious at the 2p signals because the binding energy only exhibit 0.1 eV differences [14]. The Cu⁰ and Cu¹ species, usually appear below 933 eV and Cu^{II} typically appears with binding energies higher than 933 eV. The XPS spectra of Cu/ γ -Al₂O₃ showed that oxidized Cu^{II} existed, which was indicated by both second sets of spin-orbit split peaks shifted by 1.3±0.2 eV to higher binding energy. It could be observed that the satellite peak at 942 eV for Cu^{II} which became weaker with the addition of Pd and might indicate that Cu^{II} transforms to Cu^I/Cu from the XPS spectra of the Pd-Cu/ γ -Al₂O₃ [12].

In Fig. 3, the Pd $3d_{5/2}$ appeared at 335 ± 0.1 and 336.1 ± 0.1 eV in all the catalysts, which correspond to Pd⁰ and Pd^{II}, respectively [15, 6]. The Pd primary state in the Pd/ γ -Al₂O₃ catalyst was Pd⁰ and Pd^{II}, while Pd⁰ was the main valence state in diverse Pd-Cu/ γ -Al₂O₃ samples. In Fig.3, the peaks of Pd^{II} were shifted to weaker B.E. with added Cu, which might indicate that Pd^{II} transformed into Pd⁰ [6, 16].

Furthermore, the surface atom percentages of Pd and Cu shown in Table 1 did not correspond to the preparation. According to the XPS spectra, the metals were introduced into the core of γ -Al₂O₃, or covered by the visible metal. The above results illustrated that appropriate ratio (1:1) of the surface atom percentages of Pd and Cu led to the simultaneous distribution of the two metals on the surface of the catalysts [8, 17].

3.1.3. Transmission electron microscopy

The microstructure of Pd-Cu(5:1)/ γ -Al₂O₃ catalyst was observed by TEM. Fig. 4A and B exhibited that similar spherical particles are well-dispersed on support and clearly show that the metal particles average size was about 10 nm. Electron mapping image analysis (Fig. 4C and D) showed the distribution of oxygen (O), aluminum (Al), copper (Cu) and palladium (Pd) atoms indicated with red, green, blue and white colors, respectively, further confirmed the homogeneous distribution of Pd-Cu bimetallic nanoparticles on the surface of the γ -Al₂O₃ support.

3.2. Activity measurements

The catalytic performance of catalysts was measured for selective oxygenization of cyclopentene under different conditions (Table 2). The results showed that all catalysts had the ability of catalytic oxygenization except for Cu/γ -Al₂O₃, which illustrated palladium is an essential composition of catalysts. Meanwhile, Pd-Cu(5:1)/ γ -Al₂O₃ catalyst exhibited the best catalytic ability during the reaction. Compared with Pd-Cu(5:1)/y-Al₂O₃, the catalytic activity of Pd-Cu(3:1)/y-Al₂O₃ and Pd-Cu(7:1)/y-Al₂O₃ was slightly lower. It was apparent that appropriate proportion of Pd and Cu of Pd-Cu/y-Al₂O₃ played an important role in oxygenization of cyclopentene. According to the XPS data of catalysts in Table 1 and Table 2, the Pd-Cu/y-Al2O3 (5:1) catalyst showed the highest activity with 88% conversion of cyclopentene and it could be speculated that the surface atom percentage of Pd and Cu was close to 1:1. The inferior catalytic activity of the Pd/y-Al₂O₃ sample was probably due to that plentiful PdO (according to XPS measurement) dispersed on the surface of catalyst. In addition, the catalytic activity of mixed-(Pd/ γ -Al₂O₃ + $Cu/\gamma-Al_2O_3$) was not as good as the Pd-Cu/ $\gamma-Al_2O_3$ catalyst, which illustrated that the Pd-Cu bimetal was the crucial factor in the oxygenization of cyclopentene. Simultaneously, the XPS and TEM measurements for Pd-Cu(5:1)/y-Al₂O₃ catalyst demonstrated the homogeneous distribution of Pd-Cu bimetallic nanoparticles on the sample surface. We suggest that the above reasons led to Pd-Cu(5:1)/ γ -Al₂O₃ showing the best catalytic performance. The temperature, pressure, speed (rate) and amounts of catalyst were all factors in the selective oxygenization reaction. With the changing of these factors, catalytic results were also transformed. When the values of those factors were neither too high nor too low, an optimal condition was produced. Subsequently, the impact of solvents such as 1,2-dichloroethane, ethanol, and methanol) were also studied for the reaction and we ascertained ethanol as the solvent, and 100 °C, 1 Mpa oxygen pressure, 400 rpm/min and Pd-Cu(5:1)/γ-Al₂O₃ catalyst (2.0 wt% of cyclopentene) were the optimal reaction conditions.

4. Conclusion

In conclusion, we developed the γ -Al₂O₃ supported mono- (Cu and Pd), mixed- (Pd + Cu) and bi-metallic Pd-Cu catalysts for the oxygenization reaction of cyclopentene to cyclopentanone. The best results showed that the selective conversion of cyclopentene to cyclopentanone could be simultaneously up to more than 85% by employing Pd-Cu(5:1)/ γ -Al₂O₃ catalyst under mild reaction conditions. The excellent performance of Pd-Cu(5:1)/ γ -Al₂O₃ catalyst was attributed to the homogeneous distribution of Pd-Cu bimetallic nanoparticles on the surface of support. Our protocol provides a potential method of producing cyclopentanone in commercial production.

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 $Figure \ 1. \ XRD \ patterns \ of \ (A) \ \gamma - Al_2O_3 \ (JCPDS \ 50-1496), (B) \ Cu/\gamma - Al_2O_3, (C) \ Pd/\gamma - Al_2O_3, (D) \ Pd: Cu = 3:1, (E) \ Pd: Cu = 5:1, (F) \ Pd: Cu = 7:1, (F) \$

Figure 2. XPS spectra of all catalysts. (A) Pd:Cu =3:1, (B) Pd:Cu =5:1, (C) Pd:Cu =7:1, (D) Cu



Figure 3. (A) Pd 3d peaks of Pd, (B) Pd:Cu =3:1,(C) Pd:Cu =5:1, (D) Pd:Cu =7:1



Figure 4. (A) and (B) TEM images of Pd-Cu/y-Al₂O₃=5:1, (C) and (D) electron mapping images

Table 1. XPS data of catalysts

Table 1. XPS data of catalysts				
Catalyst	Binding energy (eV)		Pd:Cu (atom%) ^a	
	Pd 3d _{5/2}	Cu 2p _{3/2}		
Pd	336.1	—	—	
Pd:Cu -3:1	335.4	852.2	0.43:0.56	
Pd:Cu -5:1	335.2	852.5	0.47:0.52	
Pd:Cu -7:1	335.4	852.1	0.55:0.44	
Cu	_	855.5	—	

^a The proportion of atomic percentage of Pd and Cu

Table 2. The Oxygenization of cyclopentene $Pd:Cu (x:y)\gamma-Al_2O_3$

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cyclopentene		cyclopen	tanone			
Entry	Catalyst	Solvent	Temp. (°C)	Time (h)	Conv. (%)	Sele. (%)
1	Pd	Ethanol	100	7	71	>95
2	Pd:Cu = 3:1	Ethanol	100	7	80	>95
3	Pd:Cu = 7:1	Ethanol	100	7	83	>95
4	Pd:Cu = 5:1	Ethanol	100	7	88	>95
5 ^b	Pd:Cu = 5:1	Methanol	100	7	67	>95
6 ^c	Pd:Cu = 5:1	1,2-Dichloroethane	100	7	—	—
7	Pd:Cu = 5:1	Ethanol	120	6	81	>95
8	Pd:Cu = 5:1	Ethanol	150	4	67	>90
9	Pd:Cu = 5:1	Ethanol	80	10	80	>95

10 ^d	Pd:Cu = 5:1	Ethanol	100	7	55	>95	
11 ^e	Pd:Cu = 5:1	Ethanol	100	7	85	>95	
$12^{\rm f}$	Pd:Cu = 5:1	Ethanol	100	7	80	>95	
13 ^g	Pd:Cu = 5:1	Ethanol	100	7	79	>95	
14^{h}	Pd+Cu	Ethanol	100	7	55	>95	
15	Cu	Ethanol	100	7	—		
16 ⁱ	Pd:Cu = 5:1	Ethanol	100	7	75	>95	
17 ^j	Pd: Cu =5:1	Ethanol	100	7	77	>95	

Reaction conditions: 0.17 mol cyclopentene, 1.03 mol ethanol, 400 rpm/min, catalyst (0.24 g, 2.0 wt% of cyclopentene) and 1.0 MPa oxygen

pressure. ^a Reaction rate= $\Delta c/\Delta t$, $\Delta c=c_{cyclopentene}$ (before reaction) - $c_{cyclopentene}$ (after reaction), Δt =reaction time (from Table 2); ^b 1.03 mol methanol; ^c 1.03 mol 1,2-dichloroethane; ^d 0.5 MPa oxygen pressure; ^e 1.5 MPa oxygen pressure; ^f 0.18 g 5:1 catalyst (1.5 wt% of cyclopentene); ^g 0. 30 g 5:1 catalyst (2.5 wt% of cyclopentene); ^h Mixture of 0.16 g Pd/Al₂O₃ and 0.16 g Cu/Al₂O₃; ¹ 300 rpm/min.