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Process Safety Considerations for the Supply of a High Energy Oxadiazole IDO1-Selective Inhibitor

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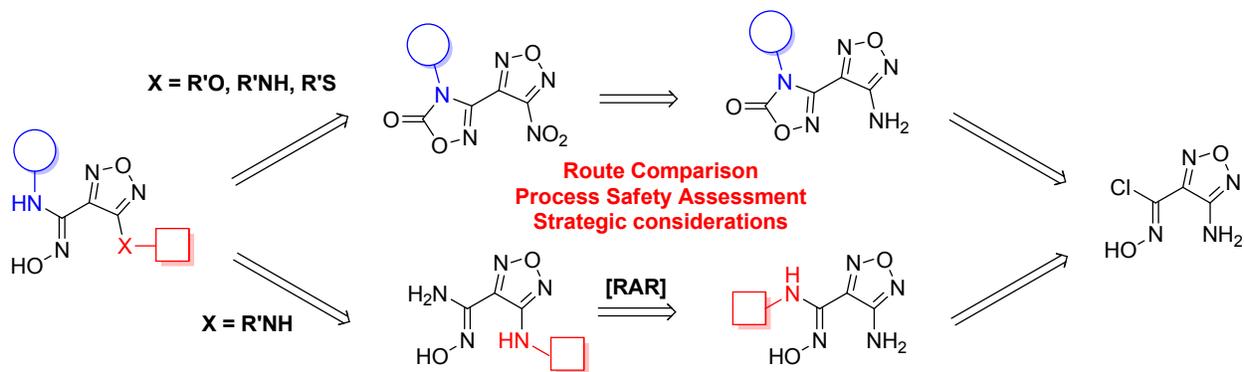
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TOC GRAPHIC



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4 ABSTRACT: The development of a stereospecific synthesis of a IDO1-selective inhibitor
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7 is described. The synthetic strategy towards enabling early discovery efforts along with
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10 additional findings pertaining to process safety which limited scalability are outlined. A
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13 convergent approach that supported the synthesis of material suitable for early pre-
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16 clinical and/or GLP toxicology studies, and which avoided the formation of key high
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19 energy intermediates is summarized.
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26 KEYWORDS: Process Safety, Oxadiazole, Benzocyclobutylamine, IDO1
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INTRODUCTION

Continued interest in immuno-oncology has been spurred by the demonstrated durable responses observed in patients treated with anti-PD1 mAb (e.g., pembrolizumab), among other therapies.¹ Indoleamine-2,3-dioxygenase-1 (IDO1) has been shown to play an important role in immunomodulation.² Moreover, IDO1 is over-expressed in multiple tumor types (including melanoma, colon, and ovarian), and this mechanism is believed to contribute to immunosuppression, which in turn may promote tolerance to the cancer.^{3,4} The combination of IDO1 inhibitors and anti-PD1 mAbs has been shown to be synergistic in efficacy models,⁵ and multiple clinical trials are currently evaluating the efficacy of this combination as a means of improving response rates while maintaining durability.

Notably, epacadostat (INCB24360; **1**, Figure 1)⁶ has been developed to this end, and is currently being evaluated in multiple clinical trials in combination with anti-PD1 mAb therapy (pembrolizumab, nivolumab, etc.). Additional IDO1 inhibitors have been developed and reported upon in the literature.⁷

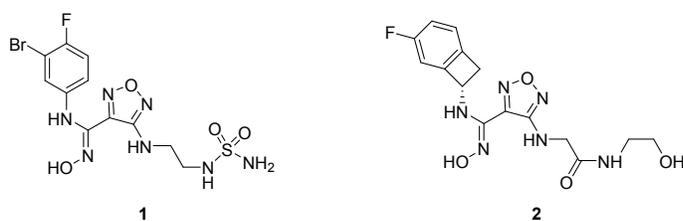


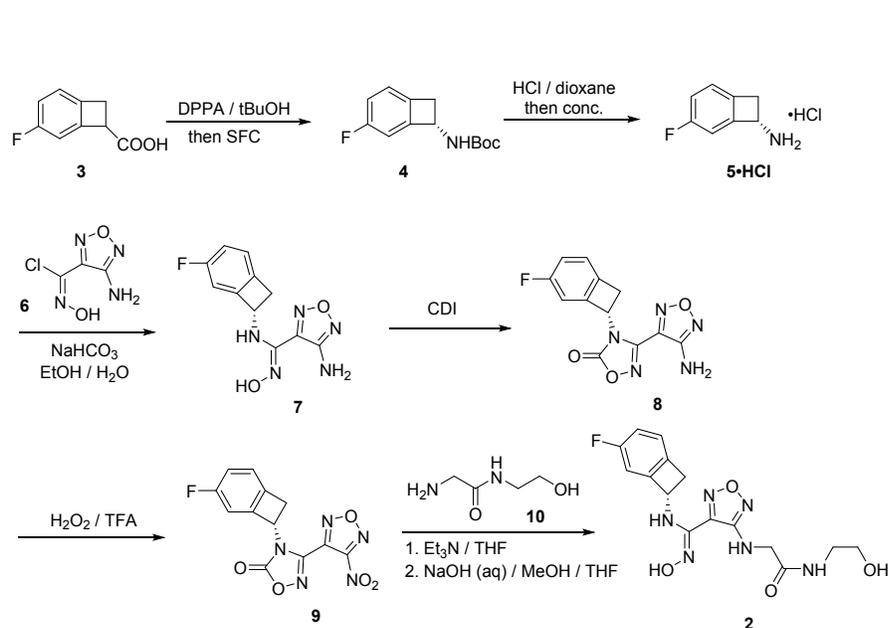
Figure 1. Structure of epacadostat (**1**) and **2**

Recently, we sought a synthetic approach to structures such as **2** that enabled the discovery effort around this target (IDO1) and facilitated the construction of Structure-Activity Relationship (SAR) around both sides of the oxadiazole.⁷ The following discussion will feature strategic elements surrounding the supply of **2**, including route planning with regards to availability of the building blocks and safety, as well as impact of the selection of these building blocks or intermediates on the delivery timeline.

INITIAL ROUTE TO **1** AND PRELIMINARY EVALUATION

Initial access to **2** (Scheme 1) started from benzocyclobutyl carboxylic acid **3**, which was initially available in small quantities, and converted to the amine using a Curtius rearrangement.⁷ Initial efforts to support SAR for this target (IDO1) carried the racemic carbamate (**rac-4**) forward, with a resolution of the final inhibitor (e.g., **2**), typically using supercritical fluid chromatography with a chiral stationary phase (“chiral SFC”).

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4 However, once the configuration of the optimal benzocyclobutylamine building block
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7 was determined to be (*S*), this intermediate was amenable to early resolution, which
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10 facilitated downstream operations by avoiding resolution of each new compound. The
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13 racemic *N*-Boc amine was resolved using chiral SFC to afford **4**. After deprotection to
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16 afford the benzocyclobutylamine hydrochloride salt (**5**•HCl), hydroxyamidine **7** was
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19 formed by condensation with commercially-available imidoyl chloride **6**.⁸ The
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22 hydroxyamidine was protected as the cyclic carbamate by reaction with
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25 carbonyldiimidazole (CDI), and the amino-oxadiazole (**8**) was oxidized to the nitro-
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28 oxadiazole (**9**) using hydrogen peroxide in trifluoroacetic acid (TFA) or sulfuric acid.⁹
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32 The final product was obtained by condensation of the ethanolamine side chain (**10**)
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35 through displacement of the nitrooxadiazole and subsequent deprotection of the
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38 carbamate.
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Scheme 1. Initial route to 2

A significant advantage of the route outlined in Scheme 1 is that intermediate **9** was a versatile building block for rapidly enabling SAR evaluation of the tailpieces, with the nitro group being a suitable leaving group for a variety of nucleophiles (amine, alcohol, thiol, etc.).¹⁰ However, the route was also limiting in that the stereogenic and arguably more precious portion of the molecule was installed first. This produced a potential bottleneck, as availability of benzocyclobutylamine **5** was limited early on in the program. Moreover, the safety element associated with handling compounds **8** and particularly **9** were a concern because of the low carbon-count relative to the number of

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3 heteroatoms (e.g., in **8**) or relative to the number of energetic functional groups in the
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7 molecule (oxadiazole, nitro, etc. in **8** and **9**).^{11,12}
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10 Differential Scanning Calorimetry (DSC) was used as a primary means of evaluating
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13 and triaging intermediates of concern. Specifically, amino-oxadiazole **8** was first
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16 analyzed by DSC (Figure 2) and showed a clean melt with an onset at 213.9 °C,
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19 followed by an exothermic decomposition, which is attributed primarily to decomposition
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22 of the oxadiazole and/or the benzocyclobutylamine. The integrated heat for this
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25 decomposition, which has an onset of 254 °C, is 1567 J/g, which is considered
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28 significant.¹³ Drop weight tests were performed on **8** at up to 30 J, and were negative (6
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32 of 6 drop tests), indicating that the compound was not shock-sensitive. The high onset
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35 of decomposition (both absolute and relative to a reaction temperature of 25 °C),
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38 coupled with the apparent high crystalline nature of the intermediate (indicated by the
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41 sharp melt) led us to conclude that **8** was an intermediate that could be synthesized and
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44 handled safely at intermediate scale (< 1 kg), as both the melt and the decomposition
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47 occur more than 100 °C above the highest achievable reaction temperature.¹⁴
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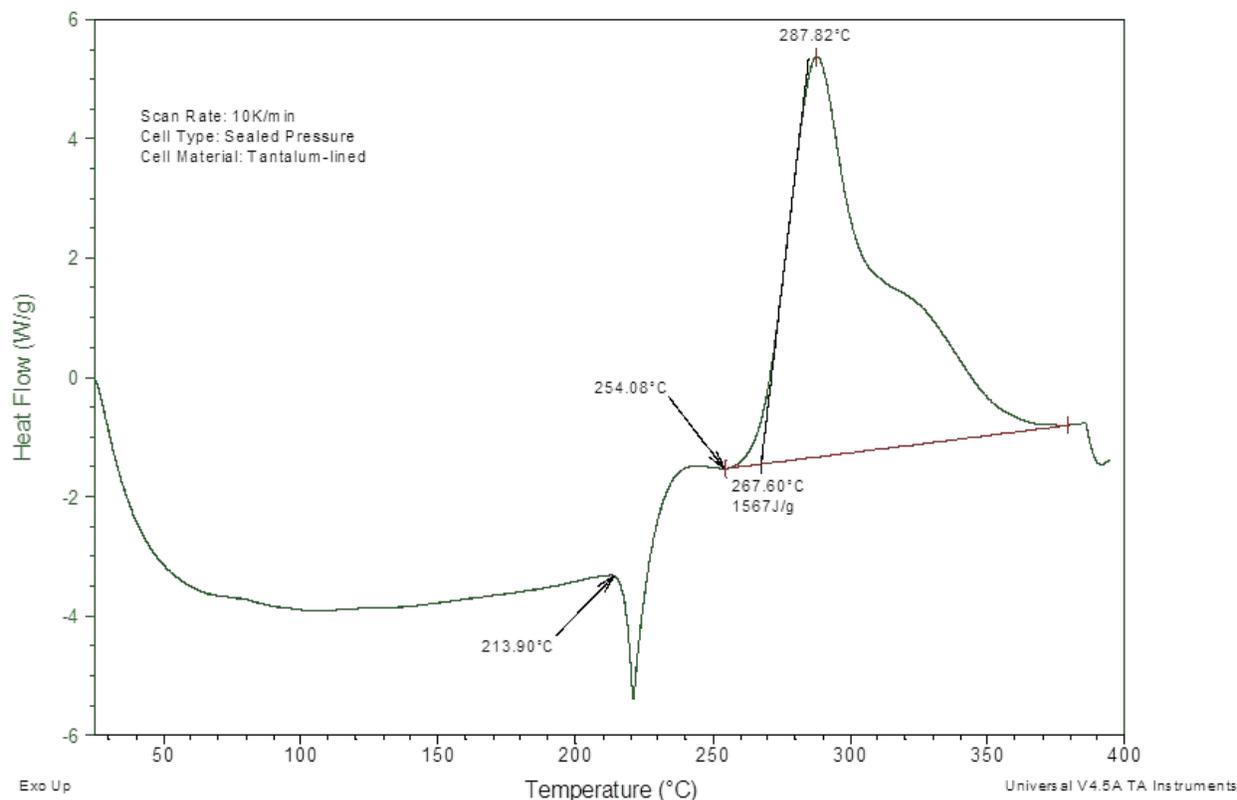
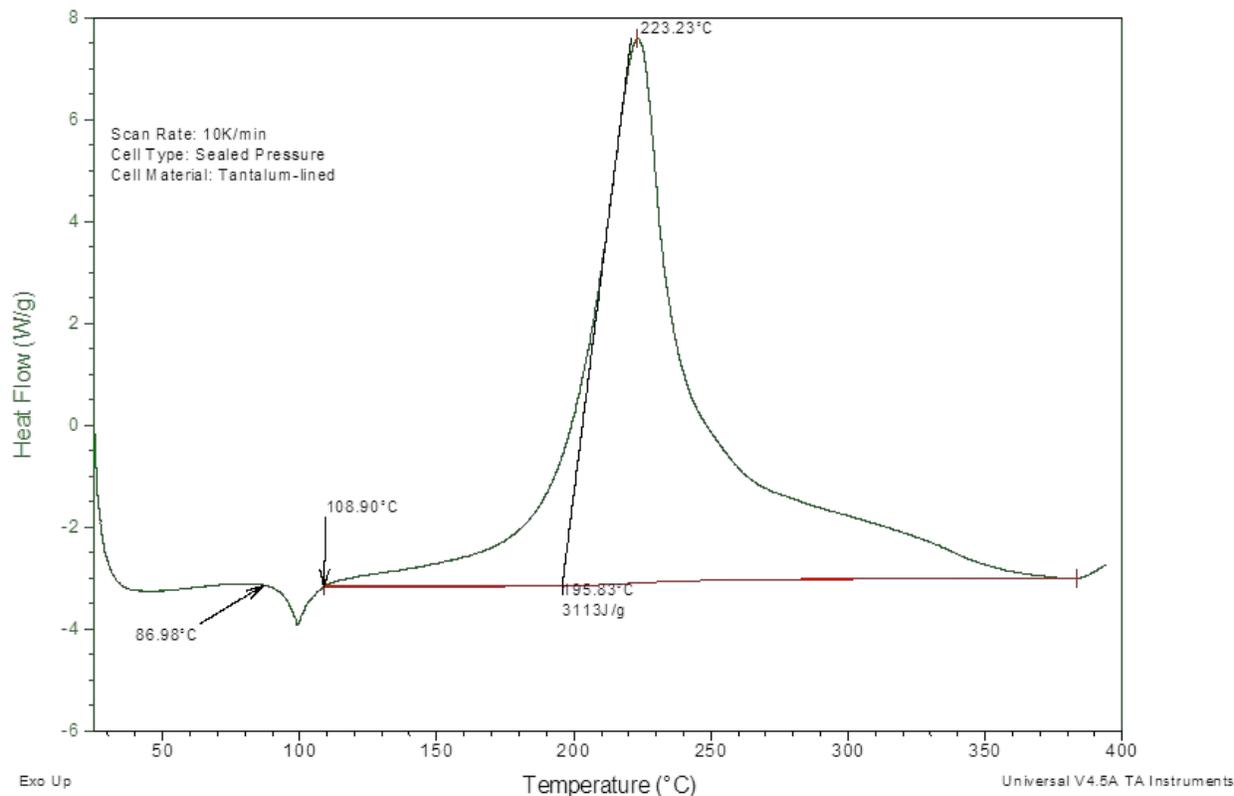


Figure 2. DSC thermogram of **8** (sample size: 5.70 mg)

A similar evaluation of **9** was conducted, but the DSC of the nitro-oxadiazole was shown to be significantly different (Figure 3). In this case, the intermediate showed a lower onset temperature for its melt (of approx. 87 °C) relative to its precursor (**8**), and that transition was also poorly defined. Following its melt, the compound showed a decomposition exotherm with an onset of 109 °C, and an integrated heat of decomposition of >3000 J/g; it is noted that the onset of each these transitions is a best

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3 case scenario, as solutions or impure phases with no melting obstacles. Drop weight
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7 tests of **9** gave 3 of 6 positive results at 30 J impact (decomposition (charring); no
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10 smoke, flame or audible report), but no positive results at 20 J intensity. Combined,
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14 these results constituted a significant safety risk for scale-up. Therefore, a better
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17 understanding of the synthetic process to the formation of **9** was deemed necessary in
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21 order to fully evaluate whether the approach to **2** outlined in Scheme 1 could be safely
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24 conducted.
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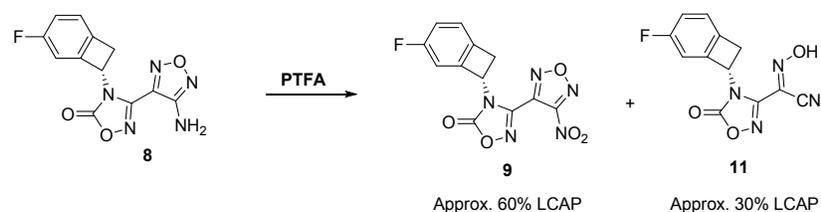


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4 **Figure 3.** DSC thermogram of **9** (sample size: 3.40 mg)
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8 FORMATION OF **9** 9

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11 The conversion of **8** to **9** can be effected by a number of different reaction conditions.
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14 The “Piranha” (sulfuric acid / hydrogen peroxide¹⁶) conditions⁹ were evaluated, but
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The conversion of **8** to **9** can be effected by a number of different reaction conditions. The “Piranha” (sulfuric acid / hydrogen peroxide¹⁶) conditions⁹ were evaluated, but resulted in a complex mixture, and alternative options were therefore considered. After some additional evaluation, it was determined that either trifluoroacetic acid (TFA)¹⁷ / urea hydrogen peroxide (UHP)¹⁸ or TFA / hydrogen peroxide afforded the cleanest reaction profile. Both sets of conditions are believed to proceed through the same reactive species (pertrifluoroacetic acid, PTFA^{19,20,21}), therefore selection of conditions was based on more practical considerations. Further development led to the conclusion that the latter set of conditions using hydrogen peroxide was likely easier to operate because hydrogen peroxide can be dosed continuously more easily than UHP (a solid), which in turn means that the individual reaction steps could be better controlled, thus avoiding potential runaway exotherms.

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3 The main impurity of the reaction is nitrile oxime **11** (Scheme 2), which is believed to
4 originate from the condensation of the intermediate nitroso-oxadiazole with the starting
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6
7 originate from the condensation of the intermediate nitroso-oxadiazole with the starting
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10 material (**8**) followed by degradation of the corresponding diazo-oxadiazole dimer.¹⁵
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23 Scheme 2. Oxidation of **8** to **9**

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27 Empirically, only **8**, **9**, and **11** have been observed (by HPLC-MS analysis) over the
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31 course of the reaction; therefore, it is believed that the relative rate for the initial
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34 oxidation to the hydroxylamine must therefore be a rate-determining step (i.e., no
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37 appreciable accumulation of the hydroxylamine or nitroso intermediates) and the
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41 formation of **11** as a byproduct of the reaction may be inevitable under these reaction
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45 conditions unless the mechanism for the formation of **9** itself were to be changed.
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48 Indeed, varying the reaction temperature, concentration, hydrogen peroxide addition
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52 rate, or stoichiometry did not have a statistically-significant effect on the ratio of **11** to **9**
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56 at the end of the reaction. While reaction temperature was shown to have an effect on
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3 the reaction conversion, there was no statistically-significant variation in the amount of
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7 impurity relative to the product under any of the conditions tested. This observation
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10 indicates that formation of the impurity under the reaction conditions used may not be
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13 easily suppressed. Fortunately, upon completion of the reaction, the reaction mixture is
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17 diluted with water, which causes the desired product (**9**) to nucleate, and most of the
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21 impurities (including **14**) can be purged through the mother liquor.
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24 In addition, reaction calorimetry for the oxidation of **8** to **9** was performed (both in a
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27 SuperCRC™ calorimeter and in a Mettler Toledo EasyMax™ equipped with the
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30 HFCal™) to determine safe operating conditions. First, the addition of hydrogen
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34 peroxide to TFA was evaluated. From the data collected in the EasyMax™, it was
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38 determined that the enthalpy associated with the addition of 0.10 mol of hydrogen
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42 peroxide to 0.78 mol of TFA and the subsequent formation of PTFA is approximately
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45 1 kJ, which corresponds to an adiabatic temperature rise (ΔT_{ad}) of < 10 K. Moreover,
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49 because this exotherm is addition-controlled with no apparent thermal accumulation or
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53 delay, the risk posed to the operator in terms of a runaway exotherm can be minimized.
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4 Separately, the enthalpy measured in the EasyMax™ for the oxidation reaction
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7 conducted on 3 g (0.010 mol) of **8** with 0.10 mol of hydrogen peroxide was determined
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10 to be approx. 6 kJ when the reaction was run at ≤ 40 °C, but increased to 16 kJ when
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13 the same reaction was run at 60 °C. These reaction enthalpies correspond to a ΔT_{ad} of
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16 40 K and 120 K, respectively. In the CRC, the same reactions performed at 25 °C and
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19 40 °C produced ΔT_{ad} of 9 K and 90 K, respectively. Though the absolute magnitude of
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22 these temperature rises do not match absolutely, the trends are compelling, and this
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25 remarkable increase in reaction enthalpy for the higher temperature experiments
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28 appears to be caused by the acceleration of the degradation of PTFA as a function of
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31 temperature. Finally, Accelerating Rate Calorimetry (ARC) performed on this reaction
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34 following a rapid addition of hydrogen peroxide showed a significant temperature and
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37 pressure increase at approx. 50 °C, which was also indicative of a potential runaway
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45 exotherm due to PTFA degradation (Figure 4).
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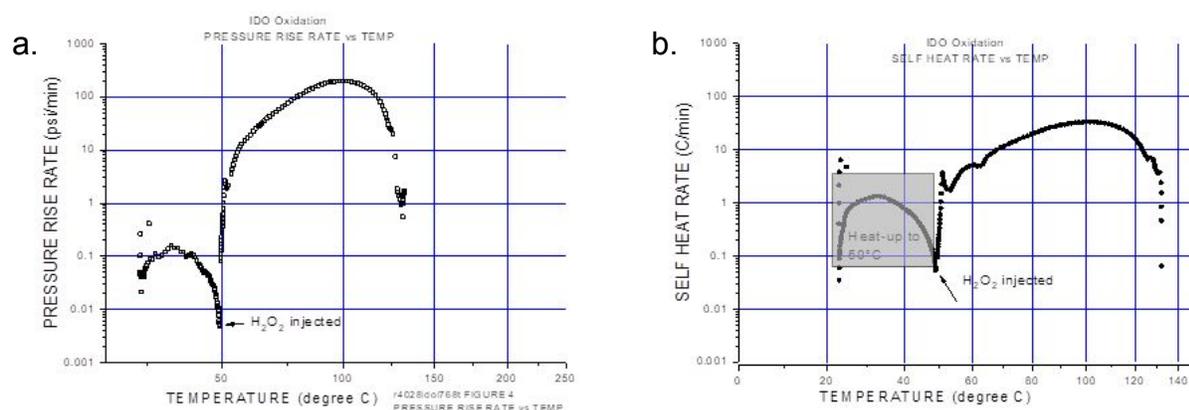


Figure 4. ARC data showing Self Heat Rate (a) and Pressure Rise Rate (b) as a function of temperature for the oxidation of **8** to **9**. Experiments were performed by dissolving **8** in TFA and heating to 50 °C, then injecting H₂O₂ at once (see annotation) with the ARC in adiabatic tracking mode.

These data as a whole indicate that care should be taken when performing this oxidation in order to avoid the thermal decomposition of the PTFA formed. Based on the results collected, as well as the lack of benefit of performing this oxidation at significantly higher temperature (Figure 5), the recommended batch temperature is ≤ 45 °C at intermediate scale (< 200 g) with a slow dosing of hydrogen peroxide: Although this temperature is close to the potential degradation of the PTFA, the slow dosing of

hydrogen peroxide allows for minimal accumulation of this reagent, and accelerates the rate of oxidation, thereby minimizing risk to the operator. It is recognized that the edge of failure for this runaway reaction has not been systematically confirmed (i.e., the temperature at which the PTFE degradation will cause the reaction to self-heat), and for this reason, alternative strategies for the assembly of **2** were strongly considered in order to avoid going through this high energy intermediate and reaction.

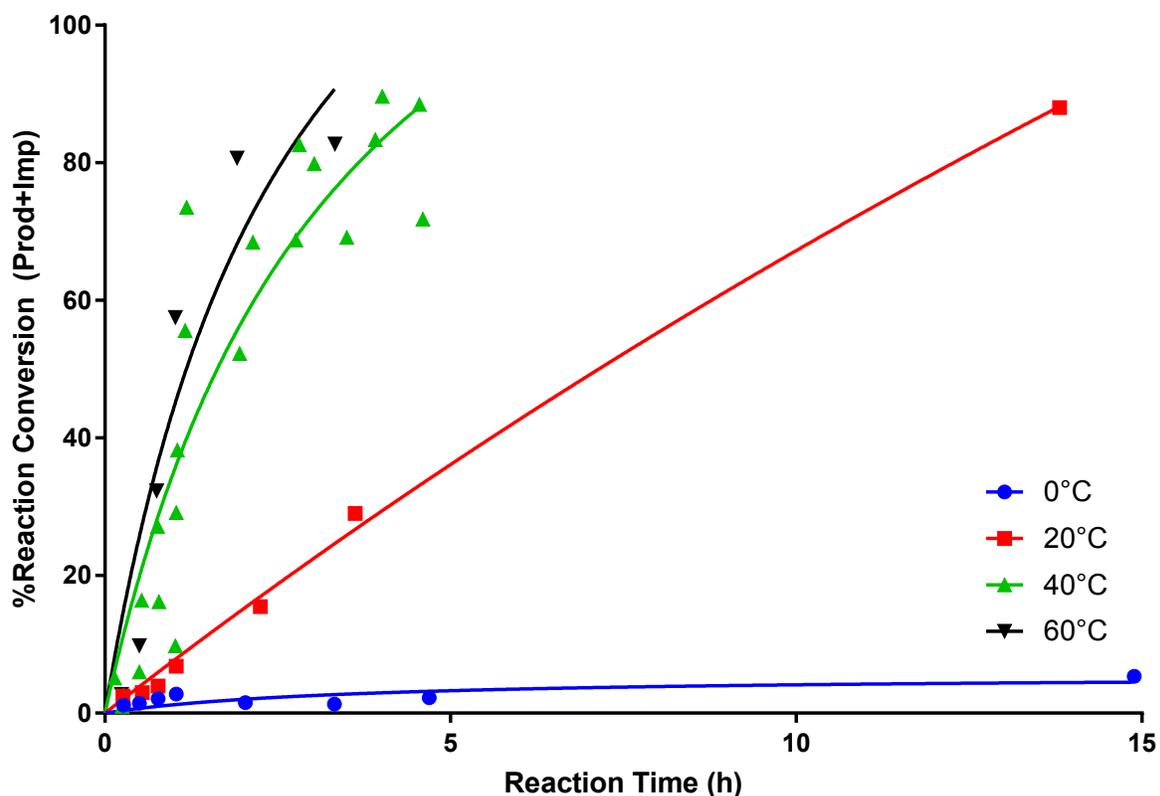
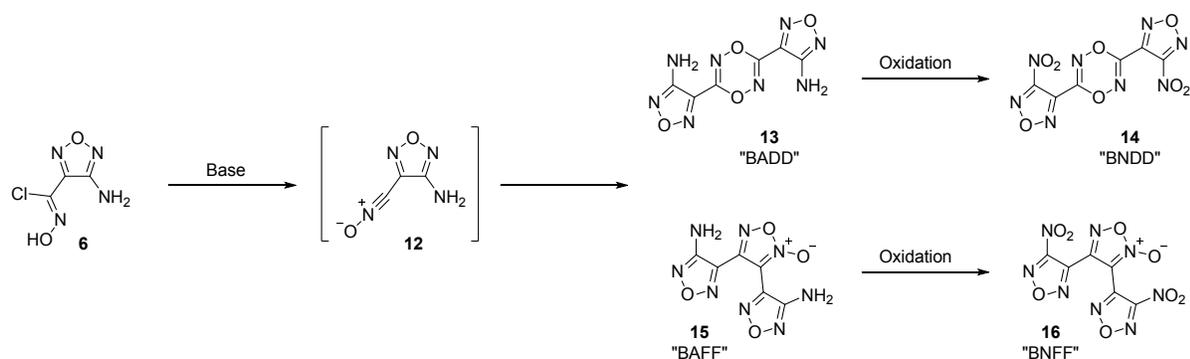


Figure 5. Effect of temperature on the reaction conversion of **8** to **9**

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4 One final concern over the approach to **2** outlined in Scheme 1 is in the condensation
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7 of benzocyclobutylamine **5** with imidoyl chloride **6**. As noted elsewhere,^{22,23} the nitrile
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10 oxide formed from treatment of imidoyl chloride **6** with base (**12**) can homodimerize to
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13 form the symmetrical dioxadiazene (**13**) and/or its isomeric oxadiazole oxide (**15**),
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16 depending on the reaction conditions used (Scheme 3). As expected, these species are
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19 highly energetic, and their corresponding oxidation products (**14** and **16**) are known
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22 explosives.^{22,23} While the outcome of the condensation of **5** and **6** seems to primarily
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25 result in the formation of **7**, we have not attempted to prove that neither **13** nor **15** are
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28 present in the isolated product from this reaction because synthesis of the
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31 corresponding markers and their handling is considered high risk. Therefore, **7** as well
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34 as **8** could technically contain these corresponding impurities, depending on the
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37 reaction parameters used. As a result of this known but uncharacterized risk, and the
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40 risk associated with the formation of nitro-oxadiazole **9**, an alternative approach to **2**
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43 was carefully evaluated.
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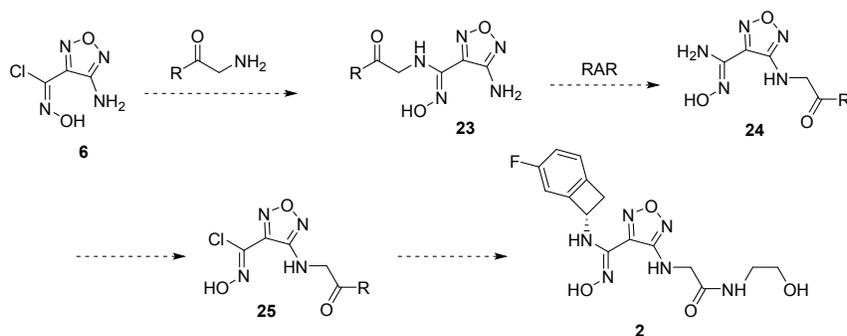


Scheme 3. Undesired dimerization of imidoyl chloride **6**^{22,23}

IMPROVED ACCESS TO THE BENZOCYCLOBUTYLAMINE

Early on in development, the synthesis of benzocyclobutylamine **5** was optimized to allow access to kilogram quantity of the desired product using the existing route. Most notable in the improved synthesis is the classical resolution of the benzocyclobutylamine,²⁴ which obviated the need for costly SFC of this intermediate. Indeed, the Process Mass Intensity (PMI) for the Curtius rearrangement step and the SFC resolution alone in the original approach was estimated at 3839 due to the high material demand (solvent and CO₂) of the chromatography. In contrast, the process outlined in Scheme 4 decreased the PMI for the Curtius rearrangement and classical

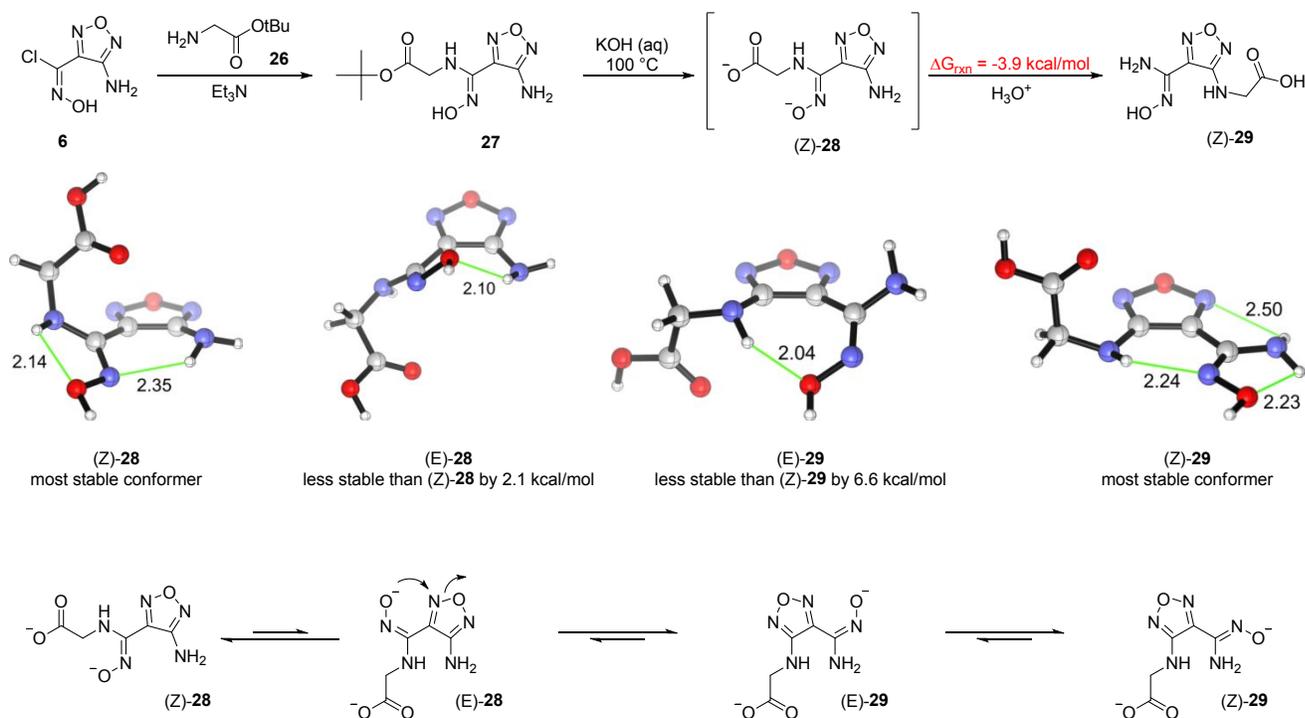
energy intermediates are used; [4] the benzocyclobutylamine **5** is introduced late, which results in a higher overall throughput when this material was of limited availability.



Scheme 5. Revised strategy to **2**

However, it was determined that under the conditions needed to effect the oxadiazole rearrangement on our substrate (aq. KOH, 100 °C),⁶ the ethanolamine amide in the fully-elaborated tailpiece is hydrolyzed. A screen aimed at finding non-aqueous conditions that effect this rearrangement failed to afford conditions that were competitive. As a result, a modified strategy was implemented that still installed the hydroxyamidine first, but with a sacrificial ester that would get saponified during the rearrangement conditions (Scheme 6). To better understand the thermodynamics of the transformation, the starting acid (**28**) and product (**29**) were modeled. From the analysis

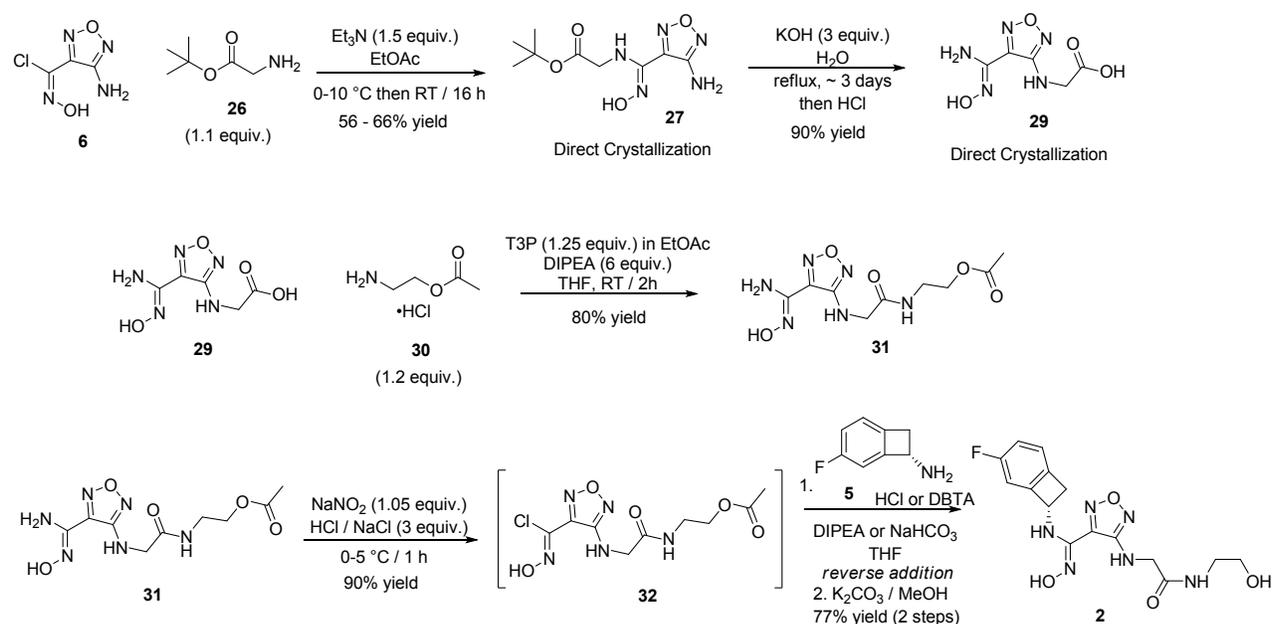
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3 performed, it is determined that the rearrangement is thermodynamically-favored
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7 ($\Delta G_{\text{rxn}} = -3.9$ kcal/mol), and that the geometry of the hydroxyamidine is very important to
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10 the conformation of the starting material and product, with the (*Z*)-isomer being favored
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14 in both cases. Therefore, because the mechanism of the Boulton-Katritzky
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17 rearrangement is believed to be concerted, these data suggest that the starting oxime
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21 ((*Z*)-**28**, presumably as the dianion due to the high pH of the reaction mixture) must first
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24 isomerize prior to rearrangement to the less favored (*E*)-isomer which then has the
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27 proper geometry to enable the rearrangement. The product of the rearrangement then
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31 will undergo isomerization to the final most stable conformer, (*Z*)-**29** (Scheme 6), and it
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35 is the release of energy from the combined rearrangement and isomerization that
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38 makes the rearrangement favorable thermodynamically.
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Scheme 6. Installation of the tailpiece and rearrangement as well as computed energies for the rearrangement (M06-2X-D3/6-311G(d,p)-SMD(water) geometries and frequencies. M06-2X-D3/def2-QZVPP-SMD(water) single-point energies.)

The optimized synthesis of **2** is provided in Scheme 7. The formation of hydroxyamidine **27** proceeded smoothly, with the product being isolated by direct crystallization from ethyl acetate. The hydrolysis and rearrangement of **27** affords **29** cleanly, although it does require a 48 h reaction time. Acid **29** is also isolated directly from the reaction mixture after neutralization, thus facilitating the process steps.

However, the condensation of **29** with **30**²⁵ to complete the tailpiece assembly was problematic at first, with varying yields of product being obtained, and unreliable outcomes requiring complex chromatography.



Scheme 7. Final delivery approach

Initially, EDC and HOBt were used as coupling reagents, but product **31** proved difficult to separate from HOBt and related reagents, thereby limiting the use of many common amide-coupling reagents.²⁶ Small-scale runs had shown propylphosphonic anhydride (T3P) to be a favorable amide coupling reagent for the transformation.

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4 However, upon repeated reactions and increase in scale, multiple byproducts including
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7 the pseudo-dimer **33** (Figure 6) were observed, resulting in low yield and purity of **31**.
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10 In order to quickly identify the key parameters driving reaction efficiency and
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12 cleanliness, a Design of Experiments (DoE) approach was taken. For this, a 24-
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14 experiment design was initially created using the JMP software.²⁷ The design allowed
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17 use of a common 24-well plate array (1 mL shot vials) to facilitate reaction setup and
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20 analysis while minimizing starting material consumption, and evaluated 4 parameters:
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23 solvent (THF, DCM and EtOAc), DIPEA charge (2 – 4 equiv.), T3P charge (0.5 – 1.5
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25 equiv.), and amine hydrochloride **30** charge (0.9 – 1.2 equiv.). Following completion of
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28 these experiments, analysis indicated that the DIPEA charge was insufficient, even at 4
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31 equiv. Therefore, the DoE was augmented with 5 additional reactions to probe the
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34 effects of higher DIPEA (up to 8 equiv.). The model generated from the data collected
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37 showed DIPEA and T3P equivalents to be the main drivers of purity (panel I, Figure 6),
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40 with THF showing the best balance of conversion and purity among the solvents.
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43 Setting response levels at >80% conversion, >95% purity of converted product and <5%
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46 LCAP **33**, the contour profile (panel II, Figure 6) predicted a T3P loading of 1.25
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equivalents and 6 equivalents of DIPEA with THF as the solvent to be ideal. Mechanistically, this makes sense, but was not obvious to us *a priori*. Each equivalent of T3P can generate, over the course of the reaction, up to 3 equiv. of phosphonic acid (therefore, the total base needed becomes: 3 x 1.25 (T3P) + 1 (amine HCl **30**) + 1 (acid **29**) = 5.75 ~ 6). With insufficient base, the amine becomes inaccessible (protonated) as the reaction proceeds and therefore the hydroxyamidine oxygen becomes the next possible nucleophile and results in the formation of **33**.

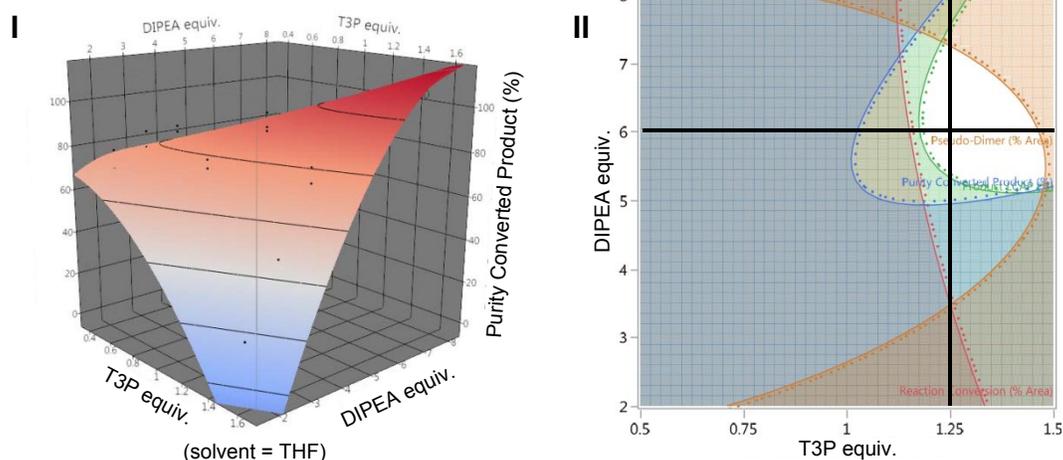
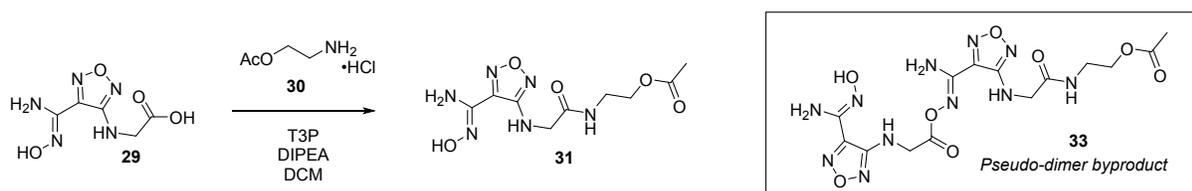
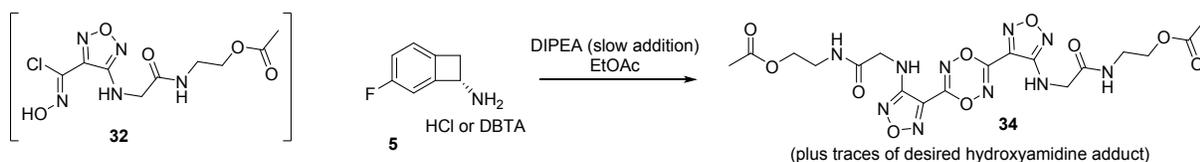


Figure 6. Optimization of the formation of **31**

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3
4 These conditions were applied to the overall delivery of **2** (approx. 200 g scale;
5
6
7 Scheme 7), allowing for a cleaner reaction, which after crystallization afforded **31** with
8
9
10 high purity and yield. The optimized conditions demonstrated a robust design space
11
12
13
14 across a wide scale range (~ mg in DoE optimization to > 200 g).
15
16

17 From **31**, the synthesis is completed by diazotization of the hydroxyamidine and *in situ*
18
19
20 formation of imidoyl chloride **32**, followed by installation of **5** and deprotection of the
21
22
23 tailpiece. As was observed for the formation of hydroxyamidine **8**, some dimerization
24
25
26 may occur if the order of addition is reversed (Scheme 8): Namely, if imidoyl chloride **32**
27
28
29 is pre-mixed with the salt of **5** (either HCl or DBTA), then base is added, the
30
31
32 deprotonation of the imidoyl chloride appears to occur faster than the neutralization of
33
34
35 the salt of **5** (i.e., the neutralization reaction may be mass-transfer limited due to
36
37
38 solubility limitations), and therefore results in formation of the corresponding nitrile
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oxide, which was found to effectively homodimerize (Scheme 8). The solution to afford
clean coupling is to first neutralize **5** by pre-mixing the salt with the base in the reaction
solvent, and then adding in the imidoyl chloride solution from the previous step. After

1
2
3
4 final deprotection, the desired product (**2**) is obtained in approx. 70% yield over three
5
6
7 steps from **31**.



Scheme 8. Homodimerization of **32**

CONCLUSION

A fit-for-purpose synthesis of high energy oxadiazole-bearing molecules has been evaluated. Taking advantage of the Boulton-Katritzky rearrangement the new approach enabled not only a more convergent route that allowed for the late-stage installation of the chiral building block **5**, but also avoided the generation of high energy intermediates such as nitrooxadiazole **9**. The optimized approach culminates in a longest linear sequence of nine (9) steps – several of which are telescoped – from commercially-available aldehyde **17**. This work ultimately enabled the safe synthesis of **2** in quantities sufficient to support toxicology studies.

EXPERIMENTAL SECTION

1
2
3 All reactions were carried out under a nitrogen atmosphere. All solvents and reagents
4
5
6
7 were purchased from commercial sources and were used without further purification. ¹H
8
9
10 NMR chemical shifts are reported relative to residual proton solvent peaks or TMS.

11
12
13
14 (S)-3-(4-amino-1,2,5-oxadiazol-3-yl)-4-(4-fluorobicyclo[4.2.0]octa-1(6),2,4-trien-7-yl)-
15
16
17
18 1,2,4-oxadiazol-5(4H)-one (8). To a 5 L 4-neck round-bottomed flask, were charged (S)-
19
20
21 4-fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine hemi L-dibenzoyl tartaric acid salt
22
23
24
25 (5•DBTA) (435 g, 1.38 mol, 1.00 equiv) and hydrogen chloride in 1,4-dioxane (4500 mL
26
27
28
29 of 4 M solution; 18 mol, 13.0 equiv.). The resulting mixture was stirred overnight at room
30
31
32 temperature. The solids were collected by filtration. This resulted in 200 g (crude) of (S)-
33
34
35 4-fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine hydrochloride as a white solid. Into a 10-L
36
37
38
39 4-neck round-bottomed flask, was charged sequentially a solution of (S)-4-
40
41
42 fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine hydrochloride (200 g, 1.15 mol, 1.00 equiv)
43
44
45
46 in acetonitrile (2000 mL, 10 vol.), a solution of sodium hydroxide (61 g, 1.53 mol, 1.30
47
48
49 equiv) in water (2000 mL, 10 vol.), a solution of (E)-4-amino-N-hydroxy-1,2,5-
50
51
52 oxadiazole-3-carbonimidoyl chloride (6) (191 g, 1.18 mol, 1.00 equiv) in acetonitrile
53
54
55
56
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60

1
2
3
4 (2000 mL, 10 vol.), a solution of potassium phosphate dibasic (302 g, 1.41 mol, 1.20
5
6
7 equiv) in water (1000 mL, 5 vol.), and the mixture was stirred at ambient temperature.
8

9
10 After confirming that the initial condensation was complete per analysis of the reaction
11
12
13 mixture by HPLC, charged diisopropylethylamine (190 g, 1.47 mol, 1.25 equiv), and CDI
14
15

16
17 (219 g, 1.53 mol, 1.30 equiv) sequentially while stirring at ambient temperature. The
18
19
20 resulting solution was stirred for 1 h at ambient temperature. The reaction was then
21
22

23
24 diluted with water (2000 mL, 10 vol.), which caused a precipitation of the product. The
25
26
27 resulting solution was extracted with ethyl acetate (2 x 3000 mL; 2 x 15 vol.) and the
28
29

30
31 organic layers were combined. The resulting mixture was washed with 1 M hydrochloric
32
33
34 acid (aq) (2 x 1000 mL; 2 x 5 vol.), then dried over anhydrous sodium sulfate, and
35
36

37
38 concentrated to dryness under reduced pressure. This resulted in 250 g (74%) of (S)-3-
39
40
41 (4-amino-1,2,5-oxadiazol-3-yl)-4-(4-fluorobicyclo[4.2.0]octa-1(6),2,4-trien-7-yl)-1,2,4-
42
43

44
45 oxadiazol-5(4H)-one (**8**) as a white solid. ¹H NMR (300 MHz, DMSO-d₆) δ 7.22 – 7.01
46
47
48 (m, 3H), 6.58 (s, 2H), 5.79 (t, *J* = 4.0Hz, 1H), 3.66–3.51 (m, 2H) ppm; ¹⁹F NMR (282
49
50

51
52 MHz, DMSO-d₆) δ -113.1 ppm; MS: *m/z* calcd for C₁₂H₉FN₅O₃ (M+H⁺) 290.1, found
53
54
55 290.1; [α]_D²⁰ +32.5 ° (c = 0.22, MeCN).
56
57
58
59
60

1
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3
4 (S)-4-(4-fluorobicyclo[4.2.0]octa-1(6),2,4-trien-7-yl)-3-(4-nitro-1,2,5-oxadiazol-3-yl)-
5
6
7 1,2,4-oxadiazol-5(4H)-one (9). (S)-3-(4-amino-1,2,5-oxadiazol-3-yl)-4-(4-
8
9
10 fluorobicyclo[4.2.0]octa-1(6),2,4-trien-7-yl)-1,2,4-oxadiazol-5(4H)-one (8) (55.27 g, 191
11
12
13 mmol, 1.00 equiv.) was charged to a 5 L 3-neck round-bottomed flask. The flask was
14
15
16
17 equipped with an overhead stirrer, reflux condenser, and thermocouple probe, and
18
19
20
21 inerted under nitrogen. Trifluoroacetic acid (1105 mL, 20 vol.) was charged and the
22
23
24
25 resulting mixture was stirred and heated with a target internal temperature of 40 °C. The
26
27
28
29 hydrogen peroxide solution (32% w/w) (183 ml, 1911 mmol, 10 equiv.) was charged to
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37
38 an addition funnel and added to the reaction mixture dropwise, maintaining a batch
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3 displacement wash with water (each with approx. 500 mL / 10 vol. of water). Solids
4
5
6
7 were deliquored, but not dried further. Nitrooxadiazole **9** was used as-is and stored cold.
8
9
10 Yield: 31.6 g (52%, uncorrected). ¹H NMR (600 MHz, DMSO-d₆) δ 7.25 – 7.19 (m, 1H),
11
12
13 7.17 (t, J = 8.9 Hz, 1H), 7.10 (d, J = 7.3 Hz, 1H), 5.67 – 5.61 (m, 1H), 3.63 (d, J = 14.2
14
15
16 Hz, 1H), 3.48 (dd, 1H) ppm.
17
18
19
20
21

22 **3-(2-bromo-4-fluorophenyl)propanenitrile (19)**. 2-Bromo-4-fluorobenzaldehyde (**17**;
23
24 200 kg, 985.2 mol, 1.00 equiv.) was charged to an appropriately-sized reactor (R1),
25
26 followed by 2-methyltetrahydrofuran (500 kg, 2.5 wts.) and stirring was initiated to form
27
28 a homogenous solution. Diethyl (cyanomethyl)phosphonate (194.2 kg, 1096.3 mol, 1.11
29
30 equiv.) was charged into a second appropriately-sized reactor (R2), followed by 2-
31
32 methyltetrahydrofuran (681.8 kg, 3.4 wts.). Anhydrous K₃PO₄ (220.3 kg, 1037.8 mol,
33
34 1.05 equiv.) was charged to R2. While mixing the contents of R2, the solution prepared
35
36 in R1 was transferred to R2 while maintaining the batch temperature of R2 at 10-15 °C.
37
38
39 The contents of R2 were stirred at 10-15 °C for 4-6 h, and sampled for reaction
40
41
42
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52
53 completion by HPLC (residual aldehyde: 0.7%; target ≤ 3.0%). Water (586 kg, 2.9 wts.)
54
55
56
57
58
59
60

1
2
3 was charged to R2 and the mixture was stirred for 1 h, then stirring was stopped and
4
5
6
7 the phases were allowed to separate (3 h). The aqueous phase was discarded. The
8
9
10 organic phase was washed first with a mixture of 400 kg of 10% Na₂SO₄ (aq) and 50 kg
11
12
13 of 10% H₃PO₄ (aq) (2.5 wts. total), then with 400 kg of 10% Na₂SO₄ (aq) (2.0 wts.).
14
15
16
17 Solvent was exchanged to THF (total 1618 kg of THF was used) and the solution
18
19
20 volume was reduced to approximately 1-2 volumes by distillation. THF (80 kg, 0.4 wts.),
21
22
23 H₃PO₄ (4.4 kg, 0.022 wts.), and methanol (306.1 kg, 1.53 wts.) were charged
24
25
26
27 sequentially to the reaction mixture, and the entire contents of the reactor were then
28
29
30 transferred to an auxiliary storage tank. To the empty reactor, sodium borohydride (99.8
31
32
33 kg, 2638.1 mol, 2.67 equiv.) and THF (900 kg, 4.5 wts.) were charged sequentially, and
34
35
36
37 the batch temperature was adjusted to 10-20 °C. The solution from the storage tank
38
39
40
41 was charged to the reactor containing the sodium borohydride solution over approx. 28
42
43
44
45 h, maintaining a batch temperature of 10-20 °C throughout, then maintained mixing for
46
47
48
49 an additional 3 h at the same temperature once addition was complete. Reaction
50
51
52 completion was monitored by HPLC. 10% H₃PO₄ (aq) (1.2 kg, 0.006 wts.) and MTBE
53
54
55
56 (300 kg, 1.5 wts.) were charged to the reaction mixture sequentially, and the batch
57
58
59
60

1
2
3 temperature was increased to 20-30 °C. After stirring for 1 h, agitation was stopped, and
4
5
6
7 the phases were allowed to separate for 2 h. The aqueous phase was drained and
8
9
10 discarded. The organic phase was washed with a mixture of 7% NaHCO₃ (206 kg, ca. 1
11
12
13 wt.) and 10% Na₂SO₄ (614 kg, ca. 3 wts.). The organic phase was concentrated to
14
15
16 approx. 1-2 volumes by distillation under reduced pressure, then MTBE (448.4 kg, 2.24
17
18
19 wts.) was charged and the organic phase was washed with 10% Na₂SO₄ (aq) (200 kg, 1
20
21
22 wt.). A solvent exchange to THF was performed (using 2142 kg of THF for the
23
24
25 exchange) with a final target volume of 1-2 volumes, then the batch was diluted with
26
27
28 THF (246 kg, 1.23 wt.). The organic phase (total weight: 692.6 kg) was assayed for
29
30
31 product content: 26.5% w/w, with a purity of 87.1% a/a, corresponding to a yield of
32
33
34 183.5 kg (81.6%). Solution was used as-is for the subsequent transformation.
35
36
37
38
39
40
41
42 Characterization data for **18**: ¹H NMR (400 MHz, CDCl₃) δ 7.99 (dd, *J* = 8.8, 5.8 Hz, 1
43
44
45 H), 7.46 (dd, *J* = 8.8, 5.8 Hz, 2 H), 7.08 (td, *J* = 8.3, 8.3, 2.5 Hz, 1 H), 5.52 (d, *J* = 11.8
46
47
48 Hz, 1 H) ppm; ¹³C NMR (100 MHz, CDCl₃) δ 163.6 (br d, *J* = 255 Hz), 147.8, 130.0 (d, *J*
49
50
51 = 4 Hz), 128.4 (d, *J* = 9 Hz), 125.3 (d, *J* = 10 Hz), 121.0 (d, *J* = 25 Hz), 117.5, 115.6 (d,
52
53
54
55 *J* = 22 Hz), 99.0 (d, *J* = 3 Hz) ppm; ¹⁹F NMR (100 MHz, CDCl₃) δ 106.4, 106.6 ppm;
56
57
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1
2
3 HRMS: m/z calcd for C₉H₅BrFN: (M+H⁺), 225.9662, Found: 225.9663 (M+ H⁺).
4
5

6
7 Characterization data for **19**: ¹H NMR (400 MHz, CDCl₃) δ 7.30 (m, 2 H), 7.03 (td, *J* =
8
9

10 8.3, 8.3, 2.5 Hz, 1 H), 3.06 (t, *J* = 7.3 Hz, 2 H), 2.66 (t, *J* = 7.3 Hz, 2 H) ppm; ¹³C NMR
11
12

13 (100 MHz, CDCl₃) δ 161.6 (br d, *J* = 250.5 Hz) 133.2 (d, *J* = 3 Hz), 131.6 (d, *J* = 8 Hz),
14
15

16 124.0 (d, *J* = 10 Hz), 120.3 (d, *J* = 23 Hz), 118.7, 115.1 (d, *J* = 10 Hz), 31.3, 17.7 (d, *J* =
17
18

19 1 Hz) ppm; ¹⁹F NMR (100 MHz, CDCl₃) δ 112.5 ppm; HRMS: m/z calcd. for C₉H₇BrFN:
20
21

22 (M+H⁺), 227.9819, Found: 227.9820.
23
24
25
26
27
28

29 **4-fluorobicyclo[4.2.0]octa-1,3,5-triene-7-carboxylic acid (3)**. THF (289.4 kg, 1.70 wts.)
30
31

32 and diisopropylamine (238 kg, 2.35 mol, 3.13 equiv.) were charged to an appropriately-
33
34

35 sized reactor (R1). The solution temperature was adjusted to a range of -20 °C to 10 °C.
36
37

38 *n*-Butyllithium (2.5 M, 646 kg, 10.08 mol, 13.44 equiv.) was charged to the reactor while
39
40

41 maintaining a batch temperature range between -20 °C and 10 °C (7 h addition time).
42
43
44
45

46 The previously-prepared solution of 3-(2-bromo-4-fluorophenyl)propanenitrile (**19**; 643
47
48

49 kg of a 26.5% w/w solution, 170.4 kg, 0.75 mol, 1.00 equiv.) was charged into a
50
51

52 separate appropriately-sized reactor (R2) followed by THF (680.6 kg, 4 wts.) and the
53
54
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56
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58
59
60

1
2
3
4 batch temperature was adjusted to -70 °C to -60 °C. The solution in R1 was added to
5
6
7 the starting material in R2 while maintaining a batch temperature of -70 °C to -60 °C
8
9
10 (9.5 h addition time), washing the transfer line with THF (19.2 kg, 0.1 wt.). The batch
11
12
13
14 was stirred for 1 h and sampled for reaction completion (1% residual SM; target \leq 5%).
15
16
17 Water (122 kg, 0.72 wts.) was charged to R2 at -70 °C to -60 °C, and the batch was
18
19
20 warmed to 10-25 °C. Water (510 kg, 3 wts.) was charged to R2, and then solvent was
21
22
23 distilled off to a target volume of 3-4 volumes. Ethanol (300 kg, 1.76 wts.) was charged
24
25
26 to R2, and then the batch was heated to 70-80 °C for 5 h, and subsequently cooled
27
28
29 back down to 20-30 °C. Solvent was distilled off to a target volume of 2-3 volumes.
30
31
32 Water (1360 kg, 8 wts.) and dichloromethane (1099.8 kg, 6.5 wts.) were charged to the
33
34
35 reaction mixture, and the phases were mixed for 0.5 h, then allowed to settle (1 h). The
36
37
38 organic phase was removed and discarded. The aqueous phase was transferred to
39
40
41 another reactor (R3). Ethanol (402 kg, 2.4 wts.) was charged to R3 and the batch was
42
43
44 warmed to 25-35 °C. 35% Hydrochloric acid (aq.) (206.8 kg, 1.21 wts.) was charged to
45
46
47 R3 and the pH was checked (result: 1; target \leq 3). The mixture was stirred for 2.5 h at
48
49
50 25-35 °C, then the batch cooled to 0-5 °C and stirred for an additional 1 h. The product
51
52
53
54
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60

1
2
3 was isolated by filtration, washing the cake with water (300 kg, 1.8 wts.). The product
4
5
6
7 was dried in a vacuum oven at 40-45 °C for 70 h. Yield: 72.25 kg of a brown solid with
8
9
10 87.3% area / 85.1% w/w purity (61.5 kg corrected), corresponding to a 50% corrected
11
12
13 yield. Characterization data for **20**: ¹H NMR (400 MHz, CDCl₃) δ 7.08 (m, 2 H), 6.98 (m,
14
15
16 1 H), 4.22 (dd, *J* = 4.9, 2.6 Hz, 1 H), 3.64 (m, 1 H), 3.51 (m, 1 H) ppm; ¹³C NMR (100
17
18 MHz, CDCl₃) δ 162.8 (br d, *J* = 249 Hz), 139.5 (d, *J* = 8 Hz), 138.1 (d, *J* = 3 Hz), 125.3
19
20
21 (d, *J* = 9 Hz), 119.0, 117.3(d, *J* = 24 Hz), 110.6(d, *J* = 24 Hz), 35.6, 28.1 (d, *J* = 3 Hz)
22
23
24 ppm; ¹⁹F NMR (100 MHz, CDCl₃) δ 110.7 ppm; HRMS: *m/z* calcd for C₉H₆FN: (M+H⁺),
25
26
27 148.0557, Found: (M+ H⁺): 148.0564. Characterization data for **3**: ¹H NMR (400 MHz,
28
29
30 CDCl₃) δ 7.06 (t, *J* = 6.1, 6.1 Hz, 2 H), 6.96 (m, 2 H), 4.31 (t, *J* = 3.9, 3.9 Hz, 1 H), 3.44
31
32
33 (br d, *J* = 3.01 Hz, 2 H) ppm; ¹³C NMR (100 MHz, CDCl₃) δ 178.4, δ 162.7 (br d, *J* = 244
34
35
36 Hz), 142.7 (d, *J* = 8 Hz), 139.0 (d, *J* = 3 Hz), 124.6 (d, *J* = 9 Hz), 116.0 (d, *J* = 24 Hz),
37
38
39 110.7 (d, *J* = 23 Hz), 44.8 (d, *J* = 3 Hz), 33.3 ppm; ¹⁹F NMR (100 MHz, CDCl₃) δ 112.5
40
41
42
43
44
45
46
47
48 ppm; HRMS: *m/z* calcd for C₉H₇FO₂: (M+H⁺), 167.0503, Found: 167.0514.
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3
4 **4-fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine (rac 5).** 4-fluorobicyclo[4.2.0]octa-1,3,5-
5
6
7 triene-7-carboxylic acid (**3**; net 61.5 kg, 370 mol, 1.00 equiv.) was charged to an
8
9
10 appropriately-sized reactor (R1) followed by toluene (826 kg, 13.4 wts.) and the batch
11
12
13 temperature was adjusted to 10-20 °C. Triethylamine (41.2 kg, 407.2 mol, 1.1 equiv.)
14
15
16 was charged to the reactor, rinsing the transfer line with toluene (25 kg). DPPA (112.2
17
18
19 kg, 407.7 mol, 1.1 equiv.) was charged while maintaining a batch temperature of 10-
20
21
22 20 °C and the transfer line was rinsed with toluene (18 kg). The batch was stirred at 10-
23
24
25 20 °C for 20 h, and sampled for reaction conversion (result: 5.2% a/a residual SM by
26
27
28 HPLC). 10% NaCl (aq) (124 kg, 2 wts.) was charged to the reaction mixture. The batch
29
30
31
32 was stirred for approx. 30 min. at 10-20 °C, then agitation was stopped, and the phases
33
34
35 were allowed to separate. The aqueous phase was drained and discarded. The organic
36
37
38 phase was washed with 10% NaCl (aq) (126 kg, 2 wts.). The organic phase was dried
39
40
41
42 with anhydrous MgSO₄ (25.6 kg, 0.42 wts.) for 2 h (resulting in a residual water content
43
44
45 of 0.01% by KF), then the solids were filtered off under nitrogen and the filtrate was
46
47
48
49 collected in a separate appropriately-sized reactor (R2), washing the cake with toluene
50
51
52
53 (91 kg, 1.5 wts.). Toluene (295 kg, 4.8 wts.) was charged to a third reactor (R3), and
54
55
56
57
58
59
60

1
2
3 stirred. The contents of R2 and R3 were heated to a temperature of 85-95 °C. The
4
5
6
7 reaction mixture was transferred from R2 to R3 over 10.5 h while maintaining the batch
8
9
10 temperature in R3 at 85-95 °C, then maintained batch temperature for an additional 2 h.
11
12
13
14 R2 was rinsed with toluene (27.6 kg, 0.5 wts.) and the rinse was added to R3. The
15
16
17 batch temperature in R3 was decreased to 55-65 °C and the solution was tested for
18
19
20 residual starting material as well as residual azide by ion chromatography (9 ppm; target
21
22
23 ≤ 10 ppm; LOQ: 10 ppm). 4 M HCl (aq) (630 kg, 10.2 wts.) was charged to a fourth
24
25
26
27 reactor (R4) and warmed to 85-95 °C. The solution in R3 was transferred to R4 over 10
28
29
30 h while maintaining a batch temperature in R4 of 85-95 °C. R3 was rinsed with toluene
31
32
33
34 (15 kg) and the rinse was added to R4. The batch in R4 was stirred for 1 h, then cooled
35
36
37 to 55-65 °C. Stirring was stopped, and the aqueous layer was separated. The aqueous
38
39
40
41 layer was clarified by passing it through an inline filter to remove the emulsion layer,
42
43
44 then cooled to 10-20 °C, which resulted in a turbid solution. 40% w/w K_2CO_3 (440 kg,
45
46
47 7.15 wts.) was charged to the batch through a polish filter to a pH of 8-9 (13 h addition
48
49
50
51 time). The batch was stirred for 2 h, then the product was isolated by filtration. The filter
52
53
54
55 cake was washed with 10% w/w Na_2SO_4 (aq) twice (132 kg then 110 kg). The wet cake
56
57
58
59
60

1
2
3
4 was sampled for residual azide (3 ppm; target \leq 5 ppm). The solids on the filter were
5
6
7 dried at 10-20 °C under vacuum for 48 h then at 20-30 °C for 71 h. Yield: 76.85 kg of a
8
9
10 solid containing 35% w/w water, and with an overall assay of 48.9% w/w (37.6 kg
11
12
13 corrected), corresponding to a 74% corrected yield. ^1H NMR (400 MHz, CD_3OD) δ 7.12
14
15
16 (dd, J = 4.9 Hz, 1 H), 6.99 (m, 2 H), 4.51 (br d, J = 2.8 Hz, 1 H), 3.52 (dd, J = 13.9, 3.6
17
18 Hz, 1H), 2.87 (br d, J = 13.8 Hz, 1H) ppm; ^{13}C NMR (100 MHz, CD_3OD) δ 162.7 (br d, J
19
20 = 242 Hz), 161.4 (br d, J = 241 Hz), 159.0 (d, J = 2 Hz), 148.4, 147.0 (d, J = 7 Hz),
21
22
23 137.9, 137.6 (d, J = 3 Hz), 135.2 (d, J = 7 Hz), 134.0 (d, J = 3 Hz), 132.3 (d, J = 8 Hz),
24
25
26 125.1 (d, J = 8 Hz), 124.9 (d, J = 9 Hz), 117.2 (d, J = 22 Hz), 160.0 (d, J = 23 Hz), 115.9
27
28
29 (d, J = 24 Hz), 112.5 (d, J = 23 Hz), 110.2 (d, J = 22 Hz), 109.3 (d, J = 22 Hz), 66.7,
30
31
32 51.4, 38.7, 37.9, 16.9 ppm; ^{19}F NMR (100 MHz, CD_3OD) δ 115.42 ppm; HRMS: m/z
33
34
35
36
37
38
39
40
41
42 calcd for $\text{C}_8\text{H}_8\text{FN}$: ($\text{M}+\text{H}^+$), 138.0714, Found: 138.0716 .
43
44
45

46 **(S)-4-fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine hemi L-dibenzoyl tartaric acid salt**
47
48
49 **(5•DBTA)**. Ethanol (151 kg, 4.0 wts.) and L-DBTA (47.2 kg, 0.13 mol, 0.48 equiv.) were
50
51
52
53 charged to an appropriately-sized reactor (R1) and the batch temperature was adjusted
54
55
56
57
58
59
60

1
2
3 to 15-25 °C. The mixture was stirred for 2 h to dissolve all the solids. Ethanol (19 kg, 0.5
4
5
6
7 wts.) was charged to R1 to rinse the walls. *rac*-4-Fluorobicyclo[4.2.0]octa-1,3,5-trien-7-
8
9
10 amine (**rac 5**; 37.5 kg, 0.27 mol, 1.00 equiv.) was charged to a separate reactor (R2)
11
12
13 followed by ethanol (446 kg, 11.9 wts.) and the batch temperature was adjusted to 15-
14
15
16
17 25 °C. The L-DBTA solution from R1 was transferred to R2 over 6 h, and R1 as well as
18
19
20 the transfer line were rinsed with ethanol (19 kg, 0.5 wts.), adding the rinse to R2. The
21
22
23
24 batch in R2 was stirred at 15-25 °C for 5 h. The product was isolated by filtration and
25
26
27
28 the solids as well as R2 were rinsed with ethanol (60 kg, 1.6 wts.). The wet cake was
29
30
31
32 reslurried in water (190 kg, 5 wts.) at 15-25 °C for 5 h. The product was isolated by
33
34
35
36 filtration and washed with water (60 kg, 1.6 wts.). The product was dried under vacuum
37
38
39 at 35-42 °C for 55 h. Yield: 36.7 kg of a white solid with 98.1% w/w purity, 99.1% a/a
40
41
42
43 purity, and 99.1% *ee* (36 kg corrected), corresponding to a net corrected yield of 41.6%.
44
45
46 ¹H NMR (400 MHz, DMSO-d₆) δ 7.96 (d, *J* = 7.3 Hz, 2 H), 7.60 (m, 1 H), 7.48 (t, *J* = 7.7
47
48
49 Hz, 2 H), 7.11 (m, 3 H), 5.63 (s, 1 H), 4.53 (br d, *J* = 2.8 Hz, 1 H), 3.36 (br dd, *J* = 14.1,
50
51
52 4.0 Hz, 1 H), 2.94 (br d, *J* = 14.3 Hz, 1 H) ppm; ¹³C NMR (100 MHz, DMSO-d₆) δ 167.7,
53
54
55
56 165.2, 162.4 (br d, *J* = 240 Hz), 161.1 (br d, *J* = 240 Hz), 158.4 (d, *J* = 3 Hz), 148.1 (d, *J*

1
2
3 = 10 Hz), 138.5 (d, $J = 3$ Hz), 135.9 (d, $J = 7$ Hz), 134.6, 133.3 (d, $J = 8$ Hz), 129.9,
4
5
6
7 129.5, 129.0, 125.9 (d, $J = 9$ Hz), 117.7 (d, $J = 22$ Hz), 116.5 (d, $J = 23$ Hz), 113.1 (d, J
8
9
10 = 22 Hz), 111.4 (d, $J = 22$ Hz), 66.7(d, $J = 2$ Hz), 38.7, 18.5 ppm; ^{19}F NMR (100 MHz,
11
12 DMSO) δ 112.87 ppm; HRMS: m/z calcd for $\text{C}_8\text{H}_8\text{FN}$ (free base): ($\text{M}+\text{H}^+$), 138.0714,
13
14 Found: 138.0720; $[\alpha]_{\text{D}}^{25} = -19.79$ ($c=1$, DMSO).
15
16
17
18
19
20
21

22 **tert-butyl (Z)-((4-amino-1,2,5-oxadiazol-3-yl)(hydroxyimino)methyl)glycinate (27)**. To a
23
24
25 10 L 4-neck round-bottomed flask equipped with a mechanical stirrer and maintained
26
27
28 under nitrogen, (E)-4-amino-N-hydroxy-1,2,5-oxadiazole-3-carbimidoyl chloride (420 g,
29
30 2584 mmol, 1.00 equiv.) and ethyl acetate (4.2 L, 10 vol.) were charged sequentially.
31
32
33
34
35
36 Stirring (150 rpm) was initiated and the mixture (a suspension) was cooled to < 5 °C
37
38
39 with an ice/water bath. A solution of tert-butyl 2-aminoacetate (373 g, 2842 mmol, 1.10
40
41
42 equiv.) in ethyl acetate (0.525 L, 1.25 vol.) was prepared, and charged to the reaction
43
44
45
46 mixture dropwise over 0.5 h. A solution of triethylamine (392 g, 3876 mmol, 1.50 equiv.)
47
48
49 in ethyl acetate (0.525 L, 1.25 vol.) was prepared, and charged to the reaction mixture
50
51
52
53 dropwise over 0.5 h. The resulting solution was stirred for 16 h at ambient temperature,
54
55
56
57
58
59
60

1
2
3 then sampled for reaction conversion by LCMS analysis. Water (2.5 L, 6.0 vol.) was
4
5
6 charged, and phases were allowed to separate. The organic phase was washed with
7
8
9
10 aqueous 1 M hydrochloric acid (1.2 L, 2.85 vol.), then with aqueous 1 M sodium
11
12
13 bicarbonate (1.2 L, 2.85 vol.). The organic phase was dried over anhydrous sodium
14
15
16 sulfate, filtered, and concentrated to dryness, producing a solid (560 g). The crude solid
17
18
19
20 was slurried in *n*-heptane (2.5 L) and filtered, then dried. Yield: 530 g of a white solid
21
22
23
24 with 82% a/a purity, 70% w/w purity (qNMR^{28,29,30}), which corresponds to a 56% yield.

25
26
27
28 ¹H NMR (600 MHz, DMSO-d₆) δ 10.72 (s, 1H), 6.61 (t, *J* = 6.8 Hz, 1H), 6.32 (s, 2H),
29
30
31 4.06 (d, *J* = 6.9 Hz, 2H), 1.34 (s, 9H) ppm; MS: *m/z* calcd for C₉H₁₆N₅O₄ (M+H⁺) 258.1,
32
33

34
35 Found 258.1.
36
37
38

39 (Z)-(4-(N'-hydroxycarbamimidoyl)-1,2,5-oxadiazol-3-yl)glycine (29). To a 10 L 4-neck
40
41
42 round-bottomed flask equipped with a mechanical stirrer and maintained under nitrogen,
43
44
45 (Z)-tert-butyl 2-(4-amino-N'-hydroxy-1,2,5-oxadiazole-3-carboximidamido)acetate (27;
46
47
48 530 g, 1442 mmol, 1.00 equiv.) was charged followed by water (4.24 L, 8 vol.). Stirring
49
50
51
52
53 (450 rpm) was initiated, and potassium hydroxide (356 g, 6346 mmol, 4.4 equiv.) was
54
55
56
57
58
59
60

1
2
3 charged at once. The appearance of the mixture gradually changed from a white
4
5
6 suspension to an orange solution. The reaction mixture was heated to a batch
7
8
9 temperature of 100 °C and maintained for 3.5 days. Reaction conversion was monitored
10
11
12 by LCMS analysis. The reaction mixture was cooled to 5 °C, and conc. aqueous
13
14
15 hydrochloric acid (12 M, 529 mL, 4.4 equiv.) was charged. The product was isolated by
16
17
18 filtration, and washed with water (approx. 0.8 L, twice). The solids were dried in a
19
20
21 vacuum oven overnight. Yield: 293.5 g of a white solid with 99% a/a purity, 90% w/w
22
23
24 purity (qNMR^{28,29,30}), corresponding to a 90% yield. ¹H NMR (600 MHz, DMSO-d₆) δ
25
26
27 12.90 (s, 1H), 10.54 (s, 1H), 6.43 (t, *J* = 5.6 Hz, 1H), 6.24 (s, 2H), 3.98 (d, *J* = 5.8 Hz,
28
29
30 2H) ppm; MS: *m/z* calcd for C₅H₈N₅O₄ (M+H⁺) 202.1, Found 202.0.
31
32
33
34
35
36
37
38

39 **(Z)-2-(2-((4-(N'-hydroxycarbamimidoyl)-1,2,5-oxadiazol-3-yl)amino)acetamido)ethyl**
40
41
42 **acetate (31)**. To a 10 L 4-neck round-bottomed flask equipped with a mechanical stirrer
43
44
45 and maintained under nitrogen, (Z)-(4-(N'-hydroxycarbamimidoyl)-1,2,5-oxadiazol-3-
46
47
48 yl)glycine (**29**; 343 g, 1.53 mol, 1.00 equiv.) and 2-aminoethyl acetate hydrochloride (**30**;
49
50
51 271 g, 1.84 mol, 1.20 equiv.) were charged. THF (6.86 L, 20 vol.) was charged, and the
52
53
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1
2
3 resulting suspension was stirred at ambient temperature. Diisopropylethylamine (1.61 L,
4
5
6
7 9.21 mol, 6 equiv.) was charged over 15 min., then stirred for 20 min. at ambient
8
9
10 temperature to result in a homogenous light pink suspension. T3P (977 g of a 50%
11
12
13 solution in ethyl acetate; 2.46 mol, 1.61 equiv.) was charged over 45 min. The resulting
14
15
16
17 reaction mixture was stirred for 4 h at ambient temperature. Water (4 L, 11.7 vol.) was
18
19
20
21 charged, then the mixture was transferred to a separatory funnel, and the phases were
22
23
24 allowed to separate. The aqueous phase was extracted with ethyl acetate (2 L, 5.8 vol.)
25
26
27
28 twice. The organic extracts were combined and washed with brine (1 L), then dried over
29
30
31 anhydrous sodium sulfate, filtered, and concentrated under reduced pressure. The
32
33
34 solids were re-slurried in ethyl acetate (1 L, 2.9 vol.), filtered, and dried. Yield: 390 g,
35
36
37
38 corresponding to a 80% yield. ^1H NMR (600 MHz, DMSO- d_6) δ 10.57 (s, 1H), 8.28 (t, J
39
40
41 = 5.0 Hz, 1H), 6.50 (t, J = 5.2 Hz, 1H), 6.21 (s, 2H), 4.01 (t, J = 5.5 Hz, 2H), 3.86 (d, J =
42
43
44 5.3 Hz, 2H), 3.36 – 3.33 (m, 2H), 2.00 (s, 2H); MS: m/z calcd for $\text{C}_9\text{H}_{15}\text{N}_6\text{O}_5$ ($\text{M}+\text{H}^+$)
45
46
47
48 287.1, Found 287.1.
49
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60

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2
3
4 **(Z)-2-(2-((4-(chloro(hydroxyimino)methyl)-1,2,5-oxadiazol-3-yl)amino)acetamido)ethyl**
5
6
7 **acetate (32)**. To a 5 L 4-neck round-bottomed flask equipped with a mechanical stirrer
8
9
10 and maintained under nitrogen, (Z)-2-(2-((4-(N'-hydroxycarbamimidoyl)-1,2,5-oxadiazol-
11
12
13 3-yl)amino)acetamido)ethyl acetate (**31**; 200 g, 0.7 mol, 1.00 equiv), water (1 L), and
14
15
16 sodium chloride (122 g, 2.1 mol, 3.00 equiv) were charged sequentially. 6N HCl (1 L, 5
17
18
19 vol.), water (1 L, 5 vol.), and ethyl acetate (1 L, 5 vol.) were then charged sequentially.
20
21
22
23
24 The reaction mixture was cooled to < 5 °C. Sodium nitrite (50.6 g, 0.73 mol, 1.05 equiv.)
25
26
27 was charged as a solution in water (400 mL, 2 vol.) dropwise over 1 h, maintaining a
28
29
30
31 batch temperature of 0-5 °C. After stirring a 0-5 °C for 1 h, the reaction mixture was
32
33
34 warmed to ambient temperature. The reaction mixture was transferred to a separatory
35
36
37 funnel and the phases were allowed to separate. The aqueous phase was extracted
38
39
40
41 with ethyl acetate (1 L, 5 vol.) three times. The organic extracts were combined and
42
43
44 washed with water (2 L, 10 vol.). The organic phase was dried over anhydrous sodium
45
46
47 sulfate, filtered and concentrated to dryness under reduced pressure. Yield: 200 g of an
48
49
50
51 off-white solid with 96% w/w purity (qNMR^{28,29,30}), corresponding to a 90% yield.
52
53
54
55
56 Material was used as-is without further purification.
57
58
59
60

1
2
3
4 **(S,Z)-2-((4-(N-(4-fluorobicyclo[4.2.0]octa-1(6),2,4-trien-7-yl)-N'-**
5
6
7 **hydroxycarbamimidoyl)-1,2,5-oxadiazol-3-yl)amino)-N-(2-hydroxyethyl)acetamide (2).**
8
9

10 To a 2 L 4-neck round-bottomed flask equipped with a mechanical stirrer and
11
12 maintained under nitrogen, (S)-4-fluorobicyclo[4.2.0]octa-1,3,5-trien-7-amine
13
14 hydrochloride (**5**•HCl; 65 g, 374 mmol, 1.00 equiv.) and THF (650 mL, 10 vol.) were
15
16 charged sequentially. The suspension was stirred and cooled to 0 °C. Solid sodium
17
18 bicarbonate (79 g, 936 mmol, 2.5 equiv.) was charged, and the resulting mixture was
19
20 stirred at 0 °C for 5 min. (Z)-2-(2-((4-(chloro(hydroxyimino)methyl)-1,2,5-oxadiazol-3-
21
22 yl)amino)acetamido)ethyl acetate (**32**; 158 g, 449 mmol, 1.20 equiv.) was dissolved in
23
24 THF (650 mL, 10 vol.) and the solution was charged to an addition funnel. This solution
25
26 was added dropwise to the reaction mixture over 1 h, maintaining a batch temperature
27
28 < 0 °C. After stirring for 3 h at 0 °C, LCMS analysis showed no detectable residual
29
30 starting material. The reaction mixture was filtered, then diluted with 2-
31
32 methyltetrahydrofuran (6.5 L, 100 vol.) and water (6.5 L, 100 vol.). The two phases were
33
34 separated, then the aqueous phase was extracted with 2-methyltetrahydrofuran (2 L, 31
35
36 vol.). The organic extracts were combined and dried over anhydrous sodium sulfate,
37
38
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1
2
3 and concentrated under reduced pressure to approx. 1 L (15 vol.). Then 2-
4
5
6
7 methyltetrahydrofuran (1.3 L, 20 vol.) was charged, and the mixture was concentrated
8
9
10 under reduced pressure to approx. 1 L (15 vol.). This operation was repeated two more
11
12
13 times (for a total of three solvent exchanges). This resulted in a solution with 0.7% w/w
14
15
16
17 water by KF titration. Methanol (975 mL, 15 vol.) was charged to the mixture, and the
18
19
20 suspension was filtered to remove **34**. This resulted in 4000 g (95.5% a/a purity) of a
21
22
23 solution that was charged to a 5 L 4-neck round-bottomed flask under nitrogen.
24
25
26
27 Potassium carbonate (46.7 g, 338 mmol, 0.90 equiv.) was charged and the resulting
28
29
30 mixture was stirred at ambient temperature for 30 min. Reaction conversion was
31
32
33 monitored by HPLC, which showed no remaining ester starting material after 1 h. The
34
35
36 reaction mixture was transferred to a separatory funnel and diluted with 2-
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38
39 methyltetrahydrofuran (3 L, 46 vol.) and water (4.5 L, 69 vol.), then mixed to disperse
40
41
42 the phases. The phases were separated, and the organic phase was washed with brine
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45
46 (3 L, 46 vol.) four times. The combined aqueous extracts were back-extracted with 2-
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48
49 methyltetrahydrofuran (3 L, 46 vol.), and the organic phases were combined, dried over
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52 anhydrous sodium sulfate, and filtered. The organic phase was concentrated under
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3 reduced vacuum to approx. 2 L (approx. 31 vol.). Ethyl acetate (1.5 L, 23 vol.) was
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5
6 charged, and the distillation was repeated down to 2 L (approx. 31 vol.), and the
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8
9 operation was repeated two more times for a total of three solvent exchanges. The
10
11
12 resulting suspension was stirred at ambient temperature overnight, and then filtered to
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14
15 afford 105 g of crude **2** (85% yield). Two batches of the crude material were combined
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17
18 and recrystallized by redissolving in THF (18 vol.), then polish-filtered. To the resulting
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21 solution, ethyl acetate (15 vol.) was charged, followed by seeding at ambient
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23
24 temperature. After stirring the resulting suspension at ambient temperature for 3 h, the
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26
27 mixture was concentrated under reduced pressure to 10 vol., followed by three
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29
30 additional cycles (add 15 vol. of ethyl acetate and distill) to remove the THF. The
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32
33 resulting suspension was aged overnight at ambient temperature, and filtered and dried
34
35
36 to afford **2**. Yield: 165 g of an off-white solid with 99.6% a/a and 99.4% w/w purity and
37
38
39 containing 7631 ppm ethyl acetate and 2459 ppm THF. ¹H NMR (400 MHz, DMSO-*d*₆,
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41
42 *ppm*) δ 10.93 (s, 1H), 8.12 (t, *J* = 5.6 Hz, 1H), 7.16 (dd, *J* = 8.1, 4.7 Hz, 1H), 7.04 (ddd,
43
44
45 *J* = 10.7, 8.0, 2.3 Hz, 1H), 6.91 (dd, *J* = 7.9, 2.3 Hz, 1H), 6.74 (d, *J* = 8.2 Hz, 1H), 6.60
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47
48 (t, *J* = 5.4 Hz, 1H), 5.46 (ddd, *J* = 7.8, 5.1, 2.4 Hz, 1H), 4.66 (t, *J* = 5.4 Hz, 1H), 3.85 (d,
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4 $J = 5.3$ Hz, 2H), 3.57 – 3.32 (m, 3H), 3.26 – 2.94 (m, 3H). LC-MS (ES, m/z) 365 [M+H]⁺.
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6

7 $[\alpha]_{\text{D}}^{20.8} = +19.4$ ° ($c = 0.51$, MeOH). *ee* (by SFC) 99.6%.
8
9

10 ASSOCIATED CONTENT

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14
15
16 **Supporting Information.** The following files are available free of charge:
17
18

19
20 Computational details regarding the energy minimization for the rearrangement
21
22

23
24 (Scheme 6).
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26

27 AUTHOR INFORMATION

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52 53 **Notes**

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3 The authors declare no competing financial interest.
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22 manuscript.
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26 ABBREVIATIONS 27

28
29
30 ARC, accelerating rate calorimetry; AY, assay yield; DCM, dichloromethane; DIPEA,
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32 diisopropylethylamine; DoE, design of experiments; DSC, differential scanning
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34 calorimetry; IDO-1, Indoleamine-2,3-dioxygenase-1; IY, isolated yield; LCAP, liquid
35
36 chromatography area percent; PMI, process mass intensity; PTFA, pertrifluoroacetic
37
38 acid; RAR, rearrangement; SAR, structure-activity relationship; SFC, supercritical fluid
39
40 chromatography; T3P, propylphosphonic anhydride; TFA, trifluoroacetic acid; THF,
41
42 tetrahydrofuran; UHP, urea hydrogen peroxide.
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