Hexachlorodisilane as a Precursor in the LPCVD of Silicon Dioxide and Silicon Oxynitride Films

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ABSTRACT

Films of silicon dioxide and silicon oxynitride were grown by LPCVD using gas-phase mixtures of Si₂Cl₆, N₂O, and NH₃ in the temperature range 550°-850°C. The activation energy for SiO₂ deposition was 29 kcal/mole. Under comparable pressure and temperature conditions, growth rates of SiO₂ from Si₂Cl₆ were at least three times higher than those obtained using SiH₂Cl₂ or SiH₄. The effect of temperature and reactant flow ratios on film composition, stress, refractive index, etch rate, and uniformity were studied, and these properties were found to be comparable to those in films deposited from SiH₂Cl₂ and SiH₄. The effect of N₂O/NH₃ ratio on physical properties was investigated for oxynitride films. The dependence of these properties on film composition was the same regardless of the CVD reactant mixture used. However, the NH₃ to oxidant ratio required to obtain a specific film composition was strongly influenced by the oxidant and silicon precursor used. Comparisons are made to the LPCVD systems: SiH₂Cl₂-N₂O-NH₃, SiH₄-NO-NH₃, and SiH₄-CO₂-NH₃.

We have recently reported on the use of hexachlorodisilane (Si₂Cl₆) in the chemical vapor deposition of polycrystalline and amorphous silicon (1) and silicon nitride (2). Hexachlorodisilane was selected as a possible safe and efficient alternative to silane and dichlorosilane, the currently preferred precursors in silicon and silicon nitride CVD. Since we found Si₂Cl₆ capable of producing high quality films of both Si and Si₃N₄ over a wide range of temperatures, an extension of the investigation to the deposition of SiO₂ and silicon oxynitride films would be clearly of interest. Although SiO2 can be deposited at moderate temperatures with nonhazardous precursors such as tetraethoxysilane (TEOS) (3,4) or diacetoxyditeriarybutoxysilane (DADBS) (5, 6), higher temperature depositions (>750°C), which lead to improved density, uniformity, and conformality, are still carried out using either SiH₂Cl₂-N₂O (7-13) or SiH₄-N₂O (8, 14, 15). Silicon oxynitride films are deposited almost exclusively from SiH₂Cl₂-N₂O-NH₃ (16-20) or SiH₄-NH₃-CO₂(NO) (21-24) gas mixtures. In contrast to SiH₄ and SiH₂Cl₂, Si₂Cl₆ is not known to autoignite under ambient conditions. It is a liquid with a vapor pressure that allows useful transport rates with minimal source temperature control and the vapor readily decomposes to provide films of silicon and silicon nitride down to 450°C.

Experimental

The SiO₂ and oxynitride films were deposited in a tubular hot-wall reactor at temperatures from 550° to 850°C. The 1 in. diam (100) silicon substrates were placed horizontally on a quartz plate. Total pressure was maintained at 0.7 torr by an automatic throttle valve located downstream. Distilled Si₂Cl₆ was supplied by Cambridge Isotope Laboratories (Cambridge, Massachusetts), and contained less than 0.01% chlorosiloxane. $N_2\!\!, NH_3\!\!, \text{and}\; N_2O$ gases were all 99.999% pure. In SiO2 film growth, the total flow of $N_2O + N_2$ was kept at 250 sccm with N_2O between 50 and 250 sccm, while the flow of Si₂Cl₆ was varied between 2-11 sccm. This resulted in an $R = N_2O/Si_2Cl_6 = 5-125$. For the growth of silicon oxynitride, the flow of Si₂Cl₆ was either 2 or 10 sccm. The total flow of $NH_3 + N_2O$ was constant at 150 sccm, whereas N_2 was fixed at 100 sccm. The ratio R' = $(N_2O + NH_3)/Si_2Cl_6$ was therefore either 15 or 75, while NH₃/N₂O varied from 2.0 to 0.07. The Si₂Cl₆ container was held at 5°C (1.2 torr vapor pressure) and flow was controlled by a needle valve. The 5°C temperature (6°C above the melting point) was chosen in order to obtain acceptable growth rates and still conserve the Si₂Cl₆ source material. The partial pressure of Si₂Cl₆ in the system ranged from 0.0055 torr (2 sccm) to 0.03 torr (11 sccm).

Film thickness and index of refraction were measured with a Gaertner ellipsometer equipped with a He-Ne laser. Auger electron spectroscopy was used for Si, N, O, and Cl analysis. Hydrogen content and Si-H and N-H bond distributions were determined with a Nicolet Model 5PC FTIR spectrometer. X-ray topography was used to measure film stress. Etch rates were measured by ellipsometry after room temperature etching in $100:1 \text{ H}_2\text{O:HF}$.

Results and Discussion

Silicon dioxide.-The silicon dioxide growth rate as a function of temperature is shown in Fig. 1 for R = 15 and 75 over the temperature range 550°-850°C. No SiO₂ growth was observed below 550°C. Since growth of Si₃N₄ occurred as low as 450°C (2), the higher minimum growth temperature for SiO₂ must be due to lower reactivity of N₂O. The dashed lines are the observed temperature-dependent growth rates for $Si_3N_4(2)$ at R = 15 and 75 with an activation energy of 29.3 kcal/mole. It can be seen that the same activation energy applies to SiO₂ deposition between 600° and 750°C where the deposition is most likely surface reactioncontrolled. The slope decreases above 750°C, suggesting the beginning of a mass transport-limited reaction. Similar growth rate saturation occurs at the same temperature in the SiH_4 -N₂O (15) and TEOS (4) systems. The 29.3 kcal/mole activation energy is comparable to the 33 kcal/mole re-



Fig. 1. Growth rate of SiO₂ and Si₃N₄ as a function of substrate temperature at R = 15 and R = 75.

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ported for SiH₄-N₂O (15), higher than the 12.0 kcal/mole found for SiH₄-O₂ (25), but lower than the 45-46 kcal/mole found for TEOS (3, 4) and SiH₂Cl₂-N₂O (13).

The SiO₂ growth rates obtained using R = 15 vary from 3.2 µm/h at 850°C to 0.02 µm/h at 550°C. If the Si₂Cl₆ flow is decreased by 80% to 2 sccm (R = 75), the growth rate also decreases by 80% at all temperatures. A 67% drop in growth rate was observed for Si₃N₄ films under the same conditions (2). The effect on growth rate of changing R by increasing N₂O flow from 50 to 250 sccm (partial pressure 0.134-0.673 torr) while Si₂Cl₆ flow remains constant at 10 sccm (partial pressure 0.027 torr) is shown in Fig. 2 for 650° and 750°C. Comparable results for Si₃N₄ are given by the dashed lines. At both temperatures, the SiO₂ growth rate is directly proportional to the N₂O flow. In contrast, Si₃N₄ growth at 650°C saturates for NH₃ flows having R > 10(2).

The growth rates obtained compare very favorably to all other moderate to high temperature CVD methods. Appreciable growth generally cannot be observed below 800°C in the SiH₂Cl₂-N₂O system. The deposition rate at 900°C is only 0.3-0.7 µm/h at a total pressure of 0.6-0.8 torr and 0.08-0.09 torr SiH₂Cl₂ partial pressure (8, 10). In contrast, the SiO_2 growth rate from $Si_2Cl_6\text{-}N_2O$ at 850°C was 3.2 $\mu m/h$ at a total pressure of 0.7 torr and Si₂Cl₆ partial pressure of only 0.03 torr. A similar comparison was noted in Si₃N₄ growth (2). Dichlorosilyene (SiCl₂), produced by homogeneous decomposition, has been singled out as the film growth precursor using chlorinated monosilanes (1). If this is the case, then the growth rate advantage of Si₂Cl₆ could be due to its considerably lower kinetic stability toward gas-phase decomposition into this intermediate. However, a growth rate advantage of Si₂Cl₆ also exists relative to SiH₄- $N_2O(8, 15)$. In this system, growth rates between 0.15- $0.30~\mu m/h$ have been observed at 850°C at 1.0 torr total pressure and 0.01-0.02 torr SiH₄ partial pressure. Deposition rates comparable to our results are obtained with TEOS(3) and DADBS(5), at 725° and 600°C, respectively, but much higher precursor partial pressures must be used (0.35 and 0.7 torr).

Auger (AES) analysis of films grown at 750°C (R = 20-100) and at 650°C (R = 75) showed the films to contain 30 atom percent (a/o) Si. Therefore, within the accuracy of AES (± 3 a/o) the films appear to be somewhat oxygen-rich. As in the case of Si₃N₄, the *R* values used to achieve this stoichiometry lie between those found for

SiO₂

--- Si3N4 IO SCCM Si2CI6 FLOW

750°C

650°C

10.00

1.00

0.10

0.01

BROWTH RATE (µm/hr

Fig. 2. Growth rate of SiO_2 and Si_3N_4 as a function of $R(N_2O/Si_2Cl_6$ or $NH_3/Si_2Cl_6).$

15

R

20

25

30

Table I. Stress and refractive index in silicon dioxide films

Growth temperature (°C)	R	Stress (10 ⁹ dynes/cm ²)	n
600	20	-2.2	1.54
650	5	-3.6	1.55
650	20	-3.1	
650	75		1.49
750	5	-4.2	1.53
750	20	-3.2	1.51
750	75	-2.3	1.47
850	all		1.47

oxide growth from SiH₂Cl₂ and SiH₄. The chlorine content was 1.3 a/o for a film grown at 750°C using R = 20, whereas it was nondetectable (<0.2 a/o) for R = 100. At 650° and 750°C with R = 75, the Cl concentration was 0.5 a/o. Chlorine is therefore in the high 10¹⁹ atom/cm³ range, about the same as reported for films grown from SiH₂Cl₂ at 800° (12) and 900°C (9). Chlorine seems to be uniformly distributed throughout the thickness of the film, within the accuracy of AES, with possibly a slight buildup at the Si/SiO₂ interface.

Deposition under optimized flow and temperature conditions led to SiO₂ films with good thickness uniformity. For example, for 750°C and R = 75, films deposited on substrates placed in the 30 cm central zone of the reactor showed less than $\pm 3.5\%$ thickness variation. Comparison with other CVD systems is difficult without having data for Si₂Cl₆ for vertically mounted close-spaced wafers. Compositional uniformity was excellent. Figure 3 reveals Auger profiles of a 300Å SiO_2 film grown at 750°C with R =100, and for comparison, a 240Å Si₃N₄ film grown from Si_2Cl_6 and NH_3 at the same temperature with R = 60. Table I provides film stress and index of refraction measurements. Stress in the oxide films was compressive. It increased with both increasing deposition temperature and decreasing R, and is very typical of SiO₂ films deposited by other methods at these temperatures (26). The higher index films in Table I are likely to be somewhat siliconrich. Using the relationship given by Learn and Jackson (15), an index change from 1.47 to 1.53 would correspond to 2.5 a/o excess silicon.

Silicon oxynitride.—The growth rate plots for silicon oxynitride (SiON) deposited at temperatures between $650^{\circ}.850^{\circ}C$ (R' = 15 or 75) lie between the plots obtained for Si₃N₄ and SiO₂ shown in Fig. 1. The effect of the reactant flow ratio ($R'' = N_2O/(N_2O + NH_3)$) on the oxygen content (O/(O + N)) is shown in Fig. 4. It is evident that the reactivity of NH₃ is higher than that of N₂O, because R'' = 0.85 is required to achieve O/(O + N) = 0.5 in the film. The effect is even more pronounced with SiH₂Cl₂-N₂O-NH₃(18, 19) as shown in Fig. 4, where R'' = 0.95 for O/(O + N) = 0.5. At O/(O + N) = 0.15, the Si concentration in the film is 44 a/o



Fig. 3. Auger depth profile of SiO₂ and Si₃N₄ films deposited on Si substrates at 750°C with R = 100 and R = 60, respectively.



Fig. 4. Effect of reactant flow ratio, R'', on SiON film composition in Si₂Cl₆ and SiH₂Cl₂ systems.

typical of Si₃N₄. For O/(O + N) \ge 0.23, the Si content is 32-34 a/o, corresponding to SiO₂, but lower than expected for these intermediate compositions. Silicon deficiencies of a few a/o are common in LPCVD oxynitride films grown from both SiH₂Cl₂ and SiH₄ (16, 19, 24). For films grown at 750°C and R' = 75, the chlorine concentrations decreased rapidly from 1.0 a/o in films with O/(O + N)) = 0.61, to values below detectibility (<0.2 a/o) for oxygen contents



Fig. 5. Effect of SiON film composition on index of refraction for several CVD systems.



Fig. 6. Effect of $R''(\text{oxidant}/(\text{oxidant} + \text{NH}_3))$ on SiON index of refraction for several CVD systems.

below 0.42. A similar trend was reported for SiH_2Cl_2 grown films (18).

The effects of oxygen content (O/(O + N)) and R" on film refractive indexes are depicted in Fig. 5 and 6, along with data for several other CVD systems (16, 19, 23, 24). Film indexes vary smoothly with composition regardless of the CVD system, as expected, but not with R'', where R'' may be considered here to be the oxidant/(oxidant + NH₃) ratio. The latter result simply reflects the effect of the relative reactivities of the precursors on film composition. The use of SiH₂Cl₂ results in a very low N₂O reactivity, requiring R'' = 0.95 to grow a film with n = 1.67, an index corresponding to O/(O + N) = 0.5. Very low NH_3 reactivities are observed in the SiH₄-based methods. The use of CO₂ results in a film with n = 1.67 when R'' = 0.23, whereas R'' =0.05 is required to achieve this index when NO is the oxidant. On the other hand a smooth variation of index with R'' over much of its range is observed using Si₂Cl₆, resulting in a minimum variation of composition with reactant flow fluctuation.

The FTIR spectra between 2000 and 3500 cm⁻¹ are shown in Fig. 7 for films of silicon nitride and SiON (O/(O + N) \approx 0.5) grown at 750°C. Using Lanford and Rand's method (27), the hydrogen concentration of both films was determined to be $\approx 3.5 \times 10^{21}$ atoms/cm³ (3.5-4 a/o), which is close to that found in films grown from SiH₂Cl₂(18). Differences in the hydrogen distributions are clearly observed for the two films. Previously, we found (2) that Si₃N₄ films grown at 750°C contained hydrogen in predominantly Si-H form; the distribution is 60% SiH and 40% N-H for the film shown in Fig. 7. The addition of oxygen to



Fig. 7. IR spectra from 2000-3500 cm $^{-1}$ for SiON and Si_3N_4 films with 3.5 \times 10^{21} cm $^{-3}$ hydrogen grown at 750 °C.



Fig. 8. IR spectra from 650-1400 cm $^{-1}$ for SiON, Si_3N_4, and SiO_2 films grown at 750 $^{\circ}\text{C}.$

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Fig. 9. SiON film stress and etch rate in 100:1 H₂O:HF as a function of film composition. All films were grown at 750°C with R' = 75.



Fig. 10. Auger depth profile of top 300Å of SiON film grown at 750°C

produce SiON yields 90% N-H/10% Si-H, a distribution commonly observed in Si₃N₄ films grown from SiH₂Cl₂-NH₃ (28, 29). Figure 8 shows IR spectra between 700 and 1400 cm⁻¹ for 2000Å films of SiO_2 , Si_3N_4 , and SiON $(O/(O + N) \simeq 0.5)$. All were grown at 750°C. The Si-O and Si-N stretching modes of the SiO2 and Si3N4 films are at 1080 and 840 cm⁻¹, respectively. The broad peak from the SiON film is at 950 cm⁻¹, indicating a different bonding matrix, not a mixture of SiO_2 and Si_3N_4 clusters. Similar observations were made for films grown from SiH₂Cl₂ (16).

Film stress and etch rate for SiON as a function of film composition are shown in Fig. 9. All films were grown at 750°C with R' = 75. Stress displays a linear decrease with increasing oxygen concentration from $8.2 \times 10^{\circ}$ dynes/cm² (Si_3N_4) to $-2.3 \times 10^{\circ}$ dynes/cm² (SiO₂). Zero stress occurs for O/(O + N) = 0.77 at R'' = 0.98. In general, film stress decreased slightly with decreasing growth temperature. Film etch rates in 100:1 H₂O:HF increase linearly with increasing oxygen content from 5 to 150 Å/min as the composition changes from pure Si₃N₄ to SiO₂. The stress and etch rate data are very typical of films grown under comparable conditions by other methods (26).

Auger measurements indicate excellent compositional uniformity. The profile of the top 300Å layer of a 1000Å film grown at 750°C (R'' = 0.5) is shown in Fig. 10. The film composition is 34.5 a/o Si, 50.3 a/o N, 15.2 a/o O, and no detectable Cl. However, the wafer-to-wafer thickness uniformity varied considerably with the N₂O/NH₃ ratio. At 750°C and R' = 75, depletion effects were very strong at high NH₃ partial pressures. Increasing N₂O partial pressure caused the thickness gradients to decrease. Thickness uniformity

over the central 30 cm segment of the reactor was $\pm 30\%$ for $Si_3N_4(2)$, whereas it is $\pm 3.5\%$ for SiO_2 under similar conditions, and lies intermediate for the oxynitride films. Depletion effects can be minimized or eliminated and thickness profiles improved by either increasing Si₂Cl₆ flow (decreasing R') or lowering the deposition temperature.

Conclusions

We have shown that high quality films of silicon dioxide and silicon oxynitride can be deposited by LPCVD using hexachlorodisilane as a precursor. Growth takes place at temperatures above 550°C. For T > 750°C, growth rates are greatly enhanced compared to monosilane and dichlorosilane, the precursors most commonly in use. The higher growth rate from Si₂Cl₆ is attributed to its lower kinetic stability and greater reactivity. Physical and chemical properties of the films are comparable to those obtained from other precursors at these temperatures. The higher growth rates and possibly greater safety margins associated with the use of Si₂Cl₆ make it an attractive alternative to silane and dichlorosilane in CVD processes for silicon and its insulators.

Acknowledgments

The authors wish to thank R. D. Estes for GC/MS analysis, I.M. Fisher for the etch rate measurements, R.G. Schad for Auger profiles, J. M. Karasinski for film x-ray data, and D. B. Beach for the FTIR spectra.

Manuscript submitted Aug. 19, 1988, revised manuscript received Nov. 10, 1988.

IBM T. J. Watson Research Center assisted in meeting the publication costs of this article.

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Chemical Vapor Deposition of Epitaxial Silicon from Silane at Low Temperatures

I. Very Low Pressure Deposition

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ABSTRACT

The deposition of epitaxial silicon films at temperatures from 600°-800°C by both very low-pressure chemical vapor deposition (VLPCVD) and plasma-enhanced chemical vapor deposition (PECVD) has been examined. The VLPCVD deposition process is first order in silane partial pressure, zero order in hydrogen partial pressure, and exhibits a low, 8-12 kcal/ mole, activation energy of 40 kcal/mole is observed. The growth rate depends upon surface orientation, decreasing in the order (100), (111), polycrystalline, indicating surface processes are rate controlling. The low activation energy regime is associated with a process controlled by silane adsorption and decomposition on a sparsely covered silicon surface. The higher activation energy regime is thought to reflect growth under conditions of high surface coverage with silane fragments and the transition temperature is thought to be pressure dependent. Conditions for the deposition of device quality epitaxial silicon at low temperatures are defined and discussed. Plasma enhancement of the VLPCVD process is discussed in a companion paper.

This paper and a companion paper examine the epitaxial deposition process under very low-pressure chemical vapor deposition (VLPCVD) and plasma-enhanced chemical vapor deposition (PECVD) conditions, respectively. Previous PECVD epitaxy research has focused on the role of a plasma in enhancing the removal of native oxide and made independent analysis of deposition enhancement difficult. In this work we examine VLPCVD and PECVD growth processes subsequent to an optimized argon plasma sputter cleaning procedure (1, 2). Plasma enhancement for crystalline deposition operates as a parallel addition to an existing heterogeneous thermal deposition process. Thus it was necessary to first isolate the nature of the VLPCVD process in order to interpret or assess any enhancement processes. The ultimate goal of this research, however, was the development and implementation of a technologically useful process for the deposition of epitaxial silicon at low temperatures.

This paper (Part I) will discuss the experimental determination of reaction orders and apparent activation energies for the VLPCVD deposition process. These results are then compared with the literature to provide a consistent picture of the interaction of silane with silicon surfaces at low temperatures. Existing deposition models will be assessed to determine their validity and to propose directions for more comprehensive modeling of silicon deposition from silane. Conditions which lead to the deposition of device quality epitaxial silicon films suitable for bipolar device fabrication will also be presented. The second paper (Part II) will discuss plasma enhancement of the deposition process within the context of the thermal deposition model. It will be shown that, as implemented here, plasma enhancement of intrinsic deposition is relatively inefficient but does not introduce any observable degradation in film quality. This will set the stage for the more crucial application of plasma enhancement to the deposition of doped epitaxial films at low temperatures which will be discussed elsewhere (3, 4). Methods for increasing the efficiency will be discussed and suggestions for future PECVD implementations will also be provided.

Intrinsic VLPCVD

Although silicon deposition from silane has been studied for over 20 years there is still a surprising lack of understanding of mechanistic details, particularly concerning surface-controlled deposition processes. Early research, carried out in atmospheric pressure systems employing surface temperatures in excess of 1000°C, typically exhibited significant gas-phase heating and silane decomposition. Deposition kinetics were generally determined by mass-transfer limitations and thus strongly coupled to the details of the reactor hydrodynamics. Modeling efforts focused on solution of the relevant mass and energy balances coupled with simplified treatment of the silane reaction network. These early models suffered from a lack of detail and thus were only able to reproduce or predict isolated features of the deposition systems and could not truly be considered predictive. Recent advances in the understanding of the basic gas-phase reaction network for homogeneous silane pyrolysis (5) and application of sophisticated hydrodynamic modeling have led to the development of detailed models for silicon deposition under conditions where gas-phase reaction and mass transport dominate the deposition kinetics (6-8). These models are quite general and are capable of predicting reactor behavior under a variety of experimental conditions provided a defined geometry is employed. A common feature of these models, however, is the lack of detail concerning the direct, heterogeneous decomposition of silane at silicon surfaces which must appear as a boundary condition in the numerical simulations.

As deposition pressures and temperatures are reduced to suppress homogeneous decomposition and improve deposition uniformity, the importance of these surface interactions increases relative to the homogeneous pyrolysis deposition pathway. Recently it was pointed out that overestimation of the rate of homogeneous silane pyrolysis under low pressure conditions has led to incorrect and misleading conclusions regarding the extent of gas-phase decomposition under low temperature, LPCVD conditions (9). As a result most silane deposition processes are completely controlled by surface chemistry which is, as yet, poorly understood and subject to considerable controversy. For the very low pressure conditions employed

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