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(Eingegangen am 20. Oktober 1982) E 5313

## Kinetics of the Hydrogen Abstraction from Hydrogen Cyanide by Trifluoromethyl Radicals

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### Freie Radikale / Gase / Reaktionskinetik

The reaction of  $\text{CF}_3$  radicals with HCN in the gas phase has been studied in the temperature range 573–673 K using  $\text{CF}_3$  radicals generated by thermal decomposition of  $\text{CF}_3\text{I}$ . Arrhenius parameters for the reaction:



relative to  $\text{CF}_3$  recombination:



are given by:

$$\log [(k_1/k_c^{1/2})/\text{cm}^{3/2} \text{mol}^{-1/2} \text{s}^{-1/2}] = 5.50 (\pm 0.26) - 57.65 (\pm 3.14) \text{ kJ mol}^{-1}/4.576 T.$$

Rate parameters are compared with those for other reactions of  $\text{CF}_3$  with polar and non-polar substrates.

### Introduction

A considerable amount of data has been accumulated over the years concerning reactions of  $\text{CF}_3$  radicals. However, very few quantitative kinetic data are available on reactions of atoms or radicals with cyano-compounds [1–3]. The reactions of  $\text{CF}_3$  [4] and  $\text{C}_2\text{F}_5$  [5] with  $\text{ClCN}$  have been studied in this laboratory, with abstraction of chlorine atom taking place at the highest temperatures of the covered range. On account of this and our interest in expanding our knowledge on reactions of this type of substrates, we undertook the present work.

### Experimental

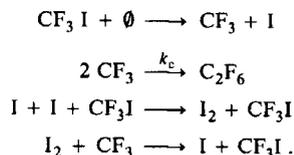
Trifluoromethyl iodide from a cylinder (PCR Research Chemicals) was twice distilled at 143 K under vacuum and a middle cut retained. Hydrogen cyanide was prepared by dropwise addition of  $\text{H}_2\text{SO}_4$  to  $\text{KCN}$  free from carbonate. The gas evolved was frozen in a liquid air trap and was purified by vacuum distillation at low temperature. In some cases, it was further purified by gas chromatography using a 3.0 m column of Triacetin at room temperature. Nitrogen (99.99%) was used without further purification. Perfluorocyclobutane (Pierce Chemical Company) was bulb to bulb distilled from 213 K to 77 K.

Reactants were stored and measured out in a mercury-free and grease-free static vacuum system. Mixtures of  $\text{CF}_3\text{I}$  and HCN were heated in a cylindrical quartz reaction vessel, volume  $109 \text{ cm}^3$ , located in a horizontal electric metal block furnace. Temperature was controlled to  $\pm 0.3^\circ\text{C}$  by a Lauda Electronic regulator type PTR 50 and was uniform in both space and time to within  $\pm 1^\circ\text{C}$ . The temperature was measured with a chromel-alumel thermocouple.

At the end of each experiment, the total content of the cell was frozen out and analyzed by gas chromatography using a Varian 200 chromatograph equipped with a Gow Mac density balance detector. Products were separated on a 2.4 m column packed with silica gel. Retention times were compared with authentic samples run under identical conditions. Qualitative identification of the products was achieved by infrared and mass spectrometry.

### Results

The thermal decomposition of trifluoromethyl iodide,  $\text{CF}_3\text{I}$ , seems to be a convenient way of generating  $\text{CF}_3$  radicals [6], the relevant reactions being:



When  $\text{CF}_3$  radicals are caused to react with HCN,  $\text{CF}_3\text{H}$ ,  $\text{C}_2\text{F}_6$ ,  $\text{CF}_3\text{CN}$  and  $\text{I}_2$  are obtained as products.

Runs were carried out over the temperature range 573–673 K. The rate of formation of  $\text{CF}_3\text{H}$  relative to  $\text{C}_2\text{F}_6$  was measured for different pressures of HCN at any given temperature. In most of our experiments, not more than 2% of the HCN was consumed (calculated from the yield of  $\text{CF}_3\text{H}$ ). Results for the complete temperature range are shown in Table 1.

Addition of inert gases such as  $\text{N}_2$  and  $\text{c-C}_4\text{F}_8$  did not substantially modify the ratio  $R_{\text{CF}_3\text{H}}/R_{\text{C}_2\text{F}_6}^{1/2} [\text{HCN}]$ .

Table 1  
Results for  $\text{CF}_3$  radical-HCN reaction<sup>a)</sup>

| T/K | time/s | reactant pressure/Torr |      |       | $R_{\text{CF}_3\text{H}}$ | $R_{\text{C}_2\text{F}_6}$ | $R_{\text{CF}_3\text{CN}}$ | $R_{\text{CF}_3\text{H}}/R_{\text{C}_2\text{F}_6}^{1/2} [\text{HCN}]^b)$ |
|-----|--------|------------------------|------|-------|---------------------------|----------------------------|----------------------------|--|
|     |        | $\text{CF}_3\text{I}$  | HCN  |       |                           |                            |                            |  |
| 573 | 21600  | 104.0                  | 15.6 | 0.308 | 0.116                     | 0.213                      | 2.08                       |  |
| 573 | 21600  | 101.4                  | 30.7 | 0.491 | 0.105                     | 0.335                      | 1.77                       |  |
| 573 | 21600  | 102.6                  | 25.4 | 0.463 | 0.113                     | 0.312                      | 1.96                       |  |
| 573 | 19800  | 102.4                  | 15.6 | 0.301 | 0.128                     | 0.186                      | 1.94                       |  |
| 573 | 28800  | 100.8                  | 20.7 | 0.356 | 0.0944                    | 0.249                      | 2.02                       |  |
| 593 | 14460  | 49.1                   | 20.0 | 0.620 | 0.165                     | 0.308                      | 2.85                       |  |
| 593 | 14400  | 49.0                   | 30.5 | 0.795 | 0.163                     | 0.457                      | 2.41                       |  |
| 593 | 10800  | 101.7                  | 33.5 | 1.46  | 0.414                     | 0.932                      | 2.54                       |  |
| 593 | 14400  | 52.9                   | 23.6 | 0.697 | 0.203                     | 0.384                      | 2.44                       |  |
| 593 | 10800  | 101.7                  | 14.9 | 0.743 | 0.511                     | 0.503                      | 2.61                       |  |
| 613 | 7200   | 30.0                   | 10.5 | 0.875 | 0.423                     | 0.405                      | 4.95                       |  |
| 613 | 7200   | 33.0                   | 20.6 | 1.42  | 0.465                     | 0.630                      | 3.89                       |  |
| 613 | 7200   | 50.2                   | 40.8 | 2.79  | 0.622                     | 1.58                       | 3.34                       |  |
| 613 | 7200   | 30.0                   | 30.0 | 1.75  | 0.366                     | 0.746                      | 3.70                       |  |
| 613 | 7200   | 25.6                   | 40.0 | 2.04  | 0.317                     | 0.866                      | 3.48                       |  |
| 633 | 3600   | 29.4                   | 30.0 | 4.53  | 1.26                      | 2.42                       | 5.37                       |  |
| 633 | 3600   | 52.1                   | 40.6 | 7.61  | 2.02                      | 4.78                       | 5.28                       |  |
| 633 | 3600   | 30.1                   | 11.3 | 2.21  | 1.71                      | 1.33                       | 5.98                       |  |
| 633 | 3000   | 25.5                   | 35.0 | 5.04  | 1.12                      | 2.65                       | 5.42                       |  |
| 633 | 1800   | 32.0                   | 17.3 | 4.02  | 2.31                      |                            | 6.08                       |  |
| 633 | 2400   | 30.2                   | 23.3 | 4.63  | 1.76                      |                            | 5.96                       |  |
| 653 | 1200   | 27.8                   | 29.0 | 11.5  | 5.15                      | 5.64                       | 7.20                       |  |
| 653 | 1200   | 26.8                   | 24.1 | 9.07  | 5.47                      | 4.97                       | 6.60                       |  |
| 653 | 600    | 30.3                   | 15.2 | 9.53  | 9.49                      | 4.15                       | 8.36                       |  |
| 653 | 600    | 28.5                   | 14.6 | 6.62  | 8.33                      | 3.37                       | 6.43                       |  |
| 653 | 600    | 29.8                   | 20.0 | 11.4  | 9.21                      |                            | 7.68                       |  |
| 653 | 1200   | 26.6                   | 39.5 | 15.5  | 5.20                      | 8.20                       | 7.09                       |  |
| 653 | 720    | 30.6                   | 10.0 | 6.18  | 8.72                      | 3.35                       | 8.59                       |  |
| 653 | 1200   | 28.8                   | 38.1 | 10.0  | 2.59                      | 3.89                       | 6.68 <sup>c)</sup>         |  |
| 653 | 1200   | 26.9                   | 40.3 | 10.8  | 2.09                      |                            | 7.62 <sup>d)</sup>         |  |
| 653 | 1200   | 25.7                   | 40.5 | 8.56  | 1.48                      |                            | 7.11 <sup>e)</sup>         |  |
| 673 | 300    | 31.3                   | 15.8 | 19.4  | 24.8                      | 8.37                       | 10.4                       |  |
| 673 | 300    | 29.2                   | 15.4 | 21.7  | 27.2                      | 8.43                       | 11.5                       |  |
| 673 | 300    | 30.6                   | 19.5 | 25.4  | 29.2                      | 10.4                       | 10.2                       |  |
| 673 | 300    | 31.3                   | 33.5 | 45.0  | 25.5                      | 21.3                       | 11.3                       |  |
| 673 | 300    | 31.7                   | 24.4 | 35.7  | 27.1                      | 16.4                       | 11.9                       |  |
| 673 | 300    | 29.1                   | 33.5 | 42.1  | 24.1                      | 16.6                       | 10.8                       |  |

a) The volume of reaction vessel was 109 cm<sup>3</sup>. Rates of formation of products,  $R$ , in units of  $10^{-12}$  mol cm<sup>-3</sup> s<sup>-1</sup>; — b) Units of cm<sup>3/2</sup> mol<sup>-1/2</sup> s<sup>-1/2</sup>; — c) With the addition of 256 Torr of N<sub>2</sub>; — d) 260 Torr of *c*-C<sub>4</sub>F<sub>8</sub>; — e) 260 Torr of *c*-C<sub>4</sub>F<sub>8</sub>.

At selected temperatures, several runs were done using, at each temperature, approximately constant pressures of  $\text{CF}_3\text{I}$  and HCN but with various reaction times. In these experiments the ratio  $R_{\text{CF}_3\text{H}}/R_{\text{C}_2\text{F}_6}^{1/2} [\text{HCN}]$  was not constant. The results of these studies of time dependence, given in Fig. 1 show that as the temperature increases the slope of

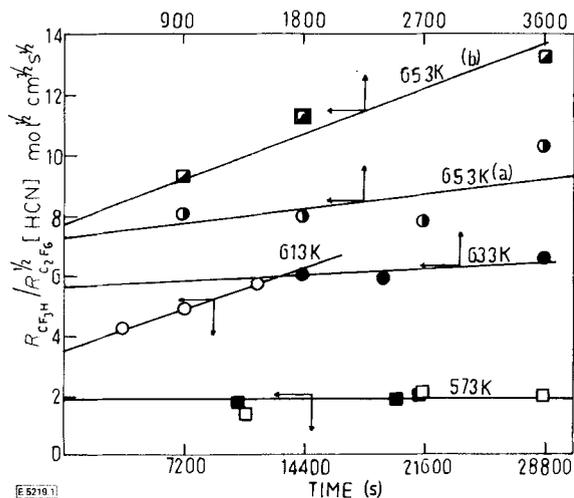


Fig. 1

Plot of  $R_{\text{CF}_3\text{H}}/R_{\text{C}_2\text{F}_6}^{1/2} [\text{HCN}]$  versus time at different temperatures. (●): With 32 Torr of  $\text{CF}_3\text{I}$  — (a); (■): With 50 Torr of  $\text{CF}_3\text{I}$  — (b); (□): With 20 Torr of HCN; (■): With 15 Torr of HCN

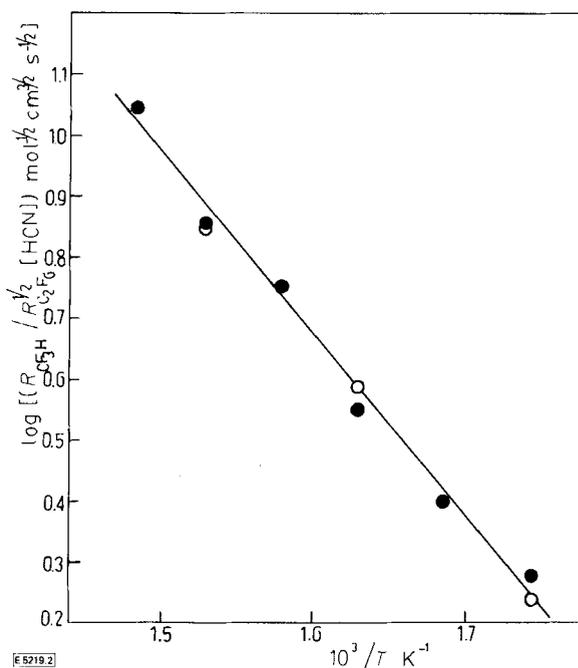


Fig. 2

Arrhenius plot for reaction of  $\text{CF}_3$  radicals with HCN. (○): Results obtained from rates of formation of products at zero time

the ratio  $R_{CF_3H}/R_{C_2F_6}^{1/2} [HCN]$  versus time increases. Moreover at 653 K for different pressures of  $CF_3I$ , the slope is greater for a larger concentration of  $CF_3I$ ; the intercepts being approximately the same within experimental error.

The temperature dependence of the ratio  $R_{CF_3H}/R_{C_2F_6}^{1/2} [HCN]$  taking the results of Table 1 is a good straight line (Fig. 2) which corresponds to the following expression calculated by the least squares method:

$$\log [(R_{CF_3H}/R_{C_2F_6}^{1/2} [HCN])/ \text{cm}^{3/2} \text{mol}^{-1/2} \text{s}^{-1/2}] = 5.50 (\pm 0.26) - 57.65 (\pm 3.14) \text{kJ mol}^{-1}/4.576 T. \quad (1)$$

Error limits are standard deviations. In this figure we have included results obtained from rates of formation of products at zero time calculated from the slopes of the plots of concentration of products versus time. These data, however, were not used in deriving the result in Eq. (1); they were only meant as evidence that the above Arrhenius parameters are reliable up to 2% conversion.

### Discussion

Possible reactions of the  $CF_3$  radicals generated by thermal decomposition of  $CF_3I$  are:



If these reactions are the sole sources of  $CF_3H$  and  $C_2F_6$ , respectively, then the following rate relation is obtained:

$$R_{CF_3H}/R_{C_2F_6}^{1/2} [HCN] = k_1/k_c^{1/2}$$

where  $R$  denotes rate of formation,  $[HCN]$  is the mean substrate concentration and  $k_1$  and  $k_c$  are the rate constants for reactions (1) and (2) respectively.

Results given in Table 1 can be interpreted in terms of these reactions, thus a plot of  $R_{CF_3H}/R_{C_2F_6}^{1/2}$  versus  $[HCN]$  at each temperature is a straight line of zero intercept and slope  $k_1/k_c^{1/2}$ . At higher conversions, however, there is an additional source of  $CF_3H$  other than the abstraction reaction itself. The fact that the slopes of the time-dependence plot increase with temperature and that for a given temperature and two different concentrations of  $CF_3I$  the slope of  $k_1/k_c^{1/2}$  versus time is larger for the larger concentration suggests that the "extra"  $CF_3H$  may arise from a reaction in which iodine and/or the iodine atom are involved. Despite the fact that we were unable to find any iodine containing products under our present analysis conditions, we think that feasible reactions leading to  $CF_3H$  formation could be:



and/or:



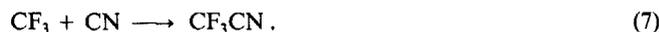
The occurrence of reactions (3) and (5) would be supported by the dependence of  $k_1/k_c^{1/2}$  with time since  $IHCN$  would accumulate as reaction proceeds. Amphlett and Whittle [7] have found that reaction (6) is very fast and have assigned  $2.1 \text{kJ mol}^{-1}$  to its activation energy.

In an attempt to provide evidence regarding the reaction between iodine and HCN, approximately 35 Torr of HCN and bisublimated iodine were heated at 673 K for about 1 hour.  $C_2N_2$  was identified by gas chromatography.

The occurrence of the above processes does not seem improbable in view of previous work on the addition of iodine to unsaturated compounds such as acetylene [8]. Walton and coworkers [9] have studied the addition of  $CF_3$  radicals to fluorosubstituted olefins and have included in their mechanism a reversible addition of iodine to the olefin.

When the reaction was carried out under ultra-violet irradiation at 573 K, the conversion effect was remarkably enhanced. The presence of a silver vane which produces fixation of iodine as silver iodide or a filter to prevent light absorption by  $I_2$  minimizes this conversion effect. Although these facts are not as yet fully understood, further experiments are being performed and results will be reported. Notwithstanding, we conclude that iodine plays an important part in this system and we stress that at his stage no further attempts were made to clarify the mechanism through which the formation of additional  $CF_3H$  may be explained. Use of an alternative source of radicals lacking iodine will probably provide definite evidence.

$CF_3CN$  formation can be explained by the following reaction:



If all the CN radicals formed in reaction (1) are trapped by  $CF_3$ , then the ratio  $R_{CF_3CN}/R_{CF_3H}$  should be equal to one. Our data show, however, that the ratio is always less than unity and approximately constant in this temperature range. We interpret this by assuming that CN radicals are being removed by self-combination or by reaction with HCN [10] as follows:



These reactions could also account for the observed conversion effect on  $k_1/k_c^{1/2}$ . We were unable to detect  $C_2N_2$  in this case due to interference from a large excess of unreacted  $CF_3I$  when products were analyzed on a chromatographic column.

Table 2  
Arrhenius parameters for some reactions of  $CF_3$  radicals  
 $CF_3 + RH \rightarrow CF_3H + R$

| Substrate | $\log (A_1/\text{cm}^3 \text{mol}^{-1} \text{s}^{-1})$ | $E_1/\text{kJ mol}^{-1}$ | Ref.      |
|-----------|--|--------------------------|-----------|
| HCl       | 11.23  | 21.3                     | [12]      |
|           | 11.38  | 22.5                     | [13]      |
|           | 11.44  | 23.0                     | [14]      |
| $H_2S$    | 11.65  | 16.2                     | [15]      |
|           | 11.81  | 17.5                     | [13]      |
|           | 11.20  | 5.0                      | [16]      |
| $H_2$     | 12.45  | 44.6                     | [17]      |
|           | 13.40  | 51.5                     | [14]      |
| $CH_4$    | 12.61  | 52.3                     | [18]      |
|           | 12.08  | 46.8                     | [19]      |
| HCN       | 12.19  | 57.7                     | this work |

In Table 2, we compare our Arrhenius parameters  $A_1$  and  $E_1$  for attack of  $CF_3$  on HCN with published data of other reactions of  $CF_3$  with polar and non-polar substrates. The absolute  $A_1$ , and  $E_1$  were all obtained assuming that, for  $CF_3$  combination,  $E_c = 0$  and  $\log A_c = 13.36$  (Ref. [11]).

Table 2 shows that our values of  $A_1$  and  $E_1$  are closer to those for a non-polar molecule which would probably seem unexpected.

ed if we think of CN as having a behaviour similar to that of a halogen atom. The polar effect is therefore off-set by the energetics factor which appears to be the driving force in this case. The H–C bond in HCN is anomalously high compared to the same bond in CF<sub>3</sub>H and this would account for the low reactivity of HCN towards CF<sub>3</sub> attack.

The heat of formation of CN has been the subject of a great deal of research effort and a considerable amount of data has been accumulated over the years ranging from 372 to 456 kJ mol<sup>-1</sup> [20]. These values lead to  $D(\text{H}-\text{CN})$  between 455 and 539 kJ mol<sup>-1</sup>. Taking 502 kJ mol<sup>-1</sup>, in accordance with the latest determinations, reaction (1) would be endothermic in 58 kJ mol<sup>-1</sup>, which allows us to set a lower limit for the activation energy of the abstraction reaction. Our value of  $E_1 = 57.7$  kJ mol<sup>-1</sup> corresponds to this limit within experimental error.

Unfortunately, we are not aware of the existence of any quantitative studies of endothermic hydrogen abstraction reactions by CF<sub>3</sub> radicals except for the work of Whittle and coworkers [21] on the hydrogen transfer from benzene. This prevents us from drawing any conclusion as to the relationship between endothermicity and activation energy any further than we have stated above. A determination of kinetic parameters of the reaction of CN radicals with CF<sub>3</sub>H would be helpful to settle the question.

$A_1$  was also calculated from the evaluation of  $\Delta S_1^\ddagger$  by the method of Benson [22]. A linear configuration, CF<sub>3</sub>...H...C≡N, was assumed for the activated complex. A value of  $A_1 = 1.21 \cdot 10^{11}$  cm<sup>3</sup> mol<sup>-1</sup> s<sup>-1</sup> was obtained; which agrees with the experimental value within the error limits of this method and bearing in mind that the method provides a lower limit for the pre-exponential factor.

The authors thank CONICET (Argentina) for partial financial support through Programa de Investigación Fisicoquímica.

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(Eingegangen am 18. Juni 1982, E 5219  
endgültige Fassung am 8. November 1982)

## Theory of Thermal Unimolecular Reactions in the Fall-off Range. I. Strong Collision Rate Constants

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### Reaktionskinetik

( $k_0/k_\infty$ )-reduced strong collision fall-off curves of thermal unimolecular reactions are analyzed. They are represented by the Lindemann-Hinshelwood expression multiplied by strong collision broadening factors  $F^{\text{SC}}$ . The factors  $F^{\text{SC}}$  are approximated by fully empirical representations of RRKM theory. Compact expressions suitable for modeling are proposed. Their quality is demonstrated by comparison with exact RRKM calculations for 20 molecular systems.

### 1. Introduction

Thermal unimolecular reactions, as well as the related radical recombination reactions, play an important role in many complex reaction systems such as atmospheric chemical kinetics

or combustion. A major practical problem of these reactions is their complicated pressure and temperature dependence which makes modeling a difficult task. Often these reactions are treated as simple first or second order processes. Sometimes,