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2	
3	<u>Highlights</u>
4	
5	Oxidation of phenol (using Fenton) decrease in the presence of OH° scavengers.
6	The theoretical Ea of liquids systems are lower than gas phases.
7	Good agreement is found between DFT studies and experimental results.
8 9	Theoretical and experimental order shows the trend: hydroquinone>catechol>resorcinol.
10	
11	

11	A Characterization of the Two-step Reaction
12	Mechanism of Phenol Decomposition by a
13	Fenton Reaction
14 15	Cristian Valdés <sup>2</sup> , Jans Alzate-Morales <sup>1</sup> , Edison Osorio <sup>3</sup> , Jorge Villaseñor <sup>2, *</sup> and Carlos Navarro-Retamal <sup>1, *</sup>
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27 28 29 30	ABSTRACT

31 Phenol is one of the worst contaminants at date, and its degradation has been a crucial 32 task over years. Here, the decomposition process of phenol, in a Fenton reaction, is 33 described. Using scavengers, it was observed that decomposition of phenol was mainly 34 influenced by production of hydroxyl radicals. Experimental and theoretical activation 35 energies (E<sub>a</sub>) for phenol oxidation intermediates were calculated. According to these Ea, phenol decomposition is a two-step reaction mechanism mediated predominantly by 36 37 hydroxyl radicals, producing a decomposition yield order given as hydroquinone > 38 catechol > resorcinol. Furthermore, traces of reaction derived acids were detected by 39 HPLC and GS-MS. 40 41 42 INTRODUCTION 43 Phenol is one of the most common contaminants ever known. This compound may 44 come from the pharmaceutical industry, oil, pesticides and others. Lower amounts of 45 phenol (in concentrations of ppm) are enough to induce high levels of toxicity [1]. 46 Phenol is considered by the United States Protection Agency (USEPA) as one of the 47 most pollutant compounds, causing considerable damage to human health and to the 48 ecosystems [2]. The hydroxylation of phenol with oxidizing agents, like ozone and 49 hydrogen peroxide, has a great impact on different fields such as environmental 50 remediation and the photography industry (by using different phenol derivatives as 51 photographic developers) [3].

52 The catalytic oxidation of phenol has proven to be really important along the last years,
53 where different derivatives of this reaction, such as catechol (CT) and hydroquinone
54 (HQ), can serve as raw materials for the generation of photographic supplies, pesticides,

55 inks and additives for medicines [4]. In order to improve the oxidation of this kind of 56 molecules, many researches have used on the last decades a specific kind of oxidation 57 process named advanced oxidation process (AOP), which usually operates at or near 58 normal temperature and pressure conditions. According to Glaze *et al.*, AOP is defined 59 as a process that "involves the generation of hydroxyl (OH) radicals in sufficient 60 quantity to affect water purification" [5]. OH radicals are extraordinarily reactive 61 species. They are able to degrade the most part of organic compounds, with constant rates in the order of the  $10^6 - 10^9 \text{ M}^{-1}\text{s}^{-1}$ [6]. OH radicals are effective in destroying 62 63 organic chemicals because they are reactive electrophiles that react rapidly and non-64 selectively with nearly all electron-rich organic compounds. It has been reported that 65 one of the best source of OH radicals corresponds to the hydrogen peroxide ( $H_2O_2$ ), 66 because it has low cost, and more importantly, because is not harmful to the 67 environment [7, 8]. On the other hand, the Fenton mechanism is based on the 68 continuous production of radicals using the decomposition of  $H_2O_2$  mediated by the ion 69 Fe (II) as catalyst at pH 3 in a homogeneous system [9]. It is also known that phenol can 70 be efficiently degraded by Fenton type processes [10]. Since Fenton processes are characterized by the generation of several radicals (i.e. OH,  $O_2^-$  and  $O_2H$ ) [11, 12], the 71 72 radical scavengers Chloroform (CF) and Isopropyl alcohol (IPA) were used in order to 73 study its effect on the oxidation of phenol, considering their highly selectivity by superoxide ( $k=3.0 \times 10^{10} \text{ M}^{-1} \text{ S}^{-1}$ ) and hydroxyl radical ( $k=9.0 \times 10^9 \text{ M}^{-1} \text{ S}^{-1}$ ) respectively 74 75 [9].

According to literature, three different intermediates are produced during the oxidation of phenol: catechol (CT), resorcinol (RC) and hydroquinone (HQ). Among them, HQ and CT are the most abundant, followed by RC [13]. It has been reported that other

radical species, such as superoxide radical, are also able to oxidase different aromaticcompounds, including phenol [3, 14].

81 Some reaction mechanisms have been proposed to explain the oxidation of phenol 82 mediated by H<sub>2</sub>O<sub>2</sub> and OH radicals [15, 16]. For instance, the oxidation of phenol by 83 OH radicals can be achieved by 3 different reaction mechanisms (Scheme 1). Each one 84 consists in a two-step reaction, where the first step corresponds to the addition of an OH 85 radical onto one of the carbons at the ortho, metha or para positions of phenol, leaving 86 a delocalized electron on aromatic ring and thereby generating an adduct intermediate. 87 The second step corresponds to the hydrogen abstraction (H-abst) at the same position 88 of the previous addition, leading to the formation of a water molecule and the 89 corresponding derivative. Depending on the carbon atom at which the second OH 90 radical is added; three different intermediates can be produced. If both reactions occur 91 at the o-carbon, the product will be CT (Scheme 1C); if instead both reactions occur at 92 the *m*-carbon, the reactions will produce RC (Scheme 1B) and if the reactions occur at 93 the *p*-carbon, the final product will be HQ (Scheme 1A). Furthermore were detected by 94 HPLC and GS- MS: traces of maloneic, malic, pyruvic and acetic acids among others 95 (data not shown).



97

98 Scheme 1. Reaction mechanism describing the different phenol intermediates based on the 99 interaction of phenol with two hydroxyl radicals. A) Generation of HQ by the interaction of the 100 hydroxyl radicals onto the *p*-carbon of phenol. B) Generation of RC by the interaction of the 101 hydroxyl radicals onto the *m*-carbon of phenol. C) Generation of CT by the interaction of the 102 hydroxyl radicals onto the *o*-carbon of phenol.

103 Until date, the addition step has been scarcely described at a theoretical level. For 104 instance, Wu et al. described the addition step of the OH radical on gas phase in 4 105 possible positions at phenol ring: *ipso, ortho, meta* and *para* of phenol. They found that 106 addition at the o-carbon was thermodynamically favorable, resulting in an overall 107 production of 96.7-99.8% of the total adduct products in the reaction [17]. In a similar 108 way, Morales-Roque et al. were able to study the same step, but now including the 109 solvent effects onto the overall system. They found that adducts at o- and p-carbons 110 were the chemical entities that showed the lower energy barriers, thereby producing a 111 bigger amount of o-adducts and p-adducts [8]. At date, there is not theoretical evidence

related to the second step of the reaction mechanism, neither in gas phase or water as asolvent.

In this research work, the main goal is twofold: first, to experimentally elucidate the importance of the OH radical during phenol decomposition; and second, to characterize the two-step decomposition reaction mechanism pathway of phenol by means of theoretical approaches. The research involves the theoretical study of the solvent effect into this kind of reaction.

119

#### 120 METHODOLOGY

121 *Quantification of Phenol and its intermediates by HPLC* 

122 The concentration of phenol was analyzed using a HPLC (Perkin Elmer series 200) 123 equipment with a LiChrospher® column RP-18 with UV absorbance detector. The 124 following conditions were used:  $\lambda$ =280 nm, flow = 1 mL / min, mobile phase methanol 125 (34%) / water (64%) / acetic acid (2%), column at temperature 35° C with an injection 126 volume of 10 µL.

127 The concentration of phenol intermediates was analyzed using a HPLC (Perkin Elmer 128 series 200) equipment with a LiChrospher® column 60 RP Select B coupled to a 129 Shimadzu Prominence RF-20-A / 20AXS fluorescence detector. The following 130 conditions were used:  $\lambda$  emission = 325,  $\lambda$  excitation = 280, flow of 1 mL / min, mobile phase 0.007 M H<sub>3</sub>PO<sub>4</sub> (90%), acetonitrile (10%), column temperature at 45 °C, with an 131 132 injection volume of 10 µL. 133 Phenol and its intermediates concentrations were determined using calibration curves 134 obtained from solutions of known concentration for each case.

136	The solutions were prepared in triplicate and transferred to the autosampler microvials
137	and samples of 200 $\mu$ L were injected into the column. Calibration curves were
138	constructed by plotting the peak area against the nominal concentration of each
139	compound.
140	Five samples of each compound were prepared at the quality control in four different
141	concentrations, in three different days, in order to determine intra- and inter-day
142	precision and accuracy.
143	The acceptance criteria for the limit of quantification was that the accuracy for three
144	analyzed samples presented less than 2 % variability and the limit of detection was
145	measured taking into account a signal-to-noise ratio of three.
146	
147	
148	Radical mediated phenol decomposition in the presence of isopropyl alcohol (IPA) and
149	chloroform (CF) as scavengers
150	Radical mediated decomposition of phenol was achieved using an Advanced Oxidation
151	Process (AOP) methodology, which is based in the application of Fenton reaction
152	mechanism. In order to verify the effect of radicals, some scavenger molecules like
153	isopropyl alcohol (IPA) and chloroform (CF) were used.
154	The system components, Fenton-Phenol-scavenger, were mixed by a continuous stirring
155	in the next concentrations: phenol 50 ppm (Fluka), $H_2O_2$ (Merck), 1 mM, Fe(SO <sub>4</sub> ) •
156	7H <sub>2</sub> O (as source of Fe (II) ions) (Merck), 0,5 g/L and 250 mM of IPA (Sigma Aldrich)
157	or 2 mM of CF (Merck), depending on each case. All the reaction assays were
158	performed at 25°C, pH 3 in a total volume of 50 mL of water. Fenton reaction was
159	stopped at basic pH using a phosphate buffer at pH 8 [18].
160	

161 Experimental determination of Activation energy

162	In order to measure the activation energy for phenol decomposition into the different
163	intermediates HQ, CT and RC, the components Fenton-Phenol were mixed by a
164	continuous stirring using phenol 50 ppm (Fluka), $H_2O_2$ (Merck) 1 mM and Fe(SO <sub>4</sub> ) •
165	$7H_2O$ (Merck) 0,5 g/L. All the assays were performed at pH 3 in a total volume of 100
166	mL of water, the reactions were stopped after one minute using a phosphate buffer at
167	pH 8 and then they were analyzed by HPLC. The experiment was performed at different
168	temperatures (5, 15, 25, 35 and 45 °C).
169	

170 In order to estimate the activation energies, the initial velocities method was used,

171 where *Ea* was measured by the Arrhenius equation as follows:

173 
$$Log V_0 = Log A - \frac{Ea}{RT}$$
 (Equation 1)

174

175 Where *R* is the ideal gas constant, *T* is the absolute experimental temperature and *Ea* is 176 the activation energy, A is a constant and  $V_0$  is the initial velocity of the reaction [19].

177

178 Computational Studies on Phenol and its byproducts

179 Phenol local reactivity

180 In order to determine the reactivity of phenol, local theoretical descriptors in the

- 181 framework of density functional theory (DFT) were used [20, 21]. The Fukui function
- 182 (adjusted to radicals) was used according to the following equation[22]:
- 183

184 
$$f^{0}\vec{r} = \frac{(\rho_{N+1}(r) - \rho_{N-1}(r))}{2}$$
 (Equation 2)

186 Where  $\rho_{N+1}(\vec{r})$  corresponds to the electron density of the N-electron species when the 187 system gains an electron (anion), and  $\rho_{N-1}(\vec{r})$  when it loses an electron (cation). In 188 order to obtain the electron density for a given region at the molecule, it is necessary to 189 divide the molecular space with subsequent integration of the Fukui function on those 190 regions. To do so, Tiznado *et al.* proposed a methodology to condense the Fukui 191 function to regions using the following expression [23, 24]:

192

193 
$$f_k^0 = \int_{w_k} f_k^0(\vec{r}) d\vec{r} \qquad (\text{Equation 3})$$

194 Where the  $\omega_k$  region is obtained from the topological analysis of the Fukui function, and 195  $f_k^0$  is the condensed value of the Fukui function in that specific region [25].

All calculations were performed with the B3LYP [26, 27] method using the 6-311+(d,

p) basis set [28] as available in Gaussian 09 electronic structure software [28-30].

198

#### 199 Characterization of Transition States for Phenol Decomposition Reactions

200

201 Transition state search was performed at an unrestricted DFT level of theory [31] using 202 the LST (Linear Synchronous Transit) method. All geometries (reactants, transition 203 states and products structures) were fully optimized at the B3LYP/6-31G (d) [26, 27] 204 level of theory. By performing frequencies analysis, the character of each stationary 205 point was evaluated, which means that geometries with only positive frequencies 206 (eigenvalues) correspond to a minimum and geometries with only one imaginary 207 frequency should correspond to a transition state geometry. The motion of the main 208 vibrational mode corresponded to the desire reaction pathway. The solvents effects were

209 introduced by a polarizable continuum model (PCM) based on both, the solute and its

electron density and the solvent as a continuum dielectric medium [32].

To check if the transition states were properly located, an intrinsic reaction coordinate algorithm (IRC) was used [33] that is defined as the steepest descent (SD) curves connecting a first-order saddle point (the transition structure) with a minimum, which is characteristic of a stationary point (corresponding to either reactants or products). IRC parameters used were: MaxPoints = 80, maxcycle = 300 and stepsize = 2.

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- 219 RESULTS AND DISCUSSION
- 220 Decomposition of phenol mediated by OH radicals

With the aim to show that decomposition of phenol by AOP process, using  $H_2O_2$  and Fe (II) ions in a Fenton reaction, is dependent on the OH radical concentration; the phenol decomposition was measured in presence of two scavengers: Isopropyl alcohol (IPA) and chloroform (CF). IPA is specific for hydroxyl radicals (OH<sup>\*</sup>) while CF is specific for superoxide radical ( $O_2^{-1}$ ).

226 Phenol decomposition was measured in three different times (10, 20 and 30 minutes) at 25 °C and using 6 different experimental conditions: a) Only H<sub>2</sub>O<sub>2</sub> (unmediated by 227 radicals), b) H<sub>2</sub>O<sub>2</sub> + IPA, c) H<sub>2</sub>O<sub>2</sub> + CF, d) Fenton, e) Fenton + IPA and f) Fenton + CF 228 229 (see Figure 1). Overall, it was found that phenol decomposition by  $H_2O_2$  barely reached 230 the 12% at 30'. When scavengers were added, there was only a 2% decrease in phenol 231 decomposition at 30' using IPA and less of 1% using CF, suggesting that H<sub>2</sub>O<sub>2</sub> is unable 232 to spontaneously decompose on radical species, which may explain the overall low 233 decomposition of phenol under those initial experimental conditions. By using a Fenton

234 system, it was found that overall decomposition of phenol increases significantly at 235 different measuring times, reaching about 30% in the first 10 minutes. Since it is well 236 known that catalysts based in transition metals are able to accelerate the decomposition 237 of  $H_2O_2$  into radical species [9, 34], this last result confirmed that radicals are the 238 mainly species involved in decomposition process of phenol. When IPA and CF 239 scavengers were added into experiment d) ( $H_2O_2 + Fe$  (II), Fenton), two phenomena 240 could be observed: By adding CF, the overall phenol decomposition process did not 241 show a marked decrease in the percentage of inhibition (barely 2%), which roughly 242 means that the superoxide radical could not be responsible of the phenol decomposition 243 process. On the other hand by adding IPA as scavenger, and comparing experiments d 244 and e, it is observed that the yield of decomposition is decreased about 3 times at all measured times, which could indicate that the OH radical is the key chemical specie 245 246 that drives the phenol decomposition process. The effect of CF in phenol decomposition 247 (experiment f) was lower only about 6% when compared with experiment d, which 248 could indicate that the effect of superoxide radical in these conditions is not relevant 249 compared to the hydroxyl radical.



#### 250

251 Figure 1. Bars representation of phenol decomposition percentages measured at different times

and using several experimental conditions.

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255

#### 256 Phenol decomposition and characterization of its intermediates

The concentrations (in ppm) of three different intermediates (CT, RC and HQ), from H<sub>2</sub>O<sub>2</sub> induced phenol decomposition, were measured during time at two different conditions: in presence and absence of Fenton reactant, now on called F and wF, respectively. The experiments were carried out at 25° C and pH 3 (Figure 2). It was found that HQ is the main intermediate produced in the experimental degradation assays, and moreover its production was enhanced by the presence of Fenton reactant (more than two times with respect to the non catalytic process). The other main

products determined in phenol degradation reactions were CT and RC, which is in
agreement with previous literature [35]. It is important to note that the amount of HQ
produced is about 5 times greater than RC, both in presence and absence of the Fenton
system. The amount of CT is produced 3 to 4 times greater than RC in the presence of
Fenton system.

269



270

Figure 2. Concentration (in ppm) of intermediates CT, RC and HQ during induced
decomposition of phenol. The experiments were carried out in presence (F) and absence (wF) of
Fenton process

274

#### 275 Experimental determination of Activation energies

- 276 In order to explain the differences in the amount of each intermediate produced during
- 277 the decomposition of phenol, the activation energy  $(E_a)$  for each reaction was measured.

Using different residence times and temperatures, Ea was estimated for the three

279 reaction mechanisms (Scheme 1) based on the slopes calculated from plots reported in 280 Supplementary Material (Figure 1S, Figure 2S and Figure 3S). It was found that the 281 production of RC presented the highest E<sub>a</sub> with a value of 2,534 kcal/mol. On the other hand, the production of CT and HQ exhibited lower activation energies (1,174 and 282 283 0,855 kcal/mol, respectively). 284 These E<sub>a</sub> differences could be explained by the electron density properties of phenol, 285 which indicates that its *m*-carbon presents a lower electron density while the *o*-carbon 286 and p-carbon present a higher electron density. It has been reported the appearance of 287 HQ and CT in electrochemical oxidation processes of phenol, and moreover these two

288 intermediates were detected in phenol oxidation processes in the presence of hydrogen

peroxide and acetone [13, 36].

290

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291 DFT Reactivity Indexes Analysis

292

As a previous step, before the theoretical characterization of the reaction mechanisms of
phenol decomposition, the electron density of phenol was studied by measuring its
Fukui local indexes for a radical reaction.

According to the radical Fukui index (FI) analysis (Figure 3 and Table 1), it was found that *o*- and *p*-carbons are more susceptible to a radical attack, by the first hydroxyl radical, than the *m*-carbon (FI values: *ortho* = 0.0387-0.0387 *meta* = 0.0251-0.0249 and *para* = 0.1241). It is worth mentioning that this type of method is useful to find regioselectivity of molecules against radicals, but it does not discriminate the type of

- 301 radical. We found that, according to FI, the most favored intermediaries are
- 302 hydroquinone (*para*) and catechol (*meta*).
- 303



316 Figure 3. Ball and sticks representation of phenol molecule that represents its Fukui local 317 indexes at each numbered carbon atom (according to Table 1). In yellow, red and grey are 318 represented the carbons, oxygen and hydrogen atoms, respectively. The electron density 319 obtained by the Fukui analysis is represented on green.

320

321 Table 1. Carbon atoms in phenol molecule and their radical Fukui index values.

Carbon atom	Fukui index (FI)
1	0,0848
2	0.0387

3	0.0251
4	0.1241
5	0.0249
6	0.0387

323

324 Characterization of transition states geometries and phenol decomposition reaction 325 paths.

326 A single imaginary frequency (lower than  $-90 \text{ cm}^{-1}$ ) was found for each of the transition

327 state species calculated both in gas or solvent phase (see Table S1).

328

329 OH radical addition as first reaction step

330

The oxidation of phenol molecules is mediated by a two-step reaction mechanism, which comprises the attack of electrophilic radicals (OH radicals) at three different positions in the phenolic ring. While the first step has been described both on gas and solvent [8, 17], to the best of our knowledge, there are not theoretical studies related to the hydrogen abstraction step neither in gas or solvent phase.

336 The reactants, TSs and products structures, as well as their corresponding activation 337 energies, for the first reaction step in each possible phenol decomposition reaction are 338 presented in Figures 4 and 5, for gas and solvent phase, respectively. The oxygen atom, 339 belonging to the hydroxyl radical, was located around 2.02 – 2.05 Å with respect to the 340 corresponding carbon atom (position ortho, meta and para) in each TS structure (Table 341 S2 and S3). The addition of the first OH radical (on the 3 different systems) showed an 342 energy barrier from 0,504 to 1,573 kcal/mol. According to previous reports, some 343 reactions between phenols and electrophilic compounds are in the order of the 4

kcal/mol [8, 17, 37]. Based on those results, the first reaction step that showed the lowest  $E_a$  in decomposition of phenol is favored on the *p*-carbon, which in turn is in agreement with our experimental data that reported more production of the HQ intermediate. The  $E_a$  values for CT and RC decomposition products are higher in energy and, thereby, their production would be disfavored.

Gas phase (step 1)	Reactants	TS	Products (radical species)
Para	0 kcal/mol	0,504 kcal/mol	-14,981 kcal/mol
Ortho	0 kcal/mol	1.573 kcal/mol	-15 451 kcal/mol
Meta	0 kcal/mol	1,771 kcal/mol	-14,244 kcal/mol

349

Figure 4: Reactants, TSs and products structures for step 1 in the gas phase, with their relativeenergies, are shown. Atom types are: Carbon (yellow), oxygen (red) and hydrogen (cyan).

Solvent phase (step 1)	Reactants	TS	Products (radical species)
Para	0 kcal/mol	0,0201 kcal/mol	-12,4250 kcal/mol
Ortho			
	0 kcal/mol	0,4118 kcal/mol	-13,1074 kcal/mol
Meta	0 kcal/mol	1,7055 kcal/mol	-11,5014 kcal/mol

353

Figure 5: Reactants, TSs and products structures for step 1 in solvent phase, with their relativeenergies, are shown. Atom types are: Carbon (yellow), oxygen (red) and hydrogen (cyan).

356

#### 357 Hydrogen Abstraction, mediated by OH radicals, as the second reaction step

358

With respect to the second reaction step, the transition state geometries showed that a second OH radical was located at 2.37 - 2.41 Å with respect to the carbon atom at the corresponding position in phenol ring. The oxygen atom from OH radical was located at a distance between 1.30 - 1.34 Å with respect to the leaving hydrogen atom (see Table S1 in Supplementary Information). According to IRC energy profiles for second reaction step in gas phase, that means the leaving of H atom mediated by a second OH radical (Figures 6 and 7), it was found that phenol decomposition reaction that showed

the highest Ea values corresponds to the H-abst onto the m-carbon that produces RC 366 367 (25.893 kcal/mol), followed by the reaction occurring onto the *p*-carbon (22.137 carbon)368 kcal/mol) that produces HQ and finally by the reaction occurring onto the o-carbon 369 (19.131 kcal/mol) that produces CT. Those calculated E<sub>a</sub> values are not in fully agreement with our experiments, however they could explain the fact that the 370 371 intermediate RC showed the lowest concentration during the phenol decomposition 372 reaction studied through our experiments. In order to fully understand the correct 373 reactivity trends in the production of RC, CT and HQ intermediates, subsequent 374 estimation of IRCs including the solvation effect were performed.

375

Since this second reaction step occurs on water, the Ea values were also estimated in 376 377 presence of a continuum dielectric field that represents an implicit water solvent. With 378 respect to the OH addition, the final transition state structures showed distances, 379 between the OH radical oxygen atom and the carbon atom in phenol ring, ranging from 2.01 to 2.12 Å (Table S1). When comparing the  $E_a$  values for this first reaction step 380 381 calculated in implicit solvent, against those obtained in gas phase, it can be seen that 382 they decreased for all three reactions in the presence of water as solvent. This 383 phenomenon could be explained by the fact that in organic reactions the electrostatic 384 component of the solvent acts as a catalyst reducing the energetic barrier of the reaction 385 [38] even in the case of reactions that involves free-radicals [39]. It has been reported that Ea is affected by the degree of polarity of the solvent in reactions of polymerization 386

387 [40] and polar organic solvents tend to decrease E<sub>a</sub> in enzymatic systems [41].



388

389 Figure 6: IRC profile with relative energies representing the second step intermediates, in the

390 oxidation of phenol, calculated in gas phase. R (Reactant), TS (Transition State), P (Product).



391

Figure 7: IRC profile with relative energies representing the second step intermediates, in the
oxidation of phenol, calculated in solvent phase. R (Reactant), TS (Transition State), P
(Product).

395

Regarding to the H-abst, the transition state structures showed distances, between the OH radical oxygen and the carbon atom, that were between 2.06 - 2.63 Å. Likewise, the distances between the OH radical oxygen and the leaving hydrogen atom showed values between 1.55 - 1.74 Å (Table S3).

400 The calculated  $E_a$  values for H-abst in solvent, when compared with their counterpart 401 values in gas phase systems, showed a marked decrease in all cases (for instance a 402 marked decrease of ~11 kcal/mol could be seen in the case of the H-abst onto the *p*-403 carbon). This seems reasonable due to the fact that all these kind of reactions occurs,

404 and are favored, on water [25, 26]. Then, the determined solvent  $E_a$  values for the

405 reaction giving RC as product confirmed us that its low production could be due to the 406 high-energy barrier of the process. With respect to the other phenol derivatives, it was 407 observed that in presence of the electrostatic component of the solvent, the  $E_a$  values for 408 production of HQ were lower than the ones for CT (11.42 and 12.99 kcal/mol, 409 respectively) indicating now the correct trend found in our experimental results, that is: 410 during phenol oxidation HQ is the most abundant phenol derivative, followed by CT 411 and finally RC (that is barely produced *in vitro*).

412

413 CONCLUSIONS

414

415 The decomposition of phenol, by using the oxidizing agent hydrogen peroxide, was 416 studied using HPLC and DFT approaches. It was found that decomposition increased 417 about 5 times in the presence of Fe (II) in a homogeneous Fenton system. Thus, decomposition of phenol in these conditions seems to be highly dependent on hydroxyl 418 419 radicals, because in the presence of scavenger IPA the performance of reaction 420 decreases to the half when using catalyst. Regarding the use of CF as scavenger, the 421 effect in lowering the performance of decomposition reaction is subtle. So, we suggest 422 that primarily hydroxyl radicals would carry out the decomposition of phenol in the 423 studied conditions. Generating a high amount of hydroxyl radicals permits efficient 424 decomposition of a variety of harmful substances because it is one of the strongest 425 oxidizing described [42, 43]. Further analysis are required to validate our hypothesis (i.e 426 spin radical experiments), but we believe that our protocol suggest an implication of 427 hydroxil radicals on phenol decomposition.

428

430 On the other hand, the two-step phenol decomposition reaction mediated by OH 431 radicals was successfully described by both theoretical and experimental studies. 432 According to our experimental approach, HQ was the derivate produced in larger 433 quantities, followed by CT and finally RC. From the *in silico* approach, it was found 434 that the activation energy profile for each reaction, estimated on a continuum solvation 435 model, showed the same trend. Finally, from experimental and theoretical approaches, it 436 was possible to determine that during this phenol decomposition reaction mechanism, 437 the intermediates HQ and CT were the main decomposition products, which is in 438 agreement with previous reported studies. The HPLC method proved highly efficient 439 for quantifying phenol and related compounds, in addition to the use of a fluorescence 440 detector that had a high sensitivity for products generated even in concentrations of 441 parts per billion.

442 To the best of our knowledge, there are no previous reports of a theoretical
443 characterization, through IRC method, of intermediates participating in the second step
444 of phenol oxidation mechanism mediated by hydroxyl radicals.

445

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