

# Hydrophobic and Electronic Properties of the E-MoS<sub>2</sub> Nanosheets Induced by FAS for the CO<sub>2</sub> Electroreduction to Syngas with a Wide Range of CO/H<sub>2</sub> Ratios

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The electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) to produce CO and H<sub>2</sub> (syngas) is a promising method for clean energy, but challenges remain, such as controlling the CO/H<sub>2</sub> ratios required for the syngas yield. Herein, hydrophobic exfoliated MoS<sub>2</sub> (H-E-MoS<sub>2</sub>) nanosheets are fabricated from bulk MoS<sub>2</sub> by a cost-effective ball-milling method, followed by decoration with fluoro-silane (FAS). H-E-MoS<sub>2</sub> is a cost-effective electrocatalyst capable of directly reducing CO<sub>2</sub> and H<sub>2</sub>O for tuneable syngas production with a wide range of CO/H<sub>2</sub> ratios (from 1:2 to 4:1). In addition, H-E-MoS<sub>2</sub> shows a high current density, 61 mA cm<sup>-2</sup> at -1.1 V, and the highest CO FE of 81.2% at -0.9 V, which are higher than those of unmodified MoS<sub>2</sub>. According to density functional theory calculations, FAS decoration on the surface of MoS<sub>2</sub> electrode can change the electronic properties of the edge Mo atom, which facilitates the rate-limiting CO-desorption step, thus promoting CO<sub>2</sub>RR. Moreover, the hydrophobic surface of H-E-MoS<sub>2</sub> depressed the H<sub>2</sub> evolution reaction and created abundant three-phase contact points that provided sufficient CO<sub>2</sub>. The hydrophobization of the electrode may provide an effective strategy for easily tuning the CO/H<sub>2</sub> ratio of syngas in a large range for the direct electroreduction CO<sub>2</sub> to syngas with an optimized CO/H<sub>2</sub> ratio.

which not only require harsh conditions, but increase the consumption of fossil fuel. Owing to its abundance, availability, and nontoxicity, CO<sub>2</sub> can be regarded as an ideal chemical feedstock. Great effort has therefore been devoted to developing an effective strategy that can beneficially use CO<sub>2</sub> to produce valuable chemicals, and thereby significantly mitigate energy consumption and environmental impact. Among the advanced CO<sub>2</sub> conversion methods, the electrochemical carbon dioxide reduction reaction (CO<sub>2</sub>RR) is promising since it provides a facile route for converting CO<sub>2</sub> to CO,<sup>[2]</sup> and other valuable chemicals.<sup>[3]</sup> The linear CO<sub>2</sub> molecule is extremely stable and CO<sub>2</sub>RR is kinetically sluggish, in need of a high overpotential for conversion, which leads to low Faradaic efficiency (FE) and selectivity. Meanwhile, the simultaneous hydrogen evolution reaction (HER) is ubiquitous during CO<sub>2</sub>RR in aqueous electrolytes under cathodic polarization.<sup>[3]</sup> Thus, there

## 1. Introduction

Synthesis gas (syngas), a gas mixture consisting primarily of carbon monoxide (CO) and hydrogen (H<sub>2</sub>), is a versatile industrial feedstock for producing various hydrocarbons through the Fischer–Tropsch process.<sup>[1]</sup> The ratio of syngas is crucial for maximizing the product yield. Conventionally, syngas is predominantly produced from the gasification of solid coal and petroleum coke, or the steam reforming of natural gas,

has been significant interest in the rational design and synthesis of CO<sub>2</sub>RR electrocatalysts capable of tuning CO<sub>2</sub>RR and HER rates for direct syngas production.<sup>[4]</sup> The direct electrochemical reduction of CO<sub>2</sub> to syngas would be more efficient, simpler, and faster, can be used directly in the Fischer–Tropsch process and can convert conventional electricity to chemical energy.

To date, a variety of materials have been explored for the electrochemical reduction of CO<sub>2</sub> into syngas, including Pd/C,<sup>[5]</sup> CdS<sub>x</sub>Se<sub>1-x</sub>,<sup>[6]</sup> Cu/(NiOH)<sub>2</sub>,<sup>[7]</sup> and others.<sup>[8–10]</sup> For example, Chen and co-workers<sup>[5]</sup> successfully fabricated syngas with controlled CO/H<sub>2</sub> ratios between 1:4 and 1:1.25 using precious metal palladium nanoparticles supported on carbon (Pd/C). The catalysis was attributed to a weakening of the binding energy for both adsorbed CO and H, caused by PdH from Pd. Zheng and co-workers<sup>[7]</sup> developed a novel ultrathin Cu/(NiOH)<sub>2</sub> hydride with a Cu(0)-enriched surface that enabled the electrochemical conversion of CO<sub>2</sub> and H<sub>2</sub>O into syngas with CO/H<sub>2</sub> ratios of 1:9 to 9:1 at potentials ranging from -0.4 to -1.0 V (vs reversible hydrogen electrode (RHE)). Considering practical applications, therefore, there is an urgent need to develop earth-abundant and easily prepared catalysts on a large scale for

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CO<sub>2</sub>RR into syngas. Recently, transition metal chalcogenides have been emerging as cost-effective promising electrocatalysts for CO<sub>2</sub>RR due to their prominent catalytic features.<sup>[8–11]</sup> For instance, Asadi et al.<sup>[9]</sup> uncovered that MoS<sub>2</sub> with Mo-terminated edges, formed by chemical vapor deposition, exhibited superior performance in the electroreduction of CO<sub>2</sub> to CO, with a high FE (95%), a high current density of 60.5 mA cm<sup>-2</sup> at -0.8 V (vs RHE), and a low overpotential (54 mV). Abbasi<sup>[10]</sup> reported that 5% niobium (Nb)-doped vertically aligned MoS<sub>2</sub> was used as a catalyst for CO<sub>2</sub>RR, in which Nb near the Mo edge atoms could enhance CO formation by modifying the binding energies of intermediates to MoS<sub>2</sub> edge atoms. Ren et al.<sup>[11]</sup> fabricated an integrated 3D TiO<sub>2</sub>@MoS<sub>2</sub> architecture for CO<sub>2</sub> electroreduction that displayed a maximum FE of 82% for CO at 0.7 V and a large partial current density of 68 mA cm<sup>-2</sup>. Zhang et al.<sup>[12]</sup> demonstrated that amorphous molybdenum sulfide (MoS<sub>x</sub>) on a polyethylenimine (PEI)-modified rGO substrate could be a highly efficient and selective electrocatalyst for the electroreduction of CO<sub>2</sub> to CO, which reached a maximum FE of 85.1% at 0.65 V (RHE). The PEI layer has been demonstrated to enhance the catalytic activity of the MoS<sub>x</sub> by suppressing HER and stabilizing the CO<sub>2</sub> intermediate during CO<sub>2</sub> reduction. Moreover, Xie and co-workers<sup>[13]</sup> showed that MoSeS alloy monolayers catalyzed the conversion of CO<sub>2</sub> and H<sub>2</sub>O into syngas with the highest FE (45.2% for CO and 51.3% for H<sub>2</sub>) by regulating off-centre charge around the Mo atoms in the alloys. Theoretical calculations showed that the partially delocalized charge around Mo atoms could stabilize the COOH\* intermediate and facilitate the rate-limiting CO desorption step. Notably, Zeng et al.<sup>[6]</sup> displayed novel work: constructed cadmium sulfoselenide (CdS<sub>x</sub>Se<sub>1-x</sub>) alloyed nanorods produced syngas with the widest range of the CO/H<sub>2</sub> ratios (from 1:4 to 4:1) by regulating the Se content from 0 to 1. Although significant progress has been made in CO<sub>2</sub> electroreduction, cost-effective and sustainable syngas production with a broad H<sub>2</sub>/CO ratio for optimum production remains a significant challenge for practical applications. Moreover, understanding the exact mechanism for CO<sub>2</sub> electroreduction toward the valuable products is widely desirable.

Here, inspired by the superhydrophobic properties of electrodes with enhanced catalytic performance, we developed a hydrophobic exfoliated MoS<sub>2</sub> (H-E-MoS<sub>2</sub>) nanosheet electrode for CO<sub>2</sub>RR, fabricated by a simple refloating method of the exfoliated MoS<sub>2</sub> (E-MoS<sub>2</sub>) nanosheets on glassy carbon electrodes, followed by the decoration of fluorosilane (FAS) on the surface of the electrode to fabricate a hydrophobic surface. The large-scale E-MoS<sub>2</sub> nanosheets with a high concentration (6.2 mg mL<sup>-1</sup>) were directly fabricated from bulk MoS<sub>2</sub> by a facile, cost-efficient, and scalable ball-milling method,<sup>[14]</sup> which provides an opportunity for their practical application. After decoration with FAS, the H-E-MoS<sub>2</sub> nanosheets displayed a hydrophobic property with a water contact angle (CA) of 135.6° ± 1.9°. Here, all the products were CO and H<sub>2</sub>, as observed by glass carbon (GC). The H-E-MoS<sub>2</sub> attained the highest FE (81.2% for CO production) at -0.9 V (vs RHE) in EMIM-BF<sub>4</sub> aqueous solution (94 mol% water), significantly larger than that for E-MoS<sub>2</sub> (41.2%) and other reported analogues.<sup>[5,6,13]</sup> Note that the H-E-MoS<sub>2</sub> electrode produced syngas with tuneable CO/H<sub>2</sub> ratios between 1:2 and 4:1 by controlling

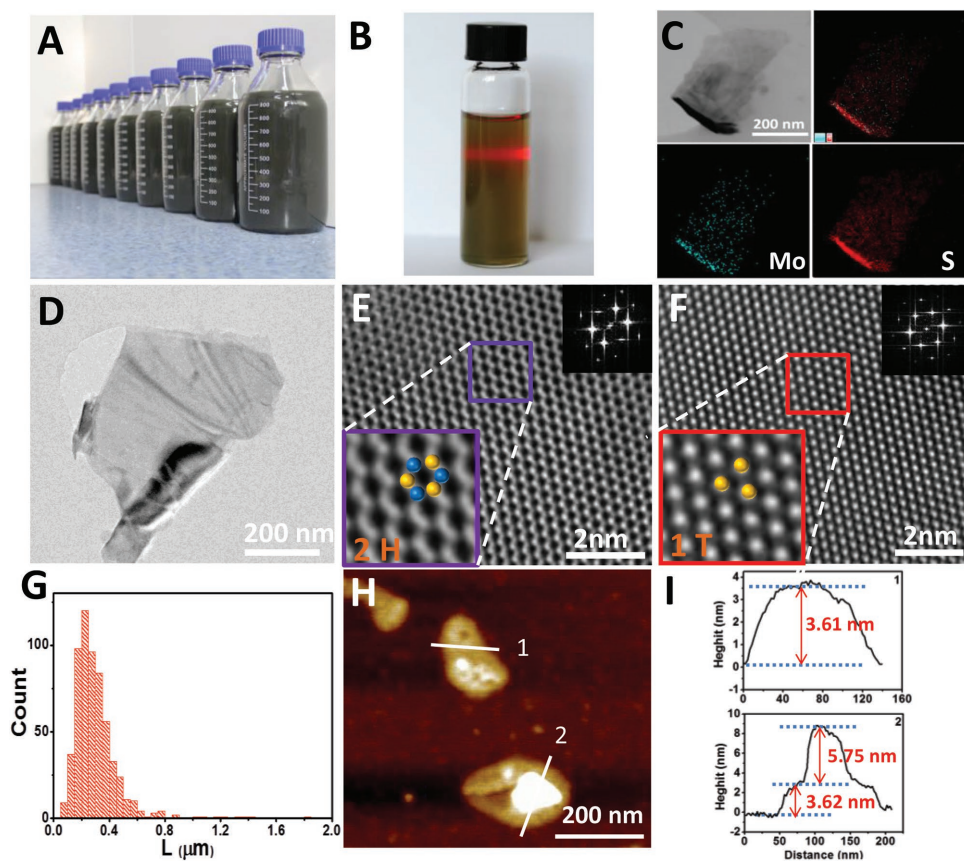
the potential, which is a greater range than that of E-MoS<sub>2</sub>. Moreover, the HER was obviously suppressed even at a potential of -1.1 V due to the hydrophobicity of the electrode. To verify these results, we performed density functional theory (DFT) calculations to investigate the CO<sub>2</sub>RR performance and HER activity on E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> surfaces. The calculation results showed that the FAS decoration of H-E-MoS<sub>2</sub> could change the electronic properties of the MoS<sub>2</sub> layer, which effectively decreased the energy barrier (0.72 eV, compared to 1.32 eV for E-MoS<sub>2</sub>) of the electrode, which may suppress hydrogen evolution and also bring sufficient CO<sub>2</sub> to the surface of the electrode, thereby enhancing CO<sub>2</sub> electroreduction to syngas and broadening the H<sub>2</sub>/CO ratio. The work presented a facile, low-cost, and effective strategy for the rational design of catalysts for the electroreduction of CO<sub>2</sub> to syngas.

## 2. Results and Discussion

### 2.1. Preparation and Characterization of Bulk-MoS<sub>2</sub> and E-MoS<sub>2</sub>

The few-layer E-MoS<sub>2</sub> nanosheets were fabricated by high-energy ball milling of bulk MoS<sub>2</sub> powder dispersed in *N*-vinyl pyrrolidone (NVP) with an initial concentration of 16 mg mL<sup>-1</sup>, as illustrated in Figure S1 of the Supporting Information. The NVP was used as a solvent because its surface free energy is very close to that of MoS<sub>2</sub>,<sup>[15]</sup> so the MoS<sub>2</sub> sheets could be easily exfoliated to obtain a maximal concentration by ball milling with a large zirconium oxide (ZrO<sub>2</sub>) ball (2 mm diameter) and a small ZrO<sub>2</sub> ball (0.2 mm diameter). After exfoliation for 18 h, the dark green colored dispersion was centrifuged at 550 rpm (centrifugation force 30 N) for 45 min to remove unexfoliated MoS<sub>2</sub>. As shown in Figure 1A, large-volume E-MoS<sub>2</sub> nanosheet dispersions were obtained, indicating that ball-milling is a well-established industrial grinding technique for the exfoliation of 2D layered materials. The concentration of the as-prepared E-MoS<sub>2</sub> dispersion was calculated to be 6.2 mg mL<sup>-1</sup>, and the yield was as high as 50.7%, much higher than what has been obtained by shear exfoliation of an MoS<sub>2</sub> dispersion (C = 0.5 mg mL<sup>-1</sup>, yield = 1%),<sup>[16]</sup> ultrasonic exfoliation of an MoS<sub>2</sub> dispersion (C = 0.3 mg mL<sup>-1</sup>, yield = 30%),<sup>[12]</sup> and other techniques<sup>[17–21]</sup> (Figure S2, Supporting Information). Moreover, the liquid exfoliation process (18 h) was faster than ultrasonic exfoliation (usually more than 100 h).<sup>[18]</sup> The dilute E-MoS<sub>2</sub> dispersion displayed an obvious Tyndall effect (Figure 1B), suggesting the successful exfoliation of the bulk material. We deduced that the bulk MoS<sub>2</sub> particles were fragmented and exfoliated to form the small and thin MoS<sub>2</sub> nanosheets by compression and shear forces of the rotating ZrO<sub>2</sub> balls during the milling process,<sup>[22]</sup> as demonstrated in Figures S3 and S6 of the Supporting Information.

The morphology of the E-MoS<sub>2</sub> was characterized by scanning electron microscopy (SEM), transmission electron microscopy (TEM), high-resolution TEM (HRTEM), and atomic force microscopy (AFM). The TEM image of the E-MoS<sub>2</sub> (Figure 1C) indicated a thin nanosheet with a length of 583 nm and crimp at the edge. Its elemental mapping showed a homogeneous distribution of sulfur and molybdenum, confirming its chemical composition. Figure 1D shows that the E-MoS<sub>2</sub> appeared to be

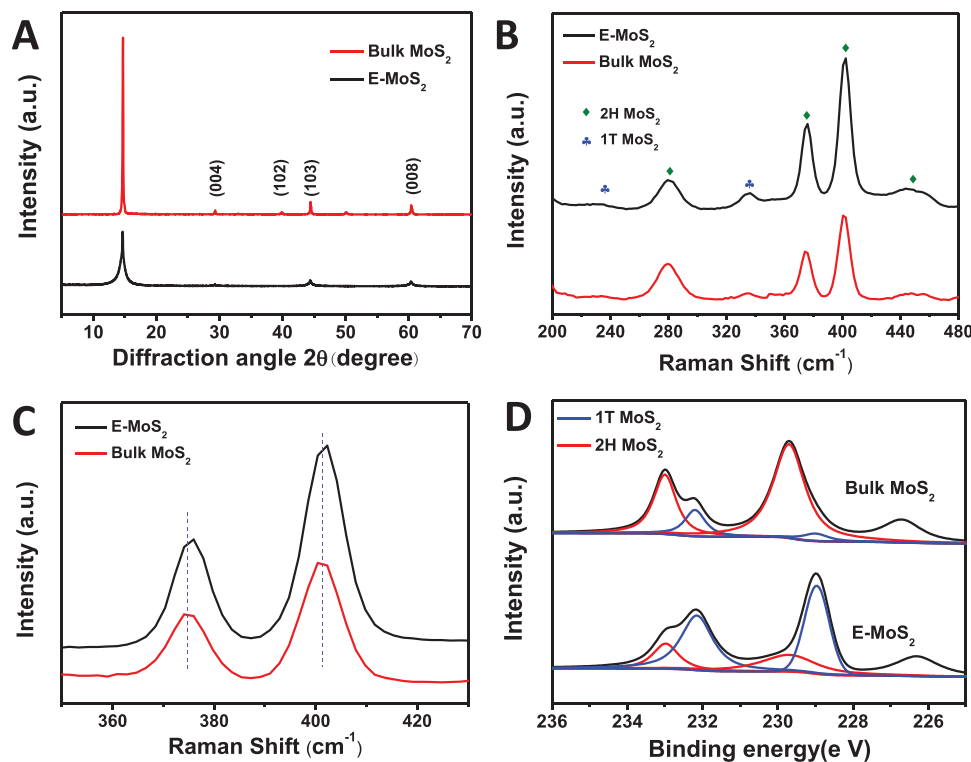


**Figure 1.** A) Digital photo of the exfoliated MoS<sub>2</sub> (E-MoS<sub>2</sub>) nanosheets in NVP with a concentration of 3 mg mL<sup>-1</sup> after ball milling. B) Tyndall effect of the diluted E-MoS<sub>2</sub> dispersion. C) TEM image of E-MoS<sub>2</sub> nanosheet and corresponding EDX maps, showing clearly the homogeneous distribution of Mo and S. D) HRTEM image of an E-MoS<sub>2</sub> nanosheet. E, F) Higher magnification HRTEM images of an E-MoS<sub>2</sub> nanosheet, showing atomic-resolution structural information, and their corresponding fast Fourier transforms (FFTs). (Insets show the 2H and 1T phases in E and F, respectively.) G) Size distribution of E-MoS<sub>2</sub> nanosheets as counted by TEM. H) AFM image of E-MoS<sub>2</sub> nanosheets. I) The corresponding height profiles; numbers 1 and 2 in (I) correspond to numbers 1 and 2 in (H), respectively.

an ultrathin layer, hundreds of nanometers in its lateral dimension, indicating that bulk MoS<sub>2</sub> has been efficiently exfoliated into few-layer nanosheets. The irregular shape of the exfoliated MoS<sub>2</sub> nanosheets was probably associated with the shear stress of the ball during the exfoliation process. The HRTEM images (Figure 1E,F) and fast Fourier transform (inset) showed that the E-MoS<sub>2</sub> layers were made of two clearly distinct structural domains consisting of a 1T (trigonal) phase and a 2H (hexagonal) phase, and the magnified images of selected regions further confirmed the coexistence of both 1T and 2H phases. The size of E-MoS<sub>2</sub> (the longest dimension) was statistically counted in TEM images of 606 flakes, revealing that the length of E-MoS<sub>2</sub> was in the range of 85 nm to 1.8  $\mu$ m and the average length was 228 nm (Figure 1G). The E-MoS<sub>2</sub> nanosheets were investigated by AFM. A previous study reported that the theoretical thickness of a monolayer of MoS<sub>2</sub> was in the range of 0.9–1.2 nm.<sup>[23]</sup> As shown in AFM images of Figure 1H and I, two E-MoS<sub>2</sub> nanosheets were stacked on each other, and the thickness of the nanosheets was measured to be 3.61–5.75 nm, corresponding to 3–5 layers of MoS<sub>2</sub>, which is consistent with the TEM results.

The molecular structure of E-MoS<sub>2</sub> was analyzed by X-ray diffraction spectroscopy (XRD), Raman spectroscopy and X-ray

photoelectron spectroscopy (XPS). Comparing the XRD patterns of the bulk MoS<sub>2</sub> powder and E-MoS<sub>2</sub> nanosheet (Figure 2A), we found that the (103) and (008) diffraction peaks of E-MoS<sub>2</sub> decreased sharply, indicating the generation of few-layered MoS<sub>2</sub> nanosheets.<sup>[23]</sup> The (002) peak became broad, indicating the expansion of the interlayer distance and the relatively small size of E-MoS<sub>2</sub>.<sup>[24]</sup> Raman spectra of bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> excited by a 532 nm laser displayed approximate resonant peaks at 282, 376, 402, and 450 cm<sup>-1</sup>, which arose from E<sub>1g</sub> and E<sub>12g</sub> and A<sub>1g</sub>, as well as the longitudinal acoustic phonon mode of 2H-MoS<sub>2</sub>, as given in Figure 2B.<sup>[25]</sup> Raman spectra also showed peaks at 223 and 335 cm<sup>-1</sup> which were ascribed to the 1T-MoS<sub>2</sub> phase.<sup>[26]</sup> The peak centered at 335 cm<sup>-1</sup> for E-MoS<sub>2</sub> nanosheets showed a slight increase in intensity. It can be speculated that both the bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> had a mixture of 1T and 2H phases, but the ratio of 1T- to 2H-MoS<sub>2</sub> in E-MoS<sub>2</sub> increased by ball milling. The carbon vibration at 1500 cm<sup>-1</sup> was not observed, indicating there were no carbon impurities in E-MoS<sub>2</sub> (Figure S5, Supporting Information). As shown in the magnified Raman spectra of Figure 2C, the bulk MoS<sub>2</sub> had two peaks at 374.1 (E<sub>12g</sub>) and 401.9 cm<sup>-1</sup> (A<sub>1g</sub>), while E-MoS<sub>2</sub> displayed corresponding peaks at 376 and 401.2 cm<sup>-1</sup>. The corresponding frequency differences between the E<sub>12g</sub> and A<sub>1g</sub> modes were



**Figure 2.** A) XRD patterns of bulk MoS<sub>2</sub> and E-MoS<sub>2</sub>. B) Raman spectra for bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> recorded using a 532 nm laser. C) Magnified Raman spectra for bulk MoS<sub>2</sub> and E-MoS<sub>2</sub>; the obvious shift of peaks ( $E_{1g}^*$  and  $A_{1g}$ ) indicate the decrease in the number of layers. D) XPS spectra of bulk MoS<sub>2</sub> and the E-MoS<sub>2</sub>. The 1T and 2H phases of MoS<sub>2</sub> in the Mo 3d spectrum are indicated by the blue and red curves, respectively.

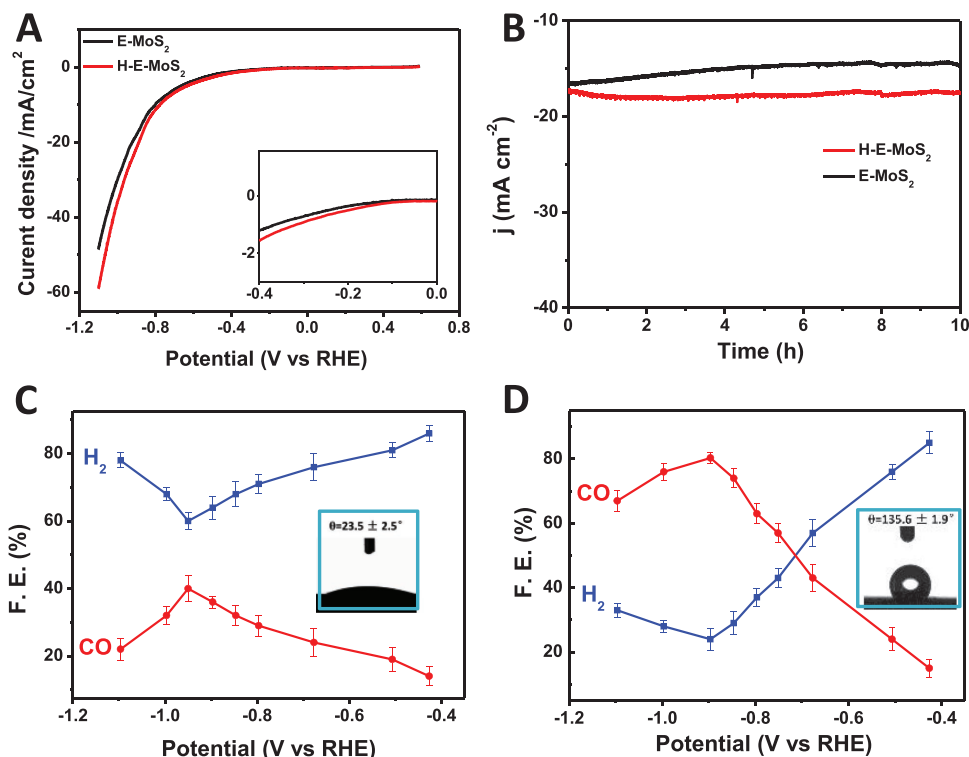
calculated to be 25.2 cm<sup>-1</sup> for E-MoS<sub>2</sub> and 27.8 cm<sup>-1</sup> for bulk MoS<sub>2</sub>, indicating that the thickness of the MoS<sub>2</sub> had been significantly reduced.<sup>[27]</sup> The XRD and Raman spectra of bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> thus confirmed that few-layered MoS<sub>2</sub> nanosheets were successfully produced. Moreover, the XPS pattern distinguished clearly the 2H and 1T phases of bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> (Figure 2D); the content of 1T phase in bulk MoS<sub>2</sub> and E-MoS<sub>2</sub> were calculated to be ≈12% and 69%, respectively. Hence, we presume that a high-energy shear effect may have induced the partial structural transformation of MoS<sub>2</sub>. It is well known that the 2H phase of MoS<sub>2</sub> is semiconducting in nature, while the 1T phase is metallic.<sup>[27]</sup> Previous studies have verified that the excellent catalytic activity of MoS<sub>2</sub> mainly derived from an increase in edge-exposed sites and the existence of the 1T phase, which facilitated electron transfer from the electrode to the active edges.<sup>[26,28]</sup> It is reasonable to assume that the high content of 1T-MoS<sub>2</sub> in E-MoS<sub>2</sub> may provide significant performance for the electroreduction of CO<sub>2</sub> to syngas.

## 2.2. CO<sub>2</sub> Electroreduction on E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> Electrodes

An E-MoS<sub>2</sub> nanosheet electrode was loaded on a 1 × 2 cm<sup>2</sup> area of GC without using any binder; instead, it picked up the assembled film floating on the surface of water. To get complete modification by FAS, E-MoS<sub>2</sub> was first treated by plasma to produce hydrophilic functional groups on E-MoS<sub>2</sub> nanosheets that would react with FAS during chemical vapor deposition (CVD, Figure S7, Supporting Information). Modification by

CVD produced (H-E-MoS<sub>2</sub>) nanosheets, which were used as a working electrode for the electroreduction of CO<sub>2</sub> to produce syngas. SEM imaging and elemental mapping (Figure S8, Supporting Information) indicated that the H-E-MoS<sub>2</sub> electrode had stacked 3D structures and a homogeneous distribution of Mo, S, and F elements, indicating FAS coverage on the E-MoS<sub>2</sub> nanosheets (Figure S8, Supporting Information). The chemical composition of H-E-MoS<sub>2</sub> was further revealed by XPS, XRD, and Raman spectra (Figures S9B and S10, Supporting Information). The XPS spectra indicated that the surface of H-E-MoS<sub>2</sub> was composed of Mo, S, C, Si, O, and F elements, indicating that FAS was successfully deposited on the surface of E-MoS<sub>2</sub> (Figure S9B, Supporting Information), in agreement with previous elemental mapping results. In addition, no obvious change in the crystal structure of E-MoS<sub>2</sub> before and after surface modification could be observed, as verified by XRD and Raman patterns. These results show that the FAS film deposited on the surface of H-E-MoS<sub>2</sub> did not change the structure or composition of the 1T and 2H phases of E-MoS<sub>2</sub>. Figure S11 of the Supporting Information gave water and air bubble CA on the surfaces of the E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes in air and underwater, respectively. The E-MoS<sub>2</sub> electrode showed hydrophilic (water CA of 23.5° ± 2.5°) and superaerophobic (air bubble CA of 162.8° ± 1.1°) properties, while the H-E-MoS<sub>2</sub> electrode showed hydrophobic (water CA of 135.6° ± 1.9°) and aerophilic (air bubble CA of 65.6° ± 1.5°) properties underwater. To assess the CO<sub>2</sub> electroreduction performances for syngas production, linear sweep voltammetry (LSV) measurements were performed in a CO<sub>2</sub>-saturated EMIM-BF<sub>4</sub> solution





**Figure 3.** A) LSV curves for E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes at a sweep rate of 0.02 V s<sup>-1</sup> in a CO<sub>2</sub> environment. B) The electrochemical stability test results of E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> catalysts at -0.8 V versus RHE in EMIM-BF<sub>4</sub> solutions (94 mol% water), showing negligible loss in current density even after 10 h. C) CO and H<sub>2</sub> Faradaic efficiency (FE%) at different applied potentials for E-MoS<sub>2</sub> catalysts, the inset is a photo of a water droplet on the surface of E-MoS<sub>2</sub>, showing its hydrophilicity. D) CO and H<sub>2</sub> FE% at different applied potentials for H-E-MoS<sub>2</sub> catalysts, the inset is a water droplet on the surface of H-E-MoS<sub>2</sub>, showing its hydrophobicity.

(94 mol% water) at a 20 mV s<sup>-1</sup> scan rate (Figure 3A). The applied voltage was swept from 0.5 to -1.1 V versus an RHE (in the present study, all potentials are reported with respect to RHE). It is known that the equilibrium potential for the reduction of CO<sub>2</sub> to CO is -0.11 V. The onset potentials for CO<sub>2</sub> reduction with the E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes were measured to be -0.3 and -0.24 V, respectively, thus suggesting a very low overpotential (190 mV) for CO formation on a H-E-MoS<sub>2</sub> electrode, and less than that of E-MoS<sub>2</sub>. In a N<sub>2</sub>-deaerated atmosphere (Figure S12C, Supporting Information), a current that was entirely attributable to the HER was observed from -0.48 and -0.5 V for E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub>, respectively. Importantly, the H-E-MoS<sub>2</sub> electrode exhibited a significantly high current density (61 mA cm<sup>-2</sup>) at -1.1 V, which was higher than that of E-MoS<sub>2</sub> nanosheets (48 mA cm<sup>-2</sup>) and previous reports.<sup>[5,6,11]</sup> Moreover, electrochemical stability is an important criterion to assess the suitability of an electrocatalyst for practical applications. Thus, chronoamperometric responses were performed at -0.8 V for 10 h in a CO<sub>2</sub>-saturated EMIM-BF<sub>4</sub> aqueous electrolyte (94 mol% water). As shown in Figure 3B, the total current density on the H-E-MoS<sub>2</sub> electrode showed long-term stability, while the total current density on the E-MoS<sub>2</sub> electrode displayed a slow decay during the reduction process. We deduced that, therefore, the electrochemical performance of CO<sub>2</sub> reduction on H-E-MoS<sub>2</sub> could be boosted by making the electrodes hydrophobicity, and FAS on an electrode could improve its electrochemical stability. The FEs for the formation of CO and

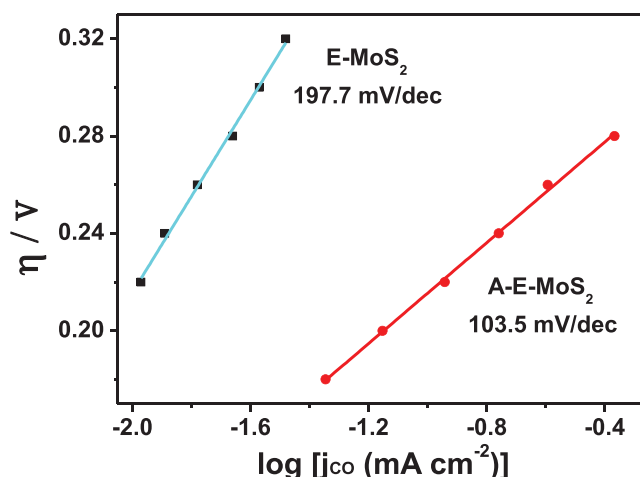
H<sub>2</sub> were calculated at a potential range from -0.3 to -1.1 V on H-E-MoS<sub>2</sub> and E-MoS<sub>2</sub> electrodes, as shown in Figure 3C,D. In our work, CO and H<sub>2</sub> were the dominant products observed by GC; no liquid products could be detected by NMR. The CO/H<sub>2</sub> ratio could be tuned by changing the wettability of the electrode and the applied potential. For H-E-MoS<sub>2</sub> nanosheets, which have a hydrophobic surface, the FE of CO production increased with decreasing applied potential and reached a maximum of 81.2% ± 1.8% at -0.9 V, larger than that for CO production using E-MoS<sub>2</sub> (41.2% ± 1.7%). Shifting to high potential, the FE of CO decreased to 65.2% ± 2.9% at -1.1 V. By contrast, the FE of H<sub>2</sub> production was ≈77.5% ± 1.3% at -0.5 V, decreased to 18.8% ± 2.8% at a potential of -0.9 V, and then rose again to 34.3% ± 1.9% at -1.1 V. Moreover, even if the potential shifted to more negative values, the HER activity on H-E-MoS<sub>2</sub> was still obviously suppressed: the FE of H<sub>2</sub> decreased by 46% at -1.1 V. As a result, the CO/H<sub>2</sub> ratio of the syngas on the H-E-MoS<sub>2</sub> electrode varied from 1:2 to 4:1 as the potential ranged from -0.6 to -1.1 V, compared with that of the E-MoS<sub>2</sub> electrode between 1:4 and 1:1.5. Taken together, the H-E-MoS<sub>2</sub> electrode with the hydrophobic surface successfully provided enhanced CO<sub>2</sub>RR performance and a broadened CO/H<sub>2</sub> ratio in the syngas by controlling the surface wettability. Compared with the CO<sub>2</sub> electroreduction performance of E-MoS<sub>2</sub>, the CO Faradaic efficiency, the onset potentials and the CO/H<sub>2</sub> ratio on bulk MoS<sub>2</sub> were measured (Figures S12A,B and S13A, Supporting Information). The bulk-MoS<sub>2</sub> electrode attained a

maximum FE of 19.8% at  $-0.9$  V, which was much lower than that of E-MoS<sub>2</sub> (41.2%) at same potential. The onset potential of CO<sub>2</sub> reduction for the bulk-MoS<sub>2</sub> and E-MoS<sub>2</sub> electrodes was measured to be at  $-0.43$  and  $-0.30$  V (vs RHE), suggesting a lower overpotential for CO formation on E-MoS<sub>2</sub> than that on bulk-MoS<sub>2</sub>. Moreover, the CO/H<sub>2</sub> ratios at different potentials with different concentrations of EMIM-BF<sub>4</sub> aqueous electrolyte on bulk-MoS<sub>2</sub> are much lower than those on the E-MoS<sub>2</sub> electrode. Therefore, we proposed that the E-MoS<sub>2</sub>, with high content of 1T-MoS<sub>2</sub>, may provide an improved performance for the electroreduction of CO<sub>2</sub> to syngas. Moreover, to consider the effect of plasma, the CO formation FEs were measured before and after plasma treatment of E-MoS<sub>2</sub>, as given in Figure 3C and Figure S14 (Supporting Information). It is noted that no obvious difference could be observed. This result indicated that plasma surface treatment improved FAS binding performance but did not affect CO<sub>2</sub> electroreduction activity.

In addition, to understand the role of the concentration of ionic liquids (ILs), the CO/H<sub>2</sub> ratios in syngas from the electrochemical reduction of CO<sub>2</sub> on the E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes at different potentials were obtained at different concentrations of EMIM-BF<sub>4</sub> aqueous electrolyte, as seen in Figure S13B,C of the Supporting Information. Syngas production on both the E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes reached the highest CO/H<sub>2</sub> ratios in 94 mol% water and 6 mol% EMIM-BF<sub>4</sub> aqueous solution. It has been said that EMIM-BF<sub>4</sub> creates protons due to the easily hydrolyzing behavior of EMIM-BF<sub>4</sub>.<sup>[9]</sup> According to previous reports,<sup>[9,29]</sup> the concentration of protons (H<sup>+</sup>) is the rate-determining part of the CO<sub>2</sub> electroreduction reaction; the maximum rate of CO<sub>2</sub> reduction could be obtained at the lowest pH value among different EMIM-BF<sub>4</sub>/H<sub>2</sub>O systems. In our work, a similar result was achieved in 6 mol% EMIM-BF<sub>4</sub>, due to its lowest pH value (4.24, Table S6, Supporting Information). It was worth noting that all CO/H<sub>2</sub> ratios in syngas on the H-E-MoS<sub>2</sub> electrode were higher than those on the E-MoS<sub>2</sub> electrode at the different potentials and different concentrations of aqueous EMIM-BF<sub>4</sub>. These results indicated that H-E-MoS<sub>2</sub> showed an enhanced CO<sub>2</sub>RR activity, but notably suppressed HER activity, even if the potentials were more negative in the EMIM-BF<sub>4</sub> aqueous electrolyte. To understand the kinetics of CO<sub>2</sub>RR on E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub>, Tafel analysis was performed on the CO partial current density. A lower magnitude of the Tafel slope for CO production is desirable, because this would indicate faster kinetics for CO formation.<sup>[30]</sup> The Tafel slope at  $\approx 118$  mV dec<sup>-1</sup> suggested that single-electron transfer was the chemical rate-determining step.<sup>[6]</sup> Tafel plots on the E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> electrodes presented good linearity with slopes of 197.7 and 103.5 mV dec<sup>-1</sup>, respectively (Figure 4). Therefore, it is clear that CO formation on the H-E-MoS<sub>2</sub> electrode had a faster rate than that on the E-MoS<sub>2</sub> electrode and single-electron transfer was the chemical rate-determining step.

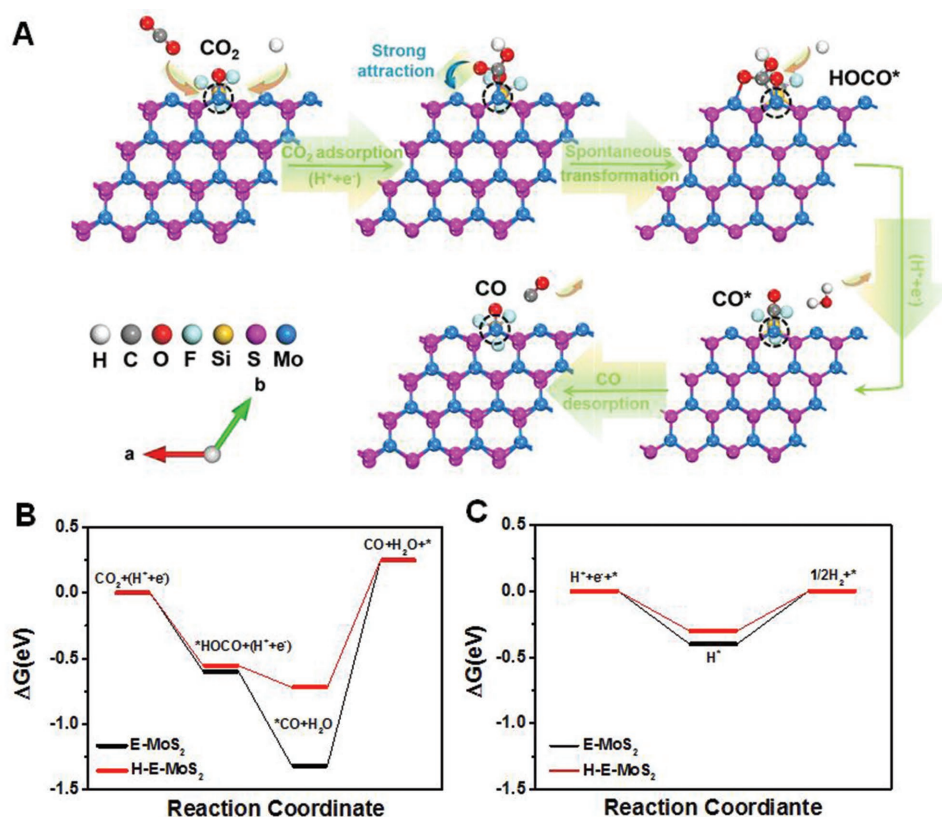
### 2.3. DFT Calculations and Reaction Mechanism of CO<sub>2</sub>RR

To deeply evaluate this reaction mechanism in the enhanced CO<sub>2</sub> electrocatalytic performance on the hydrophobic H-E-MoS<sub>2</sub> electrode, DFT calculations were performed on the CO<sub>2</sub>RR and



**Figure 4.** Tafel plots for CO production on the E-MoS<sub>2</sub> (blue) and H-E-MoS<sub>2</sub> (red) electrodes in EMIM-BF<sub>4</sub> solutions (94 mol% water).

HER processes. The energy profile is shown in Figure 5B, in which black and red lines correspond to E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub>, respectively. Our calculation results show that the adsorption of HOCO\* and CO\* on these two electrodes was exothermic, and the CO\* desorption step on E-MoS<sub>2</sub> was a highly endothermic process ( $\Delta G = 1.32$  eV, black line in Figure 5B) and the rate-limiting step in CO<sub>2</sub>RR on E-MoS<sub>2</sub>. Comparing the two lines in Figure 5B, it can be found obviously that the formation of HOCO\* on H-E-MoS<sub>2</sub> was slightly easier than it was on E-MoS<sub>2</sub> (0.55 eV vs 0.60 eV, Table S3, Supporting Information). However, the real rate-determining step (the desorption of CO\*) had  $\Delta G$  of 0.72 eV on H-E-MoS<sub>2</sub> (red line in Figure 5B) which was much lower than  $\Delta G$  of 1.32 eV on E-MoS<sub>2</sub>; this could be verified well by the elongation of the C–Mo bond (see Figure S17, Supporting Information), hence weakening the adsorption strength of CO with the Mo atom on H-E-MoS<sub>2</sub> was the real factor to promote the catalytic activity of H-E-MoS<sub>2</sub> in CO<sub>2</sub>RR. Similar results were also reported in previous studies with vertically aligned MoS<sub>2</sub> and Nb-doped vertically aligned MoS<sub>2</sub> (MoS<sub>2</sub>-Nb) as catalysts for CO<sub>2</sub>RR.<sup>[10]</sup> Meanwhile, for the HER performance, Figure 5C showed that the  $\Delta G$  for the desorption of H\* on H-E-MoS<sub>2</sub> was slightly smaller than that on E-MoS<sub>2</sub>. This little change could have almost no effect on overall activity of CO<sub>2</sub>RR. To gain deep insight into the CO formation mechanism on H-E-MoS<sub>2</sub>, we systematically investigated the process of CO<sub>2</sub>RR on its surface (Figure 5A). The Mo atoms at the H-E-MoS<sub>2</sub> nanosheet edges with high activity were the catalytic sites in CO<sub>2</sub>RR. First, the CO<sub>2</sub> combined with a proton–electron pair (H<sup>+</sup> + e<sup>-</sup>) and adsorbed on the single Mo atom, forming adsorbed HOCO\*. The HOCO\* intermediate automatically reached a more stable configuration, where HOCO\* bonded with the two neighboring Mo atoms (Figure S16, Supporting Information), which subsequently produced CO\* by consuming another proton–electron pair (H<sup>+</sup> + e<sup>-</sup>). Due to the smaller desorption energy of CO\*, the adsorbed CO\* intermediate could more easily desorb off from the catalytic sites to form free CO molecules. The catalytic activity was promoted by accelerating the rate-limiting step (desorption of CO\*). The exergonic formation of H\* in the CO<sub>2</sub>RR process would reduce the

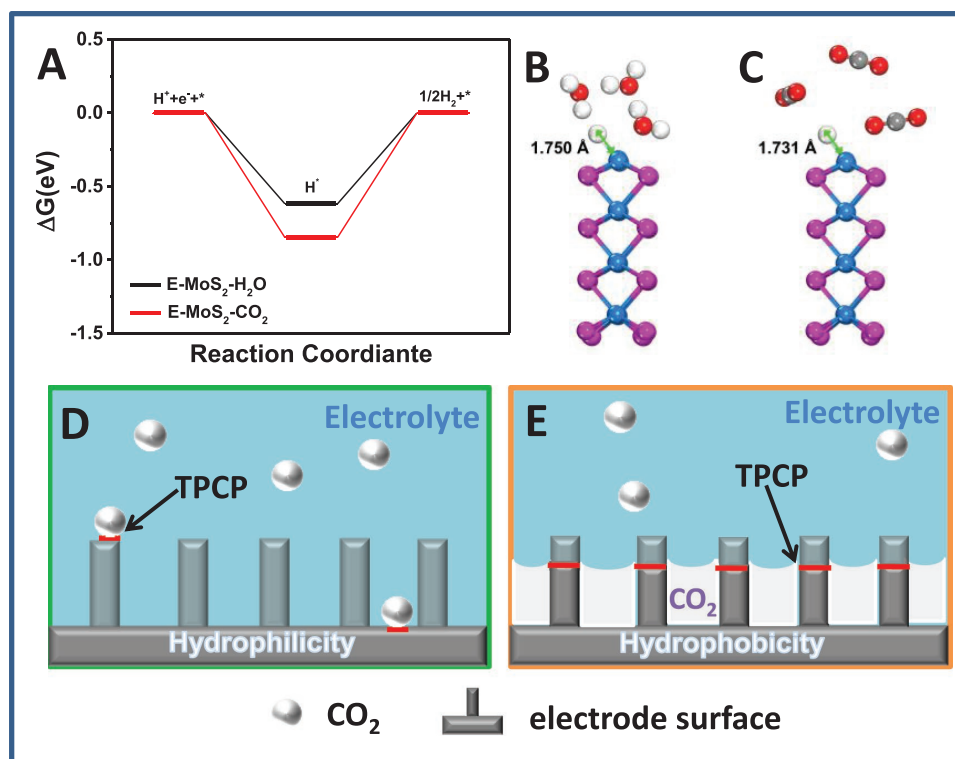


**Figure 5.** A) Schematic representation of CO formation mechanism on the H-E-MoS<sub>2</sub> monolayers. The atoms in the dashed circle are the catalytic sites (Mo atoms). Calculated free energy diagrams for B) CO<sub>2</sub> electroreduction to CO and C) the hydrogen evolution reaction (HER).

number of active sites and further result in the low CO formation FE.<sup>[31,32]</sup> Through DFT calculations, we found that the relative Gibbs free energy of H\* on H-E-MoS<sub>2</sub>, ΔG (H\*) = −0.30 eV, which was less negative than that on E-MoS<sub>2</sub> (−0.41 eV), suggesting that there could be more active sites to release for CO<sub>2</sub>RR on H-E-MoS<sub>2</sub>. In addition to that, comparing the first step of CO<sub>2</sub>RR with the adsorption of H, it can be found that on H-E-MoS<sub>2</sub>, ΔG (HOCO\*) (−0.56 eV) was ≈0.26 eV larger than ΔG (H\*) (that on E-MoS<sub>2</sub> was only 0.15 eV), which indicates that the adsorption of HOCO\* would be more competitive than H\* adsorption. At the same time, the desorption of CO on H-E-MoS<sub>2</sub> decreased (only 0.70 eV) compared to that on E-MoS<sub>2</sub> (>1.0 eV). As a result, the FE for CO formation was improved on H-E-MoS<sub>2</sub>. Recently, moreover, Xie et al.<sup>[33]</sup> synthesized a fluorine-interlayer-doped carbon catalyst that enabled highly selective CO<sub>2</sub>-to-CO conversion with a high FE (89%) for CO at the first time. The result demonstrated that fluorine dopant inserted between the graphite layers could induce positive charge density and asymmetrical spin into the neighboring carbon atoms, resulting in stronger adsorption of HOCO\* and better suppression of HER, leading to superior electrocatalytic performance toward CO<sub>2</sub>RR.<sup>[33]</sup> Accordingly, we proposed that FAS decoration on the surface could create similar effects on the H-E-MoS<sub>2</sub> due to the strong electronegativity of F, resulting in an improved CO FE compared to E-MoS<sub>2</sub>.

To evaluate the effect of hydrophilic and hydrophobic properties on CO<sub>2</sub>RR, further DFT calculations were carried out

to determine the free energy changes for HER on the E-MoS<sub>2</sub> monolayers under H<sub>2</sub>O and CO<sub>2</sub> environments, respectively (Figure 6A). Here, the H<sub>2</sub>O and CO<sub>2</sub> environments were used to simulate hydrophilic E-MoS<sub>2</sub> and hydrophobic H-E-MoS<sub>2</sub>, respectively, and simplify the DFT calculations. We think that it is a reasonable simulation, due to the inherent properties of hydrophilic and hydrophobic electrodes, as demonstrated in Figure 6B,C. Our calculated results show that the abundant CO<sub>2</sub> environment of the hydrophobic electrode could increase the energy barrier of H\* desorption to suppress the catalytic activity of HER, compared with the water environment of the hydrophilic electrode, which is consistent with the shorter H–Mo bond under the CO<sub>2</sub> environment (Figure 6A). Under the H<sub>2</sub>O environment, as shown in Figure 6B,C, the H–Mo bonds of MoS<sub>2</sub> were 1.75 Å, longer than those in the CO<sub>2</sub> environment (1.73 Å), which means that the H\* desorption could happen easier under the H<sub>2</sub>O environment for H<sub>2</sub> desorption, thus facilitating HER. Thereby, we deduce easily that hydrophobic H-E-MoS<sub>2</sub> can depress HER, and thereby improve CO<sub>2</sub>RR performance. In addition, to further illuminate the role of the hydrophobic surface for CO<sub>2</sub> electroreduction, CO<sub>2</sub> bubble adhesion to E-MoS<sub>2</sub> and H-E-MoS<sub>2</sub> were measured underwater. The hydrophobic H-E-MoS<sub>2</sub> surface showed more affinity for CO<sub>2</sub> gas than did the E-MoS<sub>2</sub> surface, as shown in Figure S15 of the Supporting Information. E-MoS<sub>2</sub> might impede the process of CO<sub>2</sub> gas diffusion due to its superhydrophobicity, causing a weak interaction between CO<sub>2</sub> molecules



**Figure 6.** A) Calculated free energy changes for the HER on the E-MoS<sub>2</sub> monolayers under an H<sub>2</sub>O environment (black line) and CO<sub>2</sub> environment (red line). Optimized geometries of the H\* intermediate on the E-MoS<sub>2</sub> monolayers under B) an H<sub>2</sub>O environment and C) a CO<sub>2</sub> environment (H–Mo bond lengths are in Å). D) A thin layer of E-MoS<sub>2</sub> film is immobilized on a GC electrode substrate that appears hydrophilic and aerophobic. When the electrode is immersed in electrolyte solution, the catalyst can only contact the few CO<sub>2</sub> molecules that dissolve in the electrolyte. The red line illustrates the liquid (electrolyte)/gas (CO<sub>2</sub>)/solid (electrode) contact point (TPCP) where electron transfer happens. E) After the wettability regulation, an H-E-MoS<sub>2</sub> film is immobilized on the GC electrode substrate, which becomes hydrophobic and aerophilic. Due to the existence of triphase interface, the catalyst can contact much CO<sub>2</sub>, which is derived from both the electrolyte and catalyst surface.

and the electrode (Figure 6D). It has been reported previously that hydrophobic residues have the ability to absorb and host the reactant gas to enhance the extent of reaction at the gas–solid–liquid interface.<sup>[13,28]</sup> Therefore, the H-E-MoS<sub>2</sub> electrode has a hydrophobic and aerophilic surface, in which more CO<sub>2</sub> molecules diffused into the electrolyte due to the abundant three-phase contact point (TPCP) on the electrode (Figure 6E), which led to there being more CO<sub>2</sub> molecules at the gas–solid–liquid interface, and then enhancing the reactivity of CO<sub>2</sub>RR. This is the first analysis of the mechanism for the electroreduction of CO<sub>2</sub> to syngas on an FAS-modified electrode by DFT calculations.

### 3. Conclusions

In summary, an E-MoS<sub>2</sub> dispersion with a large volume and high concentration has been fabricated by a cost-efficient process of wet ball milling. The H-E-MoS<sub>2</sub> nanosheet electrode for CO<sub>2</sub> electroreduction was fabricated by a facile refloating of MoS<sub>2</sub> nanosheets on a glassy carbon electrode, followed by decoration of FAS. H-E-MoS<sub>2</sub> nanosheets, with their hydrophobicity, exhibited a superior CO<sub>2</sub>RR performance with a high current density of 61 mA cm<sup>−2</sup> at −1.1 V, ≈1.25 times higher than that of E-MoS<sub>2</sub>. The CO/H<sub>2</sub> ratios of syngas on the H-E-MoS<sub>2</sub>

electrode were broadened from 1:2 to 4:1 at a wider range of potentials, compared to those of the E-MoS<sub>2</sub> electrode. In addition, H-E-MoS<sub>2</sub> attained the highest FE of 81.2% for CO production at −0.9 V. Note that HER performance could be obviously suppressed, but CO<sub>2</sub>RR activity was enhanced on the H-E-MoS<sub>2</sub> electrode. We proposed that the hydrophobicity of the electrode provided an abundant TPCP for accelerating CO<sub>2</sub> diffusion into electrode, which enhanced CO<sub>2</sub>RR performance. Our experimental results were further verified by DFT calculations. The DFT results showed that the FAS decoration of H-E-MoS<sub>2</sub> changed the electric properties of the MoS<sub>2</sub> layer, decreased the energy barrier of the rate-determining CO-desorption step, which thereby promoted CO<sub>2</sub> reduction to produce CO. Furthermore, DFT calculations of hydrophilic E-MoS<sub>2</sub> and hydrophobic H-E-MoS<sub>2</sub> electrodes also found that the CO<sub>2</sub> environment of hydrophobic MoS<sub>2</sub> increased the energy barrier of H desorption, thus suppressing HER. The method used here may provide an effective and facile method for the electrochemical conversion of CO<sub>2</sub> to syngas with a wide range of CO/H<sub>2</sub> ratios by tuning the wettability of the electrode.

### 4. Experimental Section

**Materials:** Molybdenum (IV) sulfide powder (MoS<sub>2</sub>, CAS: 1317-33-5) was supplied by Sigma-Aldrich. NVP (CAS: 88-12-0) was purchased



from Shanghai Macklin Biochemical Co. Ltd. Trimethoxy (1H,1H,2H,2H-heptadecafluorodecyl) Silane (FAS, CAS: 83048-65-1) was purchased from Alfa Aesar. 1-Ethyl-3-methylimidazolium tetrafluoroborate (EMIM-BF<sub>4</sub>, CAS: 143314-16-3) was supplied by Shanghai Cheng Jie Chemical Co. LTD. All reagents were used without further treatment.

**The Exfoliated MoS<sub>2</sub> (E-MoS<sub>2</sub>) Nanosheets:** Here, the solvent NVP was used to disperse MoS<sub>2</sub> nanosheets because they have similar surface energies. First, the MoS<sub>2</sub> nanosheet dispersion was prepared according to the reported literature.<sup>[16]</sup> In a typical experiment, the required mass of MoS<sub>2</sub> powder and ZrO<sub>2</sub> balls (1:1 mass ratio of 2 mm ball and 0.2 mm ball) were added to the jar. The NVP solvent was then added into the jar, in which the concentration of MoS<sub>2</sub> powder was 16 mg mL<sup>-1</sup>, and the solution was ground for 18 h. The dark green colored dispersion was collected and centrifuged at 550 rpm (centrifugation force 30 N) for 45 min to remove any unexfoliated MoS<sub>2</sub>. The dark green colored supernatant was decanted and retained for analysis and further experiments, while the sediment was discarded. To calculate the concentration of the exfoliated MoS<sub>2</sub> (E-MoS<sub>2</sub>) nanosheets, the dispersion was filtered using a polytetrafluoroethylene membrane (pore size: 0.1 μm) and the MoS<sub>2</sub> membrane was dried at 60 °C under vacuum for 3 days. The as-prepared E-MoS<sub>2</sub> dispersion was injected into water to form a uniform E-MoS<sub>2</sub> film on the surface of the water. Then, a GC slice (3 cm × 1 cm) was inserted below the surface of water, then slowly drawn and dried for 24 h to obtain an E-MoS<sub>2</sub>-coated electrode with 9 mg cm<sup>-2</sup> of E-MoS<sub>2</sub> nanosheets on it, which was used as the working electrode.

**The Hydrophobic E-MoS<sub>2</sub> Nanosheet (H-E-MoS<sub>2</sub>) Electrode:** E-MoS<sub>2</sub> substrates were treated with air plasma with 2 min (10.5 W) in order to introduce hydrophilic functional groups. Trimethoxy (1H,1H,2H,2H-heptadecafluorodecyl) silane (FAS) was used as the chemical vapor deposition material for the hydrophobic treatment, which was carried out in a beaker that contained liquid FAS in equilibrium with its vapor. The E-MoS<sub>2</sub> electrode was exposed to FAS vapor for 18 h at room temperature to get the hydrophobic and aerophilic E-MoS<sub>2</sub> electrode (denoted as an H-E-MoS<sub>2</sub> electrode).

**Characterization:** The surface morphology and corresponding elemental mapping analysis of samples were observed by environmental SEM (JEOL, JSM-7500F, Japan). The microstructure and lattice structure of samples were observed by HRTEM (JEOL, JEM-2100F, Japan). The topology of the surface was studied by AFM (VT STM/AFM, Germany) using a Veeco DI Nano-scope MultiMode V system. XRD patterns were obtained with a Shimadzu X-ray diffractometer (XRD-6000) equipped with a Cu-Kα1 source (λ = 1.5406 Å). XPS was performed with Al Kα radiation (Thermo Fisher Scientific, ESCALAB 250Xi, America). Raman spectra were analyzed using 532 nm laser excitation by a Raman spectroscope (LabRAM HR800). A plasma cleaning machine (PDC-32G-2) was equipped with three power settings (low: 6.8 W, medium: 10.5 W, high: 18 W).

## Supporting Information

Supporting Information is available from the Wiley Online Library or from the author.

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## Conflict of Interest

The authors declare no conflict of interest.

## Keywords

CO<sub>2</sub> electroreduction, exfoliated MoS<sub>2</sub> nanosheets, FAS, hydrophobic electrodes, syngas

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