

CrossMark
click for updatesCite this: *RSC Adv.*, 2014, 4, 58238Received 7th October 2014
Accepted 29th October 2014

DOI: 10.1039/c4ra11906a

www.rsc.org/advances

1,1,3,3-Tetramethylguanidinium hydrogen sulphate (TMG·HSO₄) ionic liquid in carbon dioxide enriched water: a highly efficient acidic catalytic system for the hydrolysis of cellulose†

Subodh Kumar, Raj Kumar Singh and Suman L. Jain*

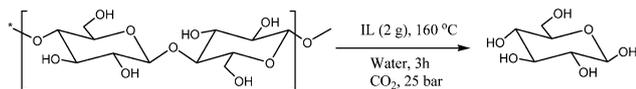
1,1,3,3-tetramethylguanidinium hydrogen sulphate (TMG·HSO₄) ionic liquid was used for the hydrolysis of cellulose using water enriched with carbon dioxide as the reaction media. The addition of carbon dioxide enhanced the reaction rates significantly and afforded glucose and total reducing sugars in 26 and 72% yields, respectively. The addition of carbon dioxide might play a dual role, it reduces the viscosity of the medium for better mass transfer and also reacts with water to give carbonic acid which subsequently dissociates to the hydronium ion and enhances the acidity of the medium. The developed ionic liquid was easily recovered and reused for a subsequent four runs without any significant change in the catalytic efficiency.

Depleting petroleum resources and the increasing demand and price of the petroleum products, has forced researchers to utilize sustainable natural resources for the production of alternative fuels (bio-ethanol, biofuels). One such important renewable resource is cellulose which is an abundantly underutilized biomass polysaccharide component consisting of a chain of β-(1,4)-linked glucose residues. For the commercial production of bio-ethanol, efficient and economical cellulose depolymerisation to produce glucose is an essential step to achieve the high conversion of cellulose to bio-ethanol through fermentation. The first important obstacle encountered in hydrolysis, processing, fusibility, and functionalization of cellulose is the insolubility of the cellulose in water and in common traditional organic solvents except under extreme conditions due to its molecular and supra molecular rigid structure as a consequence of hydrogen bonding. A second important drawback is the need for severe conditions such as the use of dilute sulphuric acid at high temperatures. To combat these issues, many solvent systems and catalytic strategies have been reported for the hydrolysis of cellulose. Solid acid catalysts have been found to be advantageous and

economical due to their reduced or even no corrosion, milder reaction conditions and ease of catalyst recovery. Conventional strong solid acid catalysts such as H-form zeolites, transition-metal oxides, cation-exchange resins, supported solid acids and heteropoly compounds, niobic acid, H-mordenite, Nafion and amberlist have been tried but showed poor efficiency^{1,2} then amorphous carbon materials bearing SO₃H, COOH and OH functions were used but the glucose yield only reached up to 4%.³ Nanostructured solid acid catalysts were also developed.⁴ The main drawback of these methods is the generation of lots of waste during the synthesis of these catalysts. Recently graphene oxide, a two-dimensional carbon lattice decorated by abundant oxygen functionalities, is demonstrated to be an efficient green catalyst towards selective hydrolysis of cellulose to glucose.⁵ Hydrolysis of cellulose into saccharides was also done utilizing magnetically separable functionalized graphene. It was observed that complete hydrolysis of cellulose takes place into glucose and small (4–5 unit size) oligomers using low (1 : 1) catalyst to cellulose ratio.⁶ As a consequence of the excellent work done by Rogers *et al.*^{7,8} who showed that the ionic liquid (IL) 1-butyl-3-methylimidazolium chloride ([C₄mim]⁺Cl⁻) is a powerful solvent for cellulose to make homogeneous solution, many efforts have been done to use the ionic liquids for the cellulose hydrolysis. Acidic catalyst in ionic liquid was demonstrated as an efficient system for hydrolysis of cellulose with improved total reducing sugars yield under mild conditions.⁹ Li and Zhao summarizes the hydrolysis conditions and yields of model substrate Sigma cell cellulose in solvent [C₄mim]⁺Cl⁻ with H₂SO₄ as the catalyst.¹⁰ To increase the efficiency of solid acid catalysts, the hydrolysis reaction was also performed in ionic liquids. In this regard, the macroporous styrene divinylbenzene resins functionalized with sulfonic groups (–SO₃H) proves to be powerful catalyst for the selective depolymerisation of cellulose dissolved in ionic liquids.^{11–13} However, due to higher cost and higher consumption of solid acid catalyst with ionic liquid makes this process unfeasible for the commercial production. Also the high activity of IL leads to further degradation of the reducing sugars and thus making their isolation

Chemical Sciences Division, CSIR-Indian Institute of Petroleum, Dehradun-248005, India. E-mail: suman@iip.res.in; Fax: +91-135-2660202; Tel: +91-135-2525788

† Electronic supplementary information (ESI) available. See DOI: 10.1039/c4ra11906a



Scheme 1 Acidic hydrolysis of cellulose.

tough. In addition to that some work on the acidic ionic liquid grafted over the nanoporous polymeric material was also reported.¹⁴ Mellvaine *et al.*¹⁵ reported the use of 1-methylimidazolium-3-ethylsulfonic acid triflate as catalyst for the depolymerisation of cellulose in an ionic liquid. Combination of solid acid catalyst, Amberlyst 15 DRY in ionic liquid (1-butyl-3-methylimidazolium chloride) and microwave irradiation provides a quite effective method which is useful for depolymerisation of natural polymers such as cellulose. However this solid catalyst is not really heterogeneous as acidity is being leached from it into IL.¹⁶ Nowadays the efforts are going to tune the activity of the ionic liquid which can work as efficient catalyst for the cellulose hydrolysis. Therefore, the development of highly active, selective and low cost new ionic liquids would be an emerging field for the conversion of cellulose into alternative fuels.

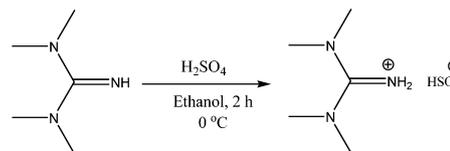
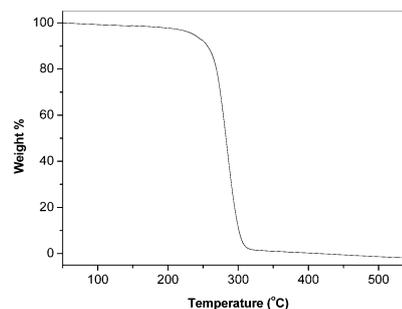
Protic ionic liquids, especially those based on the 1,1,3,3-tetramethylguanidine (TMG) are synthesized through simple neutralizing of equimolar TMG with acids have been found to be useful as catalysts for various organic transformations including Henry reaction,¹⁷ one-pot synthesis of pyran,¹⁸ synthesis of 3,4-dihydropyridin-2-(1*H*)-ones¹⁹ and direct Aldol reaction.²⁰

Inspired by literature reports on acid catalyzed reactions in CO₂ enriched high temperature liquid water²¹ and study on the viscosity of CO₂-ionic liquid system²² herein we report an efficient acidic catalytic system including 1,1,3,3-tetramethylguanidinium hydrogen sulphate ionic liquid (TMG·HSO₄) prepared from the reaction of 1,1,3,3-tetramethylguanidine and sulphuric acid in 1 : 1 molar ratio for hydrolysis of cellulose in water using CO₂ as additive at higher temperature (Scheme 1).

Synthesis and characterization of TMG·HSO₄ ionic liquid

In a typical experiment, TMG (20 mmol) was added in 100 mL of ethanol followed by the drop wise addition of H₂SO₄ (20 mmol in 30 mL of ethanol) at 0 °C under stirring. The stirring was continued for another 2 h. A white semi-solid material was isolated by decantation and washed thoroughly with ethanol, dried under vacuum for 6 h and then characterized by elemental analysis and ¹H and ¹³C NMR spectroscopy (Scheme 2).

Elemental analysis of the 1,1,3,3-tetramethylguanidinium hydrogen sulphate ionic liquid (TMG·HSO₄) reveals C = 35.71%, H = 6.59%, N = 14.12%, S = 9.53%, which was found to be in good agreement with the calculated values: C = 32.79%, H = 7.57%, N = 14.46%, S = 10.51%. Thermal stability of the catalyst was determined by thermo gravimetric analysis (TGA) under nitrogen atmosphere at 10 °C min⁻¹ of heating rate. As shown in Fig. 1, the 1,1,3,3-tetramethylguanidinium hydrogen

Scheme 2 Synthesis of TMG·HSO₄ ionic liquid.Fig. 1 TGA of TMG·HSO₄ ionic liquid.

sulphate ionic liquid (TMG·HSO₄) was found to be stable up to 250 °C and then degraded between 250–300 °C temperature range.

Furthermore, successful synthesis and identity of the synthesized ionic liquid were confirmed by ¹H and ¹³C NMR spectroscopy (Fig. S1†).

TMG·HSO₄ ionic liquid catalyzed hydrolysis of cellulose

Effect of CO₂ on cellulose hydrolysis

At first, the reaction of cellulose was carried out in water using TMG·HSO₄ as catalyst without adding CO₂. At 160 °C for 3 h the yield of total reducing sugar and glucose was found to be 48% and 14% respectively. However using CO₂ under 25 bar pressure to the reaction mixture, the yield of TRS and glucose was significantly increased and reached up to 72% and 26% respectively. As suggested in the literature,^{21,22} addition of CO₂ might be reducing the viscosity of reaction medium for better mass transfer and also it reacts with water at high temperature to yield carbonic acid, which subsequently dissociates to increase the hydronium ion concentration and in turn acidity of the medium.

To see the effect of pressure, the reaction was performed under different CO₂ pressure conditions. It is evident from Fig. 2 that beyond 25 bar pressure of CO₂ the yield of glucose unchanged. This is most likely due to the saturation of the reaction medium with carbon dioxide.

To ascertain the effect of CO₂ on the acidity of reaction medium, we also determined the acidity of the ionic liquid in water at higher temperature before and after the addition of CO₂ taking 4-nitroaniline as an indicator by using UV-visible spectroscopy (Fig. 3). The absorption spectra of IL having 4-nitroaniline in water with or without adding CO₂ is shown in Fig. 3. It is evident that absorbance of 4-nitroaniline is

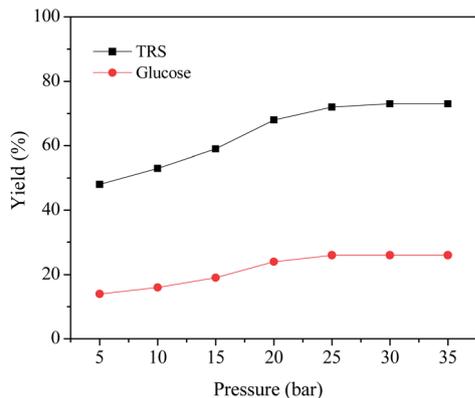


Fig. 2 Effect of CO₂ pressure on TRS and glucose yield.

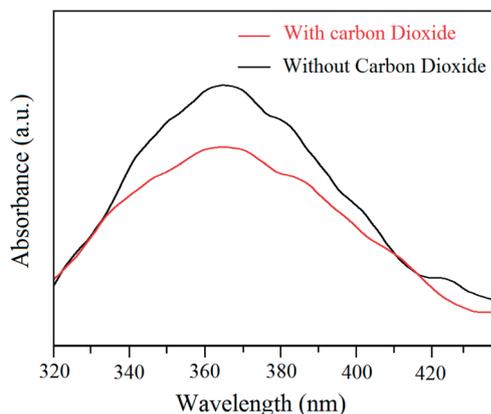


Fig. 3 UV-vis spectra of ionic liquid in water.

decreased because of protonation of 4-nitroaniline, indicating the higher acidity of the reaction mixture in presence of CO₂.

Effect of temperature

The effect of reaction temperature was studied to obtain the optimum temperature condition for the hydrolysis of cellulose in synthesized acidic ionic liquid as catalyst. To confirm the effect of hydrolysis temperature on the yield of TRS, we studied the hydrolysis of cellulose at different temperature *i.e.* 80, 100, 120, 140, 160 and 180 °C (Fig. 4). The hydrolysis rate at 160 °C was highest than the rate at other temperatures. The yield of TRS was found to be 72% in 3 h at 160 °C. While 58% of TRS yield was produced at 140 °C. At 80 °C the yield of TRS was found to be very low *i.e.* 36.2%. There is no doubt that reaction temperature has a great effect on the hydrolysis of cellulose. A higher hydrolysis temperature can shorten the reaction time and produced higher TRS yield. Meanwhile, the degradation of glucose begins earlier as shown in Fig. 4.

Effect of the TMG·HSO₄ ionic liquid concentration

The effect of acidic ionic liquid concentration on the hydrolysis of cellulose was studied. The amount of IL used was 0.1 g, 0.5 g, 1.0 g, 1.5 g, 2.0 g and 2.5 g respectively. As it was depicted in

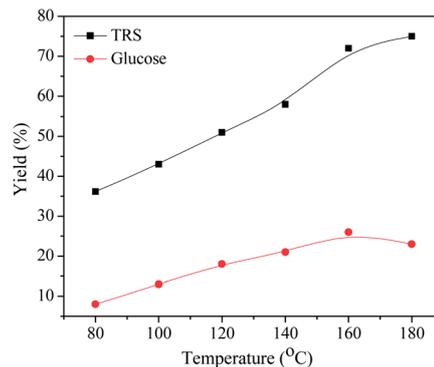


Fig. 4 Effect of temperature on TRS and glucose yield.

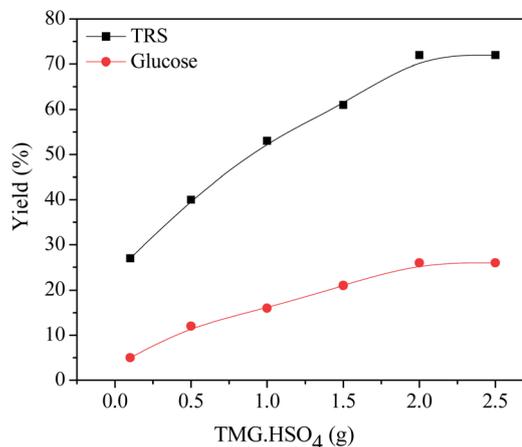


Fig. 5 Effect of TMG·HSO₄ concentration on TRS and glucose yield.

Fig. 5, when the dosage of IL is increased, TRS yield also increases at a certain point. Beyond this point, the yield of TRS becomes independent on the ionic liquid. Based on these results, the optimum conditions for hydrolysis of cellulose to produce maximum yield of TRS with effective yield of glucose was as follows: amount of ionic liquid (2.0 g), temperature 160 °C, CO₂ pressure 25 bar and reaction time 3 h.

Effect of reaction time

The TRS yields kept nearly constant and had a slowly decrease from the 4th hour due to the dehydration of monosaccharide such as glucose. It also observed that longer heating times produced excessive charring of the sample, giving black residues, and thus lowering the TRS and glucose yields (Fig. 6).

Reuse of the catalyst

The reusability of the catalyst was tested by using the same catalyst sample in four catalytic cycles using 2.0 g of catalyst at 160 °C applying 25 bar pressure of CO₂ for 3 h, and the results of these experiments are shown in Fig. 7. The yield of glucose and TRS in these recycling experiments are obtained as 26% and 72% (first run), 26% and 71.5% (second run), 25% and 71%

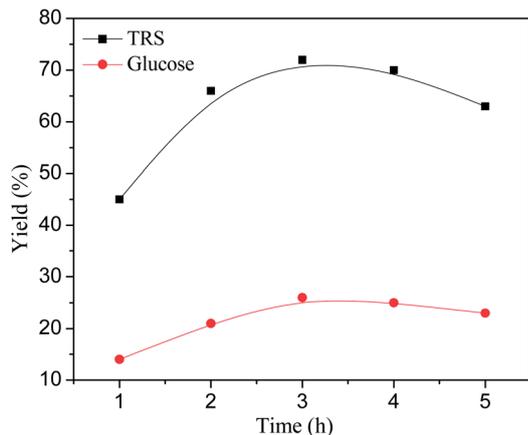


Fig. 6 Effect of time on TRS and glucose yield.

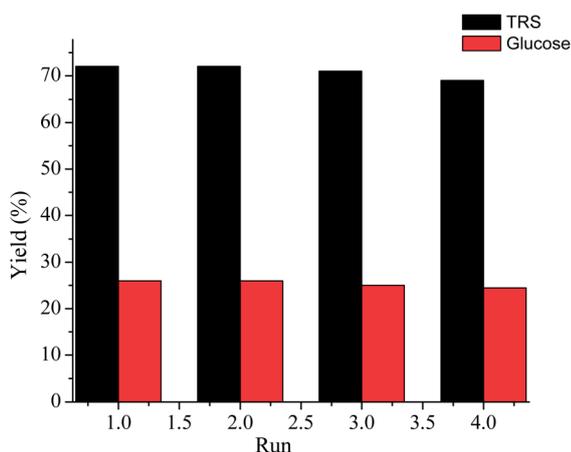


Fig. 7 Recyclability of TMG·HSO₄ ionic liquid.

(third run), 24.5% and 69% (fourth run) respectively. These results suggested that the recovered catalyst exhibited almost similar activity and can be reused at least for four runs without significant loss in catalytic activity.

In summary, we have demonstrated the significance enhancement in reaction rates by using CO₂ as additive in TMG·HSO₄ ionic liquid catalyzed hydrolysis of cellulose in water. The addition of CO₂ exhibited remarkable enhancement in product yield and afforded maximum TRS yields 72% with 26% glucose. In addition, the amount of catalyst used had great effect on the hydrolysis products. When the dosage of TMG·HSO₄ was higher, the dehydration rate of monosaccharide increased, which led to less accumulation of TRS and the increase of further dehydration products. The developed ionic liquid was found to be easily recoverable and recyclable for subsequent four runs without any significant loss in efficiency.

Typical experimental procedure for the hydrolysis of cellulose

Cellulose (0.25 g) and ionic liquid (2.0 g) was mixed in 5 mL of water. The resulting mixture was then transferred to the 15 mL

of Parr reactor. The reactor is then pressurized by carbon dioxide up to 25 bar and heated at 160 °C for 3 h. After being cooled the reaction mixture at room temperature, the CO₂ is vented out and the mixture was concentrated under reduced pressure. The resulting residue was diluted with methanol and the solid material which was settled down was separated by filtration. The methanol layer was concentrated under reduced pressure to recover the ionic liquid. The recovered ionic liquid was reused for subsequent runs. The solid thus obtained was mixed with water to dissolve the reducing sugars. The yield of total reducing sugars (TRS) was found to be 72% and the selectivity towards glucose was found to be 26%. Yield and selectivity is calculated with the help of calibration curves generated with commercially available standards using HPLC. Detailed information on the analytical method used to quantify glucose and TRS has been given in the ESI† file.

Acknowledgements

We kindly acknowledge Director IIP for his kind permission to publish these results. Analytical Science Division of the Institute is acknowledged for providing NMR and TGA analyses. SK is thankful to CSIR, New Delhi for his research fellowship.

Notes and references

- 1 F. Guo, Z. Fang, C. C. Xu and R. L. Smith Jr, *Prog. Energy Combust. Sci.*, 2012, **38**, 672–690.
- 2 Y. B. Huang and Y. Fu, *Green Chem.*, 2013, **15**, 1095.
- 3 S. Suganuma, K. Nakajima, M. Kitano, D. Yamaguchi, H. Kato, S. Hayashi and M. Hara, *J. Am. Chem. Soc.*, 2008, **130**, 12787–12793.
- 4 G. Feng and Z. Fang, *Series: Green Energy and Technology*, Springer Berlin Heidelberg, 2013, pp. 339–366.
- 5 X. Zhao, J. Wang, C. Chen, Y. Huang, A. Wang and T. Zhang, *Chem. Commun.*, 2014, **50**, 3439–3442.
- 6 D. Verma, R. Tiwari and A. K. Sinha, *RSC Adv.*, 2013, **3**, 13265–13272.
- 7 R. P. Swatloski, S. K. Spear, J. D. Holbrey and R. D. Rogers, *J. Am. Chem. Soc.*, 2002, **124**, 4974–4975.
- 8 R. C. Remsing, R. P. Swatloski, R. D. Rogers and G. Moyna, *Chem. Commun.*, 2006, 1271–1273.
- 9 C. Li, Q. Wang and Z. K. Zhao, *Green Chem.*, 2008, **10**, 177–182.
- 10 C. Li and Z. K. Zhao, *Adv. Synth. Catal.*, 2007, **349**, 1847–1850.
- 11 R. Rinaldi, R. Palkovits and F. Schuth, *Angew. Chem., Int. Ed.*, 2008, **47**, 8047–8050.
- 12 H. Watanabe, *Carbohydr. Polym.*, 2010, **80**, 1168–1171.
- 13 R. Rinaldi, N. Niklas, J. Vom Stein, R. Palkovits and F. Schueth, *ChemSusChem*, 2010, **3**, 266–276.
- 14 F. Liu, R. K. Kamat, I. Noshadi, D. Peck, R. S. Parnas, A. Zheng, C. Qi and Y. Lin, *Chem. Commun.*, 2013, **49**, 8456–8458.
- 15 W. B. Mellvaine, M. P. Foley, W. M. Reichert, J. J. Mandia, L. M. Haverhals, D. W. O. Sullivan, H. C. De Long and P. C. Trulove, *ECS Trans.*, 2010, **33**, 109–116.

- 16 I. A. Ignatyev, C. V. Doorslaer, P. G. N. Mertens, K. Binnemans and D. E. de Vos, *Holzforschung*, 2012, **66**, 417–425.
- 17 T. Jiang, H. X. Gao, B. X. Han, G. Y. Zhao, Y. H. Chang, W. Z. Wu, L. Gao and G. Y. Yang, *Tetrahedron Lett.*, 2004, **45**, 2699.
- 18 A. Shaabani, S. Samadi, Z. Badri and A. Rahmati, *Catal. Lett.*, 2005, **104**, 39–43.
- 19 A. Shaabani and A. Rahmati, *Catal. Lett.*, 2005, **100**, 177–179.
- 20 A. L. Zhu, T. Jiang, B. X. Han, J. Huang, J. C. Zhang and X. M. Ma, *New J. Chem.*, 2006, **30**, 736–740.
- 21 S. E. Hunter and P. E. Savage, *Ind. Eng. Chem. Res.*, 2003, **42**, 290–294.
- 22 Z. Liu, W. Wu, B. Han, Z. Dong, G. Zhao, J. Wang, T. Jiang and G. Yang, *Chem.–Eur. J.*, 2003, **9**, 3897–3903.