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REVERSIBLE DEHYDROGENATION-HYDROGENATION OF TETRAHYDROQUINOLINE-QUINOLINE USING A SUPPORTED COPPER NANOPARTICLE CATALYST

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Abstract – Copper nanoparticles synthesized on a titania surface (Cu/TiO₂) act as an efficient heterogeneous catalyst for the reversible dehydrogenation and hydrogenation of tetrahydroquinoline-quinoline under an atmospheric pressure of H₂.

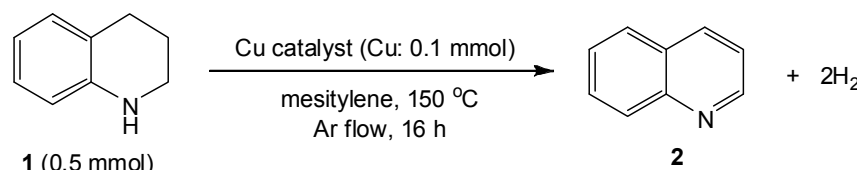
INTRODUCTION

Hydrogen has been proposed as a clean energy source and an alternative to fossil fuels for next-generation automobile and fuel cells, because only water is formed as a by-product after the consumption of hydrogen.¹ For a hydrogen-based energy infrastructure, efficient and safe storage, transportation, and supply of hydrogen are crucial issues.² Among the several approaches to accomplish this, the organic hydride strategy has attracted much attention as a promising method, wherein H₂ is stored or released from organic molecules through reversible hydrogenation and dehydrogenation using catalysts.³ The organic hydride method has significant advantages such as the safe use of recyclable organic hydrides, good handling, and no emission of CO, CO₂ or other by-products. Although reversible hydrogenation and dehydrogenation using cyclohexane/benzene and decalin/naphthalene pair systems have been reported, severe conditions of high temperature (> 200°C) and high H₂ pressure (30-80 atm) are required in these systems.^{3a-e}

This paper is dedicated to Prof. Albert Eschenmoser on the occasion of his 85th birthday

two equimolar amounts to **2**. Other inorganic materials-supported copper nanoparticles of Cu/Al₂O₃, Cu/SiO₂, Cu/MgO, and Cu/Hydroxyapatite (Cu/HAP) were prepared in similar ways and tested in the dehydrogenation of **1**. As summarized in Table 1, Cu/Al₂O₃ was also found to be an effective catalyst, whereas Cu/SiO₂, Cu/HAP, and Cu/MgO showed lower activities.⁸ The present dehydrogenation system using Cu/TiO₂ was applicable to scale-up conditions (20-mmol scale of **1**) and an identical yield of **2** could be obtained (entry 2). In heterogeneous catalysts in the liquid-phase reaction, leaching of the active metal species from the support into the reaction solvent is a significant issue. In the course of the dehydrogenation of **1** using Cu/TiO₂, the solid Cu/TiO₂ was filtered off at a 50% conversion of **1**. Further stirring of the filtrate under similar reaction conditions did not afford any products, showing that the dehydrogenation took place on the surface of Cu/TiO₂. In addition, no copper ions in the filtrate were confirmed by ICP analysis (detection limit: 0.054 ppm).

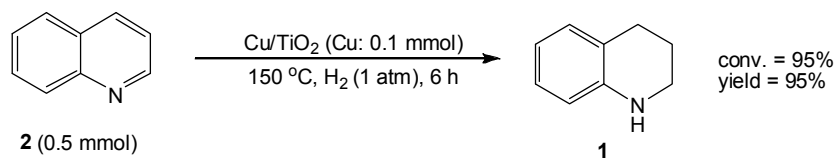
Table 1. Dehydrogenation of 1,2,3,4-tetrahydroquinoline catalyzed by various Cu catalysts^a

 1 (0.5 mmol) Cu catalyst (Cu: 0.1 mmol) 2 + 2H₂ mesitylene, 150 °C Ar flow, 16 h			
Entry	Cu catalyst	Conv. (%) ^b	Yield (%) ^b
1	Cu/TiO ₂	>99	>99
2 ^c	Cu/TiO ₂	98	97
3	Cu/Al ₂ O ₃	92	92
4	Cu/SiO ₂	69	68
5	Cu/HAP	64	64
6	Cu/MgO	29	29

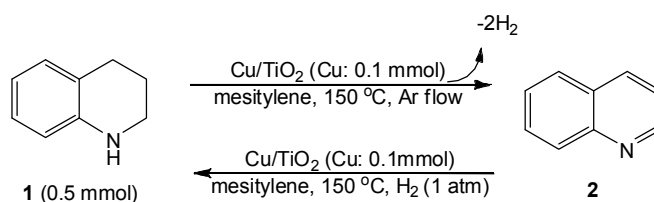
^a Reaction conditions: Cu catalyst (Cu: 0.1 mmol), mesitylene (5.0 mL), 16 h.

^b Determined by GC using an internal standard technique. ^c **1** (20 mmol), Cu/TiO₂ (5.1 g), mesitylene (50 mL), 12 h.

Next, the hydrogenation of **2** into **1** was carried out using Cu/TiO₂. We found that **2** could be successfully hydrogenated with Cu/TiO₂ at 150 °C under 5 atm of H₂ in mesitylene for 3 h, affording **1** in 92% yield. It is noted that the hydrogenation quantitatively proceeded even under an atmospheric pressure of H₂ (Scheme 2). The previously reported systems using copper catalysts required high pressure (> 30 atm) and/or temperature to achieve a high yield of **1**.⁹ From the above results, Cu/TiO₂ was found to be an effective catalyst for both the dehydrogenation of **1** and hydrogenation of **2**.

Scheme 2. Hydrogenation of quinoline catalyzed by Cu/TiO₂ under 1 atm of H₂

To further investigate the reversibility of the present tetrahydroquinoline/quinoline system, successive dehydrogenation-hydrogenation of **1/2** using Cu/TiO₂ was repeated (Table 2). After the quantitative dehydrogenation of **1** into **2** (entry 1), the Ar atmosphere was replaced with 1 atm of H₂ and the reaction mixture was heated again and stirred at 150 °C. The above treatment gave the product **1** in 95% yield for 6 h, which is shorter reaction time than that of the dehydrogenation (entry 2). Molecular hydrogen could be released and stored using the present tetrahydroquinoline/quinoline catalyst system. These reversible dehydrogenation and hydrogenation reactions could be repeated with retention of high efficiency (entries 3 and 4).

Table 2. Reversible dehydrogenation and hydrogenation between **1** and **2** using Cu/TiO₂ catalyst^a

Entry		Time (h)	Conv. (%) ^b
1	dehydrogenation (1st)	16	99
2	hydrogenation (1st)	6	95
3	dehydrogenation (2nd)	16	98
4	hydrogenation (2nd)	6	94

^a Reaction conditions: Cu/TiO₂ (0.13 g, Cu: 0.1 mmol), mesitylene (5 mL).^b Determined by GC.

CONCLUSION

In conclusion, we prepared TiO₂-supported copper nanoparticles that acted as a heterogeneous catalyst for the reversible dehydrogenation and hydrogenation of tetrahydroquinoline/quinoline. The Cu/TiO₂-catalyzed organic hydride system could be conducted under mild reaction conditions and repeated. This is the first report of a reversible organic hydride system using a heterogeneous catalyst with 1 atm of H₂. This strategy will give a clue to the development of a highly efficient, practical organic hydride system.

EXPERIMENTAL

1) General

All organic reagents were purified before use. Copper (II) trifluoromethanesulfonate was purchased from Tokyo Kasei Kogyo Co., Ltd. TiO_2 (JRC-TIO-4), Al_2O_3 (JRC-ALO-3), SiO_2 (JRC-SIO-4), MgO (JRC-MGO-1) were obtained from the Catalysis Society of Japan as reference catalysts. Hydroxyapatite (HAP) was purchased from Wako Pure Chemical Industries, Ltd. Inductively coupled plasma measurement was performed by SII NanoTechnology SPS7800. ^1H and ^{13}C nuclear magnetic resonance (NMR) spectra were recorded on JEOL JNM-AL400 and JNM-GSX270 spectrometers, respectively. Gas chromatography (GC-FID) was carried out a Shimadzu GC-2014 equipped with a KOCL-3000T column (2 m).

2) Characterization of Cu/TiO_2

Elemental analysis showed that the copper loading was 4.91 wt%. UV-vis spectra were recorded on a JASCO V-550 spectrometer equipped with integration spheres at room temperature. BaSO_4 was used as a standard reflection sample.

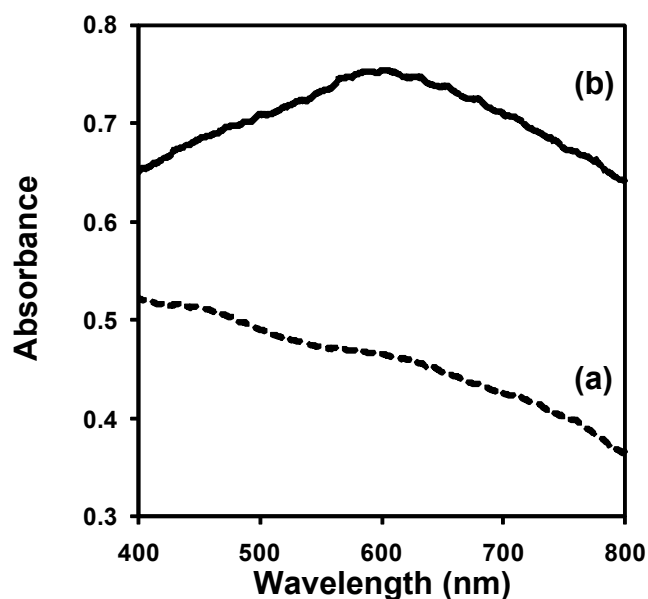


Figure 1S. UV-vis absorption spectra of (a) $\text{Cu}^{\text{II}}/\text{TiO}_2$ (dashed line) and (b) Cu/TiO_2 (solid line).

3) Typical reaction procedure

3-1) Dehydrogenation of 1,2,3,4-Tetrahydroquinoline (**1**)

A typical procedure for the dehydrogenation of **1** by Cu/TiO_2 : $\text{Cu}^{\text{II}}/\text{TiO}_2$ (0.13 g, 0.01 mmol of Cu) was placed in a Schlenk tube equipped with a reflux condenser. The vessel was evacuated and filled with 1 atm of molecular hydrogen (H_2) and the solid catalyst was stirred at 180 °C for 0.5 h. After replacing the H_2 with Ar, a mineral oil bubbler was attached to the top of the condenser, mesitylene (5 mL) and **1** (0.5

mmol) were added, and the reaction mixture was vigorously stirred at 150 °C under a stream of Ar for 16 h. The solid catalyst was removed by centrifugation and the yield was determined by GC analysis with naphthalene as an internal standard [Shimadzu GC-8A; carrier gases: N₂ (50 kPa), H₂ (50 kPa), and air (50 kPa); column: 5% KOCL-3000T (5.0 m); oven temperature program: from 100 °C, 10 °C/min up to 220 °C, hold for 10 min; injection and detection temperature: 270 °C; retention time: **1** (10.9 min), **2** (9.3 min), naphthalene (7.16 min)].

3-2) Hydrogenation of quinoline (2)

A typical procedure for the hydrogenation of **2** by Cu/TiO₂: Cu^{II}/TiO₂ (0.13 g, 0.01 mmol of Cu) was placed in a Schlenk tube equipped with a reflux condenser. The vessel was evacuated and filled with 1 atm of molecular hydrogen (H₂) and the solid catalyst was stirred at 180 °C for 0.5 h. A balloon filled with hydrogen was connected to the top of the condenser. Mesitylene (5 mL) and **2** (0.5 mmol) were added, and the reaction mixture was vigorously stirred at 150 °C for 6 h. The solid catalyst was removed by centrifugation and the yield was determined by GC analysis with naphthalene as an internal standard.

3-3) Reversible dehydrogenation and hydrogenation between **1** and **2**

A typical procedure for the dehydrogenation of **1** by Cu/TiO₂: Cu^{II}/TiO₂ (0.13 g, 0.01 mmol of Cu) was placed in a Schlenk tube equipped with a reflux condenser. The vessel was evacuated and filled with 1 atm of molecular hydrogen (H₂) and the solid catalyst was stirred at 180 °C for 0.5 h. After replacing the H₂ with Ar, a mineral oil bubbler was attached to the top of the condenser, mesitylene (5 mL) and **1** (0.5 mmol) were added, and the reaction mixture was vigorously stirred at 150 °C under a stream of Ar for 16 h. The yield of **2** was determined by GC analysis. Next, the atmosphere of the flask was replaced with 1 atm of H₂. The mixture was magnetically stirred for 6 h at 150 °C. The yield of **1** was determined by GC analysis. The above procedures were repeated.

3-4) Measurement of H₂

The dehydrogenation was carried out in a closed vessel under standard reaction conditions. After the reaction, the gas phase was subjected to GC-TCD for qualitative and quantitative analysis of H₂. GC conditions were as follows: GC using thermal conductivity detector (Shimadzu GC-8A); column: molecular sieves 13X (4.0 m); oven temperature: 40 °C; injection and detection temperature: 70 °C; carrier gas: Ar (100 kPa); current: 60 mA; retention time: H₂ (3.0 min). Evolution of H₂ was also confirmed volumetrically using a gas buret attached to the reactors.

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