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Novel Atom-Economic Nitration of Benzene with a Nitrogen Dioxide–Oxygen System using Cocatalyst of Solid Oxides and Lanthanide(III) Metal Triflates

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Abstract: Benzene is nitrated by a novel atom-economic nitration procedure with a $\text{NO}_2\text{-O}_2$ system in the presence of a mixture of solid oxides and $\text{Ln}(\text{OTf})_3$. The only by-product in this novel method is water. The efficiency of NO_2 is much higher than 50%, the theoretical efficiency of NO_2 of the known methods. Among the solid oxides and $\text{Ln}(\text{OTf})_3$ studied, HZSM-5 and $\text{Sm}(\text{OTf})_3$ were the most efficient catalysts in this process. Therewith, the yield of the benzene nitration reached 72.5%, calculated by NO_2 .

Keywords: benzene, lanthanide(III) metal triflate, nitration, nitrogen dioxide, oxygen, solid oxides

INTRODUCTION

Nitration of organic compounds is one of the most important and extensively studied organic reactions. The nitroaromatic compounds so produced are themselves widely utilized and act as chemical feedstocks for a great range of useful materials such as dyes, pharmaceuticals, perfumes, and plastics.^[1] Unfortunately, classical nitration has long been carried out using concentrated or fuming nitric acid with sulfuric acid on a high-volume scale, which leads to

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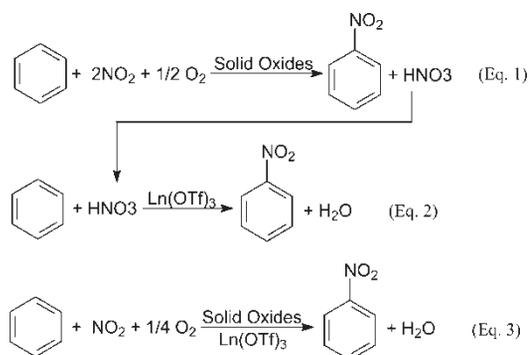
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excessive acid waste streams, overnitration, and oxidizing by-products. The obvious disadvantages associated with this procedure prompted research on alternative methods to classical nitration such as using solid acid catalysts, strong Lewis acid catalysts, and other nitrating agents.

The nonacid method for aromatic nitration using a NO_2/O_3 system as nitrating agent has demonstrated an excellent conversion of a wide variety of aromatic compounds to the corresponding nitro derivatives under mild conditions (Kyodai nitration).^[2] However, because ozone used in the nitration reaction can only be obtained by discharging oxygen at a high voltage, an expensive ozone generator and large amounts of electricity are needed for the mass production of ozone. Further efforts to find an alternative means to solve the problem has led to the Fe(III)-catalyzed nitration of aromatic compounds with an $\text{NO}_2\text{-O}_2$ system.^[3] Rather unfortunately, a long reaction time (e.g., 12 to 36 h) is needed even though large amounts of nitrogen dioxide (31 equivalents) and catalyst are used. In another modified means, zeolite was used as catalyst for this process, and high yields and significant selectivities were obtained. However, a long reaction time and large amount of nitrogen dioxide were necessary.^[4] Furthermore, according to the reaction equation [Scheme 1, Eq. (1)], the theoretical efficiency of NO_2 is only 50%. The other 50% of NO_2 converts into nitric acid as a waste acid, which is an disadvantage of this procedure.

On the other hand, it has been reported that lanthanide(III) metal triflate $[\text{Ln}(\text{OTf})_3]$ ^[5] and other perfluorinated rare-earth metal salts^[6] can be used as recyclable catalysts for the nitration of simple arenes with stoichiometric quantities of nitric acid. The only by-product is water, and the catalyst may be readily recycled and reused repeatedly.

To develop an atom-economic process for aromatic nitration, we applied the mixture of solid oxides and $\text{Ln}(\text{OTf})_3$ as catalyst for $\text{NO}_2\text{-O}_2$ system nitration. As shown in Scheme 1, our approach to the nonacid process for



Scheme 1. Proposed mechanism for nitration of benzene with $\text{NO}_2\text{-O}_2$ system as nitrating agent catalyzed by solid oxides and $\text{Ln}(\text{OTf})_3$.

nitration of benzene consisted of two steps: first, a solid oxide catalyzed the $\text{NO}_2\text{-O}_2$ system to nitrate benzene and generated a by-product of nitric acid at the same time. Second, $\text{Ln}(\text{OTf})_3$ catalyzed nitric acid to nitrate benzene in situ. The total reaction is shown in Eq. (3). The theoretical efficiency of NO_2 is 100%, and the only by-product is water. To the best of our knowledge, such cocatalyst is rare in nitration methodology. Therefore, the obtained facts may open new alternatives for atom-economic aromatic nitration.

RESULTS AND DISCUSSION

Initially, HZSM-5 and $\text{Sm}(\text{OTf})_3$ were investigated in our approach. To optimize the amount of $\text{Sm}(\text{OTf})_3$ for maximum yield, nitration of benzene was studied with varied $\text{Sm}(\text{OTf})_3$ amounts ranging from 0 to 2 mol% and 2.0 g of HZSM-5. The results (Table 1) showed that the yield of nitrobenzene increases with the amount of $\text{Sm}(\text{OTf})_3$ until $\text{Sm}(\text{OTf})_3$ loading reaches 1 mol%, and more $\text{Sm}(\text{OTf})_3$ was not beneficial to yield.

A similar process was studied with varied HZSM-5 amounts ranging from 0 to 2 g with $\text{Sm}(\text{OTf})_3$ loading of 1 mol% to optimize the amount of HZSM-5 for maximum yield. The results (Table 2) showed that the yield of nitrobenzene increases with HZSM-5 until HZSM-5 loading reaches 1.0 g. More HZSM-5 has no obvious effects on the yield.

Varied pressure ranging from 0.2 to 0.8 MPa was studied to determine the most suitable reaction pressure. The data (Table 3) show that the highest yield was obtained at 0.5 MPa. Pressure higher than 0.5 MPa was not beneficial to yield.

To optimize the reaction temperature, varied temperature ranging from 85 to 115°C was studied. The results (Table 4) show that at low temperature, the

Table 1. Effects of $\text{Sm}(\text{OTf})_3$ amount on the yield of nitrobenzene^a

Entry	$\text{Sm}(\text{OTf})_3$ (mol%)	Yield ^b (%)
1	0	51.4
2	0.5	59.5
3	1	65.4
4	1.5	65.8
5	2	65.6

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.105 mol); HZSM-5 = 2.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 85°C; reaction pressure = 0.8 MPa; reaction time = 7 h.

^bIsolated yields based on the amount of NO_2 .

Table 2. Effect of HZSM-5 amount on the yield of nitrobenzene^a

Entry	HZSM-5 amount (g)	Yield ^b (%)
1	0	59.4
2	0.5	63.2
3	1.0	65.8
4	1.5	65.7
5	2.0	65.5

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.11 mol); Sm(OTf)₃ = 1 mol%; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 85°C; reaction pressure = 0.8 MPa; reaction time = 7 h.

^bIsolated yields based on total amount of NO₂.

yield increased along with reaction temperature, and the highest yield was obtained at 100°C. However, yield decreased if reaction temperature increased further.

To optimize the reaction time, the process was studied at varied reaction times ranging from 3 to 9 h. The results (Table 5) show that the highest yield was obtained at 7 h. The yield was not changed when the reaction time was further prolonged.

We then carried out similar reactions in which various solid oxides or Ln(OTf)₃ were used as catalysts instead of HZSM-5 or Sm(OTf)₃ to determine which solid oxide, if any, would be the most applicable to benzene nitration. As shown in Tables 6 and 7, the reaction occurred in the presence of all of the solid oxides and Ln(OTf)₃. Among the solid oxides

Table 3. Effects of reaction pressure on the yield of nitrobenzene^a

Entry	Reaction pressure (MPa)	Yield ^b (%)
1	0.2	28.5
2	0.4	63
3	0.5	65.7
4	0.6	65.4
5	0.8	65.5

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.11 mol); Sm(OTf)₃ = 1 mol%; HZSM-5 = 2.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 85°C; reaction time = 7 h.

^bIsolated yields based on total amount of NO₂.

Table 4. Effects of the reaction temperature on the yield of nitrobenzene^a

Entry	Reaction temperature (°C)	Yield ^b (%)
1	85	65.7
2	95	71.8
3	100	72
4	105	71.8
5	115	68.2

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.11 mol); Sm(OTf)₃ = 1 mol%; HZSM-5 = 2.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction pressure = 0.5 MPa; reaction time = 7 h.

^bIsolated yields based on total amount of NO₂.

and Ln(OTf)₃ studied, HZSM-5 and Sm(OTf)₃ gave the most encouraging yield of 72.5% (entries 1 and 2).

Control experiments were performed according general procedure. The absence of either solid oxide (entry 9, Table 6) or Ln(OTf)₃ (entry 7, Table 7) decreased the product yields remarkably. The results clearly indicated that both solid oxide and Ln(OTf)₃ are indispensable for nitration of benzene in our method. Moreover, all entries using catalyst made up of solid oxide and Ln(OTf)₃ gave yields of more than 50%, which means by cocatalyzing the solid oxide and Ln(OTf)₃, the efficiency of NO₂ was increased more than 50%, the theoretical efficiency of NO₂ in the prior methods.

In summary, we have discovered a novel atom-economic aromatic nitration process with an NO₂-O₂ system in the presence of a mixture of solid oxides and Ln(OTf)₃. The only by-product in this process is water,

Table 5. Effects of reaction time on the yield of nitrobenzene^a

Entry	Reaction time (h)	Yield ^b (%)
1	3	41.4
2	6	59.4
3	7	72.5
4	9	72.3

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.105 mol); Sm(OTf)₃ = 1 mol%; HZSM-5 = 1.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 100°C; reaction pressure = 0.5 MPa.

^bIsolated yields based on total amount of NO₂.

Table 6. Nitration of benzene catalyzed by Sm(OTf)₃ and various solid oxides^a

Entry	Solid oxide	Yield ^b (%)
1	HZSM-5	72.5
2	V ₂ O ₅	72.2
3	Al ₂ O ₃	60.4
4	SiO ₂	65.6
5	Cr ₂ O ₃	65.4
6	ZrO ₂	60.2
7	CeO ₂	64.3
8	WO ₃	59.4
9 ^c	—	32.1

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.105 mol); Sm(OTf)₃ = 1 mol%; HZSM-5 = 1.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 85°C; reaction pressure = 0.5 MPa.

^bIsolated yields based on total amount of NO₂.

^cNo solid oxide was used.

and the efficiency of NO₂ is in excess of 50%. Efforts are under way to elucidate more mechanistic details of the nitration reaction catalyzed by this novel mixture catalyst and to identify systems enabling the nitration of other aromatic compounds and the subsequent transformations thereof.

Table 7. Nitration of benzene catalyzed by HZSM-5 and various Ln(OTf)₃^a

Entry	Ln(OTf) ₃	Yield ^b (%)
1	Sm(OTf) ₃	72.5
2	Yb(OTf) ₃	68.4
3	Nd(OTf) ₃	61.7
4	Gd(OTf) ₃	60.3
5	Er(OTf) ₃	64.5
6	Dy(OTf) ₃	62.5
7 ^c	—	27.1

^aReaction condition: 1,2-dichloroethane = 50 mL; benzene = 9 mL (0.105 mol); Sm(OTf)₃ = 1 mol%; HZSM-5 = 2.0 g; liquid nitrogen dioxide = 3.2 g (0.07 mol); reaction temperature = 85°C; reaction pressure = 0.5 MPa.

^bIsolated yields based on total amount of NO₂.

^cNo Ln(OTf)₃ was used.

EXPERIMENTAL

General

Sm₂O₃, Yb₂O₃, Nd₂O₃, Gd₂O₃, Er₂O₃, Dy₂O₃, V₂O₅, Al₂O₃, Al₂O₃, Cr₂O₃, ZrO₂, CeO₂, WO₃ were procured from Sinopharm Chemical Reagent Co., Ltd., China. Silica gel was obtained from Qingdao Haiyang Chemical Co., Ltd., China. NaZSM-5 was purchased from Wenzhou Huahua Group Co., China. Benzene was procured from Quzhou Juhua Chemical Reagent Co., Ltd., China. 1,2-Dichloroethane was obtained from Shanghai Lingfeng Chemical Reagent Co., Ltd., China. The purity of the product was analyzed by GC-MS (Agilent 6890 N/5973) and/or GC (GC-1102, China).

Catalyst Preparation

Ln(OTf)₃ (Ln = Sm, Yb, Nd, Gd, Er, Dy)

The triflate salts were prepared following a reported procedure.^[7] Typically, an excess of lanthanide(III) oxide (99.9% purity) was added to an aqueous solution of trifluoromethanesulfonic acid (50% v/v) and heated at boiling for 30 min to 1 h. The mixture was filtered to remove the unreacted oxide. The filtrate was concentrated, and the resulting hydrate was dried by heating at 120°C for 48 h.

HZSM-5

NaZSM-5 (50 g) was treated with 500 mL of 1 M aqueous ammonium chloride at 90°C for 2 h. The procedure was repeated five times, followed by filtration of the sample and washing with distilled water until the filtrate showed the absence of the chloride ions. The obtained sample was oven dried at 120°C for 10 h followed by calcination at 550°C for 4 h in an air atmosphere.

General Procedure for Nitration of Benzene

1,2-Dichloroethane (50 mL), benzene (9 mL, 0.11 mol), solid oxides, Ln(OTf)₃, and liquid nitrogen dioxide (2.2 mL, 0.07 mol) were poured into an autoclave. Next, oxygen was injected at a pressure of 0.2 to 0.8 MPa, and then the mixtures were reacted at 85 to 115°C for 3 to 9 h while the same level of pressure was maintained. After completion of the reaction, the reaction mixture was filtrated to remove the solid oxides, washed with water to recycled Ln(OTf)₃, and dried with MgSO₄. The solvent was removed under reduced pressure to afford nitrobenzene. The purity of the

product was analyzed by GC-MS (Agilent 6890 N 5973) and/or GC (GC-1102, China).

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