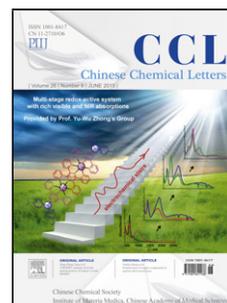


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Communication

Partially biobased polymers: The synthesis of polysilylethers *via* dehydrocoupling catalyzed by an anionic iridium complexXiao-Yong Zhai,^{a,b} Xiao-Qing Wang,^a Yi-Xuan Ding,^a Yong-Gui Zhou^{a,*}^a State Key Laboratory of Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, China^b University of Chinese Academy of Sciences, Beijing 100049, China

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Graphical abstract



Partially biobased polysilylethers (PSEs) are synthesized *via* dehydrocoupling polymerization catalyzed by an anionic iridium complex. Moderate to high yields of polymers with number-average molecular weights (M_n) up to 4.38×10^4 were obtained.

Partially biobased polysilylethers (PSEs) are synthesized *via* dehydrocoupling polymerization catalyzed by an anionic iridium complex. Different types (AB type or AA and BB type) of monomers are suitable. Levulinic acid (LA) and succinic acid (SA) have been ranked within the top 10 chemicals derived from biomass. BB type monomers (diols) derived from LA and SA have been applied to the synthesis of PSEs. The polymerization reactions employ an air-stable anionic iridium complex bearing a functional bipyridonate ligand as catalyst. Moderate to high yields of polymers with number-average molecular weights (M_n) up to 4.38×10^4 were obtained. A possible catalytic cycle *via* an Ir-H species is presented. Based on the results of kinetic experiments, apparent activation energy of polymerization in the temperature range of 0-10 °C is about 38.6 kJ/mol. The PSEs synthesized from AA and BB type monomers possess good thermal stability ($T_5 = 418$ °C to 437 °C) and low glass-transition temperature ($T_g = -49.6$ °C).

Keywords: Biodegradable polymers; Polysilylethers; Iridium catalysis; Dehydrocoupling polymerization; Levulinic acid

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Due to the programmed depletion of fossil resources, nonrenewable and nondegradable synthetic polymers produced from fossil resources pose a serious threat to the ecosystem [1, 2]. It is beneficial to develop polymeric materials sourced from renewable feedstocks [3-8]. Although a number of groups have studied the use of renewable resources-based monomers for the synthesis of polymeric materials [9-10]. The total volume of polymeric materials synthesized from nonrenewable fossil fuel resources far outweighs that from renewable biomass [11, 12]. The main reason is largely due to the renewable polymeric materials possess high cost and inferior performance compared with polymers produced from petroleum chemicals [13, 14].

Great efforts have been spent on the developing novel and promising renewable feedstocks, and applying these compounds to the synthesis of biopolymers, bioresins, and various value-added chemicals [15-18]. Some of the widely studied renewable feedstocks are: lactic acid, triglycerides fatty acids, 5-hydroxymethylfurfural [19] or its derivatives [20, 21], and vanillin. So far, several polymers based on these feedstocks have been developed, including the poly(lactic acid) [22], polyvanillin [23, 24], poly(hydroxylalkanoate)s, etc. In 2004, the concept of "Top Value Added Chemicals from Biomass" was proposed by the US Department of Energy (DOE), which pointed to clear direction for development of renewable polymeric materials [25, 26].

Among these renewable polymers, PSEs are an important class of polymers with unique and significant properties, for instance, low T_g , good thermal stability, biocompatibility and high gas permeability [27, 28]. These polymers have been applied in many fields, such as high-temperature elastomers [29-31], conductive polymeric materials [32] and chiral column packing materials [33]. As a promising degradable material, PSEs has been studied for decades. Dehydrocoupling polymerization is one of the most important methods to access PSEs [34]. Different types of monomers have been applied to the synthesis of PSEs [27, 35]. The most commonly used monomers are AA type monomers (dihydroxyl compound) and BB type monomers (silanes). Various dihydroxyl compounds are suitable substrates for the synthesis of PSEs, including diols [36], diphenols [37], water [38] and disilanolols [39]. However, most of PSEs are derived from nonrenewable feedstocks, which is the key obstacle to its sustainable development. After analyzing functional group structure of the top 10 chemicals derived from biomass, we found that more than half of these compounds can be transformed to

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diols *via* single reduction step with high yields, including succinic acid, 2-hydroxymethyl-5-furfural (HMF), levulinic acid, etc [40]. These chemicals can be transformed to 1,4-butanediol, 2,5-furandimethanol, 1,4-pentanediol, etc respectively. Driven by these considerations, we envisaged that applying these diols derived from biomass to the synthesis of PSEs.

To our knowledge, HMF based PSEs have been reported [41]. However, monomers derived from levulinic acid have not been applied to the synthesis of PSEs *via* dehydrocoupling. As an effective and highly atom-economic method to construct Si-O bond, dehydrocoupling reaction have been catalyzed by transition metal complexes such as palladium [36-38, 42], platinum [38], rhodium [37, 43-45] and manganese [41, 46-47]. Recently, we reported the synthesis of degradable PSEs from AB-type silyl alcohol monomers catalyzed by homogeneous iridium(I) complexes bearing a bisphosphine ligand [48]. Combining our interests in exploring the application of catalytic system based on iridium in dehydrogenative coupling reaction, herein, we reported an anionic iridium complex catalyzed differ-ent types (AB type or AA and BB type) of monomers to give high-molecular-weight PSEs (Scheme 1).

1,4-Bis(dimethylsilyl)benzene was obtained from Energy Chemical (Shanghai, China) and distilled from calcium hydride. 1,4-Butanediol was purchased from Aladdin Reagent Co., Ltd. (Shanghai, China) and dried by azeotropic distillation of toluene and ethanol. 1,10-Decanediol was purchased from J&K Scientific Ltd. (Beijing, China) and recrystallized from ethyl acetate. Other commercially available reagents were used without further purification. Solvents were treated prior to use according to the standard methods.

To an oven-dried 25 mL resealable Schlenk flask equipped with a magnetic stir bar was charged Ir Cat (2.8 mg, 0.005 mmol) and acetonitrile (1.5 mL) under nitrogen. The solution was stirred at room temperature for 2 min. For AB type monomers, monomer **1a-1e** (0.5 mmol) was added; for AA and BB type monomers, 1,4-bis(dimethylsilyl)benzene (0.5 mmol) and diols **1f-1h** (0.5 mmol) were added. The flask was heated at 70 °C for 24 h under nitrogen (connected to a nitrogen Schlenk line). During the last 6 h of the reaction time, H₂ produced during the reaction was replaced with nitrogen every 2 h. After the polymerization, the reaction mixture was cooled to room temperature, and the content was purified by the precipitation method.

All of the polymers are soluble in dichloromethane (DCM) and insoluble in methanol (MeOH). So, these two solvents were used in the precipitation process. The reaction mixture was first homogenized by the addition of as low as possible amount of DCM (1-2 mL), then cold MeOH was added portionwise (15-20 mL) until it turned to a biphasic mixture. The top layer was taken out, and the bottom viscous/solid layer was washed with MeOH two times until it gave a white/light yellow color viscous/solid polymer. The resulting polymer was dried to a constant weight and characterized by ¹H NMR, ¹³C NMR, GPC, TG and DSC.

(4-(3-(Dimethylsilyl)propoxy)-phenyl)methanol (**1a**) was chosen as the model monomer to conduct the condition optimization. The results were depicted in Table 1. According to the conditions in our previous work [23], the reaction was performed under neat condition at 80 °C. However, only middle-*M_n* polymer was obtained (entry 1). In order to improve the *M_n* and *D* of the product, the effects of solvent were conducted. Use tetrahydrofuran (THF) or toluene as solvent led to low-*M_n* polymers (entries 2 and 3). Reactions carried out in 1,4-dioxane resulted in no product, suggesting that the coordination ability of cyclic ethers might be the main reason for the low-*M_n* observed with THF (entries 3 and 4). Then, acetonitrile (CH₃CN) was used as solvent; a high-molecular-weight polymer with *M_n* of 14600 was obtained (entry 5). Afterwards, the effects of reaction temperature were performed carefully. Rising temperature led to polymers with lower *M_n* and broader *D* (entries 6-8). However, lowering the temperature to 60 °C resulted in apparent decrease of yield with slightly rising of *M_n* (entry 10). When reaction temperature was lowered to 70 °C, a high molecular weight polymer with narrow *D* was obtained albeit with slightly lower yield (entry 9).

Next, the effects of catalyst loading, CH₃CN loading and reaction time were conducted. The results were depicted in Table 2. Increasing or reducing catalyst loading resulted in apparent decrease of PSEs yields (entries 11 and 12). When solvent loading was added to 3.00 mL, polymer with broader *D* was obtained (entry 13). In order to achieving high *M_n* and narrow *D*, the solvent was reduced to 0.75 mL (entry 14). However, *M_n* of polymer dropped apparently. When reaction time was prolonged to 48 h and 72 h, polymers with high *M_n* were given, nevertheless, the yields of PSEs dropped to 50% and 41%, respectively (entries 15 and 16). Therefore, the optimal reaction conditions were finally established as: cat. (1 mol%)/CH₃CN (1.5 mL)/70 °C/24 h.

With the optimal reaction conditions in hand, the scope and generality of the dehydrocoupling polymerization were next evaluated (Table 2). In the first instance, four AB-type silyl alcohol monomers were examined. Gratifyingly, all the substrates afforded high molecular weight and moderate to high yields (entries 1-5). Furthermore, these polymers were obtained with similar *D* (around 1.80 *D* values).

For the AA and BB type monomers, dehydrocoupling polymerization can also proceeded smoothly (Table 4). We used a commercially available hydrosilane (1,4-bis(dimethyl-silyl)benzene) as AA type monomer. Three diols derived from biomass were chosen as BB type monomers, including 1,4-pentanediol (**1f**), 1,4-butanediol (**1g**) and 1,10-decanediol (**1h**). Among these diols, monomer **1f** and **1g** were derived from levulinic acid (LA) and succinic acid (SA) independently [25, 26]. When these two diols were applied to the dehydrocoupling polymerization, PSEs **2f** and **2g** were obtained with high *M_n* and moderate yields (entries 1 and 2). Monomer **1h** was derived from sebacic acid, a principal component of castor oil [49]. When **1h** was used, a high-molecular-weight polymer with *M_n* of 43800 was obtained (entry 3).

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To further demonstrate the utility of our methodology, a gram scale reaction was conducted, as shown in Scheme S4 (Supporting information). When monomer **3** (3 mmol) and **1h** (3 mmol) were used, a polymer with M_n of 32400 was provided in 87% yield. The M_n was slightly lower than that of the polymerization on small scale. Moreover, pre-polymerization step was also tried, as shown in Scheme S5 (Supporting information). When monomer **3** and **1h** were used in the ratio of 1:1.2, both ends of the product **2j** ($M_n = 11400$, $D = 1.45$) should be terminated by OH groups. When the ratio was 1.2:1, both ends of the product **2k** ($M_n = 6900$, $D = 1.60$) should be terminated by SiH groups. The further polymerization employed prepolymers **2j** and **2k**, providing polymer **2l** with higher M_n (yield = 51%, $M_n = 17800$).

After purification by precipitation, the PSEs produced by the Ir-catalyzed dehydrocoupling polymerization were, in general, colorless/faint yellow, viscous oils/soft solids, depending on the molar mass and backbones of polymers. Thermal properties of polymers **2f** and **2h** were investigated under nitrogen atmosphere using TGA and DSC, as shown in Figs. S23-S26 (Supporting information). For polymers **2f** and **2h**, T_{50} values were kept at around 490 °C, which indicated these polymers exhibit good thermal stability. However, the T_5 value of **2h** was higher than **2f**. For polymer **2f**, low glass transition temperatures (-49.6 °C) could be detected. Polymer **2h** exhibited indiscernible glass transition *via* DSC.

To investigate the mechanism, experiments about the generation of Ir-H species and its application in dehydrocoupling polymerization were conducted, as shown in Schemes S6 and S7 (Supporting information). Firstly, the reaction of catalyst and 1,1,3,3-tetra-methyldisiloxane was conducted. The Ir-H species was detected with almost 50% NMR yield [50]. Then, we applied this mixture to the dehydrocoupling of monomer **1a**. A high- M_n polymer was obtained ($M_n = 16700$, yield = 68%). The M_n and yield of PSEs were similar to the aforementioned result under optimal reaction conditions ($M_n = 14900$, yield = 67%). This result indicated the generation of Ir-H species may occur during the polymerization. Then, a polymerization process under room temperature was conducted. After 6 hours, an orange-red flocculent precipitate was observed. NMR spectrum of this orange-red precipitate indicated that part of the catalyst was transformed to Ir-H species. These results strongly suggested the involvement of Ir-H species in the catalytic cycle.

Based on these results and early studies [50], a plausible mechanism was proposed for the iridium-catalyzed dehydrocoupling polymerization, as shown in Scheme S8 (Supporting information). Firstly, Ir-H species **B** is formed *via* hydrolysis reaction of hydrosilane with iridium catalyst **A**. Then, Ir-H species **B** undergoes σ bond metathesis with diols to give intermediate **C** accompanied by evolution of hydrogen. Finally, intermediate **C** reacts with silane to furnish the dehydrocoupling product and regenerates Ir-H species **B** to complete the catalytic cycle.

As shown in Figs. S3-S6 (Supporting information), the kinetics of polymerization under 10 °C and 0 °C was performed. At 10 °C, the reaction conversion (x) increased quickly. Even under 0 °C, reaction conversion reached 27% within 3 h 10 min. According to these time courses at different temperatures, the relation between $\ln[1/(1-x)]$ and reaction time is found to be in linear. And the calculated reaction rate constants are 0.1051 h⁻¹ and 0.1915 h⁻¹ at 0 °C and 10 °C, respectively. According to these data, the calculated apparent activation energy of polymerization in the temperature range of 0-10 °C is about 38.6 kJ/mol.

In conclusion, we have demonstrated that an anionic iridium complex can effectively catalyze dehydrocoupling polymerization. Various PSEs were synthesized from different types (AB type or AA and BB type) of monomers. Importantly, monomers **1e-1h** were derived from renewable feedstocks, including rincinoic acid, levulinic acid (LA), succinic acid (SA) and sebacic acid. A plausible mechanism *via* an Ir-H species for the polymerization is presented. The results of kinetic experiments indicated that the apparent activation energy in the temperature range of 0-10 °C is about 38.6 kJ/mol. Further work will focus on the synthesis of optically active PSEs.

Acknowledgment

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Appendix A. Supplementary data

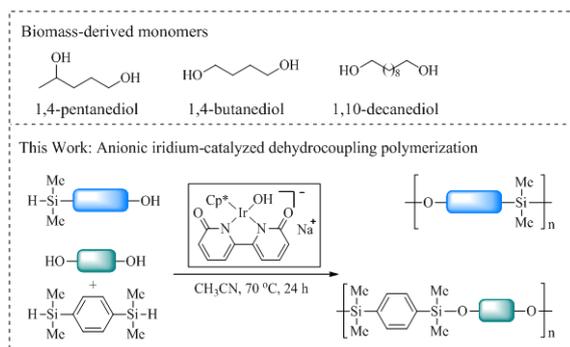
Supplementary material related to this article can be found, in the online version, at doi:

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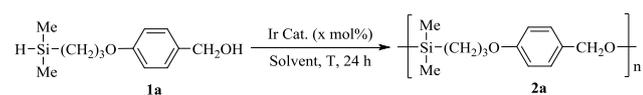
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Scheme 1. Catalytic dehydrocoupling polymerization for the synthesis of partially biobased PSEs.

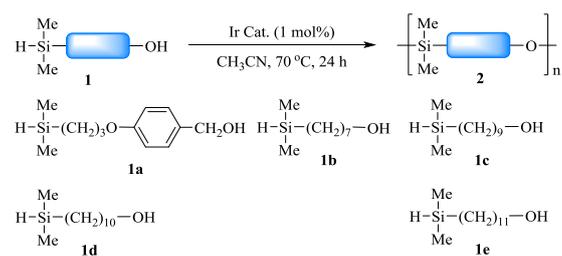
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Table 1. Condition optimization.^a

Entry	x	T (°C)	Solvent	M_n^b	\bar{D}^b	Yield (%) ^c
1	1.0	80	Neat	6800	1.75	73
2	1.0	80	Toluene	4600	1.63	54
3	1.0	80	THF	4500	1.70	43
4	1.0	80	Dioxane	-	-	-
5	1.0	80	CH ₃ CN	14600	1.93	71
6	1.0	110	CH ₃ CN	6100	1.88	39
7	1.0	100	CH ₃ CN	12600	2.21	63
8	1.0	90	CH ₃ CN	10900	2.19	70
9	1.0	70	CH ₃ CN	14900	1.75	67
10	1.0	60	CH ₃ CN	15000	1.83	54
11	0.5	70	CH ₃ CN	13700	2.06	55
12	2.0	70	CH ₃ CN	13400	1.83	44
13 ^d	1.0	70	CH ₃ CN	14500	2.65	57
14 ^e	1.0	70	CH ₃ CN	10800	1.82	59
15 ^f	1.0	70	CH ₃ CN	16600	1.89	50
16 ^g	1.0	70	CH ₃ CN	12300	1.68	41

^a Reaction conditions: **1a** (0.5 mmol), Ir Cat. (1 mol%), 70 °C, solvent (1.50 mL), 24 h.^b Determined by GPC with RI.^c Isolated yield.^d CH₃CN (3.00 mL) was added.^e CH₃CN (0.75 mL) was added.^f Reaction time was prolonged to 48 h.^g Reaction time was prolonged to 72 h.

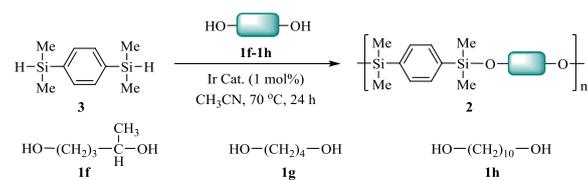
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Table 2. Substrate scope: AB-type monomers.^a

Entry	Monomer	M_n^b	\bar{D}^b	Yield (%) ^c
1	1a	14900	1.75	67 (2a)
2	1b	26000	1.89	69 (2b)
3	1c	19800	1.70	75 (2c)
4	1d	25500	1.87	81 (2d)
5	1e	36300	1.84	82 (2e)

^a Reaction conditions: **1** (0.5 mmol), Ir Cat. (1 mol%), 70 °C, CH₃CN (1.5 mL), 24 h.^b Determined by GPC with RI.^c Isolated yield.

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Table 3. Substrate scope: AA and BB type monomers.^a

Entry	Monomer	M_n^b	\mathcal{D}^b	Yield (%) ^c
1	1f	24100	2.60	60 (2f)
2	1g	29200	1.77	54 (2g)
3	1h	43800	2.15	92 (2h)

^a Reaction conditions: **1** (0.5 mmol), **3** (0.5 mmol), Ir Cat. (1 mol%), 70 °C, CH₃CN (1.5 mL), 24 h.^b Determined by GPC with RI.^c Isolated yield.