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1. Introduction

Many volatile organic compounds (VOCs), emitted from the combustion of fuels, biomass and waste, smoking, solvent use, and the surfaces of carpets, PVC flooring, adhesive products, coating mediums for furniture, and room decorations, have been regulated due to their human toxicity.^{1,2} In particular, even low-dose exposure to carcinogenic benzene and chlorinated VOCs is strongly associated with acute non-lymphocytic leukemia, aplastic anemia and chromosomal aberrations.³ The inhalation of toluene, which is one of the most commonly found VOCs, can lead to nervous system complications, such as reduction in thinking, memory and muscular abilities, as well as some level of loss in both hearing and color vision.⁴ Despite the availability of many treatment technologies, including absorption, condensation, incineration, biological oxidative filtering, and thermal plasma treatment for VOC removal, most

Advanced removal of toluene in aerosol by adsorption and photocatalytic degradation of silver-doped TiO₂/PU under visible light irradiation[†]

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We synthesized a novel Ag–TiO₂/PU material for the effective removal of gaseous toluene by both adsorption and photocatalytic degradation. The Ag particles, which were distributed on the TiO₂ surface, and the Ag dopants, which were incorporated into the TiO₂ lattice, increased the electron–hole pair separation efficiency of TiO₂. Therefore, Ag–TiO₂/PU exhibited high photocatalytic degradation of toluene even under visible light. Porous polyurethane (PU) was used to immobilize the enhanced TiO₂, to increase the adsorption capacity of the photocatalyst. The synthesized Ag–TiO₂/PU removed gaseous toluene even under dark conditions *via* adsorption. The removal of gaseous toluene by Ag–TiO₂/PU under visible light conditions was due to the combination of both adsorption and photocatalytic degradation. The oxygen content in the gas stream insignificantly affected the toluene adsorption by the Ag–TiO₂/PU. However, the photocatalytic degradation of toluene by Ag–TiO₂/PU increased with increasing oxygen content and stabilized when the oxygen content exceeded 15%. These results suggest that ambient air can be used economically as an oxygen source for the photocatalytic degradation of gaseous toluene by Ag–TiO₂/PU under visible light irradiation, 6% Ag–TiO₂/PU, which was the Ag/TiO₂ ratio that optimized the photocatalytic degradation activity of TiO₂, removed 85.2% of the toluene in 100 ppm inlet gas, of which 90.3% was mineralized into CO₂ and H₂O.

have been considered for industrial applications requiring complicated disposal techniques, high costs and skilled labor.⁵ Recently, applications for the photocatalytic degradation and removal of gaseous toluene have become a very attractive and promising alternative.^{6,7} Under or near UV irradiation, TiO₂ photocatalyst can photocatalytically degrade toluene into carbon dioxide, water and simple mineral acids.⁸ Compared to conventional treatment methods, the use of photocatalysis for toluene removal exhibited several advantages such as low cost and simplicity.⁹ However, the photocatalytic degradation of toluene by TiO₂ photocatalysis is a relative slow process with many limitations for industrial or large-scale application, along with safety issues and high-energy consumption due to UV or near UV irradiation.¹⁰

To overcome these disadvantages, numerous studies have investigated enhancing the photocatalytic activity of TiO₂ and expanding the photocatalytic applications in practical systems using visible or solar irradiation to initiate the photocatalysis.¹¹⁻¹⁵ Ag has been used as a doping or sensitivity agent to enhance the photocatalytic activity of TiO₂ due to silver's ability to act as both an electron sink and donor to increase the electron–hole pair separation efficiency of TiO₂ and thereby enhance its photocatalytic activity.¹⁶ Due to silver's antibacterial activity, the Ag-doped TiO₂ photocatalyst has been mostly used

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as a disinfection material.^{17–20} A few studies have utilized the synthesized Ag-doped TiO_2 to remove other pollutants, particularly, for removal of toluene gas.^{21–23} Thus, the present study firstly aimed to use Ag as a doping agent for enhancing the photocatalytic activity of TiO_2 when applied to the removal of gaseous toluene.

The photocatalytic activity and degradation efficiency, in particular, the degradation of pollutants in gas phase, are strongly dependent on the adsorption capacity of the photocatalyst.²⁴ Thus, the second aim of the present study was to immobilize TiO_2 and Ag-doped TiO_2 photocatalyst on a polyurethane (PU) substrate, a porous material. We hypothesize that the immobilization and doping would increase the adsorption ability of the photocatalyst for the removal of gaseous toluene. The increased adsorption ability would also increased the degradation rate and hence the toluene removal in aerosol by both adsorption and photocatalytic degradation.

In addition, the photocatalytic degradation processes in aerosol are strongly dependent on the reactions of photogenerated electrons and holes with oxygen and H_2O molecules to produce superoxide radicals (* O_2^-)and hydroxyl radicals (*OH), respectively.²⁵ Thus, the moisture and oxygen contents are the key factors affecting the photocatalytic degradation of aerosol pollutants. Several studies have investigated the effects of moisture content on the photocatalytic degradation in aerosol, but without focusing on the effects of oxygen on the degradation.²⁵⁻²⁹ Therefore, the third aim of the present study was to investigate the effects of oxygen content on the photocatalytic degradation of toluene in aerosol using Ag–TiO₂/PU under visible light conditions.

2. Materials and methods

2.1. Synthesis of Ag-TiO₂/PU

Before being used as a substrate to immobilize Ag-doped TiO₂, pristine PU was pre-treated by a mixed solution of toluene, toluene-2,4-diisocyanate, and anhydrous triethylamine to introduce isocyanate groups (NCO) onto its surface.¹⁷ The isocyanated PU was immersed into a solution of amino titanosiloxane, containing a Si–O–Ti bonds and an amine group (NH₂), which was prepared based on reaction between titanium tetraisopropoxide with γ -aminopropyl triethoxysilane. During the immersing process, the titanosiloxane was immobilized on PU

Flow rate meter

by reactions between the isocyanate groups of the isocyanated PU and the amino group (NH_2) of the amino titanosiloxane.¹⁷ After 1 h immersing, the PU immobilized titanosiloxane was taken out and a 0.1 M AgNO₃ solution, which was prepared by the dissolution of AgNO₃ in deionized water at 60 °C, was slowly added (drop-wise) onto the titanosiloxane immobilized on PU. The obtained material was cleaned using 1 M oxalic acid solution, irradiated with a UV light (60 W) for 5 h and calcined under nitrogen at 200 °C for 5 h to produce Ag-doped TiO₂ immobilized on PU (Ag-TiO₂/PU). The addition volume of AgNO₃ solution was adjusted in order to synthesize Ag-TiO₂/PU materials with Ag/TiO₂ ratios of 0, 2, 4, 6, 8 and 10 wt%.

2.2. Material characterization

X-ray photoelectron spectroscopy (XPS) spectra of the synthesized Ag-TiO₂/PU materials were obtained using a Thermo Fisher K-Alpha X-ray Photoelectron Spectrometer system. The Gaussian multi-peak shapes were applied to fit the Ag 3d_{5/2} and Ti $2p_{3/2}$ peaks in the obtained XPS spectra for determining the elemental state of the silver and titanium in Ag-TiO2/PU. A Bruker AXN model with a Cu-K α radiation ($\lambda = 1.5418$ Å) source was used to obtain X-ray diffraction (XRD) spectra of Ag-TiO₂/ PU. The surface morphology of the Ag-TiO₂/PU materials was analyzed using a Hitachi S-4700 scanning electron microscope (SEM). Before the SEM analysis, the Ag-TiO₂/PU samples were coated with Pt to increase the conductivity of the photocatalyst surface. The surface area (S_{BET}) of the synthesized Ag-TiO₂/PU materials was determined using the Brunauer-Emmett-Teller (BET) isotherm carried out by nitrogen adsorption and desorption at 77 K. The optical absorption ability of the Ag-TiO₂/PU materials in the wavelength range 300-700 nm was determined by an Evolution 300 spectrophotometer (UV-1700 Shimadzu).

2.3. Experimental apparatus

Fig. 1 shows the experimental apparatus for the continuous photocatalytic degradation and removal of gaseous toluene using Ag–TiO₂/PU. The experimental apparatus was composed of three main parts: gas generator, reaction chamber and analyzer system. The gas generator system included a mixer, a humidifier and three gas cylinders of 1000 ppm toluene in nitrogen gas, oxygen and nitrogen gases (Fig. 1). The mixer and humidifier were adjusted to control the toluene gas

Methanizer

Valve

C₇H₈ O₂ N₂ Keactor Light Source Course of Course

Fig. 1 The experimental apparatus for removal of gaseous toluene.

concentration and humidity level, respectively. The reaction chamber was composed of a dark cover cask ($25 \times 50 \times 50$ cm), two 20 W bulbs and a reactor. The bulbs were placed at the top and bottom of the reaction chamber (Fig. 1) to generate visible light in the range of 400-700 nm for the photocatalytic irradiation processes. The power density of the generated visible light in the reaction chamber was 0.05 W cm⁻². A reactor $(2 \times 4 \times 15)$ cm) was placed in the center of the reaction chamber. The top and bottom of the reactor were made of quartz to allow easy passage of the visible light generated from the light bulbs though the reactor wall. The online analyzer system included a Varian CP-3800 gas chromatograph (GC) equipped with a flame ionization detector and a packed column (Porapak Q 80/ 100 2 \times 2 mm) to analyze the concentration of the outlet toluene. A methanizer, using Ni catalyst, was integrated into the GC system to analyze the CO and CO₂ contents in the outlet gas.

2.4. Removal experiments

Flow rate meters were regulated to achieve a constant flow rate of 100 mL min⁻¹ of 100 ppm toluene in the gas mixture. The humidifier was used to ensure that the relative humidity of the gas mixture remained constant at 50%. Before the toluene removal experiments, the input gas was oriented through direction A to the GC system to re-check the concentration of the toluene in the gas mixture. When the toluene concentration in the 100 mL min⁻¹ flow of mixed gas was stabilized at 100 ppm, the input gas was oriented toward direction B where it passed through the reactor volume containing 36 cm³ of the synthesized Ag-TiO₂/PU porous material. The toluene removal experiments were carried out under conditions of both dark and visible light, achieved by turning the bulbs off/on, respectively, to determine the adsorption and photocatalytic degradation ability of the synthesized Ag-TiO₂/PU, respectively. After the removal experiments, the effluent gas was sent to the GC system using an auto sampling injector, which automatically injected 100 μ L of the effluent gas into the packed column in intervals of 10 min from the reaction start time ($t_0 = 0$). The reaction start time $(t_0 = 0)$ was estimated to be the time when the input gas was oriented flowing direction B. Helium was used as a carrier gas with a flow rate of 25 mL min⁻¹. The removal efficiency and mineralization degree of toluene by Ag-TiO₂/PU were evaluated using eqn (1) and (2), respectively:

Toluene removal efficiency
$$(\%) = \frac{C_0 - C_t}{C_0} \times 100\%$$
 (1)

Mineralization degree =
$$\frac{C_{tCO_2}}{7 \times (C_0 - C_t)} \times 100\%$$
 (2)

where C_0 (100 ppm) is the concentration of toluene at the reaction start time ($t_0 = 0$), and C_t and C_{tCO_2} are the concentrations of toluene and CO₂ at reaction time ($t_i = t$), respectively.

3. Results and discussion

3.1. Material properties

3.1.1. Elemental states of silver. The high-resolution XPS spectra of the synthesized Ag–TiO₂/PU indicated that the first

elemental state of silver was silver metallic (Ag⁰), with peaks at 374.2 and 368.2 eV (Fig. 2).³⁰ The obtained XRD results further confirmed the existence of Ag⁰ on the surface of Ag–TiO₂/PU (Fig. 3).³¹ The Ag⁰ was produced from the reduction of AgNO₃ under the effects of the UV irradiation and calcination temperature during the Ag–TiO₂/PU preparation processes.^{16,32} The UV irradiation and oxalic acid, rolled as a cleanser for the



Fig. 2 High-resolution XPS spectra of Ag in X% Ag-TiO₂/PU.



Fig. 3 XRD patterns of X% Ag-TiO₂/PU.

purification process, enhanced the reduction of AgNO₃ into Ag⁰.³³⁻³⁶ In Ag–TiO₂/PU, silver also existed in form of Ag⁺ corresponding to peaks at 373.4 and 367.4 eV in the obtained XPS spectra (Fig. 2).³⁷ However, the absence of any Ag₂O peak in the XRD spectra (Fig. 3) implied that most of the Ag⁺ ions had been incorporated into or anchored in the TiO₂ lattice *via* Ti–O–Ag bonds or that the concentration of Ag⁺ existing in form of Ag₂O was too low to be detected by the XRD analysis.^{21,32}

The Ag⁺/Ag⁰ ratios in Ag–TiO₂/PU, which are proportional to the ratios of (the area under the Ag⁺ peak)/(the area under the Ag⁰ peak) in the XPS spectra, are shown in Table 1. As the Ag/ TiO₂ ratio (controlled by increasing the added AgNO₃ volume) in Ag–TiO₂/PU was increased to 6 wt%, the Ag⁺/Ag⁰ ratio increased to a maximum of approximately 55.6%, but then slightly decreased with the further increase of the Ag/TiO₂ ratio above 6 wt%. It was because only a certain amount of Ag⁺ could be incorporated into or anchored in the TiO₂ lattice *via* Ti–O–Ag bonds. At the limitation of the incorporation, the additional Ag⁺ in the added AgNO₃ could not be further incorporated into the TiO₂ lattice, and was instead reduced into Ag⁰ and distributed on the surface of the TiO₂ layer. Thus, the Ag⁺/Ag⁰ ratio slightly decreased as the Ag/TiO₂ ratio was increased above 6 wt%.

Table 1 The ratios of Ag^0/Ag^+ and Ti^{3+}/Ti^{4+} and the BET surface area of the Ag-TiO₂/PU materials

	Ag ⁺ /Ag ⁰ ratios (%)	Ti ³⁺ /Ti ⁴⁺ ratios (%)	BET surface area (m² g ⁻¹)	
TiO ₂ /PU	_	0	110.9	
2% Ag-TiO ₂ /PU	42.4	15.5	129.2	
4% Ag-TiO ₂ /PU	48.8	19.7	155.7	
6% Ag-TiO ₂ /PU	55.6	22.6	186.6	
8% Ag-TiO ₂ /PU	54.3	23.4	176.3	
10% Ag-TiO ₂ /PU	53.1	24.2	148.1	

3.1.2. Elemental states of titanium. The obtained XPS results indicate that the elemental state of titanium in TiO₂/PU was only Ti⁴⁺, while the elemental states of titanium in the Ag-TiO₂/PU materials were both Ti⁴⁺ and Ti³⁺(Fig. 4).^{38,39} UV irradiation can reduce any Ti⁴⁺ on the TiO₂ surface to Ti³⁺.⁴⁰ However, the synthesized TiO₂/PU did not contain any Ti³⁺ ions, which indicates that the Ti³⁺ was formed due to the incorporation of silver into the TiO₂ lattice. Atla et al. reported that the incorporated Ag induced a change in the chemical state of TiO₂ leading to the reduction of Ti⁴⁺ into Ti³⁺.³² The incorporation of Ag also induced oxygen vacancies in the TiO₂ lattice, resulting in the reduction of Ti⁴⁺ to Ti³⁺.^{41,42} Table 1 shows the calculated Ti³⁺/Ti⁴⁺ ratios in the synthesized Ag-TiO₂/PU, which are proportional to the ratios of (the area under the Ti³⁺ peak)/(the area under the Ti⁴⁺ peak) in the obtained XPS spectra. The results indicate that the Ti³⁺ content in Ag-TiO₂/PU increased rapidly with increasing Ag/TiO₂ ratio, and gradually stabilized when the Ag/TiO₂ ratio rose above 6 wt%. The increase in Ti³⁺ content in Ag-TiO₂/PU was attributed to the increase in Ag content, which was incorporated into the TiO₂ lattice. However, the Ag was only incorporated into the TiO₂ lattice up to a certain limit, leading to the stabilization of Ti³⁺ content in Ag-TiO₂/PU even with the further increase in the Ag/TiO₂ ratio.

3.1.3. Morphology and surface area. Fig. 5 shows the surface morphology of the synthesized TiO_2/PU , and the 2, 4, 6, 8 and 10% Ag- TiO_2/PU materials. The obtained results indicate that the TiO_2 in TiO_2/PU was smoothly immobilized on the PU surface as a thin layer (Fig. 5A). Compared to the surface morphology of TiO_2/PU , the Ag- TiO_2/PU materials exhibited a rougher morphology due to the dispersion of the formed small Ag particles on the surface of the TiO_2 layer. The obtained HRTEM results confirmed the existences of Ag particles on surface of TiO_2 (Fig. 6). The lattice spacing of approximately 0.24 and 0.25 nm correspond to the interlayer distance of the (111) and (004) crystal planes Ag.^{43,44}



Fig. 4 High-resolution XPS spectra of Ti $2p_{3/2}$ in X% Ag-TiO₂/PU.

degree of surface roughness of Ag–TiO₂/PU increased with increasing Ag/TiO₂ ratio (increasing in Ag particle content). When the Ag/TiO₂ ratios increased up to 8 wt%, the Ag particles began to cluster into larger particles covering the TiO₂ layer.

The BET surface areas of TiO₂/PU and Ag-TiO₂/PU are shown in Table 1. The BET surface area of TiO_2/PU was 110.9 m² g⁻¹, which was much higher than that of commercial TiO₂ powder, such as AEROXIDE® TiO₂ P25 obtained from Evonik Degussa Corporation (approximately 60 m² g⁻¹). This indicates that the surface area of TiO2 was successfully enhanced by using porous honeycomb PU as a substrate for the immobilization. The obtained BET results also indicate that the surface areas of the synthesized Ag-TiO₂/PU materials were much higher than that of TiO₂/PU. This may have been due to the aforementioned effect of the Ag particles dispersed on the TiO₂ surface in increasing the degree of surface roughness of TiO₂. The BET surface areas of the synthesized Ag-TiO₂/PU materials were also greatly increased with increasing Ag/TiO₂ ratios up to 6 wt%. However, the BET surface area of the areas of the 8% Ag-TiO₂/ PU and 10% Ag-TiO₂/PU were slightly lower than that of the 6% Ag-TiO₂/PU. This was attributed to the gathering or cluster of the Ag into larger particles at the high Ag/TiO₂ ratios, according to the SEM analysis. Thus, 6% Ag–TiO₂/PU exhibited the highest surface area (186.6 m² g⁻¹).

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3.1.4. Optical absorption ability. Fig. 7 shows the optical absorption in range of 300-700 nm of the synthesized TiO₂/PU and 2, 4, 6, 8 and 10% Ag-TiO₂/PU materials. TiO₂/PU inherited the optical absorption properties of TiO₂, which exhibits a strong absorption only in the UV region and the absorption edge around 370 nm.13,45 The optical absorption of the synthesized Ag-TiO₂/PU materials was observed in both the UV and visible regions. The significant enhancement of optical absorption in the visible region of Ag-TiO₂/PU was due to a contribution of the plasmon resonance of the Ag particles dispersed onto the TiO2 surface.46 The plasmon resonance of Ag particles excited electrons of the valence band of TiO₂ and transferred the excited electrons from the valence band to the conduction band of TiO2.45 The Ag particles also provided sites for the accumulation of the excited electrons, so that Ag acted as an electron sink to hinder the recombination of the excited electrons in the conduction band with holes in the valence band of TiO2.47 Therefore, Ag-TiO2/PU absorbed the visible light for the separation of the electrons and holes. The light absorption enhancement of Ag-TiO2/PU was also due to the role of the incorporated Ag, which bonded to TiO2 via Ag-O-Ti bonding, leading to oxygen vacancies and the formation of Ti³⁺ in the



Fig. 5 SEM of TiO₂/PU (A), and 2% (B), 4% (C), 6% (D), 8% (E) and 10% (F) Ag-TiO₂/PU.

 TiO_2 lattice. It has been reported that the energy level of Ti³⁺ was located in between the conduction band and the valence band of TiO₂.⁴⁷ Therefore, the formed Ti³⁺ also acted as an intermediate agent to enhance the transfer of electrons from the valence band to the conduction band of TiO₂, contributing to the enhancement of the optical absorption of the synthesized Ag–TiO₂/PU.

Fig. 7 also shows that the optical absorption ability of Ag-TiO₂/PU increased as the Ag weight fraction in Ag/TiO₂ increased up to 6 wt%, but then slightly decreased with further increase in the Ag/TiO₂ ratio. At the high Ag/TiO₂ ratios of 8 and 10 wt%, Ag tended to gather into larger particles on the TiO₂ surface (see Section 3.1.3), leading to an uneven distribution of Ag particles on the TiO₂ layer or a decrease in the interfacial surface between Ag and TiO₂ (Table 1). Thus, Ag could not act as a more effective electron carrier/sink to enhance the electron hole pair separation efficiency of TiO2, resulting in the decreased light absorption efficiency of Ag-TiO₂/PU at the high Ag/TiO2 ratios of 8 and 10 wt%. The large Ag particles also eclipsed the light reaching the TiO2 surface, thus decreasing the optical absorption of Ag-TiO₂/PU.⁴⁸ Thus, a further increase of Ag content in Ag-TiO₂/PU further reduced the light absorption intensity (Fig. 7E and F).

3.2. Toluene removal

3.2.1. Removal mechanism. Fig. 8 shows the toluene removal results by TiO₂/PU, and 2, 4, 6, 8 and 10% Ag-TiO₂/PU. The experiments were conducted in dark conditions for the first 180 min, after which visible light was provided for an additional 180 min. Under the darkened conditions, the outlet toluene concentration gradually increased up to 100 ppm at around 165 min, which is the same as the inlet concentration. This means that toluene saturation at the given adsorbent dose (Ag-TiO₂/ PU) occurred at around 165 min (Fig. 8A). In addition, no CO₂ corresponding to the photocatalytic degradation of gaseous toluene was detected (Fig. 8B). This indicates that gaseous toluene was removed solely by adsorption by Ag-TiO₂/PU in darkened conditions. When Ag-TiO2/PU was exposed to water vapor, its surface was be hydroxylated, leading to the formation of hydroxyl groups on surface of Ag-TiO2/PU via Ti-OH or Ag-OH bonds.^{49,50} The hydroxyl groups were thus able to bond with the π -electrons of the aromatic ring of toluene, resulting in the adsorption of toluene on the Ag-TiO2/PU surface.49 The toluene was also trapped on the Ag–TiO₂/PU surface by physical bond or electrostatic interaction between the aromatic ring of toluene and the various cations, such as Ti^{4+} , Ti^{3+} and Ag^+ , existing on the Ag-TiO₂/PU surface.⁵¹



Fig. 6 TEM images of TiO₂/PU (A) and Ag–TiO₂/PU (B); HRTEM images of the selected areas in the TEM images of TiO₂/PU (A1) and Ag–TiO₂/PU (B1, B2 and B3).

Radiation with visible light after saturation did not affect the toluene concentration passing through TiO_2/PU , which indicated that TiO_2/PU did not exhibit any significant photocatalytic



Fig. 7 UV-Vis absorption spectra of TiO_2/PU and 2, 4, 6, 8 and 10% Ag-TiO_2/PU.

degradation activity to remove gaseous toluene under visible light conditions. However, the outlet toluene passing through the Ag-TiO₂/PU materials suddenly increased to a level exceeding the inlet concentration, due to the desorption of the toluene adsorbed on Ag-TiO2/PU (rolled as an adsorbent) by scrubbing of the CO₂ generated from the photocatalytic degradation of toluene by Ag-TiO₂/PU (mainly acting as a photocatalyst) under visible light conditions. Because the doped Ag enhancing the electron-hole pair generation capacity and separation efficiency of TiO2, Ag-TiO2/PU easily generated electron-hole pairs, even under visible. The generated electrons and holes then participated in reactions with the O2 and/or H2O molecules in aerosol to produce hydroxyl and superoxide radicals, which are strong oxidative agents. The mechanism by which the hydroxyl and superoxide radicals were generated by Ag-TiO₂/PU under visible light is described by the following reactions:

$$Ag - TiO_2/PU \xrightarrow{\text{visible light}} e^- + h^+$$
 (3)

$$e^- + O_2 \to *O_2^-$$
 (4)

$$h^+ + H_2O \rightarrow H^+ + *OH \tag{5}$$



Fig. 8 Toluene removal (A) and generated CO₂ concentration (B) by X% Ag-TiO₂/PU under dark and then visible light conditions.

 $2h^{+} + 2H_2O \rightarrow 2H^{+} + H_2O_2$ (6)

 $H_2O_2 \rightarrow 2^*OH$ (7)

 $36*OH + C_7H_8 \rightarrow 7CO_2 + 22H_2O$ (8)

These generated oxy radicals then participated in the degradation of toluene into CO₂ and H₂O, accompanied by a sharp increase in the CO2 concentration, as shown in Fig. 8B.⁵¹⁻⁵³ The scrubbing of the adsorbed toluene by the CO₂ generated from the photocatalytic degradation of toluene caused desorption of the toluene, which had initially been adsorbed on the Ag-TiO2/PU surface during the darkened period. This desorption led to a sudden increase in the toluene concentration in the reactor. Although Ag-TiO₂/PU photocatalytically degraded a certain amount of the toluene passing through the reactor, the outlet toluene rose above its inlet concentration (100 ppm) for a short period before the reaction time reached 255 min. After the adsorbed toluene was almost completely desorbed, the outlet toluene concentration displayed a sharp decrease due to the continuous photocatalytic degradation of toluene by the Ag-TiO2/PU photocatalyst,

accompanied by a decrease in the CO_2 concentration with a slight time lag of around 15 min (Fig. 8B). After the adsorbed toluene was almost entirely desorbed, the incoming toluene underwent continuous photocatalytic degradation. Thus, the outlet toluene concentration plateaued in the range of 15 to 38 ppm depending on the Ag content in Ag–TiO₂/PU (Fig. 8A).

When visible light was provided from the beginning of the toluene removal experiments ($t_0 = 0$), without an adsorption period under dark conditions, the outlet toluene concentrations passing through the Ag–TiO₂/PU materials plateaued at around 10 to 30 ppm after 75 or 90 min (Fig. 9A). During the initial experimental period, the toluene was removed by both adsorption and the photocatalytic degradation of Ag–TiO₂/PU. However, the CO₂ gas, generated as a main product of the photocatalytic degradation of toluene early on. Thus, if the visible light was provided for longer than 75–90 min, the input toluene was only removed by the photocatalytic degradation activity of Ag–TiO₂/PU.

3.2.2. Optimal Ag content. Fig. 8A shows that under dark condition, the slope in the outlet toluene concentration passing through 6% Ag-TiO₂/PU was the shallowest. The steep slope of



Fig. 9 Toluene removal (A) and generated CO₂ concentration (B) by X% Ag-TiO₂/PU under visible light conditions.

an adsorption curve is inversely proportional to the adsorption capacity. A material with a very steep slope in its adsorption curve reaches its adsorption saturation easily or has a low adsorption capacity, whereas a material was a shallower slope has a high adsorption capacity. Thus, among the Ag–TiO₂/PU materials, 6% Ag–TiO₂/PU exhibited the highest adsorption capacity for toluene removal because it had the highest surface area (Table 1).

Fig. 8 and 9 show that the outlet toluene and CO_2 concentrations that passed through the Ag–TiO₂/PU materials under visible light irradiation were stabilized at certain values that could be used to calculate the toluene removal efficiency and the mineralization degree of toluene into CO_2 and H_2O by Ag–TiO₂/PU at different Ag/TiO₂ ratios (Table 2). The toluene removal efficiency and the degree of mineralization by Ag–TiO₂/PU showed similar results for both conditions A and B (explained in the note at the bottom of Table 2). The removal efficiency of toluene increased as the Ag/TiO₂ ratio increased up to 6 wt%, but then gradually decreased with further increase in the ratio. These results were matched by those obtained from the XPS and UV-Vis absorption analyses of Ag–TiO₂/PU

photocatalyst. The increase in the Ag/TiO_2 ratio led to an increase in the number of both Ag ions, which were incorporated into the TiO_2 lattice, and metallic Ag, which was dispersed onto the TiO_2 layer. Consequently, the electron-hole separation efficiency and lifespan of the excited electrons in TiO_2 were both increased, which further increased the photocatalytic degradation efficiency of TiO_2 . However, the incorporation of Ag ions into the TiO_2 lattice was limited by the tendency of the Ag particles, which had dispersed onto the TiO_2 lattice and thus enhanced the electron-hole pair separation efficiency of TiO_2 , to gather into large particles at high Ag/TiO_2 ratios of 8 and 10 wt%, which decreased their enhancement role. Thus, the effect of Ag in enhancing the photocatalytic activity of TiO_2 seemed to reach a limit when the Ag/TiO_2 ratio was 6 wt%.

3.2.3. Effects of oxygen content. Fig. 10 shows the toluene removal by 6% Ag–TiO₂/PU carried out under darkened conditions for the first 180 min, followed by visible light irradiation for an additional 180 min, as a function of the oxygen content in the input gas stream. Under the darkened condition, the slopes in the outlet toluene concentrations passing through 6% Ag–TiO₂/PU, and hence its toluene adsorption ability, were not

Table 2 The toluene removal efficiency and the mineralization degree by $Ag-TiO_2/PU$ photocatalysts at different Ag/TiO_2 ratios under visible light conditions^{*a*}

	Condition A		Condition B	
	Removal efficiency (%)	Mineralization degree (%)	Removal efficiency (%)	Mineralization degree (%)
2% Ag-TiO ₂ /PU	62.5	88.2	62.9	88.5
4% Ag-TiO ₂ /PU	68.3	89.1	68.7	89.6
6% Ag-TiO ₂ /PU	85.2	90.3	85.6	90.8
8% Ag-TiO ₂ /PU	81.4	88.4	81.7	89.1
10% Ag-TiO ₂ /PU	75.6	89.3	76.5	88.4

^{*a*} Condition A: light was provided after the toluene was adsorbed during the darkened period (0–180 min), condition B: light was provided from the beginning of the toluene removal ($t = t_0$).

affected by the oxygen content. This indicated that oxygen and toluene were adsorbed at different sites on the Ag-TiO₂/PU surface, so that the adsorption of oxygen did not compete with toluene adsorption.²⁵

Under visible light conditions, the photocatalytic degradation of gaseous toluene using Ag–TiO₂/PU was significantly affected by the oxygen content in the input gas stream. The photocatalytic degradation of toluene increased with increasing oxygen content up to 15% and then stabilized (Fig. 10A). The O₂ reacted with the electrons generated on the surface of Ag–TiO₂/ PU to produce superoxide radicals (reaction (4)), which increased the photocatalytic degradation of toluene in the gas stream.⁵⁴ The reaction between the oxygen and the photogenerated electrons also prevented the recombination of the generated electrons and holes to prolong the lifetime of the generated holes, thereby increasing the production of hydroxyl radicals (*via* reactions (5) to (7)) and hence increasing the degradation of toluene.⁵⁵ The reaction between oxygen and



Fig. 10 Effect of O₂ content on outlet toluene (A) and generated CO₂ concentration (B) passing 6% Ag-TiO₂/PU.

electrons peaked at an oxygen content of 15%, above which the degradation of toluene in the gas stream was stabilized. These study results supported the conclusion that ambient air, with an oxygen content of 21%, can provide sufficient oxygen for the economic photocatalytic degradation of gaseous toluene by Ag–TiO₂/PU under visible light condition.

4. Conclusion

The synthesized Ag-TiO₂/PU exhibited high adsorption and photocatalytic degradation for the effective removal of gaseous toluene. The high adsorption ability was attributed to the use of porous PU as a substrate for the immobilization of Ag-TiO₂, which greatly increased the surface area of the adsorbents (Ag-TiO₂/PU). The high photocatalytic degradation of toluene was attributed to the Ag particles, which deposited onto the TiO₂ surface, and the Ag dopants, which incorporated into the TiO₂ lattice. The optimal Ag/TiO₂ ratio for enhancing the photocatalytic degradation activity of TiO2 for toluene removal was 6 wt%. Under dark condition, the synthesized Ag-TiO₂/PU exhibited only adsorption activity for removal of gaseous toluene, whereas under visible light irradiation condition it exhibited a combination of both adsorption and photocatalytic degradation. We investigated that the ambient air can be used economically to provide sufficient oxygen for the photocatalytic degradation of gaseous toluene by Ag-TiO₂/PU under visible light condition. Under visible light irradiation, 6% Ag-TiO₂/PU successfully removed 85.2% of the 100 ppm toluene in gas stream, while 90.3% of the removed amount was mineralized into CO₂ and H₂O.

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