

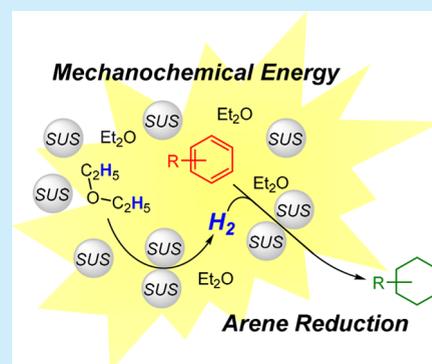
Stainless Steel-Mediated Hydrogen Generation from Alkanes and Diethyl Ether and Its Application for Arene Reduction

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Supporting Information

ABSTRACT: Hydrogen gas can be generated from simple alkanes (e.g., *n*-pentane, *n*-hexane, etc.) and diethyl ether (Et₂O) by mechanochemical energy using a planetary ball mill (SUS304, Fritsch Pulverisette 7), and the use of stainless steel balls and vessel is an important factor to generate the hydrogen. The reduction of organic compounds was also accomplished using the in-situ-generated hydrogen. While the use of pentane as the hydrogen source facilitated the reduction of the olefin moieties, the arene reduction could proceed using Et₂O. Within the components (Fe, Cr, Ni, etc.) of the stainless steel, Cr was the metal factor for the hydrogen generation from the alkanes and Et₂O, and Ni metal played the role of the hydrogenation catalyst.



Hydrogen technology is becoming of increasing importance as an alternative manner to avoid global climate changes, which are mainly based on the emission of carbon dioxide (CO₂) derived from the combustion of fossil fuels.¹ Because industrial hydrogen production methods using fossil fuels such as methane (CH₄) as its raw materials emit substantial quantities of CO₂ as a byproduct, it is quite important to spur the development of new CO₂-free practical technologies for hydrogen production resulting in the coproduction of elemental carbon.² The transition-metal-catalyzed CO₂-free hydrogen generation consisting of dehydrogenation and C–C bonds cleavage reactions (decomposition) of alkanes is a useful strategy to produce H₂ gas.^{2,3} Although such alkane-decomposition techniques have been the subject of active investigations in the past two decades, industrial practical hydrogen production (hydrogen recovery) processes have still not been developed. On the other hand, the reduction of organic compounds is a fundamental reaction in organic chemistry. In particular, the catalytic hydrogenation of resonance-stabilized arenes^{4,5} is an important method for accessing the corresponding cyclohexane derivatives, which are utilized as functional materials and are expected to be used for hydrogen storage as liquid organic hydrogen carrier (LOHC) systems in the energy field.⁶ However, the use of large amounts of industrially produced flammable H₂ gas under high pressure and temperature is constantly required.⁴ From the point of view of safety, easy handling, and the reduction of environmental burdens, the development of a CO₂-free direct arene hydrogenation (hydrogen transfer) method from a LOHC is extremely attractive. We have previously developed a heterogeneous noble metal-catalyzed arene hydrogenation reaction using isopropanol as the CO₂-free hydrogen source.⁵

Meanwhile, we have also recently accomplished a stainless-steel (SUS304) and mechanochemical energy-mediated quantitative hydrogen generation reaction from water (water splitting),^{7a} and the in-situ-generated hydrogen could be utilized as a reductant of the coexisting reducible functional groups (alkyne, alkene, aromatic halides, nitro group, azide, ketone, etc.) in a planetary ball milling vessel.^{7b} We now report the stainless-steel (SUS304) and mechanochemical energy-mediated CO₂-free hydrogenation reaction of alkenes, alkynes, and ketones using alkanes and diethyl ether (Et₂O) to generate the appropriate quantities of H₂ gas; the process is accompanied by the formation of gaseous molecular hydrocarbons such as CH₄, generated by C–C bond cleavage of the parent alkanes and Et₂O. It is noteworthy that the hydrogenation of resonance-stabilized aromatic nuclei could also be achieved by using Et₂O as the hydrogen source to give the cyclohexane derivatives without the use of any noble-metal catalysts.

Liquid alkanes as a part of the LOHCs are easily available and inexpensive, because of their production from fossil fuels, in most cases, and their frequent use as solvents in synthetic organic chemistry. First, the reactivity of alkanes in the hydrogen generation was investigated (see Table 1). Pentane (*n*-C₅H₁₂, 15 mmol) could be smoothly transformed to H₂ (0.93 mmol), along with the generation of CH₄ (2.36 mmol) and trace amounts of ethane and propane by the mechanochemical reaction using a planetary ball milling device equipped with stainless steel (SUS304) balls and a vessel at a 800 rpm rotation speed for 1 h (entry 1 in Table 1).⁸ Hexane (*n*-C₆H₁₄) and heptane (*n*-C₇H₁₆) could also serve as hydrogen

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Table 1. Hydrogen Generation Activity of Alkanes under Ball Milling Conditions^a

entry	alkane	Generated Gas ^b (mmol)	
		H ₂	CH ₄
1	<i>n</i> -C ₅ H ₁₂	0.93	2.36
2	<i>n</i> -C ₆ H ₁₄	1.06	0.84
3	<i>n</i> -C ₇ H ₁₆	2.05	0.62
4	<i>n</i> -C ₁₀ H ₂₂	not detected	not detected

^aThe reaction was carried out using a Fritsch Pulverisette 7 Premium Line 7 Ball Mill (PLP-7) that was equipped with a 80 mL SUS304 vessel and 100 SUS304 balls (diameter: ca. 5 mm). Alkanes were purchased from commercial sources and used without further purification. ^bThe total quantity of the generated gas and the proportion of hydrogen, methane, etc., including nitrogen and oxygen contaminated from the air during operation are described in the Supporting Information. Trace amounts of ethane and propane were also detected by the GC analysis.

sources (entries 2 and 3 in Table 1), while no hydrogen generation was observed using decane (*n*-C₁₀H₂₂) as a substrate (entry 4 in Table 1).

The in-situ-generated H₂ in a SUS304 ball milling vessel could be utilized for the reduction of olefin (see Table 2). 1,1-

Table 2. Hydrogenation of Olefin Using Alkane as a Hydrogen Source^a

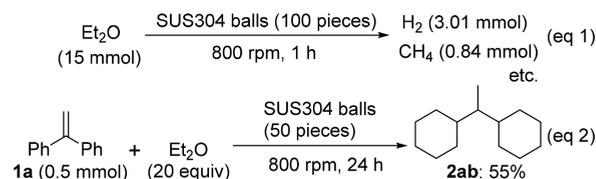
entry	alkane	Yield (%)	
		recovered 1	2aa
1	<i>n</i> -C ₅ H ₁₂	60	24
2	<i>n</i> -C ₆ H ₁₄	92	6
3 ^b	<i>n</i> -C ₇ H ₁₆	no reaction	
4 ^b	<i>n</i> -C ₁₀ H ₂₂	no reaction	
5	<i>c</i> -C ₅ H ₁₀	76	10
6	<i>c</i> -C ₆ H ₁₂	85	6
7 ^c	<i>n</i> -C ₅ H ₁₂	0	55
8 ^{c,d}	<i>n</i> -C ₅ H ₁₂	68	16

^aThe reaction was carried out using a Fritsch Pulverisette 7 Classic Line Ball Mill (PL-7) that was equipped with a 12 mL SUS304 vessel and 50 SUS304 balls (diameter: ca. 5 mm). Alkanes were purchased from commercial sources and used without further purification. ^bThe use of distilled *n*-C₇H₁₆ or *n*-C₁₀H₂₂ resulted in no reaction. ^c20 equiv of *n*-C₅H₁₂ were used, and the reaction was carried out for 24 h. ^d1.0 mol of 1a was used using a Fritsch Pulverisette 7 Classic Line Ball Mill (PL-7) equipped a 12 mL SUS304 vessel and 50 SUS304 balls (diameter: ca. 5 mm).

Diphenylethane (2aa) as a hydrogenated product was produced by the rotation (800 rpm) of a mixture of 1,1-diphenylethene (1a; 0.5 mmol), 10 equiv of *n*-C₅H₁₂ and 5 mm diameter SUS304 balls (50 pieces) in a 12 mL SUS304 vessel for 6 h in 24% yield, together with 60% of unchanged 1a (Table 2, entry 1). *n*-C₆H₁₄ was the apparent hydrogen source in this instance (Table 2, entry 2), since *n*-C₇H₁₆ and *n*-C₁₀H₂₂ were ineffective as reaction solvents (Table 2, entries 3 and 4). The hydrogenation activity was not correlated with the in-situ-generated H₂ amount (compare Tables 1 and 2). The cyclic alkanes, such as *c*-C₅H₁₀ and *c*-C₆H₁₂, possessed similar

hydrogenation activities, in comparison to *n*-C₅H₁₂ and *n*-C₆H₁₄. The use of *n*-C₅H₁₂ (20 equiv) for a longer rotation time (24 h) completed the reduction of 1a to give 2aa in moderate yield (Table 2, entry 7).⁸ A 1.0 mol scale reaction of 1a using the same vessel (12 mL) and number of balls (50 pieces) lowered the reactivity (Table 2, entry 8), which indicated that the internal capacity of the vessel and the ball number might need to be increased for scaleup.

Et₂O also proved to be an efficient hydrogen source under the same reaction conditions, as shown in Table 1, and 3.01 mmol H₂ gas and 0.84 mmol CH₄ were produced from 15 mmol Et₂O in 1 h (eq 1). Intriguingly, and contrary to our



expectations, the hydrogenation of 1a could be accomplished at 800 rpm in the presence of 20 equiv of Et₂O as a hydrogen source to generate 1,1-dicyclohexylethane (2ab). Here, hydrogenation of the olefin moiety, as well as the aromatic nuclei, occurred (eq 2).

Via this protocol, a wide variety of arene derivatives were mechanochemically hydrogenated in the presence of Et₂O as a hydrogen source (see Table 3). The detailed optimization using *n*-heptylbenzene (1b, 0.5 mmol) as a simple arene substrate has been described in the Supporting Information (Table S2). The aromatic nucleus of 1b was thoroughly hydrogenated to produce 2b in 67% yield (Table 3, entry 1). Biphenyl (1c) and diphenylmethane (1d) bearing two aromatic rings within the molecule were also hydrogenated to the corresponding bicyclohexane derivatives (2c and 2d) in moderate yields (Table 3, entries 2 and 3). Diphenylacetylene (1e) and stilbene (1f) were transformed to 1,2-dicyclohexylethane (2e) with complete hydrogenation of the aromatic nuclei as well as the alkyne and alkene moieties (Table 3, entries 4 and 5). Naphthalene (1g) was also entirely hydrogenated to give bicyclo[4,4,0]decane (decaline, 2ga and 2gb) as a mixture of *cis* and *trans* isomers (Table 3, entry 6). Benzophenone (1h) also efficiently underwent arene hydrogenation to give dicyclohexylmethane (2d), along with hydrogenolysis of the ketone function (Table 3, entry 7). 2-Dodecanone (1i) as an aliphatic ketone was less reactive, and 2-dodecanol (2i) as a secondary alcohol was obtained in 32% yield in association with the recovery of the unchanged starting material (61%, 1i). Meanwhile, the aliphatic alkyne functionalities of 1j and 1l were efficiently hydrogenated to the corresponding alkanes (2j and 2l) in good yields (Table 3, entries 9 and 10).

Mechanochemical energy could be effectively applied to various reactions,⁹ and the metallic component of the ball mill system sometimes facilitated the desired reaction.¹⁰ The present SUS304 and mechanochemical energy-mediated hydrogen generation from alkanes and Et₂O in a SUS304 ball milling vessel never proceeded when using ZrO₂ balls (diameter 5 mm) and a vessel (20 mL, Table 4, entry 1). Stainless steel (SUS304) is composed of Fe, Cr, and Ni as the main components (Fe, 69%; Cr, 18%–20%; Ni, 8%–10%). Therefore, the metal efficiencies to promote the H₂ gas generation using Et₂O (3.75 mmol) under the stated ball milling conditions were next investigated via the addition of zerovalent

Table 3. Scope of Substrates^a

substrate + Et ₂ O (0.5 mmol) (20 equiv)		SUS304 balls 800 rpm, 24 h	product	yield (%)
1				67
2				56
3				61
4				48
5				49
6				27 (30:70)
7				43
8				32 (61) ^b
9				86
10				64

^aThe reaction was carried out using a Fritsch Pulverisette 7 Classic Line Ball Mill (PL-7) equipped a 12 mL SUS304 vessel and 50 SUS304 balls (diameter: ca. 5 mm). Et₂O was purchased from commercial sources and used without further purification. ^bRecovery of the substrate.

Table 4. Essential Metal To Generate Hydrogen and Methane^a

Et ₂ O (3.75 mmol)		ZrO ₂ balls, additive (0.5 equiv)	analysis of gas component	
		800 rpm, 0.5 h	Generated Gas (mmol)	
entry	additive		H ₂	CH ₄
1			not detected	not detected
2	Fe		not detected	not detected
3	Cr		0.52	0.075
4	Ni		not detected	not detected

^aThe reaction was carried out using a Fritsch Pulverisette 7 Premium Line 7 Ball Mill (PLP-7) that was equipped with a 20 mL ZrO₂ vessel and 25 ZrO₂ balls (diameter: ca. 5 mm). Et₂O was purchased from commercial sources and used without further purification.

Fe, Cr, or Ni powder (0.5 equiv) in the ZrO₂ vessel (20 mL) with ZrO₂ balls (25 pieces). As a result, significant amounts of generated hydrogen could be observed in the presence of Cr powder (Table 4, entry 3), while the addition of Fe or Ni powder proved totally ineffective (Table 4, entries 2 and 4).

Furthermore, the role of the metal components of SUS304 that influenced the hydrogenation were also investigated under atmospheric H₂ conditions (Table 5). 1,1-Diphenylethene (**1a**)

Table 5. Essential Metals for Hydrogenation^a

substrate (0.5 mmol)		H ₂ , ZrO ₂ balls (25 pieces)	additive (1 equiv)	product	yield (%)
		800 rpm, 3 h			
entry	substrate	additive	product	yield (%)	
1		none	no reaction		
2	1a	Fe		1 (54) ^b	
3	1a	Cr	2aa	5 (62) ^b	
4	1a	Ni	2aa	63	
5		none, Fe, Cr or Ni	no reaction		
6 ^c	1b	Ni		38 (23) ^b	

^aThe reaction was carried out using a Fritsch Pulverisette 7 Premium Line 7 Ball Mill (PLP-7) equipped a 20 mL ZrO₂ vessel and 25 ZrO₂ balls (diameter: ca. 5 mm). ^bRecovery of the substrate. ^cThe reaction was carried out under H₂ (5 atm) using 75 ZrO₂ balls.

was never hydrogenated by ball milling (800 rpm for 3 h) in a ZrO₂ vessel (20 mL) in the presence of ZrO₂ balls (25 pieces) (Table 5, entry 1). While the addition of Fe or Cr powder (1 equiv) was ineffective for the hydrogenation (Table 5, entries 2 and 3), 1 equiv of Ni powder as an additive did facilitate the hydrogenation of the olefin function of **1a** to the alkane product (**2aa**) (Table 5, entry 4). While the arene hydrogenation of **1b** never proceeded without an additive or the addition of Fe, Cr, or Ni powder (1 equiv) (Table 5, entry 5), it could proceed in the presence of Ni powder under pressurized H₂ conditions (5 atm) using 75 ZrO₂ balls. Therefore, the progression of the mechanochemically mediated arene hydrogenation requires the appropriate internal pressure of the SUS304 ball milling vessel. Since the internal temperature of the SUS304 ball milling vessel under 800 rpm rotation conditions reaches ~60 °C,^{7a} the use of several organic solvents with low boiling points, such as *n*-pentane (boiling point (bp) = 36.1 °C), *c*-pentane (bp = 49 °C), and diethyl ether (bp = 34.6 °C), indicated a good progression of the hydrogenation (see Table 2 and eq 2). Therefore, *n*-heptane (bp = 98.3 °C) as a higher-boiling-point solvent may be inefficient, as shown in entry 3 in Table 2. These results indicate that Cr metal is an absolutely essential metal for the H₂ generation, and the hydrogenation is thoroughly catalyzed by Ni metal. However, both reactions were much more effectively facilitated by stainless steel 304 as an alloy of Fe, Cr, and Ni, in comparison to the independent use of Cr or Ni. Actually, a small amount of SUS304 alloy was collisionally eroded from balls in the mixture as a fine powder during the arene reduction in the presence of Et₂O (eq 2), although the precise role of each metal is still under investigation.¹¹

In conclusion, hydrogen transfer utilizing alkanes and Et₂O as hydrogen sources has been accomplished under mechanochemical (ball milling) conditions using SUS304 balls and an SUS304 vessel. The in-situ-generated hydrogen could be used

to hydrogenate a variety of reducible functionalities on the organic compounds. In particular, Et₂O was applicable as a pseudo-reductant for the hydrogenation of aromatic nuclei to produce the materially useful cycloalkane derivatives. The present reaction is an innovative hydrogenation method for the direct (one-pot) utilization of hydrogen atoms on LOHC molecules and it can also be expected to contribute to the further application of alkanes and ethers as clean energy processes without CO₂ production for the next generation.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: [10.1021/acs.orglett.8b00931](https://doi.org/10.1021/acs.orglett.8b00931).

Synthetic procedures and spectroscopic data for the products (PDF)

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Notes

The authors declare no competing financial interest.

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(11) 50 balls (5 mm diameter, total 22.9 g) was used for the reaction of **eq 2**, and total 21.9 g of balls was recovered. These results indicated that all metallic components (Fe, Cr, Ni, etc.) were eroded in the reaction mixture as a fine powder during the milling. Meanwhile, the weight of vessel fairly remained unchanged. The residual metals of product (**2ab**) were measured by atomic absorption spectrometry. Consequently, a quite trace amount of Fe species was detected [0.3 ppm of Fe metal was observed in 50 mL Et₂O solution of 0.55 mmol product **2ab** (106.9 mg)], while other metals were not detected.