

## Dioxygen Evolution from Inorganic Systems. Water Oxidation Mediated by RuO<sub>2</sub> and TiO<sub>2</sub>–RuO<sub>2</sub> Colloids

CLAUDIO MINERO, EUGENIO LORENZI, EDMONDO PRAMAURO and EZIO PELIZZETTI

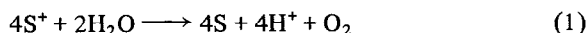
*Istituto di Chimica Analitica, Università di Torino, Turin, Italy*

Received July 1, 1983

*The kinetics of reduction of aqueous solutions of Ce<sup>IV</sup> and Ru(bpy)<sub>3</sub><sup>3+</sup> in the presence of catalytic amounts of RuO<sub>2</sub> colloids stabilized with polybrene and colloidal TiO<sub>2</sub> particles loaded with RuO<sub>2</sub> have been investigated by means of stopped-flow spectrophotometric techniques. The effect of pH, catalyst preparation and loading concentration have been considered. The TiO<sub>2</sub>/RuO<sub>2</sub> colloidal particles (45 nm radius) are extremely active catalysts.*

### Introduction

The formation of dioxygen in the reaction of water with sufficiently powerful oxidants is of interest in ascertaining the chemical mechanism in plant photosynthesis [1] and developing systems affording water cleavage by visible light [2]. Finely divided noble metal oxides (PtO<sub>2</sub>, IrO<sub>2</sub>, RuO<sub>2</sub>) have recently been shown to be capable of mediating O<sub>2</sub> evolution from water [3–5] through the reaction



where S<sup>+</sup>/S represents the redox couple; production of O<sub>2</sub> was observed when the oxidant was Ce<sup>4+</sup>, Ru(bpy)<sub>3</sub><sup>3+</sup> or Fe(bpy)<sub>3</sub><sup>3+</sup>.

Whether used as a powder [3, 4] or in colloidal form [3, 4, 6–8] or deposited onto some supporting material like TiO<sub>2</sub> [9–11], or CdS [12], or zeolite [5], RuO<sub>2</sub> is generally recognized as one of the best catalysts for dioxygen evolution.

The present paper reports on the reaction kinetics of Ce<sup>4+</sup> and Ru(bpy)<sub>3</sub><sup>3+</sup> disappearance in the presence of RuO<sub>2</sub> colloids and ruthenium dioxide bound to TiO<sub>2</sub>.

### Experimental

#### Reagents

Ruthenium tetraoxide and titanium tetrachloride were obtained from Pierce Inorganics. Polybrene was obtained from Aldrich.

Cerium(IV) sulfate purchased from C. Erba was diluted with H<sub>2</sub>SO<sub>4</sub> as required and standardized by

oxidimetric titration. Ru(bpy)<sub>3</sub>Cl<sub>2</sub> was obtained from F. Smith and the corresponding Ru(bpy)<sub>3</sub><sup>3+</sup> was obtained by electrooxidation and standardized spectrophotometrically at 675 nm ( $\epsilon = 420 \text{ M}^{-1} \text{ cm}^{-1}$ ) [13].

#### Preparation of Catalysts

The colloids of RuO<sub>2</sub> stabilized with polybrene were prepared by mixing equal amounts of a solution of RuO<sub>4</sub> in water (43 mg RuO<sub>4</sub> in 43 mL H<sub>2</sub>O at 0 °C, stirred for 30 min) and a solution (0.40 g L<sup>-1</sup>) of stabilizer. The resulting solution has a green colour and spectra (see Fig. 1) collected at different times were found to be unchanged over one day. Colloidal

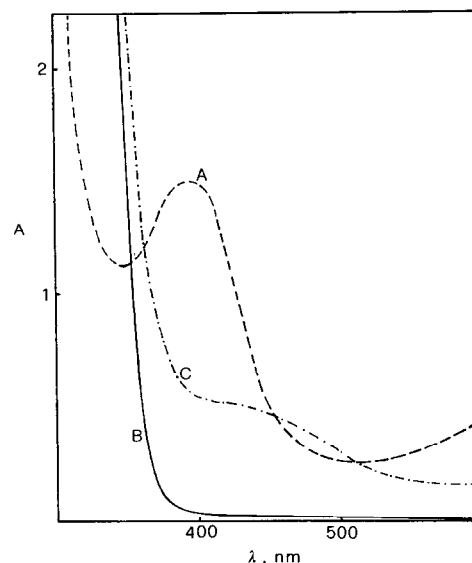


Fig. 1. Spectra of: (A) RuO<sub>2</sub> colloids stabilized with polybrene (0.41 g L<sup>-1</sup> RuO<sub>2</sub>, 0.20 g L<sup>-1</sup> polybrene; after 90 min). (B) TiO<sub>2</sub> colloids (5 g L<sup>-1</sup>) prepared according to method (A). (C) TiO<sub>2</sub> colloids, as in (B), loaded with 0.5% RuO<sub>2</sub>.

TiO<sub>2</sub> was prepared by two different methods: (A) by hydrolysis of TiCl<sub>4</sub> in water–ice mixture according to procedures previously described [14, 15]. The colloid was then dialyzed and the final pH at the end of the dialysis was adjusted to pH 2.5. (B) The hydrolysis of

$\text{TiCl}_4$  in ice-water was carried out at pH 0–1. After 15 days, a precipitate was formed; after centrifugation (3000 rpm, 5') and dilution, the aqueous phase contained colloidal  $\text{TiO}_2$  particles. This solution, kept at pH 2, was stable for months. The  $\text{RuO}_2$  loading was carried out by mixing in the proper proportions  $\text{RuO}_4$  ( $1 \text{ g L}^{-1}$ ) dissolved in water without stabilizer, with the  $\text{TiO}_2$  colloids ( $5 \text{ g L}^{-1}$ ) at room temperature; after 30 min the solution turned brown and the spectrum was stable over several weeks for both colloids (A) and (B) (at pH 3) (see Fig. 1). At pH 5 the catalyst (A) flocculates after a few minutes whereas catalyst (B) is stable for at least some hours, and for longer times at pH 12.

The Ti and Ru content was determined by atomic absorption spectroscopy. The particle size of the prepared colloids was determined by photon correlation spectroscopy as described in the next paragraph.

### Characterization of the Catalysts

Quasielastic light scattering was used to characterize the colloidal aggregates. The light scattering was detected at  $20^\circ$  (forward scatter) and  $90^\circ$  using the laser light scattering apparatus previously described [16]. The signal from the photomultiplier was put through an amplifier and discriminator to a correlator. The correlation function thus obtained yielded a diffusion coefficient  $1/\tau = 2DK^2$ , where  $\tau$  is the correlation time and  $K = 4\pi n/\lambda \sin \theta/2$  ( $n$  is the refractive index and  $\lambda$  the wavelength of the incident beam). The diffusion coefficient in turn, when substituted in the Stokes–Einstein equation gave the hydrodynamic radius ( $\eta$  is the microviscosity of the dispersion medium)

$$R_H = \frac{kT}{6\pi\eta D}$$

The hydrodynamic radii of polybrene stabilized  $\text{RuO}_2$  was found to be around 30 nm while those of the  $\text{TiO}_2$ – $\text{RuO}_2$  catalysts were 5 and 45 nm for colloids prepared by methods (A) and (B), respectively.

### Methods

Absorption spectra and slow kinetics were recorded on a Cary 219 spectrophotometer. The faster reaction kinetics were followed with a Durrum stopped-flow spectrophotometer. The  $\text{Ce}^{4+}$  reactions were monitored at 318 nm ( $\epsilon_{318} = 5580 \text{ M}^{-1} \text{ cm}^{-1}$ ) [17], while for  $\text{Ru}(\text{bpy})_3^{3+}$  452 nm was used ( $\epsilon_{452} = 1.35 \times 10^4 \text{ M}^{-1} \text{ cm}^{-1}$ ). pH was controlled with a Metrohm E 388 potentiometer and was brought to the desired value through addition of HCl or NaOH solutions.

Dioxygen evolution was measured by gas chromatography (C. Erba) using Ar as a carrier in the system  $\text{Ru}(\text{bpy})_3^{3+}$  ( $4 \times 10^{-3} \text{ M}$ ) in the presence of  $\text{TiO}_2(\text{B})$ – $\text{RuO}_2$  ( $0.05 \text{ g L}^{-1}$ , 0.32%  $\text{RuO}_2$ ).

## Results and Discussion

The ability of  $\text{RuO}_2$  to mediate  $\text{O}_2$  evolution from water using the test system  $\text{Ce}^{4+}$  has been reported by Kiwi and Grätzel [3]. The mechanism of this process has recently been investigated by different groups [18, 19].

The present results show that  $\text{Ce}^{4+}$  decays at a first order rate (see oscilloscope traces in Fig. 2) in the presence of polybrene stabilized  $\text{RuO}_2$  colloids. The first order rate constants are virtually independent of initial  $\text{Ce}^{4+}$  concentration in the range  $2$ – $5 \times 10^{-5} \text{ M}$  (and in the range  $0.0005$ – $0.02 \text{ g L}^{-1}$  of  $\text{RuO}_2$ ; the rate constants have however a tendency to increase with decreasing  $\text{Ce}^{4+}$  concentration at higher [ $\text{RuO}_2$ ] values).

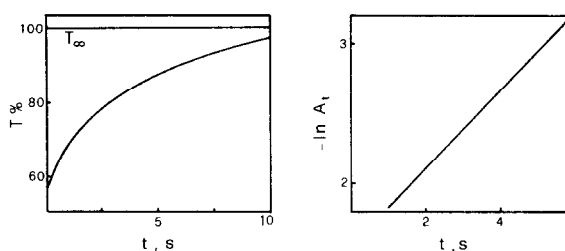


Fig. 2. Oscilloscope trace and first order plot for the  $\text{Ce}^{\text{IV}}$  decay at 318 nm.  $\text{RuO}_2$   $0.005 \text{ g L}^{-1}$ ; polybrene  $0.015 \text{ g L}^{-1}$ ;  $\text{H}_2\text{SO}_4$   $0.09 \text{ M}$ ;  $25^\circ \text{C}$ .

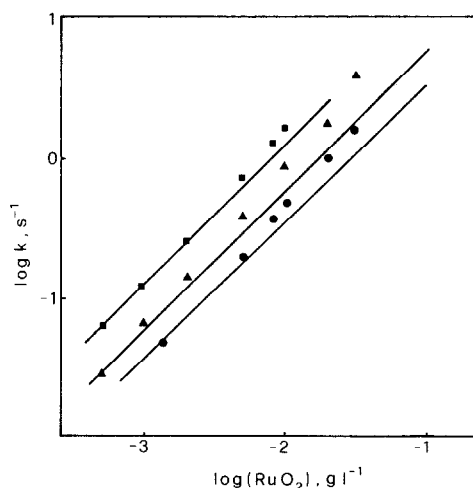


Fig. 3. Dependence of the observed rate constant of  $\text{Ce}^{\text{IV}}$  decay on  $\text{RuO}_2$  amount at different temperatures: (●)  $25^\circ \text{C}$ ; (▲)  $35^\circ \text{C}$ ; (■)  $45^\circ \text{C}$ .  $\text{Ce}^{\text{IV}}$   $4.5 \times 10^{-5} \text{ M}$ ; polybrene  $0.015 \text{ g L}^{-1}$ ;  $\text{H}_2\text{SO}_4$   $0.09 \text{ M}$ .

Figure 3 shows the dependence of the rate constants on the  $\text{RuO}_2$  concentration, at different temperatures. In the investigated range of catalyst concentration a satisfactory linearity can be observed particularly in the first part, while at increasing catalyst concentration (and particularly at lower

$[\text{Ce}^{4+}]$ ) deviation toward higher orders can be observed. A similar dependence has been reported for the  $\text{Fe}(\text{bpy})_3^{3+}$  reaction in the presence of copolymer stabilized  $\text{RuO}_2$  colloids [6], although in a more restricted concentration range, and in the presence of  $\text{MnO}_2$  based catalyst [20]. It is noteworthy that the presence of small amounts of catalyst enhances the  $\text{Ce}^{4+}$  decomposition by *ca.* three orders of magnitude; *e.g.* at 35 °C,  $[\text{Ce}^{\text{IV}}] = 4.5 \times 10^{-5} \text{ M}$ ,  $[\text{H}_2\text{SO}_4] = 0.09 \text{ M}$ , the rate constant of decay in the presence of 0.02 g  $\text{L}^{-1}$  of  $\text{RuO}_2$  is  $1.9 \text{ s}^{-1}$  (the rate constant is  $4.1 \times 10^{-3} \text{ s}^{-1}$  in the presence of 0.015 g  $\text{L}^{-1}$  of polybrene; the decay rate constant increases slightly, *i.e.* from 0.26 to  $0.41 \text{ s}^{-1}$  in going from 0.005 to  $0.021 \text{ g L}^{-1}$  of polybrene at  $[\text{Ce}^{\text{IV}}] = 4.5 \times 10^{-5} \text{ M}$ ,  $\text{RuO}_2$  0.01 g  $\text{L}^{-1}$ , 25 °C,  $[\text{H}_2\text{SO}_4] = 0.09 \text{ M}$ ). The effect of acidity has also been investigated. Table I collects the

TABLE I. Catalysed Decay Rate of  $\text{Ce}^{\text{IV}}$  at Different Acidity.<sup>a</sup>

| $[\text{H}_2\text{SO}_4], \text{ M}$ | $k_{\text{obs}}, \text{ s}^{-1}$ |
|--------------------------------------|----------------------------------|
| 0.045                                | 0.82                             |
| 0.067                                | 0.57                             |
| 0.090                                | 0.44                             |
| 0.135                                | 0.30                             |
| 0.225                                | 0.19                             |
| 0.45                                 | 0.098                            |

<sup>a</sup>  $[\text{Ce}^{\text{IV}}] = 2.3 \times 10^{-5} \text{ M}$ ,  $\text{RuO}_2 = 0.008 \text{ g L}^{-1}$ , polybrene =  $0.015 \text{ g L}^{-1}$ , 25 °C,  $I = 0.45 \text{ M}$  ( $\text{Na}_2\text{SO}_4$ ).

observed rate constants in the acidity range 0.045–0.45 M  $\text{H}_2\text{SO}_4$ . An inverse dependence on  $[\text{H}_2\text{SO}_4]$  seems to be operating in the investigated acidity range. As far as the mechanism of the reaction is concerned, a recent investigation points out that at  $[\text{Ce}^{4+}]/[\text{RuO}_2]$  ratios comparable with the present experimental conditions dioxygen evolution should be the predominant pathway; in addition it was stated that the use of a large catalytic surface area and low initial oxidant concentration should strongly decrease the corrosion of  $\text{RuO}_2$  [19].

The polybrene stabilized colloidal  $\text{RuO}_2$  catalyst was also investigated with  $\text{Ru}(\text{bpy})_3^{3+}$  as the electron acceptor. This compound is particularly interesting in connection with photochemical conversion of light energy since the  $\text{Ru}(\text{bpy})_3^{3+/2+}$  couple can participate in photoredox cycles [2]. The non catalytic reduction of  $\text{Ru}(\text{bpy})_3^{3+}$  in aqueous solution (and of related complexes such as Fe and Os complexes with 2,2'-bipyridine or 1,10-phenanthroline-like ligands) have been extensively investigated [13, 21].  $\text{O}_2$  evolution was always lower than that stoichiometrically calculated and strongly dependent on the pH of the solution. The decay rate constant of  $\text{Ru}(\text{bpy})_3^{3+}$  is enhanced by the presence of polybrene stabilized  $\text{RuO}_2$  ( $5 \times 10^{-4} \text{ g L}^{-1}$  of  $\text{RuO}_2$ ,  $0.005 \text{ g L}^{-1}$  of

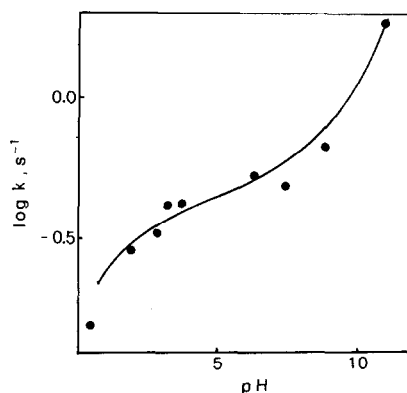


Fig. 4. Dependence of the observed rate constant of  $\text{Ru}(\text{bpy})_3^{3+}$  decay on pH.  $\text{Ru}(\text{bpy})_3^{3+} 3 \times 10^{-5} \text{ M}$ ;  $\text{RuO}_2$   $0.0005 \text{ g L}^{-1}$ ; polybrene  $0.005 \text{ g L}^{-1}$ ; 25 °C (in the range of pH 6–10, the decay is not simply first order and successive reactions take place; the reported values are based on the early part of the reaction).

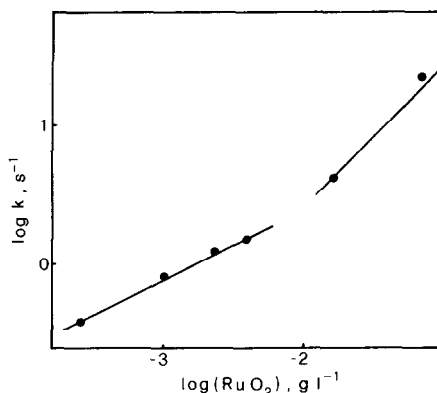


Fig. 5. Dependence of the observed rate constant of  $\text{Ru}(\text{bpy})_3^{3+}$  decay on  $\text{RuO}_2$  amount.  $\text{Ru}(\text{bpy})_3^{3+} 3 \times 10^{-5} \text{ M}$ ; polybrene  $0.005 \text{ g L}^{-1}$ ; pH 2.6; 25 °C (the straight lines are drawn with slope 1 and 2, respectively).

polybrene) by *ca.* 2 orders of magnitude. Figure 4 reports the observed rate constants as a function of pH. The dependence on  $\text{RuO}_2$  concentration shows however a deviation from a simple linear dependence (Fig. 5). The vestiges of higher order dependence on catalyst concentration that are hardly evident in Fig. 3 are evident in this system. Such behavior is not unusual in redox catalysis by colloidal particles, as has been reported before [11, 22–24].

The remarkable properties of catalysts based on semiconductor colloids loaded with redox catalysts have been recently pointed out [2, 25], in particular  $\text{RuO}_2$  loaded  $\text{TiO}_2$  has been employed in related dioxygen generating and water splitting experiments [9–11, 26]. While  $\text{O}_2$  evolution is very low in the absence of catalyst, the addition of colloidal  $\text{TiO}_2\text{--RuO}_2$  strongly enhances the  $\text{O}_2$  yield particularly in the pH range between 8 and 11. These observations are similar to previously reported  $\text{RuO}_2$  based

TABLE II.  $\text{TiO}_2$  and  $\text{RuO}_2$  Effect on  $\text{Ru}(\text{bpy})_3^{3+}$  Decay.

| $\text{TiO}_2 \text{ g L}^{-1} \text{ }^a$ | $k_{\text{obs}} (\text{s}^{-1})$ |
|--------------------------------------------|----------------------------------|
| 0.2                                        | 12.3                             |
| 0.4                                        | 7.2                              |
| 1.0                                        | 7.0                              |
| 2.0                                        | 7.7                              |
| $\text{RuO}_2 \text{ g L}^{-1} \text{ }^b$ |                                  |
| —                                          | $3.7 \times 10^{-3} \text{ }^c$  |
| $5 \times 10^{-3}$                         | 7.0                              |
| $8 \times 10^{-3}$                         | 16.1                             |
| $1 \times 10^{-2}$                         | 22.4                             |

$[\text{Ru}(\text{bpy})_3^{3+}] = 1.5 \times 10^{-5} \text{ M}$   
 $\text{pH} = 2$

<sup>a</sup>  $\text{RuO}_2 = 0.005 \text{ g L}^{-1}$  constant. <sup>b</sup>  $\text{TiO}_2 = 1 \text{ g L}^{-1}$  constant.

<sup>c</sup> In absence of  $\text{RuO}_2$ , the rate constant for the decay of  $\text{Ru}(\text{bpy})_3^{3+}$  is  $(3.2 \pm 0.5) \times 10^{-3} \text{ s}^{-1}$  in the range  $1\text{--}2 \text{ g L}^{-1}$  of  $\text{TiO}_2$ .

catalytic systems [4, 5]. The dependence of the rate constants on initial  $\text{Ru}(\text{bpy})_3^{3+}$  concentration was investigated using colloid prepared by method (A); increasing the initial oxidant concentration decreases the observed rate (e.g. with  $\text{TiO}_2$   $1 \text{ g L}^{-1}$ ,  $\text{RuO}_2$   $0.005 \text{ g L}^{-1}$ :  $[\text{Ru}(\text{bpy})_3^{3+}] = 3.2 \times 10^{-5} \text{ M}$ ,  $k = 4.9 \text{ s}^{-1}$ ;  $[\text{Ru}(\text{bpy})_3^{3+}] = 1.4 \times 10^{-5} \text{ M}$ ,  $k = 7.5 \text{ s}^{-1}$ ). However the first-order decay plots were satisfactorily linear up to three half-lives. The effect of different degrees of loading was also investigated. Table II reports the data obtained at constant  $\text{TiO}_2$  concentration and different degrees of  $\text{RuO}_2$  loading as well as the reverse situation. In going from 0.5 to 2.0 or 2.5% of  $\text{RuO}_2$  the rate constant is increased by a factor of 2–3. It was previously reported that the loading has no further relevant effect above these values [11]. Finally the effect of catalyst concentration was explored. Figure 6 shows the results: at high catalyst

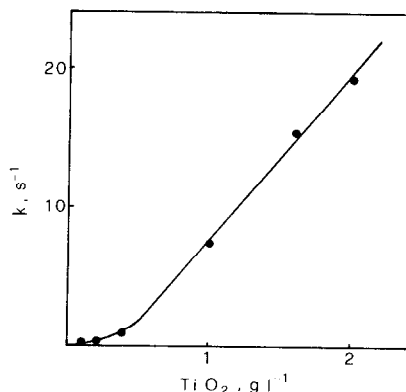


Fig. 6. Effect of the catalyst concentration on the observed rate constant for  $\text{Ru}(\text{bpy})_3^{3+}$  decay.  $\text{TiO}_2(\text{A})$ ;  $\text{RuO}_2$  0.5%;  $\text{Ru}(\text{bpy})_3^{3+}$   $1.4 \times 10^{-5} \text{ M}$ ;  $\text{pH} 2$ ;  $25^\circ \text{C}$ .

concentration ( $>0.5 \text{ g L}^{-1}$ ) a linear dependence can be observed, whereas at lower values a sharp decrease occurs:  $k = 1.1 \text{ s}^{-1}$  ( $\text{TiO}_2$   $0.4 \text{ g L}^{-1}$ ), 0.12 (0.2), 0.04 (0.1). This behavior is not unusual and similar trends were reported in  $\text{H}_2$  generation from gold [27] and platinum colloids [22–24]. The  $\text{TiO}_2\text{--RuO}_2$  colloids prepared by method (B) exhibited a higher catalytic activity compared with catalyst (A) and better stability at  $\text{pH} \geq 5$ . Figure 7 reports the observed rate constants in the presence of  $\text{TiO}_2\text{--RuO}_2$  (B) catalyst compared with those observed in the presence of  $\text{TiO}_2$  alone and in the absence of any added colloids over a wide range of  $\text{pH}$ .

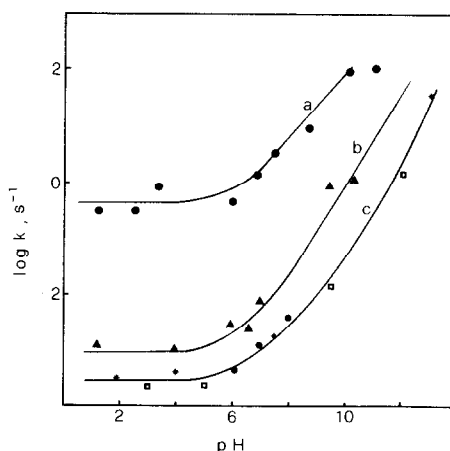


Fig. 7. Effect of  $\text{pH}$  on the observed rate constant for  $\text{Ru}(\text{bpy})_3^{3+}$  decay.  $\text{Ru}(\text{bpy})_3^{3+}$   $1.5 \times 10^{-5} \text{ M}$ ;  $25^\circ \text{C}$ . a) In the presence of  $\text{TiO}_2\text{--RuO}_2$ :  $\text{TiO}_2(\text{B})$   $0.02 \text{ g L}^{-1}$ ;  $\text{RuO}_2$  0.5%; b) in the presence of  $\text{TiO}_2$ :  $\text{TiO}_2(\text{B})$   $0.02 \text{ g L}^{-1}$ ; c) in the absence of catalyst: (\*) present work; (■) ref. 13; (●) ref. 20.

The non catalytic rate constants for the reduction of  $\text{Ru}(\text{bpy})_3^{3+}$  to  $\text{Ru}(\text{bpy})_3^{2+}$  are in agreement with previously reported data [13, 20]. Very little improvement can be obtained with  $\text{TiO}_2$  colloids, while an increase of about 2–3 orders of magnitude can be observed in the presence of  $0.02 \text{ g L}^{-1}$   $\text{TiO}_2$  loaded with  $0.0001 \text{ g L}^{-1}$   $\text{RuO}_2$ . At  $\text{pH} < 6$  the rate constant is nearly independent of acidity, while between  $\text{pH} 6$  and  $10$  a dependence can be seen. At the higher  $\text{pH}$ , the rate limit is probably the diffusional encounter between the oxidant and the colloidal particle. From the mechanistic point of view, the role of  $\text{RuO}_2$  may be envisaged as a defect electron storage system; similar concepts were previously developed to rationalize redox catalysis by  $\text{RuO}_2$  as well as by other colloids [4, 21, 22].

The present results for the  $\text{TiO}_2/\text{RuO}_2$  catalyst can be compared with a study carried out by means of combined flash photolytic and conductometric techniques on a similar confunctional catalyst [11]; although the preparation and the characteristics of the catalysts exhibit some differences, similar conclusions have been reached.

The present results confirm the superior activity of this supported catalyst over the  $\text{RuO}_2$  powder or stabilized  $\text{RuO}_2$  colloids in the acceleration of the  $\text{Ru}(\text{bpy})_3^{3+}$  reaction, particularly in the direction of  $\text{O}_2$  evolution [28]. A parallel observation is that a platinum coated  $\text{TiO}_2$  colloid showed remarkable catalytic properties toward dihydrogen evolution compared with Pt colloid alone [29]. The extremely high reaction rate observed in the present system, particularly at pH 9–10, makes these colloidal  $\text{TiO}_2$  particles loaded with  $\text{RuO}_2$  promising catalysts for cyclic water cleavage.

#### Acknowledgements

We thank Prof. M. Grätzel and Dr. J. Kiwi for providing us with the manuscript of ref. 19 before publication. Part of this work was presented in the thesis of E. L. at the University of Torino. The work was performed with financial support from Progetto Finalizzato Chimica Fine e Secondaria, CNR (Rome).

#### References

- 1 M. Calvin, *Photochem. Photobiol.*, **23**, 425 (1976); H. Metner ed., 'Photosynthetic Oxygen Evolution', Academic Press, New York, 1978; Govindjee ed., 'Bioenergetics of Photosynthesis', Academic Press, New York, 1975; A. Harriman and J. Barber in 'Topics of Photosynthesis', J. Barber ed., Elsevier, Amsterdam, 1979.
- 2 'Solar Energy Photochemical Conversion and Storage', S. Claesson and B. Holmström eds., National Swedish Board for Energy Source Development, WE 1982:14, Stockholm, 1982; J. S. Connolly ed., 'Photochemical Conversion and Storage of Solar Energy', Academic Press, New York, 1980; J. Kiwi, E. Borgarello, E. Pelizzetti, M. Visca and M. Grätzel, 'Photogeneration of Hydrogen', A. Harriman and M. A. West eds., Academic Press, London, 1982; J. Kiwi, K. Kalyanasundaram and M. Grätzel, *Struct. Bonding (Berlin)*, **49**, 37 (1982).
- 3 J. Kiwi and M. Grätzel, *Angew. Chem., Int. Ed. Engl.*, **17**, 860 (1978) and **18**, 624 (1979); *Chimia*, **33**, 289 (1979).
- 4 K. Kalyanasundaram, O. Micic, E. Pramauro and M. Grätzel, *Helv. Chim. Acta*, **62**, 2432 (1979).
- 5 J. M. Lehn, J. P. Sauvage and R. Ziessel, *Nouv. J. Chim.*, **3**, 423 (1979) and **4**, 355 (1980); J. P. Collin, J. M. Lehn and R. Ziessel, *ibid.*, **6**, 405 (1982).
- 6 E. Pramauro and E. Pelizzetti, *Inorg. Chim. Acta Lett.*, **45**, L131 (1980).
- 7 J. Kiwi, *J. Chem. Soc. Faraday Trans.*, **2**, **78**, 339 (1982).
- 8 A. Harriman, G. Porter and P. Walters, *J. Chem. Soc. Faraday Trans.*, **2**, **77**, 2373 (1981).
- 9 E. Borgarello, J. Kiwi, E. Pelizzetti, M. Visca and M. Grätzel, *J. Am. Chem. Soc.*, **103**, 6324 (1981).
- 10 E. Borgarello, J. Kiwi, M. Grätzel, E. Pelizzetti and M. Visca, *J. Am. Chem. Soc.*, **104**, 2996 (1982).
- 11 R. Humphry-Baker, J. Lilie and M. Grätzel, *J. Am. Chem. Soc.*, **104**, 422 (1982).
- 12 K. Kalyanasundaram, E. Borgarello and M. Grätzel, *Helv. Chim. Acta*, **64**, 362 (1981).
- 13 C. Creutz and N. Sutin, *Proc. Natl. Acad. Sci. USA*, **72**, 2858 (1975).
- 14 J. Moser and M. Grätzel, *Helv. Chim. Acta*, **65**, 1436 (1982).
- 15 D. Duonghong, C. Minero, M. Grätzel and E. Pelizzetti, in preparation.
- 16 M. Corti and V. Degiorgio, *Ann. Phys.*, **3**, 303 (1978).
- 17 T. J. Sworski, *J. Am. Chem. Soc.*, **79**, 3655 (1957).
- 18 A. Mills and M. L. Zeeman, *J. Chem. Soc. Chem. Comm.*, 948 (1981); A. Mills, *J. Chem. Soc. Dalton*, 1213 (1982).
- 19 J. Kiwi, M. Grätzel and G. Blondeel, *J. Chem. Soc. Dalton*, in press.
- 20 V. Y. Shafirovich, N. K. Khannanov and A. E. Shilov, *J. Inorg. Biochem.*, **15**, 113 (1981).
- 21 G. Nord and O. Wernberg, *J. Chem. Soc. Dalton*, 867 (1972) and 845 (1975).
- 22 J. Kiwi and M. Grätzel, *J. Am. Chem. Soc.*, **101**, 7214 (1979).
- 23 D. Miller and G. McLendon, *J. Am. Chem. Soc.*, **103**, 6791 (1981).
- 24 M. S. Matheson, P. C. Lee, D. Meisel and E. Pelizzetti, *J. Phys. Chem.*, **87**, 394 (1983).
- 25 E. Pelizzetti and M. Visca in 'Energy Resources by Photochemistry and Catalysis', M. Grätzel ed., Academic Press, New York, 1983.
- 26 D. Duonghong, E. Borgarello and M. Grätzel, *J. Am. Chem. Soc.*, **103**, 4685 (1981).
- 27 D. Meisel, W. A. Mulac and M. S. Matheson, *J. Phys. Chem.*, **85**, 179 (1981).
- 28 E. Borgarello and E. Pelizzetti, *Inorg. Chim. Acta*, following paper.
- 29 E. Borgarello, E. Pelizzetti, W. A. Mulac and D. Meisel, in preparation.