## CATALYTIC BEHAVIOR OF BORIA-ALUMINA PREPARED BY CHEMICAL VAPOR DEPOSITION TECHNIQUE

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Catalytic behavior of boria-alumina greatly changed with  $B_2O_3$  content. When  $B_2O_3 \le 12$  wt%, both boria-aluminas ( $H_0 \ge -8.2$ ) obtained by CVD and impregnation methods showed almost the same catalytic activity, but at higher  $B_2O_3$  contents ( $\ge 15$  wt%,  $H_0 \ge -3.0$ ) the CVD boria-alumina exhibited higher catalytic efficiency, e.g. for the vapor-phase Beckmann rearrangement of cyclohexanone oxime.

Boria-alumina is a solid acid which catalyzes the Beckmann rearrangement of cyclohexanone oxime<sup>1)</sup> and the hydrocarbon conversion reactions such as toluene disproportionation and xylene isomerizastion.<sup>2)</sup> Boria-alumina is usually obtained by impregnating  $\gamma$ - or  $\eta$ -alumina with aqueous boric acid followed by calcination. We have recently reported that the chemical vapor deposition technique (CVD) using B(OEt)<sub>3</sub> is very useful to prepare a solid acid boria-silica in which B<sub>2</sub>O<sub>3</sub> is uniformly and densely dispersed on the surface of silica.<sup>3)</sup> In comparison with the boria-alumina prepared by impregnation method (IMP), we now describe an interesting feature of the CVD boria-alumina revealed in the acid catalysis for *m*-xylene isomerization and vapor-phase Beckmann rearrangement of cyclohexanone oxime which require different optimal acid strengths to proceed effectively.

The CVD boria-alumina was prepared by bringing  $B(OEt)_3$  vapor into contact with 24-60 mesh granules of  $\gamma$ -alumina  $(JRC^4)$ -ALO-1, 0.5 g, surface area 160 m<sup>2</sup> g<sup>-1</sup>, pore volume 0.67 ml g<sup>-1</sup>) at 300 °C for 0.5-5.0 h in the presence of air; the flow rates of  $B(OEt)_3$  and air were 3.5 mmol h<sup>-1</sup> and 113 ml h<sup>-1</sup>, respectively.  $B_2O_3$  content, which was determined by the alkalimetric titration method using mannitol, attained the maximum value of 33 wt% at 5.0 h of CVD treatment. The test reactions were performed in a flow system which was equipped with a Pyrex glass reactor containing 0.2 g of catalyst. The IMP boria-alumina was calcined at 300 °C for 2 h prior to the use in the Beckmann rearrangement of cyclohexanone oxime, and both CVD and IMP boria-aluminas were pretreated at 500 °C for 3 h in the case of the isomerization of *m*-xylene. Concerning the rearrangement reaction, an activity declining owing to coking was observed for every catalyst tested, and hence the catalytic efficiency was evaluated on the basis of the initial average oxime conversion and lactam selectivity at 3-4 h after the feed of reactant was initiated.

Figure 1 illustrates the catalytic performance of boria-alumina in the isomerization of *m*-xylene. At a  $B_2O_3$  content of less than 12 wt%, both CVD and IMP boria-aluminas were almost the same in catalytic efficiency: conversion,

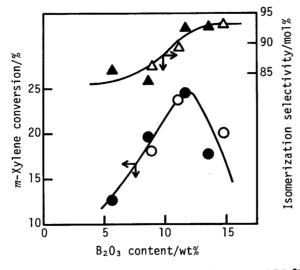


Fig. 1. *m*-Xylene isomerization at 450 °C  $W/F=41.0 \text{ g-cat h mol}^{-1}$ ; **O**,  $\Delta$ : CVD;  $\bullet$ ,  $\blacktriangle$ : IMP

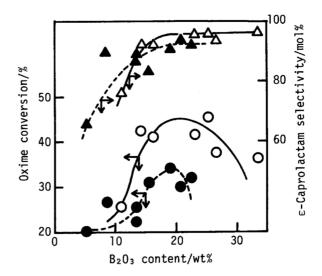


Fig. 2. Beckmann rearrangement at 250 °C W/F=143 g-cat h mol<sup>-1</sup>; oxime: $C_6H_6:N_2=$ 1:13:16;  $\bigcirc$ ,  $\triangle$ : CVD;  $\bigcirc$ ,  $\blacktriangle$ : IMP

selectivity (85-93 mol%) and p-/o-xylene isomer ratio (1.1-1.3). On the other hand, as shown in Fig. 2, at a B203 content of more than 15 wt%, the CVD boriaalumina exhibited higher efficiency than the IMP boria-alumina in catalyzing the Beckmann rearrangement. The same catalytic behavior of CVD and IMP boria-aluminas observed in the isomerization reaction can reasonably be explained by assuming that, until  $B_2O_3$  content does not exceed 12 wt%, all of the  $B_2O_3$  introduced form a surface compound by reacting with alumina independent of the preparation method to develop the strong Broensted acid sites ( $H_{0} \ge -8.2$ ) which can effectively catalyze the isomerization.<sup>2,5)</sup> At a  $B_2O_3$  content of more than 15 wt%, the acid sites of free  $B_2O_3$  ( $H_0 \ge -3.0$ ) which can selectively catalyze the rearrangement reaction become to dominate over the strong Broensted acid sites, and the maximum oxime conversions were attained at B203 contents of between 20 and 25 wt%. It was confirmed by XRD measurement that the characteristic diffraction lines of  $B_2O_3$ appeared at  $2\theta=14.5$  and  $28.0^{\circ}$  when  $B_2O_3$  content exceeded about 20 wt%. In contrast to the CVD technique, IMP method was inadequate to give the boria-alumina having a high  $B_2O_3$  content of more than 15 wt%, because large crystals of boric acid were deposited on the surface of alumina. Thus the higher catalytic efficiency of CVD boria-alumina revealed in the rearrangement reaction is probably due to the uniform dispersion of  $B_2O_3$  on the surface of alumina which was brought about by applying CVD technique. The study to elucidate the difference in acid property between CVD and IMP boria-aluminas at higher  $B_2O_3$  contents is now under way.

## References

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