

3, bp 70°C (8 mm),  $n_D^{20}$  1.4471; 83% yield. IR spectrum ( $\nu$ ,  $\text{cm}^{-1}$ ): 1160 (S=O). PMR spectrum ( $\text{CCl}_4$ , HMDS;  $\delta$ , ppm): 1.08 t (6H,  $\text{CH}_3$ ), 3.08 split q (4H,  $\text{CH}_2\text{N}$ ), 3.33 s (3H,  $\text{CH}_3\text{O}$ ). Mass spectrum (EI, 70 eV),  $m/z$  ( $I_{\text{rel}}$ , %): 151  $[\text{M}]^+$  (46), 136  $[\text{M}-\text{Me}]^+$  (47), 120  $[\text{M}-\text{OMe}]^+$  (100), 92  $[\text{M}-\text{OMe}-\text{C}_2\text{H}_4]^+$  (63), 79  $[\text{M}-72]^+$  (78), 72  $[\text{EtNH}=\text{CHCH}_3]^+$  (52), 64  $[\text{SO}_2]^+$  (68), 58  $[\text{EtNH}=\text{CH}_2]^+$  (18).

4, bp 84-85°C (8 mm),  $n_D^{20}$  1.4430; 56% yield. IR spectrum ( $\nu$ ,  $\text{cm}^{-1}$ ): 1160 (S=O). PMR spectrum ( $\delta$ , ppm): 1.08 t (6H,  $\text{CH}_3$ ), 1.31 s [9H,  $(\text{CH}_3)_3\text{C}$ ], 2.98 q (4H,  $\text{CH}_2\text{N}$ ). Mass spectrum (EI, 70 eV),  $m/z$  ( $I_{\text{rel}}$ , %): 193  $[\text{M}]^+$  (3), 137  $[\text{M}-i-\text{C}_4\text{H}_8]^+$  (6), 136  $[\text{M}-t\text{-Bu}]^+$  (1), 120  $[\text{M}-\text{OBu}-t]^+$  (67), 92  $[\text{M}-\text{OBu}-t-\text{C}_2\text{H}_4]^+$  (16), 73  $[\text{M}-i-\text{C}_4\text{H}_8-64]^+$  (37), 72  $[\text{EtNH}=\text{CHCH}_3]^+$  (14), 64  $[\text{SO}_2]^+$  (32), 58  $[\text{EtNH}=\text{CH}_2]^+$  (100).

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### DEHYDROGENATION OF ISOBUTANE WITH CARBON DIOXIDE ON MANGANESE-CONTAINING CATALYSTS

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We previously reported [1, 2] the possibility of using  $\text{CO}_2$  as an oxidant in heterogeneous catalytic processes.

The possibility of selective dehydrogenation of isobutane by a nontraditional oxidant, carbon dioxide, was demonstrated and the results of conversion of isobutane in the presence of  $\text{CO}_2$  on manganese-containing catalysts are reported in the present article.

It was shown that dehydrogenation of isobutane on manganese catalysts modified with variable-valence metal oxides by carbon dioxide, in contrast to its conversion on an aluminoplatinum catalyst [3], takes place without accumulation of coke and with stable activity and selectivity. The following reactions take place at 750°C and 3600  $\text{h}^{-1}$ : dehydrogenation into isobutylene, selective decomposition into propylene, accompanied by reduction of  $\text{CO}_2$  to CO as a result of partial binding of the carbon dioxide oxygen by hydrogen with rupture of the C-H bond in isobutane. The yield of isobutylene (for the isobutane used) is 35% for 65% conversion of isobutane.

Isobutylene is formed according to a redox scheme, and the side reaction of decomposition of isobutane into propylene is the result of thermal cleavage of the C-C bond.

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