

# Thermally stable gold/alumina aerogel catalysts prepared by a simultaneous synthesis process for solvent-free aerobic benzyl alcohol oxidation

Cite this: DOI: 10.1039/c3cy01064c

Z. Li,<sup>abc</sup> Y. Ji,<sup>a</sup> C. Cadigan<sup>a</sup> and R. M. Richards<sup>\*a</sup>Received 16th December 2013,  
Accepted 1st May 2014

DOI: 10.1039/c3cy01064c

www.rsc.org/catalysis

Gold nanoparticles supported on an alumina aerogel have been prepared through a simultaneous synthesis process in which the formation of the gold nanoclusters capped with (3-aminopropyl)triethoxysilane (APTES) and the hydrolyzation/co-condensation of the APTES and aluminum alkoxide occur concurrently. The obtained gold nanoparticles are trapped in and physically protected by the framework of the alumina aerogel providing excellent thermal stability with no observable sintering at 650 °C. In the catalysis test for the solvent-free aerobic benzyl alcohol oxidation, this catalyst exhibits significantly better activity than reference gold/alumina aerogel catalysts prepared through a deposition precipitation and conventional wet impregnation methods, especially at high temperature.

## 1. Introduction

The catalytic performance of nanoparticles can be finely tuned either by their composition, which mediates electronic structure, or by their shape, which determines surface atomic arrangement and coordination. Beyond the exciting potential for tailoring catalysts, nanostructured materials introduce additional challenges to catalyst design. By being small and containing surface atoms of varying unsaturated valencies, nanoparticles of specific shape are more susceptible to morphological change in harsh chemical reaction environments.<sup>1</sup> Given the low melting points of nanoparticles as compared to their bulk counterparts, imparting stability to nanoscale catalysts (particularly gold) remains a challenge.<sup>2</sup>

Gold has long been considered an 'inert' metal. However, with the development of nanotechnology, it has been found that nano-scale gold is highly active for CO oxidation with great selectivity even at room temperature.<sup>3</sup> Thereafter, the field of gold nanocatalysts has been thoroughly studied and has rapidly become a promising system for hydrogenation<sup>4</sup> and epoxidation<sup>5,6</sup> of alcohols<sup>7,8</sup> and aldehydes<sup>9</sup> as well as oxidation and even aerobic oxidation of alkanes.<sup>8,10,11</sup> However, most applications of gold catalysts are performed under moderate conditions with relatively low temperatures (normally 80–120 °C). Working at higher temperatures, gold nanoparticles generally

suffer from severe sintering and loss of activity, greatly limiting the practical application of gold catalysts.<sup>12</sup> In fact, the sintering of gold catalysts also happens during the moderate calcination (250–350 °C) process of catalyst preparations. The thermal stability of gold catalysts can be somewhat improved by removal of the chloride ions in the catalysts or by using expensive chloride-free gold precursors.<sup>13</sup> Numerous efforts have been made to address this problem by modifying the surface of gold nanoparticles or the surface of the supporting materials. One promising approach is to physically trap the gold catalysts in the rigid structure of metal oxides.<sup>14</sup> Very recently, atomic layer deposition (ALD) has been used to stabilize nanoporous gold with a thin layer of Al<sub>2</sub>O<sub>3</sub>, greatly improving the thermal stability of the gold.<sup>15</sup> Furthermore, in our previous work, we have reported gold catalysts intercalated in the walls of mesoporous silica with improved thermal stability.<sup>11,16</sup>

In this work, we have improved the thermal stability of Au/Al<sub>2</sub>O<sub>3</sub> catalysts by simultaneously hydrolyzing/condensing aluminum alkoxide and reducing the gold precursor in the presence of (3-aminopropyl)triethoxysilane (APTES) as a linking agent. The obtained catalyst can endure calcination temperatures up to 650 °C while maintaining excellent catalytic activity at 160 °C in the solvent-free aerobic benzyl alcohol oxidation. Au/Al<sub>2</sub>O<sub>3</sub> catalysts prepared by a conventional impregnation method and a deposition–precipitation (DP) method have also been tested as controls.

## 2. Results and discussion

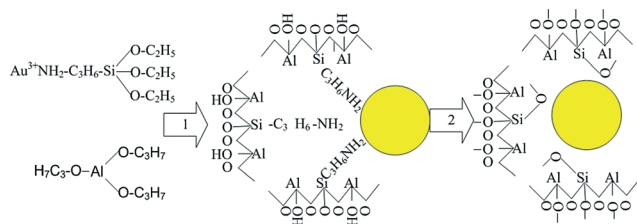
### 2.1 Synthesis of Au/Al<sub>2</sub>O<sub>3</sub> catalyst

An ultrastable Au/Al<sub>2</sub>O<sub>3</sub> catalyst was prepared by a simultaneous synthesis method, during which the reduction of Au<sup>3+</sup> and the

<sup>a</sup> Department of Chemistry and Geochemistry, Colorado School of Mines, 1500 Illinois St., Golden, CO 80401, USA. E-mail: rrichard@mines.edu; Fax: +1 303 273 3629; Tel: +1 303 273 3612

<sup>b</sup> Chemical and Materials Engineering, University of Alberta, 9107 116 St., Edmonton, AB, T6G 2V4, Canada

<sup>c</sup> National Institute for Nanotechnology (NINT), NRC, 11421 Saskatchewan Dr., Edmonton, AB, T6G 2M9, Edmonton, AB, T6G 2M9, Canada

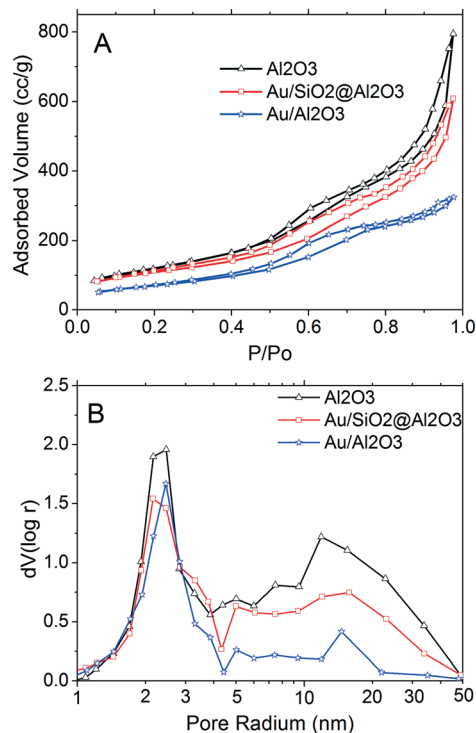


**Fig. 1** The schematic illustration of the simultaneous synthesis process of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub>. The arrow marked as '1' signifies the reduction of gold and hydrolysis and condensation of aluminum alkoxide and APTES; the arrow marked as '2' signifies the 5 hour calcination process at 500 °C.

hydrolyzation/condensation of the aluminum alkoxide took place at the same time. APTES, well-known for its affinity to gold nanoparticles, was used as a linking agent. As shown in Fig. 1, the as-formed gold nanoclusters, bonded to the (NH<sub>2</sub>) end of APTES, were further stabilized during the co-condensation of ethoxy groups and concurrent sol-gel processes occurring with aluminum alkoxide. The co-condensation process prevents the gold clusters from further growth and results in a uniform structure with tiny gold particles trapped in the framework of Al<sub>2</sub>O<sub>3</sub> (with a small amount of SiO<sub>2</sub> from APTES) after supercritical drying and calcination at 500 °C. The nomenclature Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> is used henceforth in this manuscript for this catalyst system. As a control, a pure Al<sub>2</sub>O<sub>3</sub> aerogel has been prepared under the same conditions without addition of APTES and gold precursor. The obtained Al<sub>2</sub>O<sub>3</sub> aerogel was used as supporting material to prepare the reference catalyst by impregnation method (termed Au/Al<sub>2</sub>O<sub>3</sub> herein).

## 2.2 Porous texture and chemical features of the catalyst systems

Surface area and porosity were analyzed by N<sub>2</sub>-adsorption at -196 °C. As shown in Fig. 2A, Al<sub>2</sub>O<sub>3</sub> aerogel, Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> and Au/Al<sub>2</sub>O<sub>3</sub> all exhibit type IV isotherms with H1-type hysteresis loops at  $P/P_0 = 0.5$ –1.0. This is characteristic of a combined pore system with mostly small mesopores with some larger mesopores. Compared with the other two, the hysteresis loops of Au/Al<sub>2</sub>O<sub>3</sub> are less developed at high pressure ( $P/P_0 = 0.75$ –1.0), indicating fewer large mesopores in the sample. This difference is also observed in the pore size distribution plots (Fig. 2B) calculated by the Barrett-Joyner-Halenda (BJH) model with a sharp peak centered at 2.4 nm (pore radius) in all three samples. The pores of this size are formed by the packing of the Al<sub>2</sub>O<sub>3</sub> nanoparticles. There are also broad peaks in the range of 5–50 nm, which correspond to the large pores formed during formation of the Al<sub>2</sub>O<sub>3</sub> gel. However, in the case of Au/Al<sub>2</sub>O<sub>3</sub>, this peak is significantly smaller than that of other samples, suggesting part of the pore structure formed in gelation was destroyed in the conventional wetness impregnation preparation of gold catalysts. As listed in Table 1, Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> has a large surface area (384 m<sup>2</sup> g<sup>-1</sup>), slightly lower than that of pure Al<sub>2</sub>O<sub>3</sub> aerogel (441 m<sup>2</sup> g<sup>-1</sup>), indicating that the gold nanoparticles formed



**Fig. 2** Nitrogen adsorption/desorption isotherms at -196 °C (A) and BJH pore-size distribution (B) of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub>, Au/Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> aerogel.

**Table 1** N<sub>2</sub>-adsorption data and Au content of different samples

Sample	Calcine [°C]	$S_{\text{BET}}^a$ [m <sup>2</sup> g <sup>-1</sup> ]	$V_{\text{total}}^b$ [cm <sup>3</sup> g <sup>-1</sup> ]	Au <sup>c</sup> [wt%]	Au size <sup>d</sup> [nm]
Al <sub>2</sub> O <sub>3</sub>	500	441	1.08		
Au/SiO <sub>2</sub> @Al <sub>2</sub> O <sub>3</sub>	500	384	1.07	1.1	3–5 (spheres)
Au/Al <sub>2</sub> O <sub>3</sub>	350	252	1.03	1.0	3–30 (irregular)

<sup>a</sup> The surface area  $S_{\text{BET}}$  is calculated by a multi point BET method (7 points were selected in the range of  $P/P_0 = 0.1$ –0.3). <sup>b</sup> Total pore volume. <sup>c</sup> Weight content of Au in catalysts, determined by ICP-MS analysis. <sup>d</sup> The size of gold nanoparticles is determined by TEM.

in the simultaneous deposition process did not influence the formation of the sol-gel pore structure. The impregnation and calcination processes resulted in a loss of more than 40% of the surface area of the aerogel. In fact, the effect of solvent on the support materials is an unavoidable factor in most post treatment methods to prepare heterogeneous catalysts *via* deposition-precipitation (DP) or wetness impregnation. The gold content of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> and Au/Al<sub>2</sub>O<sub>3</sub> are 1.1% and 1.0% respectively as measured by inductively coupled plasma mass spectrometry (ICP-MS) analysis. The Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> catalyst also contains around 5% SiO<sub>2</sub>, which is from APTES.

## 2.3 Structure and morphology of gold nanoparticles

Considering that the Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> catalyst was calcined at 500 °C, we are extremely interested in the morphology of the

gold nanoparticles: whether or not they agglomerated like the typical gold nanoparticles supported on  $\text{Al}_2\text{O}_3$ .<sup>17,18</sup> In order to increase the contrast between gold nanoparticles and the alumina, Scanning Transmission Electronic Microscopy (STEM-Dark field mode) was utilized to study the morphology and distribution of gold nanoparticles supported on alumina aerogel. Fig. 3A shows an overview of the  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  catalyst, where the uniform gold nanoparticles are evenly distributed on the alumina support. Those gold nanoparticles show a sphere-like structure and are 3–5 nm in diameter (Fig. 3B). No agglomeration of gold nanoparticles was observed after calcination at 500 °C. The selected area dispersive X-ray (SAEDX) analysis shown in Fig. 3C indicates the existence of Si (from APTES), Au, Al, O and C (from the carbon film on TEM grids). To evaluate the thermal stabilities of the  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  catalyst, the sample was also calcined at 650 °C and 750 °C. As seen in Fig. 3D, the gold nanoparticles retain uniform size and are well dispersed on the support after calcination at 650 °C. Furthermore, the high magnification image shown in the inset reveals that the particles are only slightly larger at 5–10 nm. Even after calcination at 750 °C, about half of the gold particles are still around 5 nm in size, but some larger agglomerations begin to appear at this calcination condition (Fig. 3E). From the inset, larger particles around 20–30 nm can be observed.

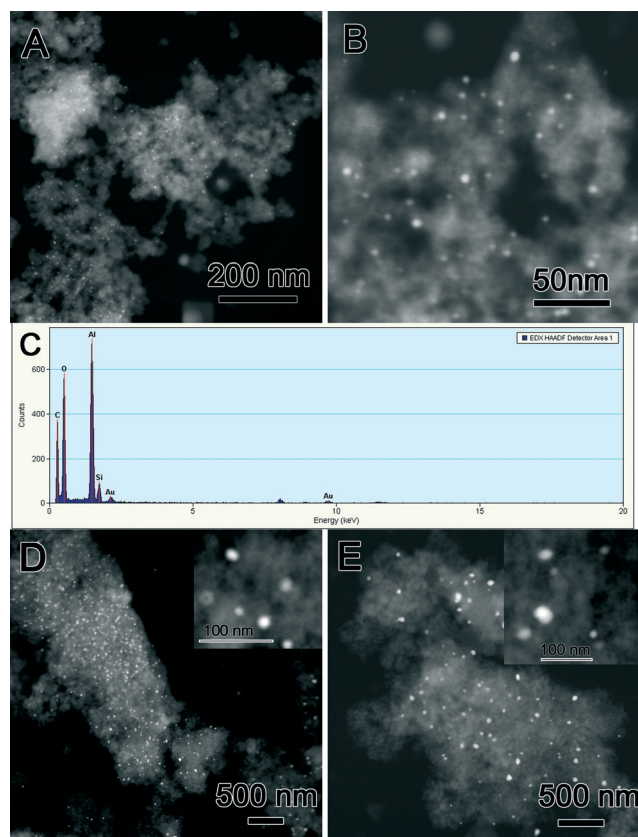


Fig. 3 HAADF-STEM images of  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  catalyst (A, B) and the EDX analysis at the selected area (C); HAADF-STEM images of  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  catalyst calcined at 650 °C (D) and 750 °C (E).

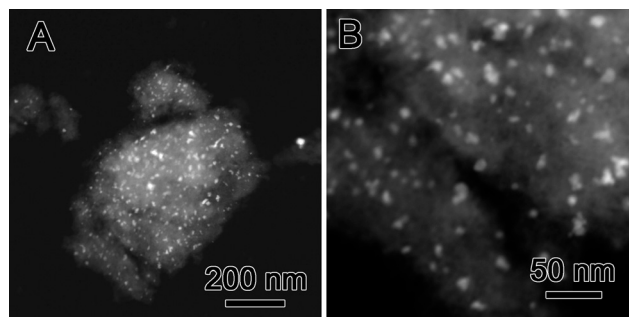


Fig. 4 HAADF-STEM images of  $\text{Au}/\text{Al}_2\text{O}_3$  at low (A) and high (B) magnification.

For comparison, Fig. 4 shows the  $\text{Au}/\text{Al}_2\text{O}_3$  catalyst prepared by the wet impregnation method. The alumina support shows a similar morphology with that of  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  and is typical of an alumina aerogel. However, the supported gold shows various shapes and sizes with some 3–5 nm spheres as well as significant agglomerations (some reaching 30 nm). Given the reference catalyst was calcined at a much lower temperature (350 °C), it is inferred that the simultaneous synthesis method yields a gold catalyst with significantly improved thermal stability than conventional gold catalysts.

Fig. 5A shows the X-ray diffraction pattern of the  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  and  $\text{Au}/\text{Al}_2\text{O}_3$  samples. The  $\text{Al}_2\text{O}_3$  supports of both samples exhibit very broad diffraction peaks indicating that they are composed of very fine nanoparticles. However, the gold peak is not observable in any of the samples. That is mainly because the two strongest diffraction peaks of Au, namely

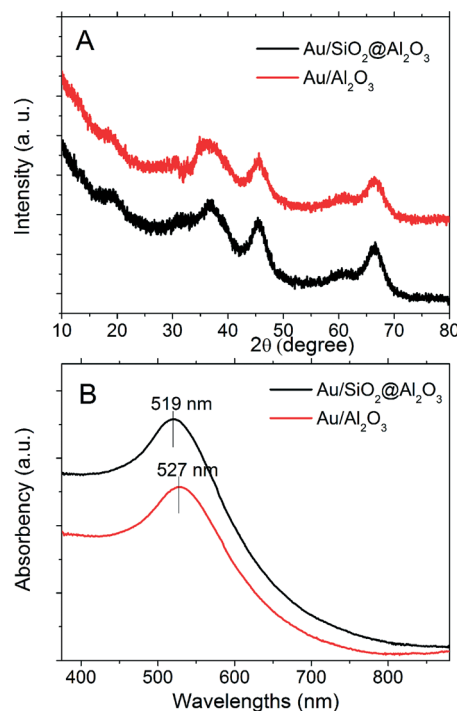


Fig. 5 XRD spectra (A) and diffuse-reflectance UV-vis spectra (B) of  $\text{Au}/\text{SiO}_2@/\text{Al}_2\text{O}_3$  and  $\text{Au}/\text{Al}_2\text{O}_3$  catalysts.

(111) at 38.18° and (200) at 44.39° will be relatively small given the low Au concentration (around 1 wt%) and the truly nanoscale size of Au particles. Additionally, the small Au peaks can be concealed by the larger broad peaks of Al<sub>2</sub>O<sub>3</sub> at similar positions (35.14° and 43.36°). However, the broad diffraction peak of Al<sub>2</sub>O<sub>3</sub> at 35.14° shows a small shoulder at around 38°, which might be attributed to the Au (111) diffraction. It is well-known that the surface plasma resonance (SPR) of gold nanoparticles is closely related to their particle size.<sup>19</sup> Diffuse-reflectance UV-vis spectra were used to investigate the SPR of the two catalysts (Fig. 5B). Both catalysts show a sharp SPR peak in the range of 500–600 nm as evidence that the gold particles are nanoscale in size. Furthermore, the SPR peak of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> (519 nm) was slightly blue shifted as compared to Au/Al<sub>2</sub>O<sub>3</sub>, indicating that the Au particles in Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> are slightly smaller.

#### 2.4 Catalytic performance of ultrastable Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> catalysts

The oxidation of benzyl alcohol, as a model reaction for primary alcohol oxidation,<sup>20</sup> was used in this work to study the activity of the Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> prepared by simultaneous synthesis. All reactions were performed in the absence of solvent with a 6 h reaction time. No detectable benzene or toluene was produced in the reactions. The byproduct is mainly benzyl benzoate rather than benzoic acid, indicating either the immediate esterification between benzoic acid and benzyl alcohol, or that oxidation occurs directly on the hemiacetal [PhCH(OH)OCH<sub>2</sub>Ph] formed from benzaldehyde and benzyl alcohol without ever forming benzoic acid.<sup>5,21</sup> Comparing the performance of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub>, Au/Al<sub>2</sub>O<sub>3</sub>, Au/Al<sub>2</sub>O<sub>3</sub> DP and pure Al<sub>2</sub>O<sub>3</sub> (to evaluate the contribution of supporting material), it can be inferred that the gold nanoparticles have minimal contributions to the overall conversion at 100 °C (Table 2). The activity of gold nanoparticles increases with temperature,

but Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> showed no significant advantage over Au/Al<sub>2</sub>O<sub>3</sub> at 120 °C and 140 °C indicating that the catalysts work similarly under those moderate conditions. However, Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> gives a conversion of 21.90% at 160 °C, more than two times the conversion demonstrated by Au/Al<sub>2</sub>O<sub>3</sub> (10.42%) with similar selectivity to benzaldehyde. Indeed, higher conversion is always desirable as long as the catalyst can handle the high temperature and still give reasonable selectivity. The Au/Al<sub>2</sub>O<sub>3</sub> DP catalyst had the lowest activities among the three Au catalysts at higher temperatures, but the highest selectivity to benzaldehyde as reaction temperature elevates to 160 °C.

To determine the Au leaching of our Au/Al<sub>2</sub>O<sub>3</sub> catalyst, the solution after catalytic reaction was collected and Au composition determined by ICP. Results indicated that at 100 °C, 0.412% of Au was leached after reaction, the leaching of Au slightly increased to 0.466% at 120 °C and finally reached 0.523% for reaction at 160 °C. Au leaching is minor in all catalytic reactions, even at a high temperature of 160 °C, suggesting a good thermal stability of simultaneous synthesized Au/Al<sub>2</sub>O<sub>3</sub> catalyst.

We attribute the good performance of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> to its thermal stability. In fact, gold nanoparticles are generally highly mobile on Al<sub>2</sub>O<sub>3</sub> surfaces due to the Au–Al<sub>2</sub>O<sub>3</sub> bond energy being substantially weaker than that of Au–TiO<sub>2</sub> (ref. 17) and small gold Au nanoparticles may be more mobile than gold atoms.<sup>18</sup> Thus, the agglomeration of gold nanoparticles is problematic for the Au/Al<sub>2</sub>O<sub>3</sub> system, especially when HAuCl<sub>4</sub> (the most common gold precursor) is involved in the preparation, because the chloride ions can significantly accelerate the agglomeration process.<sup>22</sup> Fig. 4 clearly shows the aggregation of gold deposited on Al<sub>2</sub>O<sub>3</sub> by a typical wetness impregnation method calcined at 350 °C in air. Though the oxidation of benzyl alcohol is run at relatively low temperatures, the agglomeration may be even higher due to the influence of the hot liquid. As shown in Fig. 1, in the simultaneous synthesis process, the reduction of gold takes place at the same time as the hydrolyzation and condensation of metal alkoxide and APTES. Three additional factors to stabilize the gold nanoparticles can be expected from this process, i) the amino head of APTES can promote even distribution of Au<sup>3+</sup> by anchoring it; ii) when gold nanoparticles form, the SiO<sub>2</sub> condenses with the Al<sub>2</sub>O<sub>3</sub> support and due to the well-known affinity between its amino head group and gold surface, the APTES can increase the interface between gold and Al<sub>2</sub>O<sub>3</sub> to stabilize gold nanoparticles; iii) although the APTES functional group was damaged after calcinations at 500 °C, the enhanced interfaces are still there to hamper the mobility of gold nanoparticles. To confirm the stability of the catalysts in the reaction, we have acquired bright-field TEM images of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> before and after reaction. As shown in Fig. 6, no observable changes in particle morphology or size can be found. Histogram indicated that size of Au particles in the materials both before and after reaction evenly distributed between the range of 2.5–5.5 nm, with peaking at 4.5–5 nm.

**Table 2** Comparative data for solvent-free aerobic oxidation of benzyl alcohol. The oxidation was carried out by bubbling oxygen into the reaction mixture (5 ml benzyl alcohol and 5 mg catalysts) at different temperatures. Results were obtained after 6 h of reaction<sup>a</sup>

T (°C)	Catalysts	Conversion	Selectivity (mol.%)
100	Al <sub>2</sub> O <sub>3</sub>	1.32	82.31
	AuSiO <sub>2</sub> @Al <sub>2</sub> O <sub>3</sub>	1.76	77.39
	Au/Al <sub>2</sub> O <sub>3</sub> DP	2.59	61.06
	Au/Al <sub>2</sub> O <sub>3</sub>	2.03	81.01
120	Al <sub>2</sub> O <sub>3</sub>	2.87	85.22
	Au/SiO <sub>2</sub> @Al <sub>2</sub> O <sub>3</sub>	6.09	88.52
	Au/Al <sub>2</sub> O <sub>3</sub> DP	3.55	67.28
	Au/Al <sub>2</sub> O <sub>3</sub>	5.90	84.72
140	Al <sub>2</sub> O <sub>3</sub>	3.08	83.24
	Au/SiO <sub>2</sub> @Al <sub>2</sub> O <sub>3</sub>	7.40	83.51
	Au/Al <sub>2</sub> O <sub>3</sub> DP	6.16	84.61
	Au/Al <sub>2</sub> O <sub>3</sub>	6.77	82.78
160	Al <sub>2</sub> O <sub>3</sub>	6.67	80.97
	Au/SiO <sub>2</sub> @Al <sub>2</sub> O <sub>3</sub>	21.90	72.32
	Au/Al <sub>2</sub> O <sub>3</sub> DP	8.99	89.33
	Au/Al <sub>2</sub> O <sub>3</sub>	10.42	75.96

<sup>a</sup> The selectivity to benzaldehyde.



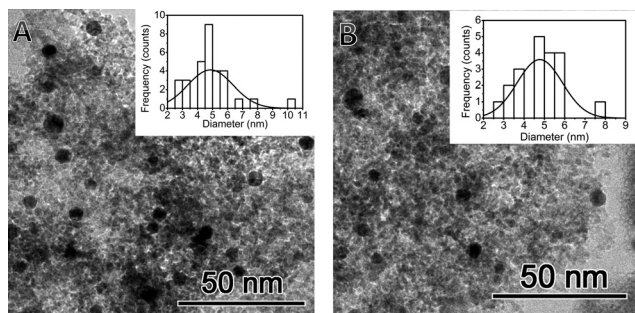


Fig. 6 Bright-field TEM images of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub> catalyst before (A) and after (B) reaction at 120 °C.

## 3. Experimental

### 3.1 Materials and instruments

Hydrogen tetrachloroaurate (HAuCl<sub>4</sub>·3H<sub>2</sub>O, 99.99%), cetyltrimethylammonium bromide (CTAB, 99%), isopropanol (99.5%) and 3-aminopropyl-triethoxysilane (APTES) were obtained from Sigma-Aldrich. Freshly calcined (550 °C) molecular sieves (4 Å) were added to the isopropanol to further remove any residual water. All other reagents were procured from Aldrich and used as received. Ultrapure deionized water (Continental Water Systems) was used throughout the experiments. Transmission electron microscopy (TEM) studies were performed on a FEI Tecnai F20 S-Twin operated at 200 kV. The samples were prepared by spreading an ethanolic suspension on carbon coated copper grids. BET and isothermal measurements were performed on a Quantachrome Nova 4000e. X-ray diffraction was acquired on a Siemens D 5000 diffractometer (Cu Kα, λ = 1.5406 Å). The diffuse reflectance UV-vis spectra were recorded on a UV4 (Unicom) spectrophotometer. Calcination was performed in a tubular furnace with a ramping rate of 3 °C per minute.

### 3.2 Synthesis of Au/SiO<sub>2</sub>@Al<sub>2</sub>O<sub>3</sub>

Hydrogen tetrachloroaurate was first dissolved in distilled water and then transferred into toluene with the help of a phase transfer agent (CTAB). Typically, an aqueous solution of hydrogen tetrachloroaurate (5 ml, 0.02 M) was added to the mixture of CTAB (50 mg) and toluene (10 ml) under vigorous stirring. After 2 h, tetrachloroaurate was completely transferred into the toluene phase to form a 0.01 M solution (solution A) and the water phase became colorless. In another flask, 1.0 g of aluminium triisopropoxide was dissolved in 50 ml pretreated anhydrous isopropanol and then 50 ml anhydrous toluene was added and stirring was maintained for 5 h to form a transparent solution. 2 ml of solution A and 0.05 ml APTES was added to this clear solution. After stirring for one more hour, 15 ml isopropanol solution containing 0.2 ml water and 5 mg sodium borohydride was added dropwise to the flask over 30 min. The gelation process was performed by maintaining stirring for 24 h at room temperature. The Al<sub>2</sub>O<sub>3</sub> gel doped with gold nanoparticles was washed three times by centrifuging, re-dispersing in a 100 ml solution

of isopropanol and toluene (1:1 by volume) and drying by supercritical treatment at 265 °C in a Parr autoclave. The obtained powder was calcined at 500 °C for 5 h under the protection of argon. The Al<sub>2</sub>O<sub>3</sub> aerogel was prepared under the same conditions without adding the gold precursor, APTES and sodium borohydride.

### 3.3 Synthesis of reference Au/Al<sub>2</sub>O<sub>3</sub> catalyst

The Au/Al<sub>2</sub>O<sub>3</sub> sample was prepared following a reported method.<sup>23</sup> In a typical experiment, 1.0 g of Al<sub>2</sub>O<sub>3</sub> aerogel was stirred in 50 ml 9.7 mM chloroauric acid for 5 h at 70 °C. Then the powder was filtered and re-suspended in 50 ml DI water. After refluxing at 70 °C for 1 h, the powder was filtered again and calcined at 350 °C for 5 h. The final product was a light pink powder, denoted as Au/Al<sub>2</sub>O<sub>3</sub>.

### 3.4 Synthesis of reference Au/Al<sub>2</sub>O<sub>3</sub> DP catalyst

The preparation of Au/Al<sub>2</sub>O<sub>3</sub> DP follows literature reports.<sup>24</sup> Typically, a solution of HAuCl<sub>4</sub>·3H<sub>2</sub>O (10 mg) in 100 ml of DI water was heated to 80 °C and adjusted to pH = 8.5 with NaOH. Al<sub>2</sub>O<sub>3</sub> aerogel (0.5 g) was then added to the solution under vigorous stirring while the pH was still maintained at 8.5 using NaOH and HCl. Once the pH stabilized, the mixture was stirred at 80 °C for 2 h. The precipitation was collected, washed several times and dried at 100 °C. The obtained powder was calcined at 450 °C for 4 h and denoted as Au/Al<sub>2</sub>O<sub>3</sub> DP.

### 3.5 Benzyl alcohol oxidation

The liquid phase oxidation of benzyl alcohol over the supported Au catalysts were carried out in a magnetically stirred 25 ml three-neck flask with oil bath heating and reflux condenser, under the following general reaction conditions: reaction mixtures = 5 ml benzyl alcohol + 5 mg catalyst, reaction time = 6 h, temperature varied from 100 °C to 160 °C in different experiments, 99.9% oxygen was bubbled into the reaction mixture at the rate of approximately 2 ml min<sup>-1</sup>. After the reaction, the reaction mixture was filtered and the liquid phase from was analyzed by a gas chromatograph equipped with a flame ionization detector, using N<sub>2</sub> as a carrier gas. The reaction products and unconverted reactants were identified by comparison with authentic standard samples. The conversion and product selectivity were calculated as follows: conversion (%) = (moles of reactant converted)/(moles of reactant in feed) × 100 and product selectivity (%) = (moles of product formed)/(moles of reactant converted).

## 4. Conclusions

In this work, we demonstrate a simultaneous synthesis process which can significantly increase the thermal stability of gold/alumina aerogel catalysts by increasing the Au–Al<sub>2</sub>O<sub>3</sub> interface and trapping gold nanoparticles in the framework of an alumina aerogel. No agglomeration was found even after 5 h calcination at 650 °C. Furthermore, the Au/Al<sub>2</sub>O<sub>3</sub> prepared by this process demonstrated superior performance

at high temperatures than that of systems prepared by deposition precipitation and wetness impregnation methods.

## Acknowledgements

The authors gratefully acknowledge Prof. Vasile I. Pârvulescu for the Diffuse-reflective UV-vis spectra measurement. RR would like to thank the National Science Foundation for support under grant CHE-1214068.

## Notes and references

- 1 A. Leyva-Perez and A. Corma, *Angew. Chem., Int. Ed.*, 2012, **51**, 614.
- 2 M. Rudolph and A. S. K. Hashmi, *Chem. Soc. Rev.*, 2012, **41**, 2448.
- 3 M. Haruta, S. Tsubota, T. Kobayashi, H. Kageyama, M. J. Genet and B. Delmon, *J. Catal.*, 1993, **144**, 175; M. Haruta, N. Yamada, T. Kobayashi and S. Iijima, *J. Catal.*, 1989, **115**, 301.
- 4 S. Bhattacharjee, D. M. Dotzauer and M. L. Bruening, *J. Am. Chem. Soc.*, 2009, **131**, 3601; A. Corma and P. Serna, *Science*, 2006, **313**, 332; V. I. Parvulescu, V. Parvulescu, U. Eudruschat, G. Filoti, F. E. Wagner, C. Kubel and R. Richards, *Chem. – Eur. J.*, 2006, **12**, 2343.
- 5 V. R. Choudhary and D. K. Dumbre, *Top. Catal.*, 2009, **52**, 1677.
- 6 A. Zwijnenburg, M. Makkee and J. A. Moulijn, *Appl. Catal., A*, 2004, **270**, 49; A. Zwijnenburg, M. Saleh, M. Makkee and J. A. Moulijn, *Catal. Today*, 2002, **72**, 59; G. Mul, A. Zwijnenburg, B. van der Linden, M. Makkee and J. A. Moulijn, *J. Catal.*, 2001, **201**, 128.
- 7 K. M. Kosuda, A. Wittstock, C. M. Friend and M. Baumer, *Angew. Chem., Int. Ed.*, 2012, **51**, 1698; P. Rodriguez, Y. Kwon and M. T. M. Koper, *Nat. Chem.*, 2012, **4**, 177; H. F. Guo, A. Al-Hunaiti, M. Kemell, S. Rautiainen, M. Leskela and T. Repo, *ChemCatChem*, 2011, **3**, 1872; J. C. Hu, L. F. Chen, K. K. Zhu, A. Suchopar and R. Richards, *Catal. Today*, 2007, **122**, 277; D. I. Enache, J. K. Edwards, P. Landon, B. Solsona-Espriu, A. F. Carley, A. A. Herzing, M. Watanabe, C. J. Kiely, D. W. Knight and G. J. Hutchings, *Science*, 2006, **311**, 362; Z. Li, C. V. Ciobanu, J. C. Hu, J. P. Palomares-Baez, J. L. Rodriguez-Lopez and R. Richards, *Phys. Chem. Chem. Phys.*, 2011, **13**, 2582.
- 8 H. Tsunoyama, Y. M. Liu, T. Akita, N. Ichikuni, H. Sakurai, S. H. Xie and T. Tsukuda, *Catal. Surv. Asia*, 2011, **15**, 230.
- 9 A. Corma and M. E. Domine, *Chem. Commun.*, 2005, 4042; M. Besson and P. Gallezot, *Catal. Today*, 2000, **57**, 127.
- 10 J. M. Thomas, R. Raja, G. Sankar and R. G. Bell, *Nature*, 1999, **398**, 227; H. Zhao, J. C. Zhou, H. Luo, C. Y. Zeng, D. H. Li and Y. J. Liu, *Catal. Lett.*, 2006, **108**, 49; R. Zhao, D. Ji, G. M. Lv, G. Qian, L. Yan, X. L. Wang and J. S. Suo, *Chem. Commun.*, 2004, 904.
- 11 K. K. Zhu, J. C. Hu and R. Richards, *Catal. Lett.*, 2005, **100**, 195.
- 12 F. Boccuzzi, A. Chiorino, M. Manzoli, P. Lu, T. Akita, S. Ichikawa and M. Haruta, *J. Catal.*, 2001, **202**, 256; E. D. Park and J. S. Lee, *J. Catal.*, 1999, **186**, 1.
- 13 S. Ivanova, W. Pitchon, Y. Zimmermann and C. Petit, *Appl. Catal., A*, 2006, **298**, 57.
- 14 P. M. Arnal, M. Comotti and F. Schüth, *Angew. Chem.*, 2006, **118**, 8404.
- 15 M. M. Biener, J. Biener, A. Wichmann, A. Wittstock, T. F. Baumann, M. Baumer and A. V. Hamza, *Nano Lett.*, 2011, **11**, 3085.
- 16 L. F. Chen, J. C. Hu and R. Richards, *J. Am. Chem. Soc.*, 2009, **131**, 914; X. Wang, L. F. Chen, M. Shang, F. Lin, J. C. Hu and R. M. Richards, *Nanotechnology*, 2012, **23**, 294010.
- 17 S. Lee, C. Y. Fan, T. P. Wu and S. L. Anderson, *J. Phys. Chem. B*, 2005, **109**, 11340.
- 18 J. Carrey, J. L. Maurice, F. Petroff and A. Vaures, *Surf. Sci.*, 2002, **504**, 75.
- 19 S. Eustis and M. El-Sayed, *J. Phys. Chem. B*, 2005, **109**, 16350.
- 20 N. Dimitratos, J. A. Lopez-Sanchez and G. J. Hutchings, *Chem. Sci.*, 2012, **3**, 20.
- 21 V. R. Choudhary, R. Jha and P. Jana, *Green Chem.*, 2007, **9**, 267; V. R. Choudhary, A. Dhar, P. Jana, R. Jha and B. S. Uphade, *Green Chem.*, 2005, **7**, 768.
- 22 J. H. Yang, J. D. Henao, C. Costello, M. C. Kung, H. H. Kung, J. T. Miller, A. J. Kropf, J. G. Kim, J. R. Regalbuto, M. T. Bore, H. N. Pham, A. K. Datye, J. D. Laeger and K. Kharas, *Appl. Catal., A*, 2005, **291**, 73.
- 23 J. T. Calla and R. J. Davis, *Ind. Eng. Chem. Res.*, 2005, **44**, 5403.
- 24 V. R. Choudhary and D. K. Dumbre, *Catal. Commun.*, 2009, **10**, 1738.