## Effects of Sodium Tetraborate as an Additive on the Reaction of a-Alumina with Sodium Carbonate

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Effects of sodium tetraborate as an additive in the reaction of  $\alpha$ -alumina with molten sodium carbonate have been studied mainly in a N<sub>2</sub> atmosphere. Addition of sodium tetraborate accelerates the reaction, the  $\alpha$ -alumina reacted increasing from 31.7% to 99.3% by addition of sodium tetraborate corresponding to the initial B<sub>2</sub>O<sub>3</sub>/Na<sub>2</sub>O molar ratio of only 1/15 under the other same conditions. By means of the Jander equation the activation energy was found to be 53 kcal/mol for the  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system. X-Ray diffraction and thermal data were analyzed in relation to the phase equilibrium of the melt.

Production of alumina from resources other than bauxite is becoming important. A number of reports have appeared on the production of alumina from various low-grade sources such as clay, aluminous shale, anorthosite, nephelite, etc.<sup>1-8)</sup>

A lime-soda sinter process is one of the most important methods for extracting alumina from low-grade sources to which the Bayer process can not be applied because of high silica content. Raw materials reacted with molten sodium carbonate form sodium aluminate which is soluble in both acidic and basic aqueous solutions. The reaction of various types of alumina with sodium carbonate is fundamental in the complex lime-soda sinter process.

In a previous paper the lime-soda sinter process was discussed with use of Korean diaspore, cyanite and kaolinite as starting materials.<sup>9)</sup> Christie *et al.* studied the reaction rate of  $\alpha$ -alumina with sodium carbonate in relation to gasification of coal in melts containing sodium carbonate, showing that the reaction process is considerably hindered by diffusion.<sup>10)</sup>

Sodium tetraborate is often used as a flux for the decomposition of minerals by molten Na<sub>2</sub>CO<sub>3</sub>. The purpose of the present work is to clarify the promoting action of sodium tetraborate on the reactivity of α-alumina with sodium carbonate.

## **Experimental**

Reagent grade  $\alpha$ -alumina was ground and sized into -150 -+200 mesh (No. 1) and -200 mesh (No. 2). The specific surface area of No. 2 was found to be  $0.90 \, \mathrm{m}^2/\mathrm{g}$  by the BET method. Reagent grade anhydrous sodium carbonate and sodium tetraborate decahydrate (borax) were dried at  $500 \, ^{\circ}\mathrm{C}$  for 1 h. Nitrogen and oxygen were purified by the usual methods. Other materials were of reagent grade and used without further purification.

The percentage of  $\alpha$ -alumina reacted with sodium carbonate,  $\eta$ , was determined as follows: Samples in a platinum boat were laid in an electric furnace at 900—1250 °C. The sinter was cooled down to room temperature as fast as possible in  $N_2$  gas, and leached with hot  $1 \text{ mol/dm}^3$  HCl solution for 30 min. The leachate was filtered. Al(OH)<sub>3</sub> was precipitated by adding aqueous ammonia to the filtrate and weighed in the form of  $Al_2O_3$  after heating. The value of  $\eta$  was calculated from the weight of alumina leached.

## Results and Discussion

Effect of Gas Atmosphere. α-Alumina reacts with sodium carbonate to form sodium aluminate:

$$Al_2O_3(s) + Na_2CO_3(1) = 2NaAlO_2(s) + CO_2(g).$$
 (1)

From the large negative value of Gibbs free energy for this reaction<sup>11)</sup> α-alumina is expected to react completely with molten Na<sub>2</sub> CO<sub>3</sub> at temperatures above 900 °C. However, the experimental results (Fig. 1)

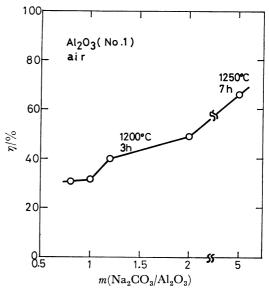


Fig. 1. Variation of the percents of α-alumina reacted with initial Na<sub>2</sub>CO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub> molar ratio.

indicate that the reaction is not complete in the air. For example, the value of  $\eta$  was found to be low at 66% even for the initial molar ratio(m) 5 of Na<sub>2</sub>CO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub> and reaction time 5 h at 1250 °C. The sinters obtained in the air were colored brown, the Pt boat containing the sinter being considerably corroded. In spite of the disappearance of  $\alpha$ -alumina in X-ray diffraction patterns of the sample sintered for a long time, the value of  $\eta$  was much lower than 100% (Fig. 3a).

Maegawa found that the atmosphere influences the sintering process, and that  $H_2O$  gas atmosphere enhances the rate of reaction of  $\alpha$ -alumina with sodium carbonate in comparison with  $O_2$ ,  $H_2+CO$ , or  $CO_2$  gas atmos-

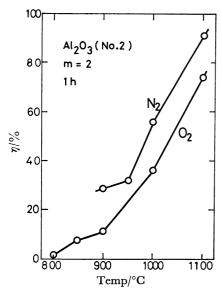


Fig. 2. Difference between the effect of N<sub>2</sub> and O<sub>2</sub> gas atmospheres on the reaction of Al<sub>2</sub>O<sub>3</sub> with Na<sub>2</sub>CO<sub>3</sub>.

phere. Pigure. 2 shows changes in the  $\eta$  values with reaction temperature in purified  $N_2$  and  $O_2$  with constant flow rates of 80 ml/min. The values of  $\eta$ 

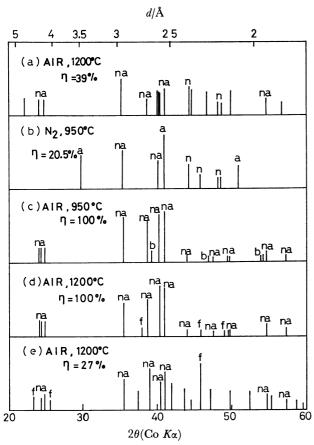


Fig. 3. X-Ray diffraction data for the sinters obtained under conditions as follows: (a)  $\alpha$ -Al $_2$ O $_3$  (No.1)+Na $_2$ -CO $_3$ , m=5 (b)  $\alpha$ -Al $_2$ O $_3$  (No. 1)+Na $_2$ CO $_3$ , m=2 (c)  $\alpha$ -Al $_2$ O $_3$  (No.1)+Na $_2$ CO $_3$ +Na $_2$ B $_4$ O $_7$ , m=1.7 and n=1/15 ( $X_{\rm B,O_1}\!=\!0.053)$  (d)  $\alpha$ -Al $_2$ O $_3$  (No. 1)+Na $_2$ CO $_3$ +AlF $_3$  (20 wt%), m=2 (e)  $\alpha$ -Al $_2$ O $_3$  (No. 1)+Na $_2$ CO $_3$ +AlF $_3$  (20 wt%), m=1, 1 Å=0.1 nm.

obtained in  $O_2$  were found to be lower than those obtained in  $N_2$ , the corrosion of the Pt boat being much enhanced in  $O_2$ . The sinter obtained in  $N_2$  remained white with no corrosion of the Pt boat; those obtained in  $O_2$  were colored red-brown as in the air. The same results were obtained when a Ni boat was used. By comparing Fig. 3a with 3b, we see that there are compounds other than  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(a), Na<sub>2</sub>CO<sub>3</sub>(n), and NaAlO<sub>2</sub>(na). Carbon dioxide, <sup>10)</sup> as well as O<sub>2</sub> seems to hinder the sinter process.

Effect of Additives. Sodium tetraborate and aluminium fluoride were used as additives to facilitate Reaction 1. Addition of sodium tetraborate was found to be very effective (Fig. 4). The greater the initial

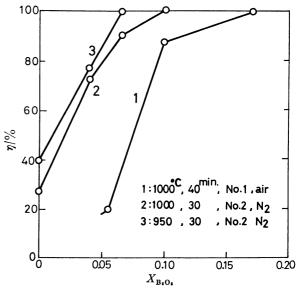


Fig. 4. Effect of the addition of borax on the reaction of α-Al<sub>2</sub>O<sub>3</sub> with Na<sub>2</sub>CO<sub>3</sub>.

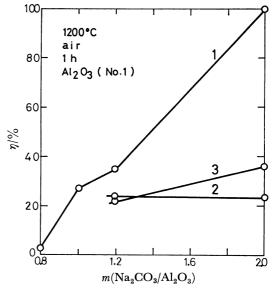


Fig. 5. Effect of the addition of AlF3 and NaF on the reaction of Al2O3 with Na2CO3. Curve 1;  $\alpha\text{-Al}_2O_3+Na_2CO_3+AlF_3$  (20 wt%), 2;  $\alpha\text{-Al}_2O_3+Na_2CO_3+NaF(20 \text{ wt%}),$  3;  $\alpha\text{-Al}_2O_3+Na_2-CO_3$ .

 $B_2O_3/Na_2O$  molar ratio(n), the greater the effect. The sinters to which sodium tetraborate had been added remained white, causing no corrosion of the Pt boat. The sinter having  $\eta = 100\%$  obtained for the  $Al_2O_3-Na_2CO_3-Na_2B_4O_7$  system gave only the diffraction patterns of  $NaAlO_2$  and probably sodium borate(b) (Fig. 3c).

The effects of  $AlF_3$  and NaF as additives were also studied. The effect of  $AlF_3$  on Reaction 1 depends a great deal on the value of m (Fig. 5). When 20 wt%  $AlF_3$  was added to a mixture with m of 2.0, the value of  $\eta$  increased from 36% to 100%. Aluminium fluoride reacts with molten  $Na_2CO_3$  partly to form  $NaAlO_2$ :

$$AlF_3 + 2Na_2CO_3 = 3NaF + NaAlO_2 + 2CO_2,$$
 (2)

$$AlF_3 + 3NaF = Na_3AlF_6. (3)$$

If all the AlF<sub>3</sub> added were converted into NaF, the effect of NaF would be observed similar to that of AlF<sub>3</sub>. However, this was not the case (Fig. 5). X-Ray diffraction analysis of the sinter obtained in the case of m=2 and  $\eta=100\%$  showed the presence of NaAlO<sub>2</sub> and a fluoride compound(f), probably Na<sub>3</sub>AlF<sub>6</sub>. In the case of m=1 and  $\eta=27\%$ ,  $\eta$  was found to be low, in spite of the absence of the diffraction pattern for  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>. This suggests that  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> might merely dissolve in Na<sub>3</sub>AlF<sub>6</sub> formed by the reaction of AlF<sub>3</sub> with Na<sub>2</sub>CO<sub>3</sub>.

Reaction Rate as a Function of Temperature. Figures 6 and 7 show changes in  $\eta$  with reaction time, t, at three temperatures for  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>(m=2) and  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub>(m=2 and n=1/15).

Since a protective layer of sodium aluminate having very low solubility in molten Na<sub>2</sub>CO<sub>3</sub>,<sup>10</sup>) is formed on alumina, the diffusion of CO<sub>3</sub><sup>2-</sup> ion through the sodium aluminate layer would be the rate-determining step.<sup>10</sup>,<sup>12</sup>) The results were analyzed by means of the Jander equation

$$[1 - (1 - \eta)^{1/3}]^2 = kt, \tag{4}$$

$$k = \frac{2DC_0}{\rho r_0^2},\tag{5}$$

where k is a rate constant, D diffusion coefficient,  $C_0$  the concentration of  $\mathrm{CO_3}^{2-}$  ion in the bulk,  $\rho$  is the density of

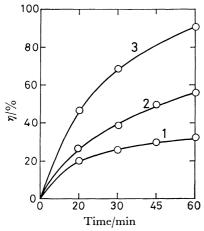


Fig. 6. Changes in the percents of  $\alpha$ -alumina reacted vs. time in the N<sub>2</sub> atmosphere for  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system (m=2).

Curve 1: 950 °C, 2: 1000 °C, 3: 1100 °C.

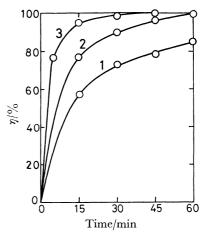


Fig. 7. Changes in the percents of α-alumina reacted vs. time in the N<sub>2</sub> atmosphere for α-Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> system (m=2, n=1/15).
Curve 1: 900 °C, 2: 950 °C, 3: 1000 °C.

NaAlO<sub>2</sub> layer (2.72 g/cm<sup>3</sup>), and  $r_0$  the average size of  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> (0.28  $\mu$ m) calculated from the special area of 0.09 m<sup>2</sup>/g. Figures 8 and 9 show linear relationships,

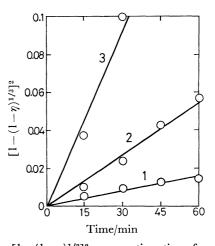


Fig. 8.  $[1-(1-\eta)^{1/3}]^2$  vs. reaction time for α-Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system. 1: 950 °C, 2: 1000C°, 3: 1100 °C.

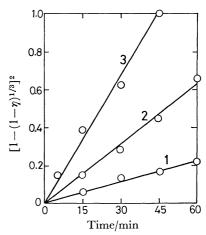


Fig. 9.  $[1-(1-\eta)^{1/3}]^2$  vs. reaction time for α-Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> system. 1: 900 °C, 2: 950 °C, 3: 1000 °C.

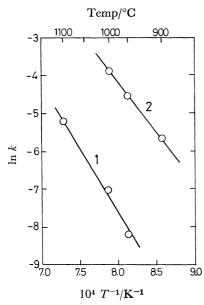


Fig. 10. Variation of rate constant, k, with temperature. 1:  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system, 2:  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> system.

the slopes giving the k values. At 1000 °C the k value for  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> system is larger by ca. 11 times than that for  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system. Figure 10 shows Arrhenius-type plots of k vs.  $10^4/T$ . The activation energy calculated from the slopes is 53 kcal/mol for the former, lower by 10 kcal/mol than that for the latter (kcal means kcal<sub>th</sub>; 1 kcal<sub>th</sub>=4184 J). For the Arrhenius activation energy for the reaction of  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> with Na<sub>2</sub>CO<sub>3</sub>, Christie et al.<sup>10</sup> and Maegawa et al.<sup>12</sup>) reported the values of 62±3 and 58.8 kcal/mol, respectively, which agree with our results.

Discussion on the Effect of Sodium Tetraborate as an Additive. Molten  $Na_2CO_3$  is completely ionized and consists of species such as  $Na^+$ ,  $CO_3^{2-}$ , and ion pair  $(Na^+CO_3^{=})^-$ , the dissociation of  $CO_3^{2-}$  into  $CO_2$  and  $O^{2-}$  ion being finite at temperatures above melting point. Thus the reaction of  $\alpha$ -alumina with  $Na_2CO_3$  can be expressed by a series of elementary steps as follows:

$$Na_2CO_3(1) = Na^+(1) + (Na^+CO_3^-)^-(1),$$
 (6)

$$(Na^+CO_3^-)^-(1) = Na^+(1) + CO_3^{2-}(1),$$
 (7)

$$CO_3^{2-}(1) = O^{2-}(1) + CO_2(g),$$
 (8)

$$Al_2O_3(s) + O^{2-}(1) = 2AlO_2^{-}(1),$$
 (9)

$$Na^{+}(1) + AlO_{2}^{-}(1) = NaAlO_{2}(s).$$
 (10)

According to the Lux-Flood concept of basicity of oxides, <sup>14,15)</sup> a base is defined as an oxide donor and an acid as an oxide acceptor:

$$(acid) + O^{2-} = (base)$$
 (11)

The reaction of  $\alpha$ -alumina with sodium carbonate might be the neutralization between acidic  $Al_2O_3$  and basic  $Na_2O$ . Thus  $pO^{2-}[i.e.-\log a(O^{2-})]$  was chosen as a scale of basicity. According to the calculation of the relative basicity of oxides by Yagisawa *et al.*,  $B_2O_3$  is more acidic than  $Na_2O$  and  $Al_2O_3$ .<sup>16)</sup> Duffy and Ingram,<sup>17)</sup> who presented a concept of optical basicity for the melt, reported that an increase in  $B_2O_3$  content lowers the basicity of  $Na_2O-B_2O_3$  melt;  $B_2O_3$  has a

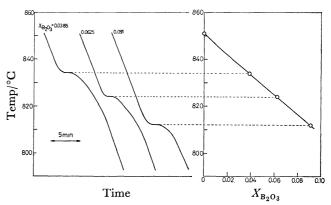


Fig. 11. Cooling curves for mixed melts of  $Na_2CO_3$  and  $Na_2B_4O_7$ , and the melting points vs.  $X_{B_2O_3}$ .

tendency to consume O<sup>2-</sup> ion:

$$B_2O_3 + 5O^{2-} = 2BO_4^{5-}$$
 (12)

It is thus concluded that the effect of the addition of sodium tetraborate is not caused by the increase in the basicity of the melt.

The phase diagram of Na<sub>2</sub>O-B<sub>2</sub>O<sub>3</sub> system has been reported only for the region  $B_2O_3 \ge 50\%$ . 18) sodium borates such as  $5Na_2O \cdot B_2O_3$ ,  $2Na_2O \cdot B_2O_3$ , and  $3Na_2O \cdot B_2O_3$  are known in the region  $B_2O_3 \le 50\%$ . Figure 11 shows cooling curves for Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> Addition of sodium tetraborate to sodium carbonate give rise to the lowering of solidification point of the melt in proportion to the molar fraction of B<sub>2</sub>O<sub>3</sub>. With the progress of Reaction 1, the concentration of B<sub>2</sub>O<sub>3</sub> in the melt increases as a result of consumption of Na<sub>2</sub>CO<sub>3</sub>, lowering the melting point; the nearer the reaction approaches 100% completion, the greater the lowering in melting point. The activation energy for diffusion is approximately proportional to melting point.19) The activation energy for the  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>B<sub>4</sub>O<sub>7</sub> system, having lower melting points, was found to be lower by 10 kcal/mol than for the α-Al<sub>2</sub>O<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system. The lowering of the melting point results in the lowering of the viscosity of the melt, promoting the contact of α-alumina with the melt and the diffusion of CO<sub>3</sub><sup>2-</sup> and/or (Na+CO<sub>3</sub><sup>=</sup>)-ion(s) through a porous layer of NaAlO2 formed on the surface of α-alumina.

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