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A mesoporous "shell-in-shell" structured nanocatalyst with large surface area, enhanced synergy, and improved catalytic performance for Suzuki–Miyaura coupling reaction[†]

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A novel mesoporous "shell-in-shell" structured nanocatalyst (@Pd/meso-TiO₂/Pd@meso-SiO₂) with large surface area, enhanced synergy, and improved catalytic performance is created for catalyzing Suzuki–Miyaura coupling and 4-nitrophenol reduction reactions.

Heterogeneous catalysis, a promising route to obtain desired targets, has aroused great research interest because it is widely applicable in various catalytic reactions with good recovery capacity and recyclability.¹ Noble metal nanocatalysts have been widely investigated in heterogeneous catalysis.^{2,3} However, the noble metal nanocatalysts tend to aggregate, leading to the loss of catalytic activity under high temperature treatment or reaction conditions.⁴ Loading noble metal nanoparticles on surface-modified supports is an ideal approach to solve this problem,^{5,6} because diverse supports can limit the migration of noble metal nanoparticles and prevent aggregation. In addition, the synergetic effects between the noble metal nanoparticles and the supports are in favor of improving catalytic performance.⁷

Among the investigated metal oxide supports, TiO_2 is the most promising one due to its excellent redox ability and chemical and thermal stability.⁸ In order to pursue the optimum catalytic performance, TiO_2 with diverse morphologies has been widely studied.^{9,10} Among these studies, the hollow mesoporous TiO_2 nanocatalyst has been extensively investigated in recent years, due to its superior catalytic properties.¹¹⁻¹³ Furthermore, the TiO_2 nanocatalyst can be further integrated by loading the noble metal nanoparticles in the cavity^{14,15} on the internal¹⁶ or external surfaces of the hollow TiO_2 sphere¹⁷ to enhance its catalytic performance.

Mesoporous SiO₂ (meso-SiO₂) coating is an effective route to improve the stability of nanocatalysts.^{18,19} The meso-SiO₂ shell can resist the aggregation of active species, reduce the leaching of noble metal, and improve the accessibility of active species.²⁰ Meanwhile, the selectivity of reactants can also be tuned *via* changing the pore size of meso-SiO₂ and hydrophilicity or hydrophobicity of the meso-SiO₂ surface.^{21,22} Furthermore, a resorcinol-formaldehyde (RF)-resin polymer, a common easily removable hard template, has been widely used to synthesize carbon spheres²³ and various hollow sphere materials.^{24,25}

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Herein, we design a novel mesoporous "shell-in-shell" structured nanocatalyst (@Pd/meso-TiO₂/Pd@meso-SiO₂). The nanocatalyst is composed of mesoporous double TiO₂ and SiO₂ shells with the ultrafine Pd nanoparticles (PNPs) uniformly distributed on the external and internal surfaces of the meso-TiO₂ shell. Such a structural configuration endows the nanocatalyst with large surface area due to the mesoporous shells, enhanced synergy between PNPs and the TiO₂ shell, and independent chambers formed by two shells. Ultimately, the nanocatalyst, which is used as an effective nanoreactor, exhibits improved catalytic activity and selectivity for Suzuki-Miyaura coupling reaction and high catalytic activity and stability for 4-nitrophenol reduction reaction. Depending on the restriction of mesopores of the outer meso-SiO2 shell on reactant molecules, the catalytic selectivity for Suzuki-Miyaura coupling is successfully realized.

The synthesis of the "shell-in-shell" structured @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst follows the procedures illustrated in Scheme 1. Initially, a layer of TiO₂ is coated onto SiO₂ spheres *via* a sol-gel process to obtain SiO₂@TiO₂ spheres. Then, the SiO₂ spheres are removed by etching with NaOH solution to obtain @TiO₂ spheres. After modifying the @TiO₂ spheres with –NH₂ groups using (3-aminopropyl)triethoxysilane (APTES) to render a hydrophilic surface, a Pd²⁺ ion-diffusion process is carried out. With this step, Pd²⁺ ions can be diffused easily into the central cavity of the @TiO₂ spheres through mesoporous TiO₂ shells. Then, the @TiO₂ spheres with Pd²⁺ ions loaded on the internal and external surfaces are subsequently

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 $\label{eq:scheme1} \begin{array}{l} \mbox{Scheme1} & \mbox{Scheme1}$

coated with the layers of resorcinol formaldehyde (RF) and mesoporous SiO₂. Following the calcination and reduction under a hydrogen atmosphere, the $@Pd/meso-TiO_2/Pd@meso-SiO_2$ nanocatalyst is obtained.

The resultant @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst shows good monodispersibility and possesses a well-defined "shell-in-shell" structural configuration consisting of mesoporous TiO₂ and SiO₂ shells with ultrafine PNPs loaded on both internal and external surfaces of the meso-TiO₂ shell (Fig. 1a and b, Fig. S3 and S4, ESI†). The diameters of hollow TiO₂ and SiO₂ spheres are estimated to be ~170 and ~300 nm, respectively. The thickness of TiO₂ and SiO₂ shells is around ~35 and ~24 nm, respectively. The mesopores on TiO₂ and SiO₂ shells can be clearly observed from the enlarged image (inset in Fig. 1a). Due to the "shell-in-shell" structural feature, an interlayer chamber of ~50 nm is created. The STEM images further confirm the "shell-in-shell" structural configuration



Fig. 1 TEM (a and b), STEM (c, d, and e), SEM images (g and h), and the XRD pattern (i) of the "shell-in-shell" $@Pd/meso-TiO_2/Pd@meso-SiO_2$ nanocatalyst; (f) EDX elemental mapping of Ti, Si, O, and Pd in the "shell-in-shell" $@Pd/meso-TiO_2/Pd@meso-SiO_2$ nanocatalyst shown in (e). The inset image of (a) is the partially enlarged image of (b) showing the existence of mesoporosity in TiO_2 and SiO_2 shells.

with an interlayer chamber existing between TiO₂ and SiO₂ shells (Fig. 1c-e). In addition, light spots on both sides of TiO₂ shells further suggest the good distribution of PNPs on the internal and external surfaces of the TiO₂ shell. The highly dispersed PNPs on the TiO2 support may enhance the catalytic activity and stability.¹⁶ EDX elemental mapping clearly shows that the @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst is composed of inner TiO₂ and outer SiO₂ shells with PNPs uniformly distributed on the internal and external surfaces of TiO₂ shells (Fig. 1f). In particular, it can be confirmed from the EDX elemental mapping image that a large quantity of PNPs with very small size (~ 5 nm) exists in the nanocatalyst, which may be advantageous for improving the catalytic performance.²⁶ The SEM images further indicate that the "shell-in-shell" structured @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst has a relatively smooth surface, better monodispersity, and good integrity (Fig. 1g and h, and Fig. S3, ESI[†]).

Fig. 2 shows the nitrogen adsorption–desorption isotherm and BJH pore size distribution of the @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst. It displays a typical IV isotherm with H1-type hysteresis loops ($P/P_0 > 0.5$), indicating the presence of mesopores in TiO₂ and SiO₂ shells. The nanocatalyst has a relatively high surface area ($\sim 700 \text{ m}^2 \text{ g}^{-1}$). The BJH pore size distribution shows that the nanocatalyst has two obvious pore sizes ($\sim 2.2 \text{ and } \sim 3.8 \text{ nm}$) attributed to the mesoporous SiO₂ and TiO₂ shells^{12,27} consistent with the SAXRD result (Fig. S7, ESI†), which is beneficial for improving its catalytic activity.

In order to verify the superiority of such a featured nanocatalyst in catalysis, the Suzuki–Miyaura coupling and 4-nitrophenol reductions are employed as model reactions to evaluate the catalytic capability of the @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst. In contrast, the @meso-TiO₂/Pd@meso-SiO₂, @meso-TiO₂/Pd@SiO₂,



Fig. 2 Nitrogen adsorption-desorption isotherm (A) and BJH pore size distribution (B) of (a) <code>@meso-TiO_2/Pd@meso-SiO_2</code>, (b) <code>@Pd/meso-TiO_2/Pd@meso-SiO_2</code>, and (c) <code>@meso-TiO_2/Pd^2+@RF@SiO_2</code> nanocatalysts.

 Table 1
 Suzuki–Miyaura coupling reactions of aryl halides on the @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst^a

$R_1 - \left(\begin{array}{c} \\ \\ \\ \end{array} \right) - X + R_2 - \left(\begin{array}{c} \\ \\ \end{array} \right) - B(OH)_2 - \begin{array}{c} Catalyst \\ \hline EtOH, 80 \ ^{\circ}C \end{array} - \left(\begin{array}{c} \\ \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} \right) - \left(\begin{array}{c} \\ \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} - \left(\begin{array}{c} \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} - \left(\begin{array}{c} \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} - \left(\begin{array}{c} \\ \end{array} \right) - \left(\begin{array}{c} \\ \end{array} - \left(\end{array}) - \left(\end{array}) - \left(\end{array}) - \left(\begin{array}{c} \\ \end{array} - \left(\end{array}) - \left(\end{array}) - \left(\end{array}) - \left(\begin{array}{c} \\ \end{array} - \left(\end{array}) - \left$							
Entry	Х	R ₁	R_2	Base	T/min	Con./% ^b	TOF/h ⁻¹ c
1	Ι	-H	-H	Cs_2CO_3	10	99	15 390
2	Br	-H	-H	Cs_2CO_3	60	99	3961
3	Ι	$-NO_3$	-H	Cs_2CO_3	10	100	15546
4	Ι	$-\mathbf{F}$	-H	Cs_2CO_3	10	99	15 390
5	Ι	-OH	-H	Cs_2CO_3	10	99	15 390
6	Ι	-COOH	-H	Cs_2CO_3	10	97	15078
7	Ι	$-OCH_3$	-H	Cs_2CO_3	10	96	14925
8	Ι	$-CH_3$	-H	Cs_2CO_3	10	95	14769
9	Ι	$-NH_2$	-H	Cs_2CO_3	10	88	13 680
10	Ι	-COCH ₃	-H	Cs_2CO_3	10	53	8220
11	Ι	Н	- <i>n</i> Bu	Cs_2CO_3	10	90	13 992
12	Ι	Н	−tBu	Cs_2CO_3	10	Trace	—

 a Reaction conditions: 80 °C, ethanol (10 mL), iodobenzene or bromobenzene (0.5 mmol), phenylboronic acid (1 mmol), K₂CO₃ or Cs₂CO₃ (1 mmol), catalyst (10 mg or 25 mg), and reaction time (10 min or 60 min). b Determined by HPLC using pentamethylbenzene as internal standard. c TOF is defined as the moles of reacted aryl halide molecules per mole of the Pd atom in the catalyst per hour.

(a)Pd/meso-TiO₂/Pd, and (a)meso-TiO₂/Pd nanocatalysts were also synthesized according to the synthetic procedures illustrated in Scheme S1 (Fig. S8, ESI[†]). The catalytic performance of different nanocatalysts in Suzuki–Miyaura coupling reaction under various base, solvent, and temperature conditions (Tables S1–S4, ESI[†]) was investigated. (a)Pd/meso-TiO₂/Pd(a)meso-SiO₂ displays outstanding catalytic performance in the Suzuki–Miyaura coupling reaction of halogeno benzene and phenylboronic acid (Table 1, entries 1 and 2).^{3,28} 99% conversion of iodobenzene can be realized within 10 min, and the turnover frequency (TOF) can reach as high as 15 390 h⁻¹, higher than most of the previously reported heterogeneous catalysts.¹⁶ It also exhibits high bromobenzene conversion with a conversion of 99% and a TOF of 3961 h⁻¹ within 60 min.

For comparison, the catalytic performance of the contrasting @meso-TiO₂/Pd@meso-SiO₂, @meso-TiO₂/Pd@SiO₂, @Pd/ meso-TiO₂/Pd, and @meso-TiO₂/Pd nanocatalysts is also evaluated (Table S1, ESI[†]). It can be clearly seen that the "shell in shell" structured @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst exhibits higher catalytic activity than @meso-TiO2/Pd@meso-SiO2, (ameso-TiO2/Pd(aSiO2, (aPd/meso-TiO2/Pd, and (ameso-TiO2/Pd nanocatalysts. Combining with the Pd content in different catalysts, we deduce that the outstanding catalytic performance of the @Pd/meso-TiO₂/Pd@meso-SiO₂ nanocatalyst may be mainly ascribed to its unique structural configuration.²⁹ First, two independent chambers composed of double shells of TiO₂ and SiO₂ in the nanocatalyst can act as a nanoreactor to gather the reactants and further accelerate the catalytic reaction rate due to the confinement effect of microenvironments, which is proven by the absorption experiments (Fig. S9, ESI⁺). Second, the "shell-inshell" architecture also allows the Pd nanoparticles to be uniformly dispersed on the internal and external surfaces of the TiO₂ shell, which may enrich the active sites of PNPs and increase the contact area between reactants and catalysts to enhance the

synergy between PNPs and TiO2. In addition, the "shell-in-shell" @Pd/meso-SiO2/Pd@meso-SiO2 catalyst shows less leaching of Pd in comparison with the traditional catalyst (Table S5, ESI⁺). This suggests that the double-shell architecture of the @Pd/meso-TiO₂/ Pd@meso-SiO₂ catalyst may be effective in preventing the leaching of Pd from the internal and external surfaces of inner TiO₂ walls, which may be beneficial for the improvement of catalytic performance.²⁰ XPS results show that the PNPs in a double-shell nanoreactor exist in the valence state of Pd⁰ (Fig. S10, ESI[†]), which may possess superior catalytic activity. Third, the -OH group on the surface of the amorphous TiO₂ shell, as proven by FT-IR results (Fig. S11 and S12, ESI⁺), is in favor of catalyzing Suzuki-Miyaura coupling reaction.³⁰ Fourth, the mesoporous TiO₂ and SiO₂ shells facilitate the fast diffusion of reactants and products from the active sites on the TiO₂ shell, which is beneficial for heterogeneous catalysis according to the tests shown in Table S6 (ESI⁺).²⁷ Last, the large specific surface area can increase the exposure of the active component in the nanocatalysts, thus promoting the catalytic performance. Thus, the double-shell architecture can be expected to be a unique catalyst system for tuning the catalytic performance by manipulating its shell porosity, interstitial spaces, and configuration on micro- and nano-scales.³¹ In addition, various aryl iodides with different substituents are used to investigate the reaction scope of the @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst (Table 1, entries 2–10). The results show that the $(a)Pd/meso-TiO_2/$ Pd@meso-SiO2 nanocatalyst possesses outstanding catalytic performance for iodobenzene containing -CH3, -OCH3, -NH2, -NO3, -COOH, -F, -COCH₃ and -OH groups. The biaryl yields can reach 53-99% within 10 min. Meanwhile, according to the catalytic results shown in Table 1 (entries 11 and 12), we can infer that the mesopores in the SiO_2 shell may selectively make the reactants diffuse into the nanoreactor owing to the pore size and shape to achieve catalytic selectivity for different reactants depending on the reactant molecules.^{21,22} Due to the unique "shell-in-shell" architectural configuration, the "shell-in-shell" (aPd/TiO2/Pd(ameso-SiO2 nanocatalyst also shows super performance with high catalytic activity and stability for the reduction of 4-nitrophenol to 4-aminophenol (Fig. S13, ESI†).

We presented a well-controlled strategy to construct a novel mesoporous "shell-in-shell" @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst composed of mesoporous double TiO₂ and SiO₂ shells with PNPs uniformly distributed on the external and internal TiO₂ shell. The unique structural configuration endows the nanocatalyst with unusual features of large specific surface area, mesoporous TiO2 and SiO2 shells, two independent nanoreactors, good dispersity and decreased leaching of PNPs, and enhanced synergistic effects. These features can largely improve the catalytic activity and stability of the nanocatalyst, leading to extremely high catalytic activity for Suzuki Miyaura coupling and 4-nitrophenol reduction reactions with TOFs of 15390 h^{-1} and 760 h^{-1} , respectively for the mesoporous "shell-in-shell" @Pd/meso-TiO2/Pd@meso-SiO2 nanocatalyst. The catalytic stability is also superior with the conversion remaining over 89% even after ten cycles of catalytic reaction for 4-nitrophenol reduction. The synthetic methodology may provide an effective route to create highly efficient

nanocatalysts. As the synthetic procedures involve multi-steps, the simplification of the synthetic process is under investigation and will be addressed elsewhere.

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