

# Rate Constant of the $\alpha$ -Pinene + Atomic Hydrogen Reaction at 295 K

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## Abstract

The rate constant of the reaction of  $\alpha$ -pinene with atomic hydrogen was determined at 295 K using the fast-flow reactor technique directly coupled to a mass spectrometric detection technique. The value was found to be equal to  $(9.8 \pm 3.3) \times 10^{-13} \text{ cm}^3 \text{ molecules}^{-1} \text{ s}^{-1}$  and independent of the helium pressure between 1 and 2 torr. The major reaction product formed is pinane showing that the stabilization of the adduct radical  $\text{C}_{10}\text{H}_{17}^*$ , followed by a subsequent hydrogen atom addition step, is the important reaction route. © 1994 John Wiley & Sons, Inc.

## Introduction

It is well known that terpenes and in particular  $\alpha$ -pinene are very important biogenic hydrocarbons emitted on a global scale [1]. Although the rate constants of the primary destruction reactions of  $\alpha$ -pinene under atmospheric conditions involving hydroxyl and nitrate radicals and ozone are relatively well established [2], not much is known of the further kinetics and mechanism of its degradation path [3]. One possible way to clarify this complex reaction mechanism is an investigation of the  $\alpha$ -pinene/OH reaction with a fast-flow reactor technique. Since the OH-radicals are produced by the  $\text{H} + \text{NO}_2$  titration reaction, it was noticed that in the absence of  $\text{NO}_2$ , a fraction of the  $\alpha$ -pinene disappears in a reaction with atomic hydrogen.



In order to estimate the possible interference of reaction (1) in the  $\text{C}_{10}\text{H}_{16}$ /OH system, the rate constant of reaction (1) has to be determined separately and its relative importance in this fast-flow reactor study established.

From fundamental point of view hydrogen atom addition reactions to double bonds are of interest and especially the kinetic behavior of the energized adduct [4,5] is likewise important. Recent work on the hydrogen atom reactions with cycloalkenes [6] and *trans*-2-butene [7] has to be mentioned here also.

In this contribution a mass spectrometric detection technique directly coupled to a fast-flow reactor will be used to determine for the first time the rate constant  $k_1$ . In view of the complexity of mass fragmentation spectra and large number of isotope contributions, a detailed reaction product analysis was impossible. In order to carry out such an analysis a GC-MS technique would be required. It will be shown though that at a pressure of 2 torr stabilization of the adduct  $\text{C}_{10}\text{H}_{17}^*$  is the dominant path relative to its decomposition into other hydrocarbon molecules or fragments.

## Experimental Technique

### *Fast-Flow Reactor and Detection*

Although the use and characteristics of the fast-flow reactor technique is very well known in gas-phase kinetic studies, a brief description will be given here since this particular experimental set-up has not been described elsewhere.

A schematic view of the system is given in Figure 1. It consists of a quartz reactor with an internal diameter of 2.8 cm and a length of 70 cm. By means of an oil rotary pump with a nominal pump capacity of  $35 \text{ m}^3 \text{ hr}^{-1}$  a flow velocity  $v$  of  $(10.9 \pm 0.2) \text{ m s}^{-1}$  is obtained at 295 K with helium as a carrier gas. Reagent flows are maintained by mass flow controllers in the range from 1 to  $1000 \text{ cm}^3 \text{ min}^{-1}$ . The addition of  $\alpha$ -pinene is realized by flowing a fraction of the carrier gas through a separate pyrex vessel across the  $\alpha$ -pinene liquid.

Weight loss measurements of the  $\alpha$ -pinene containing vessel allowed a calculation of the  $\alpha$ -pinene concentrations in the gas phase in the reactor. While the  $\alpha$ -pinene/He flow is introduced through the central quartz probe with an external diameter of 0.6 cm, the hydrogen atoms are generated by a microwave discharge in a 0.1%  $\text{H}_2/\text{He}$  mixture. The reaction time  $t$  is determined by the axial position of the  $\alpha$ -pinene inlet with respect to the detection point downstream of the fast-flow reactor. At this point a mass spectrometric detection system is directly coupled to the fast-flow reactor for on-line reactant analysis. It is a magnetic instrument of the type Micromass 8-80 from Vacuum Generators with a magnetic field sector of  $80^\circ$  and radius of 8 cm and it is equipped with a "closed" ionization source with both a variable electron energy and electron emission current of respectively 5 to 100 eV and 10 to  $400 \mu\text{A}$ . The detector consist of a 17 Cu/Be dynode ion multiplier operating at 2.5 kV. A fine metering valve with a range from  $1 \times 10^{-4}$  to  $2 \times 10^{-2} \text{ atm min}^{-1}$  allowed a pressure of  $2 \times 10^{-6}$  torr inside the mass spectrometer to be set which was independent of the reactor pressure. The latter is determined by means of a Barocel absolute pressure gauge. In

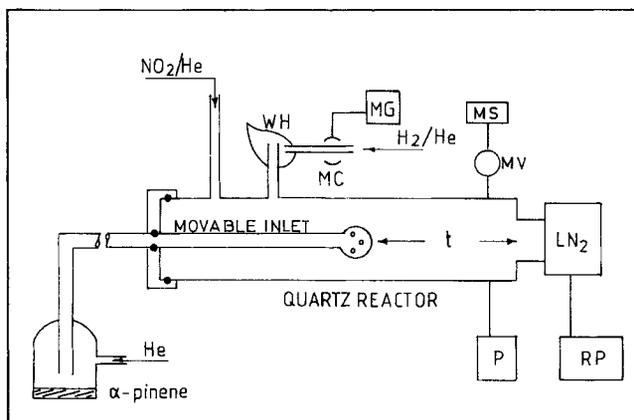


Figure 1. Schematic view of the experimental set up. (MC): Microwave cavity; (MG): Microwave generator; (WH): Wood's horn; (MS): Mass spectrometer; (MV): Metering value; (P): Absolute pressure gauge; (LN2): Liquid nitrogen trap; (RP): Oil rotary pump; and (t): Reaction time.

order to determine the rate constant  $k_1$  the decay of the mass spectrometric signal of the  $\alpha$ -pinene fragment at mass 93 was followed as a function of the reaction time in excess of hydrogen atoms. The latter concentration  $[H]$  has been determined by means of the  $H + NO_2$  titration with the end point taken at the appearance of the  $NO_2$  signal. Detection limits for most components are in the 0.1 to 2 ppm range.

### *Flow Characteristics*

In order to be able to derive reliable kinetic data from fast flow reactor experiments, a few experimental criteria must be fulfilled [8]. First, it is clear that laminar flow conditions must be established with a Reynolds Number  $Re$  of less than 2000. In this case at 2 torr helium pressure and 295 K, one finds  $Re = 6.9$ . Second, the time for reagent mixing must be sufficiently long to realize a radially flat concentration profile for all reagents added. This is not a problem for both H-atoms and  $NO_2$  since both inlets are located upstream of the mixing point. It may be a problem for  $\alpha$ -pinene added through the central probe. One can calculate that the distance  $z$  for complete mixing must be larger than  $v \times d^2/2D$  where  $d$  is the radial distance between the mixing point and the reactor wall and  $D$  the binary diffusion coefficient of  $\alpha$ -pinene in helium. The latter is not well known but can be estimated to be about  $80 \text{ cm}^2 \text{ s}^{-1}$  at 2 torr and 295 K. With a value of  $d = 0.9 \text{ cm}$  one arrives at a minimal mixing distance  $z > 6 \text{ cm}$  which on the time scale corresponds to 5 ms. Since all the experiments are carried out at  $z \geq 15 \text{ cm}$ , poor mixing of the reagents cannot not be a problem.

Finally in order to be allowed to neglect axial diffusion, the dimensionless parameter  $D \times k_1 \times [H]/v^2$  must be much smaller than 1 [8]. In view of the rather small value of  $k_1$  (see section on experimental results) leading to pseudo-first-order decay constants never exceeding  $40 \text{ s}^{-1}$ , the above criterion is easily met.

### *Reagents*

Gases and gas mixtures are from Indugas. Hydrogen is added from a 0.1%  $H_2/He$  mixture while nitrogen dioxide is a 0.85%  $NO_2/He$  mixture each prepared in helium with a purity of 99.9996%. The  $\alpha$ -pinene liquid is from Aldrich and has a purity of 98%.

## **Results and Discussion**

### *Loss of Hydrogen Atoms on the Wall*

Since the pseudo-first-order decay constant  $k_{\text{obs}} = k_1 [H]$  of reaction (1) will be determined in excess of hydrogen atoms it must be checked how the hydrogen concentration is affected by the reactor wall condition. With a freshly cleaned reactor the H-atom concentration remained constant within 5% in the whole kinetic zone. After about one week the reactor wall condition seemed to deteriorate somewhat leading to a higher H-atom loss. As an example the natural logarithm of the H-atom concentration as a function of time is shown in Figure 2 for the worst case.

A straight line is obtained with as slope  $k_w = (13.0 \pm 0.4) \text{ s}^{-1}$ . In view of this relatively low value for  $k_w$  one knows that the loss of H-atoms is controlled by its

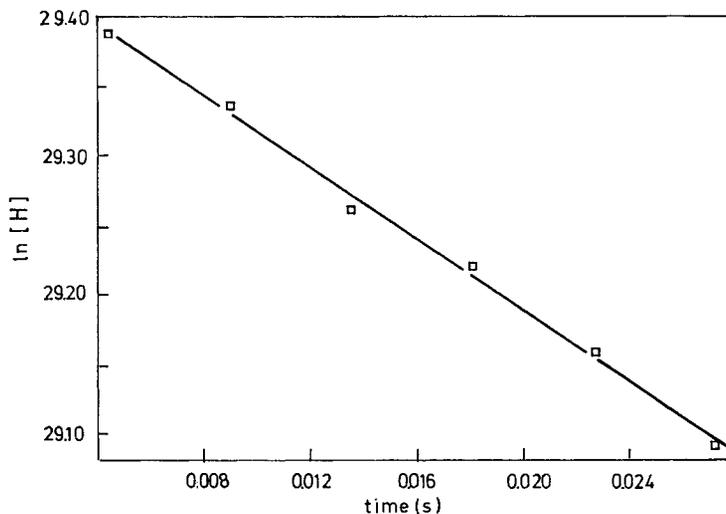


Figure 2. Natural logarithm of H-atom concentration as a function of the time: Reactor pressure  $P_r$  and temperature  $T_r$  are respectively 2 torr and 295 K.

sticking coefficient and thus  $k_w$  is given by [9].

$$(2) \quad k_w = \frac{\gamma_H c}{2r(1 - \gamma_H/2)}$$

with  $c$  being the average thermal velocity of the hydrogen atoms,  $(8RT/\pi M)^{0.5}$  and  $\gamma_H$  the sticking coefficient of the H-atoms on the quartz wall, i.e., the fraction of H-atoms which recombines upon collision. Equation 2 allows us to calculate the sticking coefficient  $\gamma_H$  on quartz equal to  $(1.6 \pm 0.05) \times 10^{-4}$ . This value is almost a factor of 5 larger than found for clean reactor walls [10]. The magnitude of  $\gamma_H$  is important since plug-flow conditions for active species lost on the reactor wall can only be achieved when  $\gamma \ll \frac{D}{r} \left( \frac{2\pi M}{RT} \right)^{0.5}$  [8]. This criterion which requires a  $\gamma$ -value smaller than  $10^{-3}$  is largely fulfilled for hydrogen atoms in the reactor geometry used.

Concerning the hydrogen atom concentrations, two corrections had to be applied. Since the concentrations were at the  $1 \times 10^{13}$  atoms  $\text{cm}^{-3}$  level the hydrogen atom/ $\text{NO}_2$  titration reaction will yield too high a concentration. Indeed OH radicals formed in the titration reaction will undergo subsequent reactions consuming additional  $\text{NO}_2$ . A simple kinetic model using the reaction and rate constant set given by Wayne et al. [11] allows to calculate by numerical integration the concentrations of the various species involved. It was found that depending on the initial hydrogen atom concentration a correction factor of 6 to 22% had to be applied. In addition depending on the reactor wall condition, an average hydrogen atom loss between 5 and 10% over the entire kinetic zone must also be taken into account.

#### Rate Constant $k_1$ of the Reaction $\alpha$ -Pinene + H-Atoms

Due to fragmentation in the ionization source the parent ion of  $\alpha$ -pinene at  $m/e = 136$  is only weak and therefore the  $\alpha$ -pinene decay was followed at the major fragment ion  $m/e = 93$  [12]. The experiments were carried out at 1 and 2 torr

total helium pressure. Initial  $\alpha$ -pinene concentrations in the range from  $5 \times 10^{10}$  to  $5 \times 10^{11}$  molecules  $\text{cm}^{-3}$  are mixed with an excess of atomic hydrogen in a ratio from 10 to 50. Since reaction 1 must yield a radical as reaction product which is in principle either the adduct  $\text{C}_{10}\text{H}_{17}^*$  or in case of hydrogen abstraction  $\text{C}_{10}\text{H}_{15}$ , further consecutive reactions might deplete the hydrogen atom concentration. In order to suppress these reactions the well known radical scavenger NO is added in two different concentrations:  $9.4 \times 10^{13}$  and  $3.25 \times 10^{15}$  molecules  $\text{cm}^{-3}$ . At the highest concentration another correction for H-atom concentration must be applied in view of the termolecular loss process  $\text{H} + \text{NO} + \text{He} \rightarrow \text{HNO} + \text{He}$ . Taking a rate constant of  $4.3 \times 10^{-32}$   $\text{cm}^6$  molecules $^{-2}$  s $^{-1}$  for this reaction [13], one arrives at an additional H-atom decay of 9.1 s $^{-1}$ . Depending on the reactor wall conditions an overall H-atom loss in the kinetic zone between 13 and 31 ms of 20 to 35% must be taken into account.

While the uncertainties in reactor pressure, flow velocity, and temperature lead to an uncertainty of 5% at the most, an overall uncertainty of 30% on the average H-atom concentration seems reasonable.

As an example the natural logarithm of the  $\alpha$ -pinene concentration as a function of the reaction time is shown at 1 and 2 torr, respectively (Fig. 3 and Fig. 4). The slopes of these straight lines directly yield  $k_{\text{obs}} = k_1 [\text{H}]$  (Table I).

When  $k_{\text{obs}}$  is plotted as a function of the hydrogen atom concentration a reasonably good straight line is obtained (Fig. 5). As can be seen from the 2 torr data, the large excess of NO in Experiment 2 does not have a systematic effect on the observed decay constants  $k_{\text{obs}}$ . This is a strong indication that secondary reactions leading to an additional depletion of  $\alpha$ -pinene are unimportant.

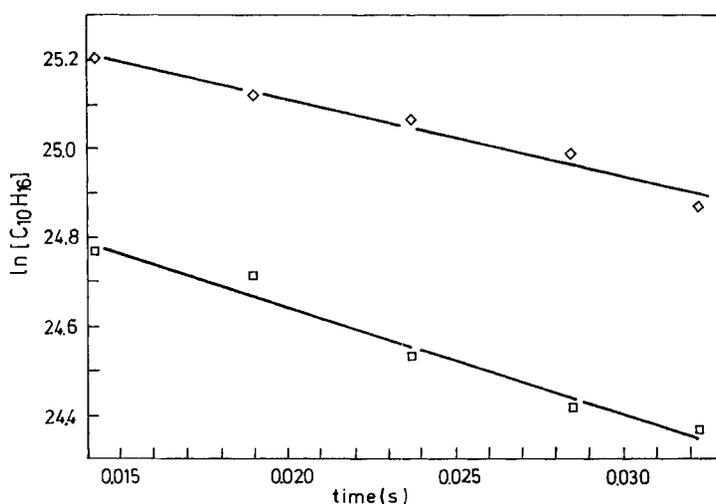


Figure 3. Natural logarithm of the  $\alpha$ -pinene concentration as a function of the reaction time. Reactor pressure  $P_r = 1$  torr, hydrogen atom concentrations are: ( $\diamond$ )  $[\text{H}] = 1.59 \times 10^{13}$  atoms  $\text{cm}^{-3}$  and ( $\square$ )  $[\text{H}] = 2.13 \times 10^{13}$  atoms  $\text{cm}^{-3}$ . The NO concentration is  $9.4 \times 10^{13}$  molecules  $\text{cm}^{-3}$ .

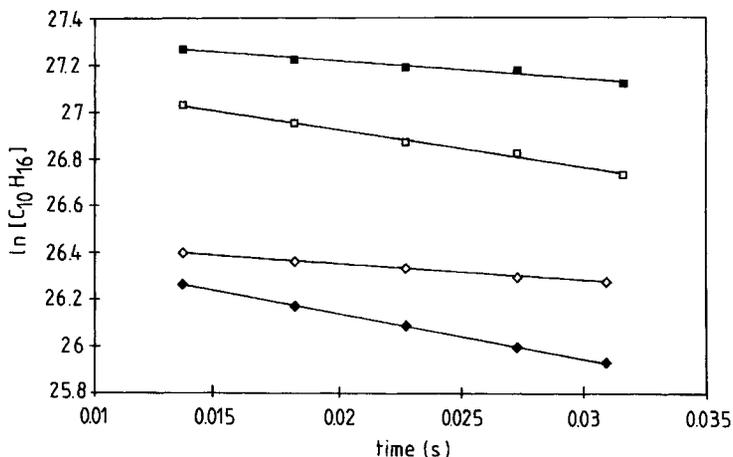


Figure 4. Natural logarithm of the  $\alpha$ -pinene concentration as a function of the reaction time. Reactor pressure  $P_r = 2$  torr, hydrogen concentrations are: (■)  $[H] = 0.60 \times 10^{13}$  atoms  $\text{cm}^{-3}$ ; (□)  $[H] = 1.65 \times 10^{13}$  atoms  $\text{cm}^{-3}$ ; (◇)  $[H] = 0.51 \times 10^{13}$  atoms  $\text{cm}^{-3}$ ; and (◆)  $[H] = 1.81 \times 10^{13}$  atoms  $\text{cm}^{-3}$ .

NO-concentrations are: (■, □)  $3.25 \times 10^{15}$  molecules  $\text{cm}^{-3}$  and (◇, ◆)  $9.4 \times 10^{13}$  molecules  $\text{cm}^{-3}$ .

A weighted linear regression on both the 1 and 2 torr data using SAS statistical [14] package yields the slope  $k_1 = (9.8 \pm 3.3) \times 10^{-13} \text{ cm}^3 \text{ molecules}^{-1} \text{ s}^{-1}$ . The intercept is equal to  $(0.4 \pm 0.8) \text{ s}^{-1}$  which indicates that heterogeneous wall reactions are unimportant. In addition since no pressure effect on the value of  $k_1$  was observed, the rate constant has already reached its high pressure limit.

While this is the first determination of the rate constant of the  $\alpha$ -pinene with atomic hydrogen, its value can only be compared though with the rate constants of other olefins/hydrogen atom addition reactions [7,15–17]. Olefins with a number of carbon atoms  $\geq 3$  with one double bond have a rate constant for hydrogen atom addition in the range of  $0.6$  to  $1.5 \times 10^{-12} \text{ cm}^3 \text{ molecules}^{-1} \text{ s}^{-1}$ . One sees that  $k_1$  falls neatly within this range.

#### Formation of Pinane $\text{C}_{10}\text{H}_{18}$

As said in the introduction, a detailed product analysis was not carried out in view of the complexity of the fragmentation spectra. Only the presence of pinane has been checked. With an initial concentration of  $[\alpha - \text{C}_{10}\text{H}_{16}] = 7 \times 10^{12} \text{ molecules cm}^{-3}$ ,  $[H] = 8.4 \times 10^{13} \text{ atoms cm}^{-3}$  and a reaction time of about 30 ms, pinane could be identified beyond doubt. It shows two major ion fragments at  $m/e = 55$  and 95. If the same sensitivity for pinane is assumed as for  $\alpha$ -pinene and the ion intensities at the various fragments are summed up, one can estimate that the conversion yield of  $\alpha$ -pinene to pinane was at least 50%. In view of the complex reaction mechanism involving a competition between stabilization and decomposition processes, it is known that the product distribution is a function of initial  $[\text{Hydrocarbon}]/[H]$  ratio [6,7]. The relatively high yield of pinane observed is in agreement with the results obtained for the cyclohexene and cyclopentene / atomic hydrogen reaction where the respective

TABLE I. The pseudo-first-order decay constants  $k_{\text{obs}} = k_1 [\text{H}]$  of the  $\alpha$ -pinene + H reaction as a function of the hydrogen atom concentration at 1 and 2 torr total pressure. The carrier gas is helium. The NO-concentrations are as follows: Experiments 1 and 3:  $9.4 \times 10^{13}$  molecules  $\text{cm}^{-3}$  and Experiment 2:  $3.25 \times 10^{15}$  molecules  $\text{cm}^{-3}$ .

Experiment 1		Experiment 2	
$k_{\text{obs}}$ (1 torr) ( $\text{s}^{-1}$ )	[H] ( $10^{13}$ atoms $\text{cm}^{-3}$ )	$k_{\text{obs}}$ (2 torr) ( $\text{s}^{-1}$ )	[H] ( $10^{13}$ atoms $\text{cm}^{-3}$ )
$8.4 \pm 0.8$	0.65	$5.3 \pm 0.4$	0.44
$9.2 \pm 1.1$	0.86	$6.7 \pm 0.9$	0.60
$11.8 \pm 1.9$	1.05	$8.8 \pm 1.4$	0.94
$14.2 \pm 1.2$	1.40	$15.0 \pm 1.1$	1.30
$17.2 \pm 1.9$	1.59	$15.7 \pm 1.1$	1.65
$22.6 \pm 1.4$	1.77	$23.0 \pm 1.7$	1.85
$23.3 \pm 1.3$	1.98		
$24.4 \pm 2.3$	2.13		

Experiment 3	
$k_{\text{obs}}$ (2 torr) ( $\text{s}^{-1}$ )	[H] ( $10^{13}$ atoms $\text{cm}^{-3}$ )
$7.0 \pm 0.1$	0.51
$10.5 \pm 0.1$	1.1
$12.6 \pm 0.09$	1.5
$17.2 \pm 0.4$	1.6
$19.4 \pm 0.2$	1.8
$21.1 \pm 0.5$	2.1
$21.1 \pm 0.6$	2.3
$25.6 \pm 0.5$	2.6
$27.7 \pm 0.7$	3.1
$33.1 \pm 0.1$	3.2
$34.4 \pm 0.6$	3.8

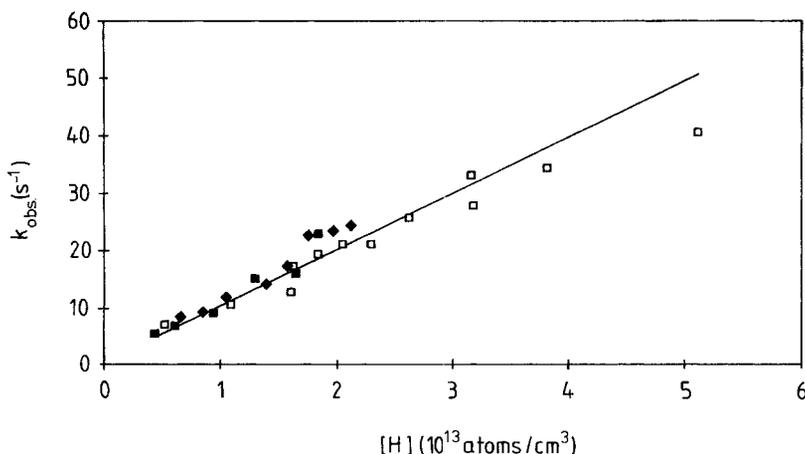


Figure 5. The observed first-order rate constant  $k_{\text{obs}} = k_1 [\text{H}]$  of the  $\alpha$ -pinene + H reaction as a function of the hydrogen atom concentration: ( $\blacklozenge$ )  $P_r = 1$  torr,  $[\text{NO}] = 9.4 \times 10^{13}$  molecules  $\text{cm}^{-3}$ ; ( $\square$ )  $P_r = 2$  torr,  $[\text{NO}] = 9.4 \times 10^{13}$  molecules  $\text{cm}^{-3}$ ; and ( $\blacksquare$ )  $P_r = 2$  torr,  $[\text{NO}] = 3.2 \times 10^{15}$  molecules  $\text{cm}^{-3}$ .

products cyclohexane and cyclopentane were found to be by far the major reaction products [6]. Stabilization of the  $C_{10}H_{17}^*$ -adduct formed is more important than its decomposition. Addition of nitric oxide in a concentration of  $1.1 \times 10^{15}$  molecules  $cm^{-3}$  completely suppressed the pinane formation. Taking into account that the  $[NO]/[H]$  ratio is then of the order of 14, one can estimate that the rate constant for the NO-addition to the  $C_{10}H_{17}$  radical is at least a factor of 0.1 times the rate constant of the hydrogen atom addition reaction.

When the magnitude of  $k_1$  is compared with the rate constant of the  $\alpha$ -pinene + OH reaction [18] which is of the order of  $5 \times 10^{-11}$   $cm^3$  molecules $^{-1}$  s $^{-1}$  one sees the latter being a factor of about 50 larger than  $k_1$ . Possible interferences of hydrogen atom reactions on the primary removal of  $\alpha$ -pinene with OH-radicals in flow tube studies may indeed completely be neglected taking into account that the initial  $[OH]/[H]$  ratio is at least  $\geq 10$ .

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