

Methanol as the Hydrogen Source in the Selective Transfer Hydrogenation of Alkynes Enabled by a Manganese Pincer Complex

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O lefins play an important role in bioactive molecules, pharmaceuticals, polymers, and functional materials.^{1,2} Furthermore, olefins can be functionalized into a vast variety of different compounds.³ A common method for the synthesis of (*Z*)-olefins is the semihydrogenation of alkynes using the Pd-based Lindlar catalyst and hydrogen gas (Scheme 1A).⁴ In

Scheme 1. Different Methods for the (Transfer) Hydrogenation of Alkynes



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addition, several *cis*-selective hydrogenation methods that mainly rely on the use of noble metals have been developed.⁵ To avoid the use of pressurized hydrogen gas, transfer hydrogenation methods that apply hydrogen donors, such as ammonia formates,^{6a} formic acid,^{6b,c} silanes,^{6d} and boranes,^{6e} evolved as alternatives. However, these methods may have disadvantages due to functional group tolerance, their relatively high prices, and significant byproduct formation (Scheme 1B). In this regard, alcohols, especially methanol, are highly desirable as hydrogen donors.⁷ Methanol is a very attractive hydrogen source, is produced on a large scale, and is one of the most important C₁ building blocks for the production of bulk and fine chemicals. The possibility of producing methanol from the greenhouse gas carbon dioxide highlights the sustainability of this hydrogen donor. In the proposed

"methanol economy", methanol is considered as a promising hydrogen storage material, which can also be directly used as an alternative fuel for internal combustion and other engines, either in combination with gasoline or neat and in methanol fuel cells.⁸ In the case of methanol, the dehydrogenation step is more energy demanding than for other alcohols.⁹ Hence, it is challenging to develop catalysts that are active for both the dehydrogenation step of methanol and the semihydrogenation of unsaturated triple bonds to selectively form (*Z*)-olefins. This research field is so far rather underdeveloped, and to the best of our knowledge, no general studies of the base metalcatalyzed highly selective semihydrogenation of alkynes toward the formation of (*Z*)-olefins using methanol as a hydrogen source have been published.

Recently, the field of manganese pincer-catalyzed (de-) hydrogenation reactions has received a great deal of attention.^{9,10} Various publications described the manganese complex-catalyzed activation and synthetic utilization of methanol, whereby methanol was mainly applied as a methylating reagent.¹¹ However, recently reported manganese-catalyzed hydrogen borrowing and transfer hydrogenation catalysis^{11,12} indicated that manganese pincer complexes may be suitable for the activation of methanol in the semitransfer hydrogenation of alkynes (Scheme 1C).

Thus, we evaluated different manganese complexes Mn-1– Mn-5 as catalysts in the transfer hydrogenation of 1-methoxy-4-(phenylethynyl)benzene (1a) (Table 1, entries 1–5, respectively). Surprisingly, complex Mn-1, which is known to be active in the alkylation of ketones and nitriles, ^{12a,v} gave a

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Table 1. Optimization of the Reaction Conditions^a



^{*a*}Reaction conditions: 1a (0.1 mmol), [Mn], Cs₂CO₃, methanol (0.1 mL), 14 h, 135 °C for entries 1–10 and 150 °C for entries 11–17. ^{*b*}Yields were determined by ¹H NMR spectroscopy using acetonitrile as the internal standard. Heating inside an aluminum block. ^cMethanol (0.2 mL). ^{*d*}Toluene as the cosolvent (0.1 mL). ^{*c*}Methanol (0.2 mL) and toluene (0.2 mL).

yield of 49%, forming almost exclusively the corresponding *Z*-isomer **2a** (Table 1, entry 1).

On the other hand, the pyridyl-based complex Mn-2, previously used in the α -methylation of ketones,¹¹ⁱ was shown to be completely inactive in this transformation (Table 1, entry 2). To evaluate the importance of the phosphine moiety, we applied the aliphatic phosphine-based complex Mn-3 in the transformation. Although this complex is also known to be active in the alkylation of ketones,^{12a} only trace amounts of product 2a were obtained (Table 1, entry 3).

Also, the bidentate complex **Mn-4**, which is catalytically active in ester hydrogenation,¹³ was inactive in the transfer hydrogenation reaction (Table 1, entry 4), highlighting the non-innocent behavior of the pincer backbone. Furthermore, N-Me-based complex **Mn-5** did not give any yield, illustrating the necessity of the NH functionality (Table 1, entry 5). The catalyst screening emphasized the importance of the aliphatic pincer backbone and the significance of aromatic phosphines in the semitransfer hydrogenation of alkynes. Increasing the amount of methanol and the amount of catalyst improved the yield (Table 1, entries 6 and 7).

In contrast, the catalytic activity decreased for a higher base loading (Table 1, entry 8). Moreover, the utilization of toluene as a cosolvent increased the yield significantly (Table 1, entry 9), while decreasing the concentration of the reaction system did not improve the yield (Table 1, entry 10). More detailed base and cosolvent screening is summarized in the Supporting Information.

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Increasing the reaction temperature provided an almost quantitative yield of 97% with (Z)-product 2a formed predominantly (Table 1, entry 11). Control experiments proved the efficiency of the chosen catalytic system (Table 1, entries 14–17). When other alcohols such as ethanol and isopropanol were used as hydrogen sources, quantitative yields were also obtained (see the Supporting Information). Additionally, no impact was observed when a drop of mercury was added to the reaction mixture, which suggests the homogeneous nature of the catalyst under these reaction conditions.¹⁴

After the kinetic profile of the reaction had been measured (see the Supporting Information), the reaction time was set to 14 h. In the further course of the work, we applied the optimized reaction conditions (Table 1, entry 11) in the transfer hydrogenation of various internal alkynes (Scheme 2). Unfortunately, terminal alkynes proved to be inactive in the transfer hydrogenation reaction.

Generally, the alkyne derivatives **1a–1x** were reduced to the corresponding olefins 2a-2x with high selectivity in moderate to quantitative yields. Stilbene 2a was isolated in a very good vield of 88% with a Z/E ratio of 98/2. In the further course of the evaluation of scope, both electron-donating (2b-2g) and 2n) and electron-withdrawing substituents (2j-2m) were tolerated in ortho, meta, and para positions of the aromatic moiety of the alkynes. Various heterocycle-containing alkynes (10 and 1q-1u) were tolerated in the transformation. Also, the longer chain internal olefins 2v and 2w were isolated in high yields with good selectivity. It is important to note that for substrates such as 1h, 1j, 1l, 1w, and 1x some overhydrogenation into the corresponding diarylethanes was observed. To present the generality of the transformation, we applied our catalytic system in a gram scale synthesis of (Z)stilbene (2b) (Scheme 3). The desired product 2b was obtained in quantitative yield with an excellent Z/E ratio of 97/3. When (Z)- or (E)-stilbenes 2b were used, no isomerization or hydrogenation occurred (see the Supporting Information).

Next, we used fully deuterated methanol CD_3OD to investigate the incorporation position of hydrogen (Scheme 4).

In the olefinic position, the value of deuterium incorporation reached 94% and this result indicates the possibility of *cis*-selective deuterium incorporation. Due to the importance of deuterium-labeled compounds,¹⁵ this transformation might be evaluated in further work (Scheme 4). Beyond that, we observed significant H/D exchange in the *ortho* position next to the methoxy group of **2a**.

On the basis of these observations, we propose the following catalytic cycle (Scheme 5). In the first step, the air and moisture stable precursor Mn-1 is activated by a base to give the active species Mn-1a. Methanol coordinates to the active species Mn-1a, which is the deprotonated via metal ligand interactions, forming the manganese methoxide complex Mn-1b.^{12d} The following deprotonation of the methoxide moiety results in formaldehyde elimination, so that the hydride species Mn-1c is obtained. Subsequent alkyne coordination and insertion into the manganese—hydride bond leads to the formation of Mn-1d. In the next step, the elimination of (Z)-stilbene occurs, to regenerate the active Mn-1a catalyst. However, an alternative pathway starting from Mn-1d is conceivable in which methanol facilitates elimination of the (Z)-stilbene and directly provides the Mn-1b intermediate.

Ph-==

P٢

P٢

Рń

-R + CH₃OH

OMe

SMe

OMe

2a, 88%, 98:2 Z/E (2)

2d, 95%, 98:2 Z/E (5)

2g, 86%, 99:1 Z/E (2)

2j, 99%, 99:1 Z/E (7)

2m^[c], 93%, 99:1 Z/E (5)

Pł

Scheme 2. Manganese-Catalyzed Transfer Hydrogenation of Alkynes

2

È

Me

2c, 96%, 95:5 Z/E (2)

2f, 93%, 95:5 Z/E (3)

2i, 99%, 91:9 Z/E (3)

21, 98%, 99:1 Z/E (6)

20, 75%, 99:1 Z/E (2)

Ph

н

D٢

P٢

Mn-1

Cs₂CO₃, 14 h

2b, 98%, 97:3 Z/E (3)

Me

CE

Pr

2n, 97%, 95:5 Z/E (3)

2k^[c], 89%, 98:2 Z/E (2)

Ph

2e, 94%, 99:1 Z/E (2)

2h^[c], 93%, 99:1 Z/E (8)

Рń









^aReaction conditions: 1 (0.3 mmol), Cs₂CO₃ (0.6 mmol), Mn-1 (2 mol %) in CH₃OH (0.3 mL) and toluene (0.3 mL) at 150 °C. ^bAt 130 °C. ^cMn-1 (4 mol %). The overhydrogenation product is presented in parentheses. Heating inside an aluminum block.





Alternatively, Mn-1a can also be directly converted to Mn-1c via a six-membered transition state.¹²⁶

In conclusion, we developed the first base metal-catalyzed semitransfer hydrogenation of alkynes, using methanol as a hydrogen donor. The applicability of this transformation was demonstrated for a variety of different alkynes, giving the corresponding (Z)-olefins in moderate to quantitative yields and high chemoselectivity. The reaction is scalable, and deuterium labeling experiments demonstrate the cis-selective hydrogen incorporation.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acs.orglett.0c02151.

2r, 75%, 99:1 Z/E (0) 2p, 96%, 99:1 Z/E (5) **2q**^[c], 35%, 99:1 Z/E (0) **2u**^[b], 83%, 99:1 *Z/E* (4) 2t, 97%, 99:1 Z/E (5) 2s 35%, 91:9 Z/E (2)

2v, 99%, 97:3 Z/E (4)



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Experimental procedures and characterization of compounds (PDF)

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Notes

The authors declare no competing financial interest.

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