

CrossMark  
click for updatesCite this: *RSC Adv.*, 2014, 4, 61817

# Equilibrium and kinetic studies of Se(vi) removal by Mg–Al layered double hydroxide doped with Fe<sup>2+</sup>

Tomohito Kameda,\* Eisuke Kondo and Toshiaki Yoshioka

Mg–Al layered double hydroxide (Mg–Al LDH) doped with Fe<sup>2+</sup> was found to be superior to undoped Mg–Al LDH in the removal of Se(vi) from aqueous solutions. For both systems, Se(vi) as SeO<sub>4</sub><sup>2−</sup> was removed through anion exchange with intercalated Cl<sup>−</sup>. In the Fe<sup>2+</sup>-doped Mg–Al LDH, however, some of the Se(vi) was reduced to Se(iv) upon oxidation of Fe<sup>2+</sup> to Fe<sup>3+</sup> in the LDH host layer to produce SeO<sub>3</sub><sup>2−</sup>, which was also adsorbed by the Fe<sup>2+</sup>-doped Mg–Al LDH through anion exchange. The reduction of Se(vi) to Se(iv) is advantageous for Se(vi) removal by Fe<sup>2+</sup>-doped Mg–Al LDH due to the larger charge density of SeO<sub>3</sub><sup>2−</sup>. The Fe<sup>2+</sup>-doped Mg–Al LDH effectively removed Se(vi) from an aqueous solution because of the anion exchange properties of Mg–Al LDH and activity of Fe<sup>2+</sup> as a reducing agent. Se(vi) removal occurs through Langmuir-type adsorption, where the maximum adsorption and equilibrium adsorption constant were 1.4 mmol g<sup>−1</sup> and 1.6, respectively. Se(vi) removal is well expressed as a pseudo second-order reaction. The apparent rate constants at 10, 30, and 60 °C were 1.2 × 10<sup>−3</sup>, 1.5 × 10<sup>−3</sup>, and 2.2 × 10<sup>−3</sup> g mmol<sup>−1</sup> min<sup>−1</sup>, respectively, and the apparent activation energy was 10.0 kJ mol<sup>−1</sup>. The rate-determining step is chemical adsorption through anion exchange of SeO<sub>4</sub><sup>2−</sup> and SeO<sub>3</sub><sup>2−</sup> with intercalated Cl<sup>−</sup>.

Received 2nd October 2014  
Accepted 10th November 2014

DOI: 10.1039/c4ra11645c

www.rsc.org/advances

## Introduction

Layered double hydroxides (LDHs) are typically represented by the formula [M<sub>1−x</sub><sup>2+</sup>M<sub>x</sub><sup>3+</sup>(OH)<sub>2</sub>] → [M<sub>1−x</sub><sup>2+</sup>M<sub>x</sub><sup>3+</sup>(OH)<sub>2</sub>], where M<sup>2+</sup> and M<sup>3+</sup> are divalent and trivalent metal ions, respectively; x denotes the M<sup>3+</sup>/(M<sup>2+</sup> + M<sup>3+</sup>) molar ratio (0.20 ≤ x ≤ 0.33); and A<sup>n−</sup> is, for example, CO<sub>3</sub><sup>2−</sup> or Cl<sup>−</sup>.<sup>1–4</sup> An LDH consists of stacked M<sup>3+</sup>-bearing brucite-like octahedral layers, where some of the M<sup>3+</sup> is replaced by M<sup>2+</sup>, in which the charge of the positive layer is electrically neutralized by interlayer anions. The interlayer space is occupied by water molecules in the hydration shell of these intercalated anions. LDHs have been investigated as promising materials for water preservation and purification. For example, LDHs can adsorb oxometalates such as arsenite, arsenate, chromate, selenite, and selenate from aqueous solutions.<sup>5–13</sup> We have also examined the removal of antimonate using LDHs.<sup>14–16</sup> On the other hand, magnetic chitosan composites are known to be a novel material that exhibits good sorption behavior toward various toxic metal in aqueous solution.<sup>17</sup>

In our recent study, a Mg–Al LDH doped with Fe<sup>2+</sup> was prepared by co-precipitation, where some Mg<sup>2+</sup> ions in the LDH host layer were replaced with Fe<sup>2+</sup>, and used to remove Cr(vi) from an aqueous solution through anion exchange.<sup>18</sup> Cr(vi) was

reduced to Cr(III) upon the oxidation of Fe<sup>2+</sup> to Fe<sup>3+</sup>, and the resultant Cr(III) combined with OH<sup>−</sup> to produce Cr(OH)<sub>3</sub>. In this study, the Fe<sup>2+</sup>-doped Mg–Al LDH was applied to the removal of Se(vi) from aqueous solutions, as Se also forms toxic compounds. Se commonly exists as Se(vi) and Se(iv) in aqueous solutions. Although Se was added as one of harmful substances in the effluent standards in Japan in 2001, the treatment method of Se wastewater is not established sufficiently. New treatment method for Se wastewater must be developed. While Se(iv) can be removed by co-precipitation with Fe(III),<sup>19</sup> similar treatment of Se(vi) is difficult due to its high stability in aqueous solutions. In general, for adsorption method, activated carbon is known to be less effective for the removal of Se(vi) and Se(iv). Activated alumina is known to be less effective for the removal of Se(vi), although it is effective for the removal of Se(iv). However, the Fe<sup>2+</sup>-doped Mg–Al LDH can adsorb Se(vi) from an aqueous solution and reduce Se(vi) to Se(iv), which is advantageous for its removal to be adsorbed. Furthermore, equilibrium and kinetic studies were conducted to determine the properties of Se(vi) removal by the Fe<sup>2+</sup>-doped Mg–Al LDH.

## Experimental methods

Fe<sup>2+</sup>-doped Mg–Al LDH was prepared through the dropwise addition of a Mg–Fe–Al chloride solution to a NaOH solution at a constant pH, as reported in our previous paper.<sup>18</sup> The Fe<sup>2+</sup>-doped Mg–Al LDH contained 16.6 wt% Mg<sup>2+</sup>, 6.3 wt% Al<sup>3+</sup>, 8.7 wt% Fe<sup>2+</sup>, and 4.4 wt% Fe<sup>3+</sup>. An undoped Mg–Al LDH was also

Graduate School of Environmental Studies, Tohoku University, 6-6-07 Aoba, Aramaki, Aoba-ku, Sendai 980-8579, Japan. E-mail: kameda@env.che.tohoku.ac.jp; Fax: +81-22-795-7212; Tel: +81-22-795-7212

prepared through the dropwise addition of a Mg–Al chloride solution to a NaOH solution at a constant pH, and it contained 25.0 wt%  $\text{Mg}^{2+}$  and 6.8 wt%  $\text{Al}^{3+}$ .

An aqueous  $\text{Se}(\text{vi})$  solution containing  $\text{SeO}_4^{2-}$  ions was prepared by dissolving  $\text{Na}_2\text{SeO}_4$  in deionized water. The  $\text{Fe}^{2+}$ -doped Mg–Al LDH and undoped Mg–Al LDH were added to 500 mL of 1 mM  $\text{Se}(\text{vi})$  solution, and the resultant suspension was stirred at 10–60 °C for 120 min, with continuous  $\text{N}_2$  bubbling. Samples of the suspension were collected at different time intervals and immediately filtered through a 0.45  $\mu\text{m}$  membrane filter. The filtrates were analyzed for residual Se. In order to determine the adsorption isotherm of  $\text{Se}(\text{vi})$  adsorbed by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH, 20 mL of 0.5–25 mM  $\text{Se}(\text{vi})$  solution and 0.2 g of  $\text{Fe}^{2+}$ -doped Mg–Al LDH were placed in 50 mL screw-top tubes and shaken at 30 °C for 24 h.

The two types of LDHs before and after removal of  $\text{Se}(\text{vi})$  were analyzed by X-ray diffraction (XRD) using  $\text{Cu K}\alpha$  radiation. The  $\text{Fe}^{2+}$ -doped Mg–Al LDH after removal of  $\text{Se}(\text{vi})$  was dissolved in 1 M HCl, and the  $\text{Fe}^{2+}$  concentration was determined by performing UV-Vis spectroscopy at 510 nm using the phenanthroline method. Furthermore, the oxidation state of Se in the LDH after removal of  $\text{Se}(\text{vi})$  was investigated using X-ray photoelectron spectroscopy (XPS). For the adsorption experiments, the residual concentration of Se in the filtrates was determined using inductively coupled plasma-atomic emission spectrometry (ICP-AES), with an error of 0.1  $\text{mg L}^{-1}$ .†

## Results and discussion

Fig. 1 and 2 show the variations in  $\text{Se}(\text{vi})$  removal over time with  $\text{Fe}^{2+}$ -doped Mg–Al LDH and Mg–Al LDH. The molar ratios of Al in the LDH to  $\text{Se}(\text{vi})$  in the solution (Al/Se molar ratios) were set at 1 to 3. For both LDHs,  $\text{Se}(\text{vi})$  removal increased with time for all Al/Se molar ratios, showing that the LDHs could remove  $\text{Se}(\text{vi})$  from aqueous solution. The  $\text{Se}(\text{vi})$  removal also increased with increasing Al/Se molar ratios, indicating that increased amounts of LDH resulted in increased uptake of  $\text{Se}(\text{vi})$ . This was caused by the increase of adsorption site for  $\text{Se}(\text{vi})$ . However,  $\text{Se}(\text{vi})$  removal for the  $\text{Fe}^{2+}$ -doped Mg–Al LDH was consistently larger than that for the undoped Mg–Al LDH when Al/Se = 1 and 2. This implies the activity of the  $\text{Fe}^{2+}$  as a reducing agent, and is discussed later. When Al/Se = 3, the  $\text{Se}(\text{vi})$  removal by  $\text{Fe}^{2+}$ -doped Mg–Al LDH was almost the same as that by undoped Mg–Al LDH, suggesting that the amount of undoped LDH was sufficiently high to remove  $\text{Se}(\text{vi})$  even without the activity of the  $\text{Fe}^{2+}$ . The  $\text{Fe}^{2+}$ -doped Mg–Al LDH had a great advantage in  $\text{Se}(\text{vi})$  removal when Al/Se = 1 and 2.

Fig. 3 shows the XRD patterns for the  $\text{Fe}^{2+}$ -doped Mg–Al LDH and undoped Mg–Al LDH before and after  $\text{Se}(\text{vi})$  removal. The XRD peaks for all samples were assigned to hydroxycarbonate of magnesium and aluminum with the formula  $\text{Mg}_6\text{Al}_2(\text{OH})_{16}\text{CO}_3 \cdot 4\text{H}_2\text{O}$  and structure of a LDH, proving that all samples had the basic LDH structure. The presence of hydroxycarbonate suggests

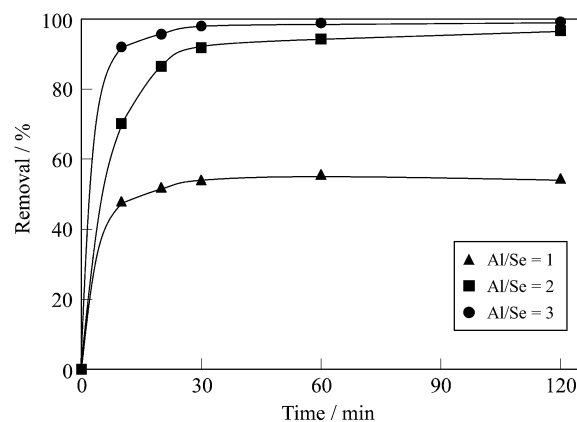


Fig. 1 Variations in  $\text{Se}(\text{vi})$  removal over time by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH with various molar ratios of Al in the LDH to  $\text{Se}(\text{vi})$  in solution at 30 °C.

that the removal of  $\text{Se}(\text{vi})$  from aqueous solution by the LDHs is due to anion exchange, that is, the intercalation of  $\text{SeO}_4^{2-}$  into the interlayers of the LDH. The XRD patterns for  $\text{Fe}^{2+}$ -doped Mg–Al LDH and undoped Mg–Al LDH after  $\text{Se}(\text{vi})$  removal (Fig. 3(b) and (d)) display (003) reflections corresponding to the basal spacing of the LDH that are broader and weaker than those before  $\text{Se}(\text{vi})$  removal (Fig. 3(a) and (c)). These reflections are likely attributable to the structural disorganization that arises from the intercalation of  $\text{SeO}_4^{2-}$ , which has a sterically bulky molecular structure. For undoped Mg–Al LDH, the basal spacing ( $d_{003}$ ) increased from 8.1 Å to 8.3 Å upon the removal of  $\text{Se}(\text{vi})$  (Fig. 3(c) and (d)), which confirms anion exchange occurred between  $\text{Cl}^-$  intercalated in the interlayer of the Mg–Al LDH and  $\text{SeO}_4^{2-}$  in the aqueous solution. On the other hand, for  $\text{Fe}^{2+}$ -doped Mg–Al LDH, the basal spacing ( $d_{003}$ ) decreased from 8.1 Å to 7.8 Å upon the removal of  $\text{Se}(\text{vi})$  (Fig. 3(a) and (b)). Table 1 shows the oxidation states of Fe and Se in the  $\text{Fe}^{2+}$ -doped Mg–Al LDH after removal of  $\text{Se}(\text{vi})$ . It was found that  $\text{Fe}^{2+}$  was oxidized to  $\text{Fe}^{3+}$  and  $\text{Se}(\text{vi})$  was reduced to  $\text{Se}(\text{iv})$ . Therefore,

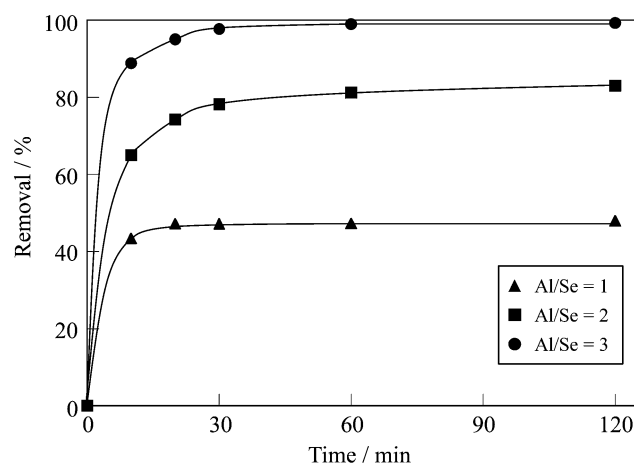


Fig. 2 Variations in  $\text{Se}(\text{vi})$  removal over time by the undoped Mg–Al LDH with various molar ratios of Al in the LDH to  $\text{Se}(\text{vi})$  in solution at 30 °C.

† Mg–Al LDH, Mg–Al layered double hydroxide; XRD, X-ray diffraction; XPS, X-ray photoelectron spectroscopy.

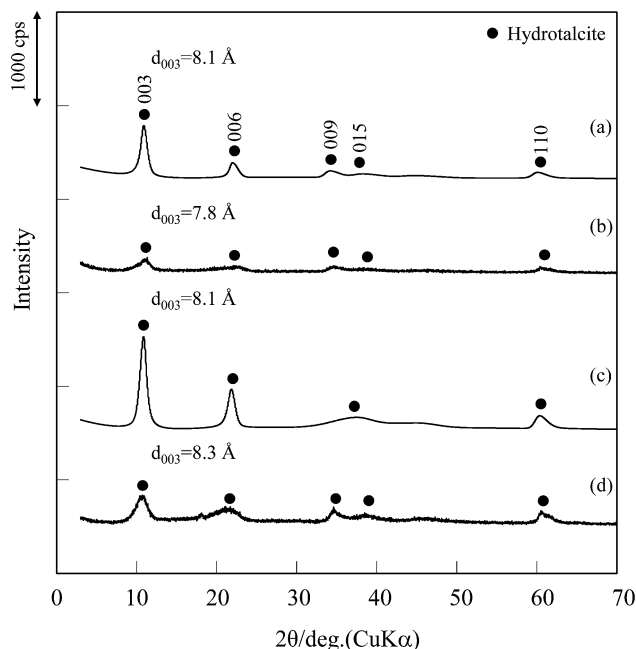


Fig. 3 XRD patterns for the  $\text{Fe}^{2+}$ -doped Mg–Al LDH (a) before and (b) after Se(vi) removal and undoped Mg–Al LDH (c) before and (d) after Se(vi) removal.

Table 1 Oxidation states of Fe and Se in  $\text{Fe}^{2+}$ -doped Mg–Al LDH after removal of Se(vi)

$\text{Fe}^{2+}/\text{Fe}$	$\text{Fe}^{3+}/\text{Fe}$	$\text{Se(IV)}/\text{Se}$	$\text{Se(vi)}/\text{Se}$
0	1	0.69	0.31

the decrease in basal spacing ( $d_{003}$ ) for the  $\text{Fe}^{2+}$ -doped Mg–Al LDH is attributed to the intercalation of  $\text{SeO}_3^{2-}$ , which has a smaller ionic radius than  $\text{SeO}_4^{2-}$ . Thus, the increased Se(vi) removal by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH compared with the undoped Mg–Al LDH is attributed to the increased charge density of  $\text{SeO}_3^{2-}$ , which is more easily exchanged with intercalated  $\text{Cl}^-$  than  $\text{SeO}_4^{2-}$ .

The schematic diagram for Se(vi) removal by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH is shown in Fig. 4. The  $\text{Fe}^{2+}$ -doped Mg–Al LDH adsorbs Se(vi) as  $\text{SeO}_4^{2-}$  from an aqueous solution through anion exchange with intercalated  $\text{Cl}^-$ . Se(vi) is reduced to Se(IV) upon oxidation of  $\text{Fe}^{2+}$  to  $\text{Fe}^{3+}$  in the LDH host layer, and the Se(IV) produced as  $\text{SeO}_3^{2-}$  is again adsorbed by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH through anion exchange with intercalated  $\text{Cl}^-$ . Se(IV) adsorption does not occur in undoped Mg–Al LDH as only  $\text{SeO}_4^{2-}$  is adsorbed by this structure. The reduction of Se(vi) to Se(IV) is advantageous for Se(vi) removal by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH due to the increased charge density of  $\text{SeO}_3^{2-}$ . The  $\text{Fe}^{2+}$ -doped Mg–Al LDH can effectively remove Se(vi) from an aqueous solution because of anion exchange properties of the LDH and activity of  $\text{Fe}^{2+}$  as a reducing agent.

Fig. 5 shows the adsorption isotherm of Se(vi) adsorbed by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH where the equilibrium adsorption increased rapidly with increasing equilibrium concentration.

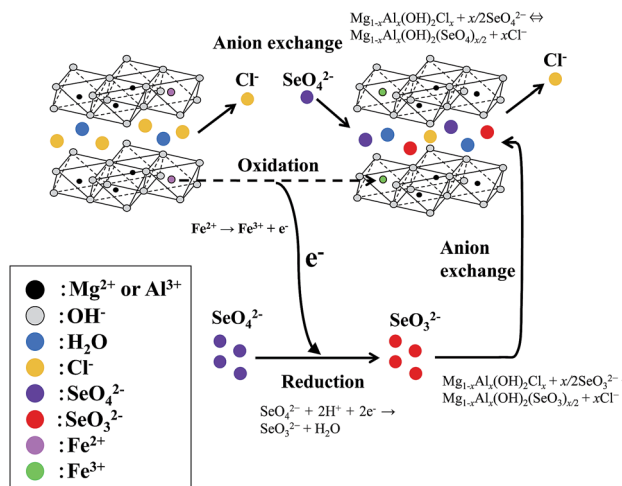


Fig. 4 Schematic diagram for Se(vi) removal by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH.

The adsorption isotherm showed Langmuir-type behavior, which was confirmed by arranging the experimental data according to the Langmuir equation, expressed as

$$q_e = C_e q_m K_L / (1 + C_e K_L), \quad (1)$$

where  $q_e$  ( $\text{mmol g}^{-1}$ ) is the equilibrium adsorption,  $C_e$  ( $\text{mM}$ ) is the equilibrium concentration,  $q_m$  ( $\text{mmol g}^{-1}$ ) is the maximum adsorption, and  $K_L$  is the equilibrium adsorption constant. This equation can also be expressed as

$$C_e/q_e = 1/q_m K_L + C_e/q_m. \quad (2)$$

Fig. 6 shows plots of  $C_e/q_e$  versus  $C_e$  for the adsorption isotherm of Se(vi) adsorbed by the  $\text{Fe}^{2+}$ -doped Mg–Al LDH. The high linearity indicates that this process follows a Langmuir-type adsorption. The values of  $q_m$  and  $K_L$ , determined from the slope and intercept of the straight line in Fig. 6, were  $1.4 \text{ mmol g}^{-1}$  and 1.6, respectively.

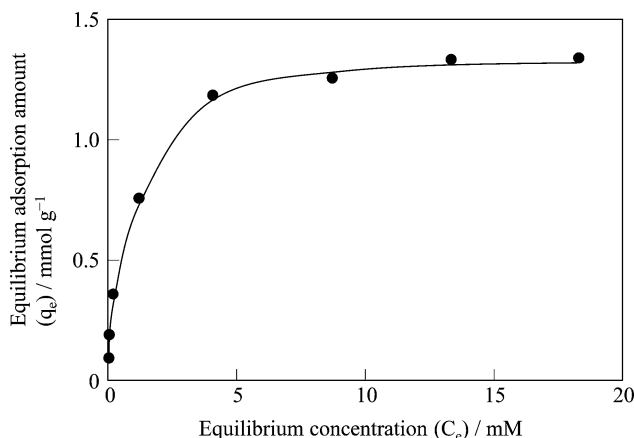


Fig. 5 Adsorption isotherm of 0.5–25 mM Se(vi) adsorbed by 0.2 g  $\text{Fe}^{2+}$ -doped Mg–Al LDH at 30 °C after 24 h.

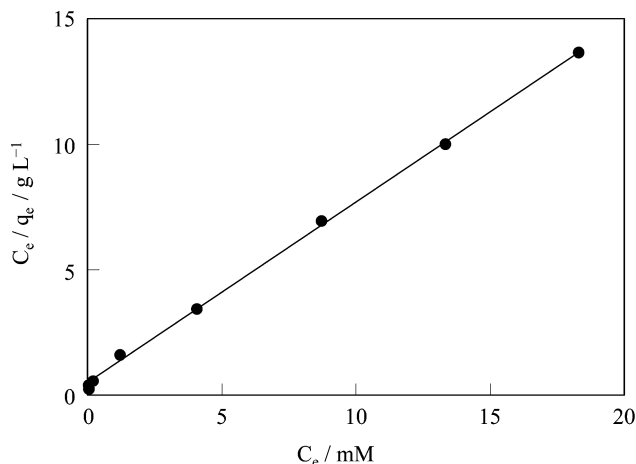


Fig. 6 Plots of  $C_e/q_e$  versus  $C_e$  for the adsorption isotherms of 0.5–25 mM Se(vi) adsorbed by 0.2 g Fe<sup>2+</sup>-doped Mg–Al LDH at 30 °C after 24 h.

Fig. 7 shows the variations in Se(vi) removal by the Fe<sup>2+</sup>-doped Mg–Al LDH over time at various temperatures. Se(vi) removal increased with time and increasing the temperature from 10 to 30 °C, but was almost constant when the temperature increased from 30 to 60 °C. These results suggest that higher temperatures enhance chemical adsorption (*i.e.* anion exchange of SeO<sub>4</sub><sup>2-</sup> and SeO<sub>3</sub><sup>2-</sup> with intercalated Cl<sup>-</sup>).

Next, the kinetics of Se(vi) removal by the Fe<sup>2+</sup>-doped Mg–Al LDH were examined based on the data shown in Fig. 7. First-order kinetics, which depend on the concentration of Se(vi), may be expressed by

$$-\ln(1 - x) = kt, \quad (3)$$

where  $x$  is the degree of Se(vi) removal,  $t$  (min) is the reaction time, and  $k$  (min<sup>-1</sup>) is the rate constant for Se(vi) removal. Fig. 8 presents the first-order plots of Se(vi) removal at various temperatures. None of the plots show good linearity, regardless

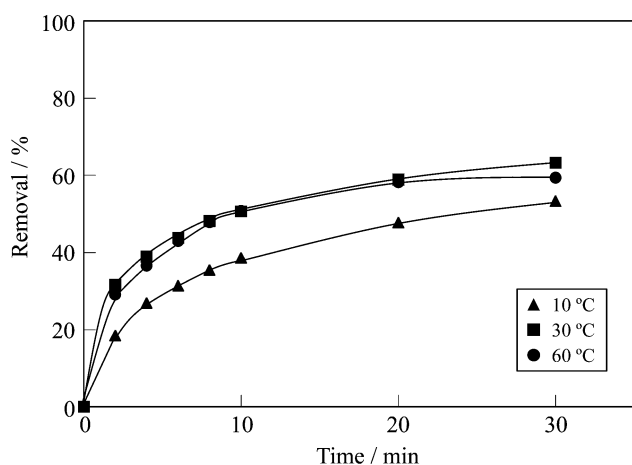


Fig. 7 Variations in Se(vi) removal by the Fe<sup>2+</sup>-doped Mg–Al LDH over time at various temperatures for Al/Se = 1.

of temperature, indicating that Se(vi) removal cannot be represented by first-order reaction kinetics. Thus, pseudo second-order kinetics may be expressed by<sup>20–22</sup>

$$dq_t/dt = k(q_e - q_t)^2 \quad (4)$$

where  $q_t$  (mmol g<sup>-1</sup>) is the amount of Se(vi) removed at reaction time  $t$ ,  $q_e$  (mmol g<sup>-1</sup>) is the amount of Se(vi) removed at equilibrium, and  $k$  (g mmol<sup>-1</sup> min<sup>-1</sup>) is the rate constant for Se(vi) removal. Integration of eqn (4) gives

$$t/q_t = 1/(kq_e^2) + t/q_e. \quad (5)$$

The pseudo second-order reaction can predict the adsorption behavior by assuming that the rate-determining step consists of chemical adsorption involving valence forces through the sharing or exchange of electrons between the adsorbent and adsorbate.<sup>20,21,23–25</sup> Fig. 9 displays the pseudo second-order plot for Se(vi) removal at various temperatures, which shows good linearity at all temperatures and confirms that Se(vi) removal can be represented by pseudo second-order reaction kinetics. The apparent rate constants at 10, 30, and 60 °C were  $1.2 \times 10^{-3}$ ,  $1.5 \times 10^{-3}$ , and  $2.2 \times 10^{-3}$  g mmol<sup>-1</sup> min<sup>-1</sup>, respectively. Thus, the apparent rate constant clearly increased with increasing temperature. An Arrhenius plot of the rate constants, determined from the slopes of the lines in Fig. 9, is shown in Fig. 10 and yields an apparent activation energy of 10.0 kJ mol<sup>-1</sup>.

There are two main types of adsorption: physical and chemical. Typically, the forces involved in physical adsorption are weak and have activation energies of no more than 4.2 kJ mol<sup>-1</sup>. Chemical adsorption, however, is highly specific and involves forces much stronger than those in physical adsorption. With chemical adsorption, the reaction rate varies with temperature according to a finite activation energy (8.4–83.7 kJ mol<sup>-1</sup>) in the Arrhenius equation.<sup>25–27</sup> The apparent activation energy of 10.0 kJ mol<sup>-1</sup> for Se(vi) removal is within the finite activation energy range of chemical adsorption. Therefore, this

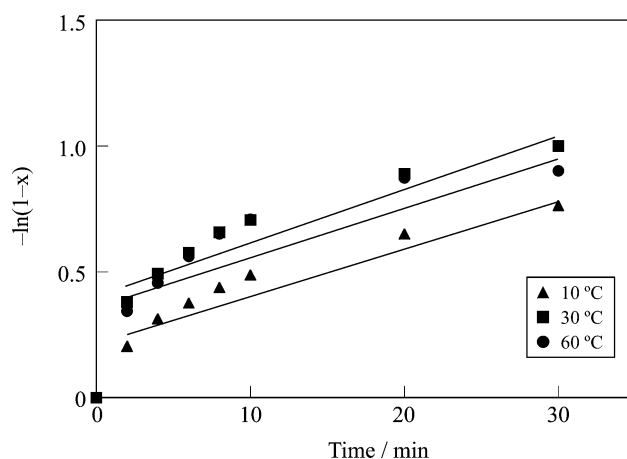


Fig. 8 First-order plot of Se(vi) removal by the Fe<sup>2+</sup>-doped Mg–Al LDH at various temperatures.

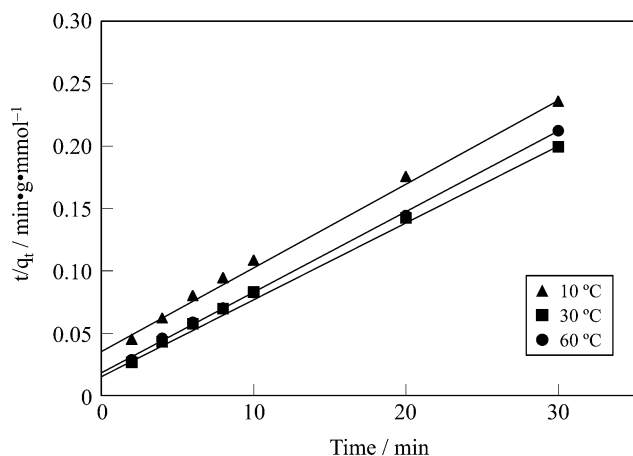


Fig. 9 Pseudo second-order plot of Se(vi) removal by the Fe<sup>2+</sup>-doped Mg-Al LDH at various temperatures.

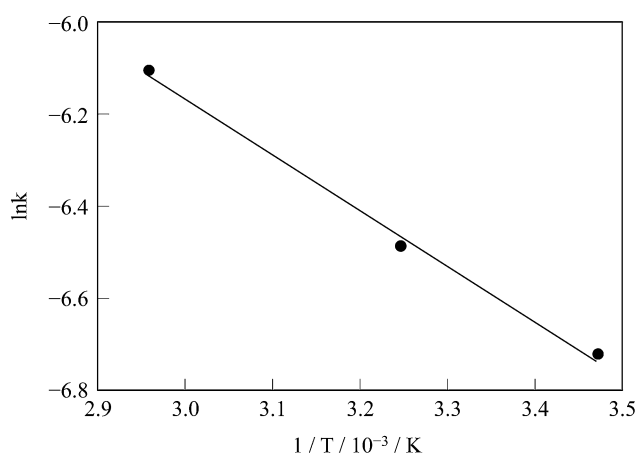


Fig. 10 Arrhenius plot of the apparent rate constant of Se(vi) removal by the Fe<sup>2+</sup>-doped Mg-Al LDH.

result confirms that the rate-determining step in Se(vi) removal by the Fe<sup>2+</sup>-doped Mg-Al LDH is chemical adsorption involving anion exchange of SeO<sub>4</sub><sup>2-</sup> and SeO<sub>3</sub><sup>2-</sup> with intercalated Cl<sup>-</sup> and that Se(vi) removal is well expressed as a pseudo second-order reaction.

## Conclusions

The Se(vi) removal efficiencies of undoped and Fe<sup>2+</sup>-doped Mg-Al LDH were compared in this study, and the latter was proved to be superior. Both LDHs adsorbed Se(vi) as SeO<sub>4</sub><sup>2-</sup> through anion exchange with intercalated Cl<sup>-</sup>. However, in the Fe<sup>2+</sup>-doped Mg-Al LDH, Se(vi) was reduced to Se(IV) upon oxidation of Fe<sup>2+</sup> to Fe<sup>3+</sup> in LDH host layer. Se(IV), available as SeO<sub>3</sub><sup>2-</sup>, was also adsorbed by the Fe<sup>2+</sup>-doped Mg-Al LDH through anion exchange. Reduction of Se(vi) to Se(IV) is advantageous for Se(vi) removal by the Fe<sup>2+</sup>-doped Mg-Al LDH due to the increased charge density of SeO<sub>3</sub><sup>2-</sup>. The Fe<sup>2+</sup>-doped Mg-Al LDH could remove Se(vi) effectively from an aqueous solution because of the anion exchange properties of the LDH and activity of the

Fe<sup>2+</sup> as a reducing agent. This process was considered to occur through Langmuir-type adsorption, where the maximum adsorption and equilibrium adsorption constant were 1.4 mmol g<sup>-1</sup> and 1.6, respectively. Se(vi) removal could be well expressed as a pseudo second-order reaction. The apparent rate constants at 10, 30, and 60 °C were  $1.2 \times 10^{-3}$ ,  $1.5 \times 10^{-3}$ , and  $2.2 \times 10^{-3}$  g mmol<sup>-1</sup> min<sup>-1</sup>, respectively, and the apparent activation energy was 10.0 kJ mol<sup>-1</sup>. The rate-determining step in Se(vi) removal by the Fe<sup>2+</sup>-doped Mg-Al LDH was confirmed to be chemical adsorption involving anion exchange of SeO<sub>4</sub><sup>2-</sup> and SeO<sub>3</sub><sup>2-</sup> with intercalated Cl<sup>-</sup>.

## Acknowledgements

This research was partially supported by the Ministry of Education, Science, Sports, and Culture, Grant-in-Aid for Challenging Exploratory Research, 23651061, 2011–2013.

## References

- 1 F. Cavani, F. Trifiro and A. Vaccari, *Catal. Today*, 1991, **11**, 173.
- 2 L. Ingram and H. F. W. Taylor, *Mineral. Mag.*, 1967, **36**, 465.
- 3 R. Allmann, *Acta Crystallogr., Sect. B: Struct. Crystallogr. Cryst. Chem.*, 1968, **24**, 972.
- 4 S. J. Mills, A. G. Christy, J.-M. R. Genin, T. Kameda and F. Colombo, *Mineral. Mag.*, 2012, **76**, 1289.
- 5 K.-H. Goh, T.-T. Lim and Z. Dong, *Water Res.*, 2008, **42**, 1343.
- 6 S. Mandal, S. Mayadevi and B. D. Kulkarni, *Ind. Eng. Chem. Res.*, 2009, **48**, 7893.
- 7 X. Wu, X. Tan, S. Yang, T. Wen, H. Guo, X. Wang and A. Xu, *Water Res.*, 2013, **47**, 4159.
- 8 A. G. Caporale, M. Pigna, S. M. G. G. Azam, A. Sommella, M. A. Rao and A. Violante, *Chem. Eng. J.*, 2013, **225**, 704.
- 9 D. Kovacevic, B. N. Dzakula, D. Hasenay, I. Nemet, S. Roncovic, I. Dekany and D. Petridis, *Croat. Chem. Acta*, 2013, **86**, 273.
- 10 X. Yuan, Y. Wang, J. Wang, C. Zhou, Q. Tang and X. Rao, *Chem. Eng. J.*, 2013, **221**, 204.
- 11 S. Kaneko and M. Ogawa, *Appl. Clay Sci.*, 2013, **75–76**, 109.
- 12 S. Paikaray and M. J. Hendry, *Appl. Clay Sci.*, 2013, **77–78**, 33.
- 13 S. Paikaray, M. J. Hendry and J. E. Dugan, *Chem. Geol.*, 2013, **345**, 130.
- 14 T. Kameda, M. Honda and T. Yoshioka, *Sep. Purif. Technol.*, 2011, **80**, 235.
- 15 T. Kameda, M. Nakamura and T. Yoshioka, *J. Environ. Sci. Health, Part A: Toxic/Hazard. Subst. Environ. Eng.*, 2012, **47**, 1146.
- 16 T. Kameda, M. Nakamura and T. Yoshioka, *Fresenius Environ. Bull.*, 2012, **21**, 1323.
- 17 D. H. K. Reddy and S.-M. Lee, *Adv. Colloid Interface Sci.*, 2013, **201–202**, 68.
- 18 T. Kameda, E. Kondo and T. Yoshioka, *Sep. Purif. Technol.*, 2014, **122**, 12.
- 19 Sangyou Kanri Kyoukai, Shin Kougai Boushi no Gijyutsu to Houki 2011, Suishitsu hen II, Maruzen, Tokyo, 2011.
- 20 Y. S. Ho and G. McKay, *Process Biochem.*, 1999, **34**, 451.

- 21 Y. S. Ho, *J. Hazard. Mater.*, 2006, **B136**, 681.
- 22 F. C. Wu, R. L. Tseng, S. C. Huang and R. S. Juang, *Chem. Eng. J.*, 2009, **151**, 1.
- 23 Z. P. Liang, Y. Q. Feng, Z. Y. Liang and S. X. Meng, *Biochem. Eng. J.*, 2005, **24**, 65.
- 24 Z. P. Liang, Y. Q. Feng, S. X. Meng and Z. Y. Liang, *Process Biochem.*, 2005, **40**, 3218.
- 25 M. Kragovic, A. Dakovic, M. Markovic, J. Krstic, G. D. Gatta and N. Rotiroti, *Appl. Surf. Sci.*, 2013, **283**, 764.
- 26 Z. Aksu, *Process Biochem.*, 2002, **38**, 89.
- 27 W. Zou, R. Han, Z. Chen and Z. Jinghua, *Colloids Surf., A*, 2006, **279**, 238.