



Short communication

Enhanced catalytic performance of porphyrin cobalt(II) in the solvent-free oxidation of cycloalkanes (C5~C8) with molecular oxygen promoted by porphyrin zinc(II)



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ABSTRACT

Dual-metalloporphyrins catalytic system based on T(p-Cl)PPCo and T(p-Cl)PPZn was presented to enhance the oxidation of cycloalkanes, especially for cyclohexane, the selectivity towards KA oil increasing from 90.7% to nearly 100.0%, meanwhile the conversion increasing from 3.42% to 4.29%. Enhancement on conversion and selectivity was realized simultaneously. In the dual-metalloporphyrins system, T(p-Cl)PPCo served the role to activate molecular oxygen and promote the decomposition of cyclohexyl hydroperoxide, and T(p-Cl)PPZn catalyzed the decomposition of cyclohexyl hydroperoxide to avoid unselective thermal decomposition. This protocol is also very applicable to other cycloalkanes and will provide a applicable strategy to enhance the oxidation of alkanes.

1. Introduction

The selective oxidation of alkanes to corresponding alcohols, aldehydes, ketones and carboxylic acids is an extremely important and challenging transformation in both chemical industry and academic research, in which the abundant and inexpensive alkanes in petroleum and natural gas are converted to high-value chemical intermediates and fine chemicals [1,2]. Among these significant reactions, the oxidation of cycloalkanes to cycloalkanols and cycloalkanones has gained a continuous and considerable interest, especially for the cyclohexane [3,4], since the obtained cyclohexanol and cyclohexanone (KA oil) can be further converted to caprolactam and hexanedioic acid which are the irreplaceable intermediates in the production of various polymers such as nylon-6 and nylon-66 [5,6]. And the oxygenated products from other cycloalkanes, such as cyclopentane, cycloheptane and cyclooctane, not only are important precursors of a series of macromolecule polymers [7], but also are building blocks in several valuable chemicals [8]. In order to realize these essential transformations, several oxidants have been explored, including iodosylbenzene [9], *m*-chloroperoxybenzoic acid [10], *tert*-butyl hydroperoxide [11], hydrogen peroxide [12], molecular oxygen [13], and so on. It is obvious that molecular oxygen is the most promising one according to the requirements of green chemistry, which possesses low cost, readily availability and environmental harmlessness with innocuous water as the only by-product. But

compared with other oxidants, the activation of molecular oxygen in the oxidation of cycloalkanes is very difficult. Thus the industrial oxidation of cyclohexane is conducted at 150–170 °C and 1.0–2.0 MPa oxygen pressure employing homogeneous cobalt salt as catalyst with conversion of 3%–8% for cyclohexane and selectivity of 80%–85% towards KA oil [14,15], which suffers from the low selectivity seriously. To some extent, the low selectivity in oxidation of cycloalkanes can be attributed to the high reaction temperature, because the autoxidation of cycloalkanes and thermal decomposition of cycloalkyl hydroperoxides which are the main intermediate products in the oxidation of cycloalkanes [16], would occur at high temperature. Both of them process through unselective free radical chain reaction pathway, and give rise to a lot of undesired oxydates, including hexanedioic acid which is very difficult to separate from the oxidation products. Despite the fact that most of the KA oil is employed as intermediate to produce hexanedioic acid, the formation of hexanedioic acid in the production of KA oil is a troublesome issue. Hence, it is highly urgent to develop the selective oxidation of cycloalkanes to cycloalkanols and cycloalkanones under mild conditions.

To smooth the oxidation of cycloalkanes to their corresponding alcohols and ketones using molecular oxygen, various catalytic systems have been explored, including transition metal complex catalysis [17], metal nanoparticle catalysis [18], molecular sieve catalysis [19], photocatalysis [20], biocatalysis [21], and so on. Synthetic

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metalloporphyrins which are the chemical models of cytochrome P-450 enzymes, are a type of transition metal complexes and have been widely applied in the oxidation of cycloalkanes as biomimetic catalysts for their high efficiency in activation of molecular oxygen and satisfying selectivity in oxidation of C–H bond [9,13,17,22,23]. A number of satisfying results were achieved. For example, Huang and co-workers reported tetrakis(4-carboxylphenyl)porphyrin iron(III) chloride, tetrakis(pentafluorophenyl) porphyrin iron(III) chloride, tetrakis(4-sulfonatophenyl)porphyrin iron(III) chloride and tetrakis(4-carboxylphenyl) porphyrin iron(II), cobalt(II), manganese(II), which were immobilized onto zinc oxide(ZnO), zinc sulfide(ZnS) and chitosan respectively to boost their stability and catalytic performance, were employed as catalysts in the oxidation of cyclohexane at the temperature range of 150–165 °C, and the most satisfying selectivity towards KA oil was 56.5% with the conversion of 39.8% [17,22,24]. Liu and co-workers reported 5,15-di(4-chlorophenyl)-10,20 -diphenylporphyrin cobalt(III) chloride immobilized onto zinc oxide(ZnO) catalyzed oxidation of cyclohexane with molecular oxygen at 155 °C, and the selectivity towards KA oil reached up to 72.1% with the conversion of 13.1% [25]. Yang and co-workers reported the synthesis of porous polymeric metalloporphyrins using tetrakis(4-bromophenyl)porphyrin iron(III) chloride, tetrakis(4-bromophenyl) porphyrin manganese(III) chloride and 1, 4-phenyldiboronic acid as building blocks, which were applied in the oxidation of cyclohexane at 150 °C, and the selectivity was up to 72.2% with the conversion of 29.9% [26]. Pamin and co-workers investigated the performance of three generations of porphyrin cobalt(II) in the oxidation of cycloalkanes with molecular oxygen systematically, and found that the generation II porphyrin cobalt(II) showed higher activity [13]. Evidently, the oxidation of cyclohexane with molecular oxygen was promoted by metalloporphyrins, especially for the conversion and yield, but still suffered from the high temperature and low selectivity, which would lead to a lot of undesired by-products and pollute the environment. Thus, how to increase the selectivity and lower the reaction temperature is still an enormous challenge lied in the progress of cycloalkanes oxidation.

In our attempt to increase the selectivity in oxidation of cycloalkanes catalyzed by metalloporphyrins with molecular oxygen [27–29], the formation of carboxylic acid and other undesired by-products from unselective free radical reaction occurred at higher temperature, became the primary issue to consider. To solve this problem, an idea to conduct the oxidation of cycloalkanes at lower-temperature and decompose the cycloalkyl hydroperoxides through catalytic pathway emerged in our minds. After systematic investigation on the autoxidation temperature of cycloalkanes(C5–C8) [30], the catalytic oxidation of cycloalkanes was conducted at the temperature not higher than their autoxidation temperature in our following work. Meanwhile, in order to realize the catalytic decomposition of cycloalkyl hydroperoxides, dual-metalloporphyrins system was introduced to the catalytic oxidation of cycloalkanes, in which one metalloporphyrin mainly served the decomposition of cycloalkyl hydroperoxides. Encouraging outcomes were obtained, especially for the selectivity towards KA oil. The selectivity towards KA oil was increased from 90.7% to nearly 100.0%, meanwhile the conversion of cyclohexane was also increased from 3.42% to 4.29%. Thus, in this work we reported the enhanced performance of porphyrin cobalt(II) in the solvent-free oxidation of cycloalkanes (C5–C8) with molecular oxygen promoted by porphyrin zinc(II), which not only reveals a strategy to enhance the conversion and selectivity in the oxidation of cycloalkanes, but also act as an important reference in the selective oxidation of other alkanes. To the best of our knowledge, our work is a very scarce example in the oxidation of alkanes, in which the conversion and selectivity is enhanced simultaneously through the delicate cooperation of two different metalloporphyrins.

2. Experimental

2.1. Materials and reagents

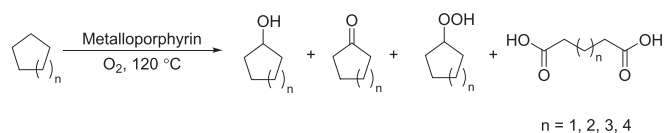
Cyclohexane in 99% purity was purchased from Hangzhou Shuanglin Chemical Reagent Co. Ltd., China. Cyclopentane and cycloheptane in 98% purity were purchased from TCI Co. Ltd. Cyclooctane in 99% purity was purchased from Alfa Aesar Co. Ltd. All of the above cycloalkanes were dried over sodium and redistilled before use. All the other common reactants and reagents were analytical grade, and all of them were used as received without further purification unless otherwise noted.

2.2. Catalytic oxidation of cycloalkanes

The catalytic oxidation of cycloalkanes employing metalloporphyrins as catalysts and molecular oxygen as oxidant was conducted in a 100 mL autoclave reactor equipped with an inner Teflon liner and a magnetic stirrer. In a typical procedure, metalloporphyrin ($1.2 \times 10^{-3}\%$, mol/mol) was suspended in cycloalkane (200 mmol) in the 100 mL autoclave reactor, and the reactor was heated to the desired reaction temperature after sealing. When the reaction temperature reached, oxygen was fed into the autoclave to obtain a desired pressure. The resultant reaction mixture was stirred at the desired temperature and desired pressure for 8.0 h, then cooled to room temperature. Triphenylphosphine (25 mmol, 6.5573 g) was added into the reaction mixture to reduce the cycloalkyl hydroperoxide to corresponding cycloalkanol quantitatively. After stirring for 30 min, the reaction mixture was dissolved in acetone and transferred into a 100 mL volumetric flask totally. Then the GC and HPLC analyses were performed to determine the yields of the oxidized products. The oxidized products were determined by comparison with the authentic samples. The yields of cycloalkanol and cycloalkanone were determined by GC employing toluene as internal standard, and the yield of cycloalkyl hydroperoxide was determined through the amount of $\text{O}=\text{PPh}_3$ obtained from reduction of cycloalkyl hydroperoxide with PPh_3 using GC. GC analyses were performed on a Thermo Scientific Trace 1300 instrument using a TG-SMS column (30 m \times 0.32 mm \times 0.25 μm). The yields of aliphatic diacids were determined by HPLC with benzoic acid as internal standard. HPLC analyses were performed on a Thermo Scientific Ultimate 3000 chromatography equipped with a Ultimate 3000 Photodiode Array Detector using a Amethyst C18–H column (250 mm \times 4.6 mm \times 0.25 μm).

3. Results and discussion

In this work, the catalytic oxidation of cycloalkanes was carried out in a 100-mL stainless steel autoclave reactor equipped with an Teflon liner and a magnetic stirrer under solvent-free condition with metalloporphyrins as catalysts and molecular oxygen as oxidant as shown in Scheme 1. The representative metalloporphyrins employed in this work were tetrakis(2-chlorophenyl)porphyrin cobalt(II) (T(o-Cl)PPCo), tetrakis(3-chlorophenyl)porphyrin cobalt (II) (T(m-Cl)PPCo), tetrakis(4-chlorophenyl)porphyrin cobalt(II) (T(p-Cl)PPCo), tetrakis(4-chlorophenyl) porphyrin iron(II) (T(p-Cl)PPFe), tetrakis(4-chlorophenyl) porphyrin manganese(II) (T(p-Cl)PPMn), tetrakis(4-chlorophenyl)porphyrin zinc(II) (T(p-Cl)PPZn), which were synthesized through the



Scheme 1. Selective oxidation of cycloalkanes (C5–C8) with molecular oxygen catalyzed by metalloporphyrins

Table 1
Catalytic oxidation of cyclohexane with O₂ catalyzed by various metalloporphyrins.^a

Entry	Catalyst	Conversion ^b (%)	Selectivity ^b (%)			
			Alcohol	Ketone	Hydroperoxide	Total
1	/	N. D.	N. D.	N. D.	N. D.	N. D. ^c
2	T(o-Cl)PPCo	3.88	39.9	44.3	4.4	88.6
3	T(m-Cl)PPCo	3.72	45.2	41.1	4.0	90.3
4	T(p-Cl)PPCo	3.43	42.3	43.4	5.0	90.7
5	T(p-Cl)PPMn	3.54	43.8	29.4	23.4	96.6
6	T(p-Cl)PPFe	1.08	19.4	31.5	49.1	100.0
7	T(p-Cl)PPZn	N. D.	N. D.	N. D.	N. D.	N. D.
8 ^d	T(o-Cl)PPCo	3.48	41.7	41.1	11.8	94.6
	T(p-Cl)PPZn					
9	T(m-Cl)PPCo	3.01	44.2	45.2	5.3	94.7
	T(p-Cl)PPZn					
10	T(p-Cl)PPCo	4.18	42.6	33.0	20.8	96.4
	T(p-Cl)PPZn					
11	T(p-Cl)PPMn	1.25	28.8	20.8	46.4	96.0
	T(p-Cl)PPZn					
12	T(p-Cl)PPFe	1.09	6.4	24.8	60.6	91.8
	T(p-Cl)PPZn					

^a Reaction condition: cyclohexane (200 mmol, 16.83 g), metalloporphyrin ($1.2 \times 10^{-3}\%$, mol/mol), O₂ (1.40 MPa), 120 °C, 8.0 h.

^b The conversion and selectivity of cyclohexanol and cyclohexanone were determined by GC after treatment with PPh₃ employing toluene as internal standard, and the selectivity of cyclohexyl hydroperoxide was determined through the amount of O=PPh₃ obtained from reduction of cyclohexyl hydroperoxide with PPh₃. The products were determined by comparison with the authentic samples.

^c No obvious reaction was detected.

^d The molar ratio of two metalloporphyrins was 1:1, and the total concentration of metalloporphyrins was kept at $1.2 \times 10^{-3}\%$, mol/mol.

Table 2
Effect of molar ratios between T(p-Cl)PPCo and T(p-Cl)PPZn on the catalytic oxidation of cyclohexane^a.

Entry	Molar ratio ^b	Conversion ^c (%)	Selectivity ^c (%)			
			Alcohol	Ketone	Hydroperoxide	Total
1	1.0:1.0	4.18	42.6	33.0	20.8	96.4
2	1.0:1.5	4.28	52.6	37.4	8.6	98.6
3	1.0:2.0	4.29	49.7	31.7	18.6	100.0 ^d
4	1.0:2.5	3.90	55.6	33.4	11.0	100.0
5	1.0:3.0	3.55	45.6	29.9	24.5	100.0

^a Reaction condition: cyclohexane (200 mmol, 16.83 g), T(p-Cl)PPCo ($6.0 \times 10^{-4}\%$, mol/mol), T(p-Cl)PPZn as shown in table, O₂ (1.40 MPa), 120 °C, 8.0 h.

^b $m_{[T(p-Cl)PPCo]} : m_{[T(p-Cl)PPZn]}$.

^c Same with Table 1.

^d No obvious by-product was detected.

Table 3
Decomposition of *tert*-butyl hydroperoxide in the presence or absence of metalloporphyrins.^a

Entry	Metalloporphyrin	Decomposition ratio ^b (%)	Yield ^c (%)	Selectivity ^c (%)
1	/	5.2	N. D.	N. D.
2	T(p-Cl)PPZn	36.9	30.0	81.3
3	T(p-Cl)PPCo	59.0	39.3	66.6
4	T(p-Cl)PPCo T(p-Cl)PPZn	21.7	16.9	77.9

^a Reaction condition: *t*-BuOOH (5.0 mmol, 70% aqueous solution, 0.6437 g) in cyclohexane (20 mmol, 1.6832 g), metalloporphyrin ($2.5 \times 10^{-3}\%$, mol/mol), 80 °C, 4.0 h.





^b Determined by GC employing toluene as internal standard through the amount of O=PPh₃ obtained from reduction of the residual *t*-BuOOH with PPh₃. The products were determined by comparison with the authentic samples.

^c Yield and selectivity of *tert*-butanol, determined by GC employing toluene as internal standard.

condensation of freshly distilled pyrrole with corresponding chlorobenzaldehyde in propionic acid followed by the metallation in DMF [31]. All the metalloporphyrins were purified by silica column chromatography and characterized through ¹H NMR, ¹³C NMR and ESI-MS. With metalloporphyrins in hand, the catalytic oxidation of cyclohexane was selected as probe reaction to test and verify our ideas at the reaction temperature of 120 °C, at which the autoxidation would not happen. And the major products were KA oil, cyclohexyl hydroperoxide and a little of carboxylic acids which were analyzed by GC and HPLC to determine the conversion and selectivity. Because a small amount of cyclohexyl hydroperoxide could be converted to KA oil smoothly after reaction, the selectivity towards cyclohexyl hydroperoxide was considered as a part of KA oil. As shown in Table 1, no oxidation occurred in the absence of metalloporphyrins (Entry 1). When the metalloporphyrins were introduced to the reaction, the conversion of cyclohexane reached up to 3.43%–3.88% for porphyrin cobalt and porphyrin manganese with an acceptable selectivity of 88.7%–96.6% towards KA oil. But there are still some hexanedioic acid and undesired by-products formed, especially for the porphyrin cobalt. As for T(p-Cl)PPFe, a lower catalytic performance was observed, and T(p-Cl)PPZn did not exhibit any catalytic activity in the oxidation of cyclohexane at all. However, when dual-metalloporphyrins systems were applied to the oxidation of cyclohexane, the catalytic performance of T(p-Cl)PPCo was enhanced considerably by T(p-Cl)PPZn. The conversion of cyclohexane increased from 3.43% to 4.18% meanwhile the selectivity towards KA oil increased from 90.7% to 96.4% (Entry 3, Entry 10). The increase in the conversion did not consume the selectivity. Increase in both of the conversion and selectivity were realized as a result of the promotion of porphyrin zinc. Thus, T(p-Cl)PPCo employed as catalyst combined with T(p-Cl)PPZn as promoter was considered as the most successful dual-metalloporphyrins system in this work. For other dual-metalloporphyrins systems, the unsatisfying catalytic performance might be ascribed to the undesired interactions between two metalloporphyrins such as the formation of dimers and the intermolecular redox [32,33].

With the optimized dual-metalloporphyrins system established, the molar composition of T(p-Cl)PPCo and T(p-Cl)PPZn was investigated deeply, in which the loading of T(p-Cl)PPCo was set as $6.0 \times 10^{-4}\%$ (mol/mol), and the molar ratios between T(p-Cl)PPCo and T(p-Cl)PPZn varied from 1: 1.0 to 1: 3.0. It was illustrated in Table 2 that, when the

Table 4Oxidation of cycloalkanes (C5-C8) catalyzed by dual-metallporphyrins system based on T(*p*-Cl)PPCo and T(*p*-Cl)PPZn.^a

Entry	Cycloalkane	Conversion ^b (%)	Selectivity (%) ^b			
			Alcohol	Ketone	Hydroperoxide	Total
1 ^c		1.84	11.4	35.3	7.5	54.2
2 ^c		4.29	49.7	31.7	18.6	100.0 ^f
3 ^d		2.20	N. D. ^g	18.2	81.8	100.0
4 ^e		2.29	N. D.	16.2	83.8	100.0

^a Reaction condition: cycloalkane (200 mmol), T(*p*-Cl)PPCo ($6.0 \times 10^{-4}\%$, mol/mol), T(*p*-Cl)PPZn ($1.2 \times 10^{-3}\%$, mol/mol), O₂ (1.40 MPa), 8.0 h.^b Same with Table 1.^c 120 °C.^d 110 °C.^e 100 °C.^f No obvious by-product was detected.^g No obvious cycloalkanol was detected.**Table 5**

Catalytic performance of some metallporphyrins in the oxidation of cyclohexane with molecular oxygen under solvent-free condition.

Entry	Catalyst	Temperature (°C)	Conversion (%)	Selectivity ^a (%)	Ref.
1	T(penta-F)PPCo immobilized onto chitosan	165	38.5	62.8	[34]
2	T(<i>p</i> -COOH)PPCo immobilized onto ZnS	165	67.8	34.2	[17]
3	T(<i>p</i> -COOH)PPMn immobilized onto ZnS	160	46.1	46.1	[17]
4	T(<i>p</i> -COOH)PPFe immobilized onto ZnS	160	51.8	42.3	[17]
5	T(<i>p</i> -COOH)PPMnCl immobilized onto chitosan	155	14.7	76.9	[35]
6	T(<i>p</i> -COOH)PPFeCl immobilized onto chitosan	155	17.3	75.3	[35]
7	T(<i>p</i> -SO ₃ H)PPFeCl immobilized onto chitosan	155	51.4	55.8	[24]
8	T(<i>p</i> -COOH)PPMn	150	9.76	74.7	[23]
9	T(<i>p</i> -COOH)PPMn immobilized onto ZnO	150	7.98	91.0	[23]
10	T(penta-F)PPFeCl	150	23.4	64.0	[22]
11	T(penta-F)PPFeCl immobilized onto ZnO	150	39.8	56.5	[22]
12	Porous polymeric T(<i>p</i> -Br)PPMnCl	150	29.9	72.3	[26]
13	Porous polymeric T(<i>p</i> -Br)PPFeCl	150	27.5	69.8	[26]
14	Porous polymeric T(<i>p</i> -Br)PPMnCl	135	12.5	84.8	[26]
15	T(<i>p</i> -Cl)PPCo	120	3.43	90.7	This work
16	T(<i>p</i> -Cl)PPCo & T(<i>p</i> -Cl)PPZn	120	4.29	100.0	This work

^a Selectivity towards KA oil.

molar ratio of T(*p*-Cl)PPCo to T(*p*-Cl)PPZn was changed from 1.0:1.0 to 1.0:1.5, the selectivity towards KA oil increased from 96.4% to 98.6%. Further increasing the ratio of T(*p*-Cl)PPZn to 1.0: 2.0, no obvious by-product was detected with satisfying conversion of 4.29%. Thus, with the promotion of T(*p*-Cl)PPZn, it was achieved to enhanced the conversion and selectivity in the oxidation of cyclohexane catalyzed by T(*p*-Cl)PPCo. With the acceptable conversion of 4.29%, nearly 100% selectivity towards KA oil was obtained, which would simplify the separation process and reduce the production costs remarkably in the industrial oxidation of cyclohexane. As mentioned above, the exciting conversion and selectivity in our work was mainly attributed the low-temperature oxidation and the catalytic decomposition of cyclohexyl hydroperoxide promoted by T(*p*-Cl)PPZn. At lower reaction temperature, the unselective autoxidation of cyclohexane, cyclohexanol and cyclohexanone, and the unselective thermal decomposition of cyclohexyl hydroperoxide were inhibited. On the other hand, the cyclohexyl hydroperoxide was decomposed to cyclohexanol catalyzed by T(*p*-Cl)PPZn. Both of them reduced the formation of undesired by-products and improved the selectivity in the oxidation cyclohexane. The catalytic performance of T(*p*-Cl)PPZn in the decomposition of cyclohexyl hydroperoxide was verified in our work employing *tert*-butyl hydroperoxide as representative. It was demonstrated in Table 3 that when *tert*-

butyl hydroperoxide was stirred in cyclohexane at 80 °C for 4.0 h, the decomposition ratio was just 5.2%, but when T(*p*-Cl)PPCo or T(*p*-Cl)PPZn was added, the decomposition reached up to 59.0% and 36.9% respectively with *tert*-butanol as major product. Both of T(*p*-Cl)PPCo and T(*p*-Cl)PPZn can catalyze the decomposition of *tert*-butyl hydroperoxide and T(*p*-Cl)PPZn possesses better selectivity towards *tert*-butanol. With the results obtained in Table 1 that T(*p*-Cl)PPCo was an effective catalyst in the oxidation of cyclohexane with molecular oxygen and T(*p*-Cl)PPZn did not exhibit any catalytic activity, and the catalytic mechanism in the oxidation of cyclohexane with molecular oxygen catalyzed by metallporphyrins that molecular oxygen was activated by metallporphyrins [17,24,25], it could be concluded that in this dual-metallporphyrins catalytic system, T(*p*-Cl)PPCo not only served the role to activate molecular oxygen, but also possessed the function to promote the decomposition of cyclohexyl hydroperoxide, and T(*p*-Cl)PPZn served the decomposition of cyclohexyl hydroperoxide exclusively. Their delicate cooperation made the high selective oxidation of cyclohexane realized. As for the optimized molar ratio of T(*p*-Cl)PPCo to T(*p*-Cl)PPZn was 1.0: 2.0, it should be attributed to the high efficiency of T(*p*-Cl)PPCo in activation of molecular oxygen and formation of cyclohexyl hydroperoxide, and the lower transformation rate of cyclohexyl hydroperoxide to cyclohexanol and cyclohexanone. More

catalytic active centers were needed to enhance the transformation of cyclohexyl hydroperoxide to cyclohexanol and cyclohexanone. What should be mentioned additionally is that cyclohexanol and cyclohexanone at negligible levels compared with *tert*-butanol were also detected in the decomposition of *tert*-butyl hydroperoxide in cyclohexane.

Based on the results obtained from the selective oxidation of cyclohexane catalyzed by the dual-metalloporphyrins system, the substrates were extended from cyclohexane to cyclopentane, cycloheptane and cyclooctane. All the catalytic transformations were conducted at the temperature no autoxidation would occur. As shown in Table 4, nearly 100% selectivity towards alcohol, ketone and hydroperoxide was achieved for the cycloalkanes involved, except for the cyclopentane. The lower selectivity in cyclopentane oxidation was mainly attributed to the higher strain in cyclopentane molecule. And the major product in the oxidation of cyclopentane is pentanedioic acid illustrated in Tables S1 and S2. For the satisfying substrate tolerance, the dual-metalloporphyrins catalytic system presented in this work has enormous potential application in the selective oxidation of cycloalkanes, and will serve as an applicable strategy in the enhancement of various alkanes oxidation.

At last, the catalytic oxidation of cyclohexane in this work was compared with some reported cyclohexane oxidation systems employing metalloporphyrins as catalysts and molecular oxygen as oxidant under solvent-free condition, as shown in Table 5. It is clear that, in the term of conversion, the dual-metalloporphyrins catalytic system in this work is not so competitive, but in the aspects of reaction temperature and selectivity towards KA oil, our protocol in the oxidation of cyclohexane is very promising without any obvious by-product produced, which will not only simplify the separation process remarkably in the industrial oxidation of cyclohexane, but also cut down the chemical waste discharged to the environment. Although the conversion in this work is comparable to the industrial level, the attempt to further improve the conversion of cyclohexane with high selectivity is still in process in our group at present.

4. Conclusion

In conclusion, a strategy to enhance the selectivity in the catalytic oxidation of cycloalkanes was presented in this work, especially for the cyclohexane, the selectivity towards KA oil was increased from 90.7% to nearly 100.0%, meanwhile the conversion of cyclohexane was increased from 3.42% to 4.29%. The increase in the conversion and selectivity was achieved simultaneously. The encouraging results in the oxidation of cyclohexane were mainly attributed to the low temperature reaction and the delicate cooperation between T(p-Cl)PPCo and T(p-Cl)PPZn in the dual-metalloporphyrins catalytic system, in which T(p-Cl)PPCo served the role to activate molecular oxygen and promote the decomposition of cyclohexyl hydroperoxide, and T(p-Cl)PPZn could catalyze the decomposition of cyclohexyl hydroperoxide selectively. For the low temperature reaction and the delicate cooperation of T(p-Cl)PPCo and T(p-Cl)PPZn, the unselective autoxidation of cyclohexane and the unselective thermal decomposition of cyclohexyl hydroperoxide were inhibited, resulting in the higher selectivity. This protocol to enhance the oxidation of cyclohexane is also very applicable to other cycloalkanes, such as cyclopentane, cycloheptane and cyclooctane. To the best of our knowledge, this work is a very scarce example in the oxidation of alkanes, in which the conversion and selectivity is enhanced simultaneously, and will provide an applicable strategy to increase the conversion and selectivity in the oxidation of alkanes. And the attempt to further improve the conversion of cycloalkane with high selectivity is still in process in our group at present.

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Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.catcom.2019.105809>.

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