# A Comparative Analysis of Pseudophase Ion-Exchange (PIE) Model and Berezin Pseudophase (BPP) Model: Analysis of Kinetic Data for Ionic Micellar-mediated Semi-ionic Bimolecular Reaction

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Pseudo-first-order rate constants ( $k_{obs}$ ) for the reaction of N-benzylphthalimide (NBPT) with HO<sup>-</sup> have been determined at  $2.0 \times 10^{-4}$  M NBPT,  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH as well as varying concentrations of cetyltrimethylammonium bromide ([CTABr]<sub>T</sub> = 0.0- $1.7 \times 10^{-1}$  M). The effects of [CTABr]<sub>T</sub> – CMC (with CMC representing the critical micelle concentration of CTABr) on  $k_{obs}$  have been analyzed in terms of Berezin's pseudophase (BPP) model and pseudophase ion-exchange (PIE) model. Although both models give the best observed data fit with least-squares values not significantly different from each other, the calculated values of  $K_S$  from BPP model appear to be more reliable compared to those from PIE model because the values of  $K_S$  from BPP model are similar to the corresponding  $K_S$  values determined spectrophotometrically.

**Key Words:** *N*-Benzylphthalimide, Rate constant, Binding constant, Pseudophase ion-exchange (PIE) model, Berezin pseudophase (BPP) model

#### Introduction

The occurrence of ion-exchange between counterions and ionic reactants of charge similar to the charge of counterions of micellar-mediated ionic reactions or semi-ionic reactions has been detected kinetically in the late 1960 s. The quantitative analysis of the kinetic data on such reactions involves largely the following two alternative theoretical approaches for the distribution of counterion-like reactants between micellar and aqueous pseudophase. (i) The most commonly used approach is the pseudophase ion-exchange (PIE) model<sup>2</sup> and (ii) a less commonly used approach is to write micellar counterion binding in terms of ionic micellar surface electrical potential.3 Both approaches are semi-empirical and have limitations.<sup>3</sup> The frequent use of PIE model may be attributed, at least partly, to its practical and theoretical simplicity. Both approaches might result in kinetic parameters of varying degree of reliability. The parameters, such as micellar binding constants (K<sub>S</sub>) of reactants and ion-exchange constant  $(K_X^Y)$ , seem to be the only kinetic parameters which could be compared with those obtained independently by using different experimental techniques. The reports on a comparison of this sort are rare especially under strictly kinetic conditions. An attempt is made in the present study to compare K<sub>S</sub> values obtained by the use of kinetic models (PIE model and Berezin's pseudophase model) and UVvisible spectrophotometric technique. The results and probable explanations are described in this manuscript.

# **Experimental Section**

**Materials.** Reagent-grade chemicals such as cetyltrimethylammonium bromide (CTABr) and sodium hydroxide (NaOH) were of the highest commercially available purity. All other

chemicals used were also of reagent grade. *N*-benzylphthalimide (NBPT) was synthesized as described elsewhere. Stock solutions of NBPT (0.01 M) were prepared in CH<sub>3</sub>CN and stored at low temperature whenever they were not in

**Kinetic Measurements.** (a) Alkaline Hydrolysis of N-Benzylphthalimide (NBPT) in the Presence of Different Total Concentration of CTABr ([CTABr]<sub>T</sub>) at 35 °C: The rate of alkaline hydrolysis of NBPT was studied by monitoring the disappearance of reactant (NBPT) spectrophotometrically at 300 nm using Shimadzu UV-Visible Spectrophotometer with the help of UV-1601 PC software. Details of the kinetic procedure have been described elsewhere.<sup>5</sup> The observed data followed eqn. (1)

$$A_{\text{obs}} = \delta_{\text{app}} [X_0] \exp(-k_{\text{obs}} t) + A_{\infty}$$
 (1)

where  $A_{\rm obs}$  is the absorbance at any reaction time t,  $\delta_{\rm app}$  is the apparent molar extinction coefficient of reaction mixtures,  $[X_0]$  is the initial concentration of the reactant,  $A_{\infty} = A_{\rm obs}$  at  $t = \infty$  and  $k_{\rm obs}$  represents pseudo first-order rate constant for alkaline hydrolysis of NBPT. The rates of reactions were generally monitored for the reaction period of more than 7-9 halflives.

(b) Spectrophotometric Determination of Cationic Micellar Binding Constant of NBPT: Since the rate of cationic micellar-mediated hydrolysis of NBPT is highly sensitive to [HO<sup>-</sup>] at  $\geq 1.0 \times 10^{-3}$  M NaOH, the CTABr micellar binding constant of NBPT was determined spectrophotometrically at [NaOH] = 0. The maximum initial absorbance,  $A_{\rm obs}^0$ , (i.e. observed absorbance at reaction time t=0) change within [CTABr]<sub>T</sub> (total concentration of CTABr) range 0.0-1.7  $\times 10^{-1}$  M was observed at 314 nm and 35 °C. The values of  $A_{\rm obs}^0$  were determined at  $2.0 \times 10^{-4}$  M NBPT and within [CTABr]<sub>T</sub> range  $6.0 \times 10^{-4} - 1.7 \times 10^{-1}$  M. These values of

**Table 1.** Values of parameters,  $\delta_W$ ,  $\delta_M$  and  $K_S$ , calculated from eqn.  $(2)^a$ 

$10^4 [X_0]$	10 <sup>4</sup> CMC	Ks	$\delta_{ m w}$	$\delta_{\mathrm{M}}$	
M	M	$\mathbf{M}^{-1}$	$M^{-1}cm^{-1}$	$M^{-1}cm^{-1}$	$10^4 \Sigma d_i^2$
$2.0^{b}$	3.01	$1105 \pm 251^{c}$	$1520 \pm 68^{\circ}$	$721 \pm 335^{c}$	3.800
	3.66	$1031\pm219$	$1466 \pm 54$	$721 \pm 313$	3.800
	3.84	$1012\pm210$	$1453 \pm 50$	$721 \pm 307$	3.800
	4.99	$907 \pm 169$	$1376\pm33$	$721 \pm 276$	3.800
$3.0^{d}$	3.01	$1019\pm188$	$1410 \pm 52$	$697 \pm 267$	3.541
	3.66	$955 \pm 165$	$1366 \pm 43$	$697 \pm 251$	3.541
	3.84	$939 \pm 160$	$1355 \pm 40$	$697 \pm 247$	3.541
	4.99	$848 \pm 130$	$1290\pm29$	$697 \pm 224$	3.541
$5.0^{e}$	3.01	$975 \pm 91$	$1503\pm29$	$670\pm130$	5.514
	3.66	$917 \pm 81$	$1454 \pm 24$	$670\pm123$	5.514
	3.84	$902\pm78$	$1441 \pm 22$	$670 \pm 121$	5.514
	4.99	$818 \pm 64$	$1368\pm16$	$670 \pm 110$	5.514
$3.0^{f}$	5.00	$1580 \pm 410$	$1470 \pm 50$	$810 \pm 430$	22.47
	6.00	$1370 \pm 305$	$1380 \pm 32$	$810 \pm 380$	22.47

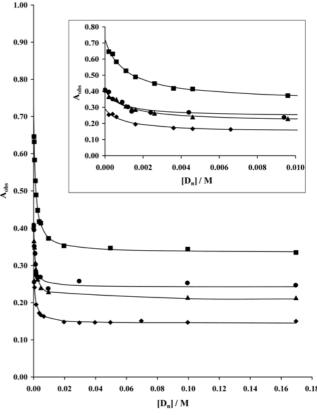
 $^a$ [NaOH] = 0, T = 35 °C,  $\lambda$  = 314 nm.  $^b$ 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture.  $^c$ Error limits are standard deviations.  $^d$ 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture.  $^c$ 5% v/v CH<sub>3</sub>CN in the aqueous reaction mixture.  $^f$ [NaOH] =  $1.2 \times 10^{-3}$  M.

 $A_{\rm obs}^0$  were used to calculate  $K_{\rm S}$ ,  $\delta_{\rm W}$ , and  $\delta_{\rm M}$  from eqn. (2)

$$A_{\text{obs}}^{0} = \frac{(\delta_{W} + \delta_{M} K_{S}[D_{n}])[X_{0}]}{1 + K_{S}[D_{n}]}$$
 (2)

where  $K_S$  is CTABr micellar binding constant of NBPT,  $[D_n] =$ [CTABr]<sub>T</sub> – CMC with CMC representing critical micelle concentration of CTABr surfactant,  $\delta_{\rm W}$  and  $\delta_{\rm M}$  represent molar extinction coefficients of NBPT at 314 nm in aqueous pseudophase and micellar pseudophase, respectively, and  $[X_0]$  is the initial concentration of NBPT. In the absence of experimentally known value of CMC, the values of  $\delta_{\rm W}$ ,  $\delta_{\rm M}$  and  $K_{\rm S}$  were calculated from eqn. (2) at different presumed values of CMC ranging from 3.01  $\times 10^{-4} - 4.99 \times 10^{-4}$  M. These results, as summarized in Table 1, show the values of least-squares,  $\Sigma d_i^2$  (where  $d_i = A_{\text{obs}i}^0 - A_{\text{calcd}i}^0$  with  $A_{\text{obs}i}^0$  and  $A_{\text{calcd}i}^0$  representing observed and calculated initial absorbance at ith total concentration of CTABr), remain almost unchanged with change in CMC from  $3.01 \times 10^{-4} - 4.99 \times 10^{-4}$ 10<sup>-4</sup> M. The quality of the fitting of observed data to eqn. 2 is evident from the standard deviations associated with the calculated parameters,  $\delta_{\rm W}$ ,  $\delta_{\rm M}$  and  $K_{\rm S}$ , and from the plot of Figure 1 where solid line is drawn through the calculated values of absor-

bance using eqn. (2) with parameters listed in Table 1. The initial absorbance change  $\Delta A_{\rm obs}^0$  {=  $(\delta_{\rm W}-\delta_{\rm M})$  [ $X_0$ ]} is rather low ( $\approx 0.14$ ) at [ $X_0$ ] =  $2.0 \times 10^{-4}$  M and consequently the calculated values of  $\delta_{\rm W}$ ,  $\delta_{\rm M}$  and  $K_{\rm S}$  under such conditions are rather less reliable. In order to increase the value of  $\Delta A_{\rm obs}^0$ , the value of  $A_{\rm obs}^0$  at different [CTABr]<sub>T</sub> were also determined at [ $X_0$ ] =  $5.0 \times 10^{-4}$  M. These observed data were used to calculate  $\delta_{\rm W}$ ,  $\delta_{\rm M}$ ,  $K_{\rm S}$  and  $\Sigma d_i^2$  from eqn. (2) and these results are summarized in Table 1. Although the values of  $\delta_{\rm W}$ ,  $\delta_{\rm M}$  and  $K_{\rm S}$  are not appreciably different from the corresponding values obtained at [ $X_0$ ] =  $2.0 \times 10^{-4}$  M (Table 1), the standard deviations associated with these parameters are significantly lower at [ $X_0$ ] =  $5.0 \times 10^{-4}$  M than those at [ $X_0$ ] =



**Figure 1.** Plots of  $A_{\text{obs}}$  versus  $[D_n]$  for  $(\spadesuit)$ ,  $[X_0] = 2.0 \times 10^{-4} \,\text{M}$ , [NaOH] = 0;  $(\spadesuit)$ ,  $[X_0] = 3.0 \times 10^{-4} \,\text{M}$ , [NaOH] = 0;  $(\spadesuit)$ ,  $[X_0] = 3.0 \times 10^{-4} \,\text{M}$ , [NaOH] = 0;  $(\bullet)$ ,  $[X_0] = 3.0 \times 10^{-4} \,\text{M}$ ,  $[\text{NaOH}] = 1.2 \times 10^{-3} \,\text{M}$ ; and  $(\blacksquare)$ ,  $[X_0] = 5.0 \times 10^{-4} \,\text{M}$ , [NaOH] = 0. The solid lines are drawn through the calculated values of absorbance using eqn. (2) for  $(\spadesuit)$ ,  $10^4 \,\text{CMC} = 3.84 \,\text{M}$ ,  $K_S = 1012 \,\text{M}^{-1}$ ,  $\delta_W = 1453 \,\text{M}^{-1} \,\text{cm}^{-1}$ ,  $\delta_M = 721 \,\text{M}^{-1} \,\text{cm}^{-1}$ ;  $(\spadesuit)$ ,  $10^4 \,\text{CMC} = 3.84 \,\text{M}$ ,  $K_S = 939 \,\text{M}^{-1}$ ,  $\delta_W = 1355 \,\text{M}^{-1} \,\text{cm}^{-1}$ ;  $\delta_M = 697 \,\text{M}^{-1} \,\text{cm}^{-1}$ ;  $(\spadesuit)$ ,  $10^4 \,\text{CMC} = 6.00 \,\text{M}$ ,  $K_S = 1370 \,\text{M}^{-1}$ ,  $\delta_W = 1380 \,\text{M}^{-1} \,\text{cm}^{-1}$ ,  $\delta_M = 810 \,\text{M}^{-1} \,\text{cm}^{-1}$ ; and  $(\blacksquare)$ ,  $10^4 \,\text{CMC} = 3.84 \,\text{M}$ ,  $K_S = 902 \,\text{M}^{-1}$ ,  $\delta_W = 1441 \,\text{M}^{-1} \,\text{cm}^{-1}$ ,  $\delta_M = 670 \,\text{M}^{-1} \,\text{cm}^{-1}$ .

 $2.0 \times 10^{-4}$  M. The satisfactory fit of observed data, obtained at  $[X_0] = 5.0 \times 10^{-4}$  M, to eqn. (2) is evident from the plot of Figure 1 where solid line is drawn through the calculated data points.

Although the rate of alkaline hydrolysis of NBPT is very sensitive to [HO<sup>-</sup>] both in the presence and absence of CTABr micelles, an attempt has been made to determine  $K_{\rm S}$  at  $1.2 \times 10^{-3}$  M NaOH. The values of were obtained at 314 nm and different values of [CTABr]<sub>T</sub> in the presence of  $1.2 \times 10^{-3}$  M NaOH and  $3.0 \times 10^{-4}$  M NBPT. The least squares calculated values of  $\delta_{\rm W}$ ,  $\delta_{\rm M}$ ,  $K_{\rm S}$  and  $\Sigma d_i^2$  from eqn. (2) using these values are shown in Table 1. The calculated parameters,  $K_{\rm S}$  and  $\delta_{\rm M}$ , are associated with unusually large standard deviations which could be attributed to rather low value of  $\Delta A_{\rm obs}^0$  ( $\approx 0.15$ ) and large uncertainty in the determination of  $A_{\rm obs}^0$  values due to high rate of hydrolysis of NBPT under such conditions.

(c) Product Characterization: The alkaline hydrolysis product of NBPT is affirmed as N-benzylphthalamate ion (NBPA<sup>-</sup>) by comparing the final UV absorption spectra of hydrolytic products with the authentic sample of N-benzyl-

**Table 2.** Alkaline hydrolysis  $(1.0 \times 10^{-3} \text{ M NaOH})$  of NBPT at different [CTABr]<sub>T</sub>, calculated from eqn.  $(3)^a$ 

[CTABr]	$10^3 k_{\text{obs}}^b$	$\delta_{ ext{app}}^{b}$	10 <sup>3</sup>	$10^3 k_{\text{calcd}}^c$
M	$s^{-1}$	$M^{-1}cm^{-1}$	$A_{\infty}{}^b$	s <sup>-1</sup>
$5.0 \times 10^{-4}$	$24.2 \pm 0.2^d$	$2343 \pm 11^{d}$	$8 \pm 1^d$	31.4
$6.0\times10^{-4}$	$30.9 \pm 0.5$	$2452 \pm 26$	$11 \pm 1$	37.3
$7.0\times10^{-4}$	$36.0 \pm 0.5$	$2228 \pm 19$	$12 \pm 1$	42.4
$8.0\times10^{-4}$	$40.9 \pm 0.9$	$2116 \pm 34$	$13 \pm 1$	46.9
$1.0\times10^{-3}$	$48.2 \pm 1.2$	$2269 \pm 51$	$15 \pm 1$	54.0
$1.5\times10^{-3}$	$62.7 \pm 1.4$	$2006 \pm 48$	$19 \pm 1$	65.6
$2.0\times10^{-3}$	$81.9 \pm 2.1$	$2315 \pm 75$	$11 \pm 1$	72.1
$3.0\times10^{-3}$	$92.4 \pm 1.3$	$2049 \pm 37$	$8 \pm 1$	77.9
$5.0\times10^{-3}$	$88.2 \pm 1.6$	$2025 \pm 45$	$10 \pm 1$	78.9
$7.0\times10^{-3}$	$77.5 \pm 1.5$	$2254 \pm 47$	$10 \pm 1$	75.9
$1.0\times10^{-2}$	$67.8 \pm 0.9$	$2119 \pm 23$	$10 \pm 1$	70.0
$2.0\times10^{-2}$	$43.0 \pm 0.8$	$2113 \pm 25$	$11 \pm 1$	53.1
$3.0\times10^{-2}$	$34.2 \pm 0.7$	$2251 \pm 21$	$14 \pm 2$	42.3
$5.0\times10^{-2}$	$22.7 \pm 0.5$	$2151 \pm 23$	$17 \pm 2$	29.9
$7.0\times10^{-2}$	$16.4 \pm 0.4$	$2052 \pm 20$	$20 \pm 2$	23.1
$1.0\times10^{-1}$	$11.6 \pm 0.3$	$2016\pm18$	$19 \pm 2$	17.2
$1.7\times10^{-1}$	$7.40 \pm 0.23$	$2105 \pm 24$	$30 \pm 3$	10.8

<sup>a</sup>[NBPT]<sub>0</sub> = 2.0 × 10<sup>-4</sup> M, [NaOH] = 1.0 × 10<sup>-3</sup> M, T = 35 °C,  $\lambda$  = 300 nm, 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture. <sup>b</sup>Calculated from eqn. (1). <sup>c</sup>Calculated from eqn. (3) with 10<sup>4</sup> CMC = 3.66 M,  $k_{\rm W}^2$  = 21.6 M<sup>-1</sup>s<sup>-1</sup>, 10<sup>3</sup>  $k_{\rm M}$  = 2.03 ± 0.13 M s<sup>-1</sup>,  $K_{\rm OH}$  = 60 M<sup>-1</sup> and  $K_{\rm S}$  = 831 ± 195 M<sup>-1</sup> where 10<sup>4</sup> Σ $d_t^2$  = 9.229. <sup>d</sup>Error limits are standard deviations.

**Table 3.** Alkaline hydrolysis  $(2.0 \times 10^{-3} \text{ M NaOH})$  of NBPT at different [CTABr]<sub>T</sub>, calculated from eqn.  $(3)^a$ 

[CTABr]	$10^3 k_{\rm obs}{}^b$	$\delta_{\!\! ext{app}}^{b}$	$10^{3}$	$10^3 k_{\text{calcd}}^c$
M	$\mathrm{s}^{-1}$	$M^{-1}cm^{-1}$	${A_{\scriptscriptstyle \infty}}^b$	$s^{-1}$
$6.0 \times 10^{-4}$	$65.5 \pm 0.8^d$	$2197 \pm 24^d$	$7 \pm 1^d$	71.9
$8.0\times10^{-4}$	$75.9 \pm 1.6$	$2136 \pm 40$	$11 \pm 1$	85.5
$1.0\times10^{-3}$	$105 \pm 2$	$1905 \pm 56$	$9 \pm 1$	95.4
$2.0\times10^{-3}$	$125 \pm 3$	$1946 \pm 67$	$11 \pm 1$	119.2
$4.0\times10^{-3}$	$130 \pm 3$	$1964 \pm 76$	$12 \pm 1$	128.1
$5.0\times10^{-3}$	$124 \pm 3$	$1960 \pm 65$	$12 \pm 1$	127.4
$7.0\times10^{-3}$	$117 \pm 3$	$1999 \pm 53$	$12 \pm 1$	123.2
$2.0\times10^{-2}$	$97.2 \pm 1.5$	$2128 \pm 34$	$11 \pm 1$	90.8
$3.0\times10^{-2}$	$77.6 \pm 1.0$	$2292 \pm 26$	$11 \pm 1$	74.3
$4.0\times10^{-2}$	$57.1 \pm 0.7$	$2168\pm18$	$13 \pm 1$	62.7
$5.0\times10^{-2}$	$56.4 \pm 0.5$	$2229 \pm 16$	$12 \pm 1$	54.2
$7.0\times10^{-2}$	$41.7 \pm 0.5$	$2336\pm16$	$14 \pm 1$	42.6
$1.0\times10^{-1}$	$29.8 \pm 0.4$	$2286 \pm 14$	$17 \pm 1$	32.2
$1.7 \times 10^{-1}$	$20.4 \pm 0.5$	$2342\pm19$	$27 \pm 3$	20.5

 $^a [NBPT]_0 = 2.0 \times 10^{-4}$  M, [NaOH] =  $2.0 \times 10^{-3}$  M, T = 35 °C,  $\lambda = 300$  nm, 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture.  $^b Calculated$  from eqn. (1).  $^c Calculated$  from eqn. (3) with  $10^4$  CMC = 3.84 M,  $k_W^2 = 25.25$   $M^{-1} s^{-1}$ ,  $10^3$   $k_M = 39.6 \pm 3.0$  M s  $^{-1}$ ,  $K_{OH} = 44 \pm 7$   $M^{-1}$  and  $K_S = 986 \pm 240$   $M^{-1}$  where  $10^4$   $\Sigma d_i^2 = 4.090$ .  $^d Error$  limits are standard deviations.

phthalamic acid under the same condition.<sup>4</sup> Molar absorptivities of NBPA<sup>-</sup> ion and phthalic acid at 300 nm are nearly zero. Therefore, the apparent molar absorptivity of the reaction mixture,  $\delta_{app} \approx \delta_{NBPT}$  at 300 nm because  $\delta_{app} = \delta_{NBPT} - \delta_P$  where  $\delta_{NBPT}$  and  $\delta_P$  represent the molar absorptivity of NBPT and products, respectively. The calculated values of  $\delta_{app}$  turned out to be almost independent of the total

concentration of CTABr and NaOH (Tables 2 and 3). The values of  $A_{\infty}$  (Tables 2 and 3) show that the products of the reaction do not absorb to a detectable level at 300 nm.

## **Results and Discussion**

The cleavage of *N*-benzylphthalimide (NBPT) was studied within [CTABr]<sub>T</sub> range 0.0- $1.7 \times 10^{-1}$  M at  $1.0 \times 10^{-3}$  M NaOH. Pseudo-first-order rate constants,  $k_{\rm obs}$ , are shown in Table 2. Similar observations were obtained at  $2.0 \times 10^{-3}$  M NaOH and the observed data are summarized in Table 3. The study<sup>4</sup> on alkaline hydrolysis of NBPT reveals that the reactants for the reaction under present experimental conditions are HO<sup>-</sup> and NBPT. The variation of  $k_{\rm obs}$  with [CTABr]<sub>T</sub> at the constant [NaOH] clearly reveals the well defined maxima at both  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH. Such observations on related reaction systems have been explained in terms of either less commonly used Berezin's pseudophase (BPP) model<sup>6</sup> or more widely used pseudophase ion-exchange (PIE) model.<sup>2,7,8</sup>

**Berezin's Pseudophase (BPP) Model.** The reaction scheme for the alkaline hydrolysis of NBPT, in the presence of CTABr micelles,  $D_n$ , is shown in Scheme 1, where subscripts W and M represent aqueous pseudophase and micellar pseudophase, respectively,  $P_S$  and  $P_{OH}$  are the partition coefficients for the distribution of respective NBPT and  $HO^-$  between aqueous and micellar pseudophases. Observed rate law (rate =  $k_{obs}$  [NBPT]<sub>T</sub> with [NBPT]<sub>T</sub> = [NBPT<sub>W</sub>] + [NBPT<sub>M</sub>]) and Scheme 1 can lead to eqn. (3) provided  $P_S >> 1$ ,  $P_{OH} >> 1$  and  $[D_n]V_M << 1$  where  $[D_n]$  and  $V_M$  represent molar concentration of micelles and molar volume of the micellar reaction region, respectively.

$$k_{\text{obs}} = \frac{k_{\text{W}} + k_{\text{M}} K_{\text{S}} K_{\text{OH}}[D_n]}{(1 + K_{\text{S}}[D_n])(1 + K_{\text{OH}}[D_n])}$$
(3)

In eqn. (3),  $k_{\rm W}=k_{\rm W}^2\,[{\rm HO^-}]_{\rm T},\,k_{\rm M}=k_{\rm M}^{mr}\,[{\rm HO^-}]_{\rm T}$  and  $k_{\rm M}^{mr}=k_{\rm M}^2\,/V_{\rm M}.$ 

An attempt to fit the observed data ( $k_{\rm obs}$  versus  $[D_n]$ ) to eqn. 3 requires knowledge of CMC values under the present experimental conditions. The values of CMC were determined by graphical technique<sup>10</sup> as  $3.66 \times 10^{-4}$  and  $3.84 \times 10^{-4}$  M at  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH, respectively. The values of  $k_{\rm M}^{mr}$ ,  $K_{\rm S}$  and  $K_{\rm OH}$  were calculated from eqn. (3) considering  $k_{\rm W}^{av}$  as known parameter. The values of  $k_{\rm W}^{av}$ 

 $[HO^{-}]_{T}$  at  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH were obtained from  $k_{\rm obs}$  values determined experimentally at [CTABr]<sub>T</sub> < CMC including at  $[CTABr]_T = 0$  and thus the values of  $k_{\rm W}^2$  [HO<sup>-</sup>]<sub>T</sub> at  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH are (21.6 ± 0.3)  $\times 10^{-3}$  and (50.5 ± 1.7)  $\times 10^{-3}$  s<sup>-1</sup>, respectively. The observed data at  $2.0 \times 10^{-3}$  M NaOH (Table 3) fit to eqn. 3 and nonlinear least-squares calculated values of  $k_{\rm M}$ ,  $K_{\rm S}$ ,  $K_{\rm OH}$ and least-squares ( $\Sigma d_i^2$ ) are (39.6 ± 3.0) × 10<sup>-4</sup> M s<sup>-1</sup>, 986 ± 240  $M^{-1}$ , 44 ± 7  $M^{-1}$ , and 4.09 × 10<sup>-4</sup>, respectively. The extent of reliable fit of observed data to eqn. (3) is evident from the calculated values of rate constants ( $k_{\text{calcd}}$ ) as shown in Table 3. The values of  $k_{\rm M}$ ,  $K_{\rm S}$  and  $K_{\rm OH}$  were also calculated at different presumed values of CMC (ranging from  $3.84 \times 10^{-4}$  M to  $5.26 \times 10^{-4}$  M) at which the percent residual errors {RE =  $100 \times (k_{\text{obs }i} - k_{\text{calcd }i})/k_{\text{obs }i}$  where  $k_{\text{obs }i}$ and  $k_{\text{calcd }i}$  represent respective experimentally determined and calculated values of rate constant at the ith value of [CTABr]<sub>T</sub>} were only slightly changed. But the respective values of  $k_{\rm M}$ ,  $K_{\rm S}$  and  $K_{\rm OH}$  changed from 39.6 × 10<sup>-4</sup> M s<sup>-1</sup> to  $41.3 \times 10^{-4} \,\mathrm{M \ s^{-1}}$ , 986  $\mathrm{M^{-1}}$  to 1710  $\mathrm{M^{-1}}$ , and 44  $\mathrm{M^{-1}}$  to 39  $\mathrm{M^{-1}}$ , with change in CMC from  $3.84 \times 10^{-4} \,\mathrm{M}$  to  $5.26 \times 10^{-4} \,\mathrm{M}$ .

The observed data at  $1.0 \times 10^{-3}$  M NaOH (Table 2) did not fit to eqn. (3) in the sense that the nonlinear least-squares regression analysis could not converge such a data fit to a minimum least-squares value when  $k_{\rm M}$ ,  $K_{\rm S}$  and  $K_{\rm OH}$  were considered as unknown parameters. However, the same observed data fit to eqn. (3) when only  $k_{\rm M}$ , and  $K_{\rm S}$  were considered as unknown parameters. The nonlinear leastsquares treatment of observed data to eqn. (3) gave  $10^3 k_{\rm M} =$  $2.03 \pm 0.13 \text{ M s}^{-1}$ ,  $K_S = 831 \pm 195 \text{ M}^{-1}$ , and  $10^4 \Sigma d_i^2 = 9.229$ with  $10^4$  CMC = 3.66 M,  $10^3$   $k_W$  = 21.6 s<sup>-1</sup> and  $K_{OH}$  = 60 M<sup>-1</sup>. The value of  $K_{OH}$  (69 M<sup>-1</sup> at 25 °C) was determined experimentally as described elsewhere.3 The increase in CMC from  $3.66 \times 10^{-4}$  M to  $4.99 \times 10^{-4}$  M resulted in the change in  $k_{\rm M}$  from  $2.03 \times 10^{-3} \,{\rm M \ s^{-1}}$  to  $1.95 \times 10^{-3} \,{\rm M \ s^{-1}}$  and in  $K_{\rm S}$ from 831 M<sup>-1</sup> to 1141 M<sup>-1</sup> while the RE values were slightly  $(\le 5\%)$  changed within [CTABr]<sub>T</sub> range  $5.0 \times 10^{-4} - 1.7 \times 10^{-4}$ <sup>1</sup> M.

Although the fitting of observed data to eqn. (3) is better at  $2.0 \times 10^{-3}$  M NaOH than at  $1.0 \times 10^{-3}$  M NaOH in terms of RE values, the values of  $k_{\rm M}^{mr}$  (=  $k_{\rm M}/[{\rm HO}^-]_{\rm T}$ ) and  $K_{\rm S}$  are almost independent of [NaOH] within the domain of experimental uncertainties. In view of the basic assumptions of BPP and pseudophase (PP) micellar models,  $k_{\rm M}^{mr}$  and  $K_{\rm S}$ should be independent of [NaOH]. The values  $k_{\rm M}^2$  (=  $k_{\rm M}^{mr}$   $V_{\rm M}$  with  $V_{\rm M}=0.3~{\rm M}^{-1})^3$  are 0.61 and 0.59  ${\rm M}^{-1}{\rm s}^{-1}$  at  $1.0\times10^{-3}$  and  $2.0\times10^{-3}$  M NaOH, respectively. These  $k_{\rm M}^2$  values are ~35to 40-fold smaller than  $k_{\rm W}^2$  (= 22 to 25 M<sup>-1</sup>s<sup>-1</sup>) which cannot be attributed to only lower polarity of the reaction medium for micellar-mediated reaction because the increase in the content of acetonitrile from 2 – 70% v/v in mixed aqueous solvent decreases  $k_{\text{obs}}$  for alkaline hydrolysis of NBPT at 2.0 × 10<sup>-3</sup> M NaOH by only ~7.5-fold. Experimental observations indirectly show that the polarity and concentration of water decrease continuously as the distance increases from Stern region to the micellar centre i.e. core and consequently the micellar pseudophase is non-homogeneous in terms of the

distribution of micellized molecules of different hydrophilicity. Hydroxide ion is certainly highly hydrophilic while NBPT is highly hydrophobic. Hence it is plausible to propose that either different average locations of HO $^-$ ions and NBPT molecules in the micellar pseudophase or considerably low value of HO $_{\rm M}^-$  in the vicinity of NBPT $_{\rm M}$  molecules due to continuous decrease in [H2O] with increase in distance from exterior to core of micelle are partly responsible for considerably lower value of  $k_{\rm M}^2$  compared with  $k_{\rm W}^2$ .

**Pseudophase Ion Exchange (PIE) Model.** This model uses pseudophase micellar model coupled with an ion-exchange formalism at ionic micellar surface as shown by eqn. (4)<sup>2,7-10</sup>

$$HO_{M}^{-} + Br_{W}^{-} = HO_{W}^{-} + Br_{M}^{-}$$
 (4)

where Br<sup>-</sup> is inert counterion of CTABr surfactant,  $K_{\text{OH}}^{\text{Br}} = K_{\text{Br}}/K_{\text{OH}}$  with  $K_{\text{Br}} = [\text{Br}_{\text{M}}^{\text{-}}]/[\text{Br}_{\text{W}}^{\text{-}}][D_n]$  and  $K_{\text{OH}} = [\text{HO}_{\text{M}}^{\text{-}}]/[\text{HO}_{\text{W}}^{\text{-}}][D_n]$ . The observed rate law (rate =  $k_{\text{obs}}$  [NBPT]<sub>T</sub>) and pseudophase micellar model coupled with eqn. (4) can lead to eqn. (5)<sup>2,7-9</sup>

$$k_{\text{obs}} = \frac{k_{\text{W}}^{2}[\text{HO}^{-}]_{\text{T}} + (k_{\text{M}}^{mr}K_{\text{S}} - k_{\text{W}}^{2})m_{\text{OH}}[D_{n}]}{1 + K_{\text{S}}[D_{n}]}$$
(5)

where [HO<sup>-</sup>]<sub>T</sub> = [HO<sup>-</sup><sub>W</sub>] + [HO<sup>-</sup><sub>M</sub>],  $m_{\text{OH}}$  = [HO<sup>-</sup><sub>M</sub>]/[ $D_n$ ],  $k_{\text{W}}^2$  is second-order rate constant for the reaction of HO<sup>-</sup><sub>W</sub> with NBPT<sub>W</sub> and  $k_{\text{M}}^{mr} = k_{\text{M}}^2/V_{\text{M}}$ . The values of  $m_{\text{OH}}$  at different [ $D_n$ ] and at a constant [HO<sup>-</sup>]<sub>T</sub> were calculated from eqn. (6) at a given value of  $K_{\text{OH}}^{\text{Br}}$  with known values of [HO<sup>-</sup>]<sub>T</sub>, [Br<sup>-</sup>]<sub>T</sub>, and  $\beta$  (= 0.8)<sup>2c</sup> where [Br<sup>-</sup>]<sub>T</sub> = [Br<sup>-</sup><sub>W</sub>] + [Br<sup>-</sup><sub>M</sub>] (= [ $D_n$ ] + CMC),  $\beta$  =  $m_{\text{OH}}$  +  $m_{\text{Br}}$  and  $m_{\text{Br}}$  = [Br<sup>-</sup><sub>M</sub>]/[ $D_n$ ]. These calculated values of  $m_{\text{OH}}$ 

$$m_{\text{OH}}^2 + m_{\text{OH}} \left\{ \frac{[\text{HO}^-]_{\text{T}} + [\text{Br}^-]_{\text{T}} K_{\text{OH}}^{\text{Br}}}{(K_{\text{OH}}^{\text{Br}} - 1)[D_n]} - \beta \right\} - \frac{\beta [\text{HO}^-]_{\text{T}}}{(K_{\text{OH}}^{\text{Br}} - 1)[D_n]} = 0$$
(6)

were subsequently used in eqn. (5) to calculate  $k_{\rm M}^{mr}$ ,  $K_{\rm S}$  and least-squares,  $\Sigma d_i^2$ , values using the nonlinear least-squares technique. Such calculations were carried out at different arbitrarily assigned values of  $K_{\rm OH}^{\rm Br}$  and the calculated values of  $k_{\rm M}^{mr}$ ,  $K_{\rm S}$  and  $\Sigma d_i^2$  are shown in Tables 4 and 5 at a  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH, respectively.

It is evident from Tables 4 and 5 that the values of  $\Sigma d_i^2$  and  $K_{\rm S}$  are almost invariant while the value of  $k_{\rm M}^{mr}$  increases by ~10-fold with increase in  $K_{\rm OH}^{\rm Br}$  from 5 to 100. Thus, it is almost impossible to decide the correct value of  $K_{\rm OH}^{\rm Br}$ . This seems to be a general problem with PIE model. However, the reported values of  $K_{\rm OH}^{\rm Br}$ , and  $\beta$  determined experimentally under conditions not strictly similar to those of reaction kinetics, are 7-31<sup>2a</sup> and 0.8<sup>2c</sup>, respectively. But, the kinetic data are generally fitted with values of  $K_{\rm OH}^{\rm Br}$  in the range 12-20<sup>2c</sup>. The values of  $K_{\rm M}^{mr}$  are almost independent of [NaOH] while the values of  $K_{\rm S}$  decrease by ~40% with increase in [NaOH] from  $1.0 \times 10^{-3}$  M to  $2.0 \times 10^{-3}$  M at a constant value of  $K_{\rm OH}^{\rm Br}$  and  $\beta$ . Nearly 40% decrease in  $K_{\rm S}$  with increase in [NaOH] from  $1.0 \times 10^{-3}$  M to  $2.0 \times 10^{-3}$  M is apparently

**Table 4**. Alkaline hydrolysis  $(1.0 \times 10^{-3} \text{ M NaOH})$  of NBPT at different [CTABr]<sub>T</sub>, calculated from eqn.  $5^a$ 

[CTABr] <sub>T</sub>	$K_{\mathrm{OH}}^{\mathrm{Br}} =$	5	10	20	100
M	$10^3 k_{\rm obs}{}^b$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$
171	$s^{-1}$	$s^{-1}$	$s^{-1}$	$s^{-1}$	$s^{-1}$
$5.0 \times 10^{-4}$	$24.2 \pm 0.2^d$	32.4	32.1	31.8	31.3
$6.0 \times 10^{-4}$	$30.9 \pm 0.5$	38.8	38.5	38.1	37.4
$7.0 \times 10^{-4}$	$36.0 \pm 0.5$	44.2	43.9	43.4	42.8
$8.0\times10^{-4}$	$40.9 \pm 0.9$	48.8	48.5	48.1	47.5
$1.0\times10^{-3}$	$48.2 \pm 1.2$	56.2	56.0	55.7	55.3
$1.5 \times 10^{-3}$	$62.7 \pm 1.4$	68.3	68.3	68.3	68.5
$2.0\times10^{-3}$	$81.9 \pm 2.1$	75.0	75.2	75.5	75.9
$3.0\times10^{-3}$	$92.4 \pm 1.3$	80.9	81.2	81.6	82.4
$5.0 \times 10^{-3}$	$88.2 \pm 1.6$	80.8	81.2	81.6	82.2
$7.0\times10^{-3}$	$77.5 \pm 1.5$	76.3	76.5	76.8	77.1
$1.0\times10^{-2}$	$67.8 \pm 0.9$	68.4	68.5	68.5	68.5
$2.0\times10^{-2}$	$43.0 \pm 0.8$	48.5	48.4	48.2	47.9
$3.0 \times 10^{-2}$	$34.2 \pm 0.7$	37.1	36.9	36.7	36.3
$5.0\times10^{-2}$	$22.7 \pm 0.5$	25.1	24.9	24.7	24.4
$7.0\times10^{-2}$	$16.4 \pm 0.4$	18.9	18.8	18.6	18.3
$1.0\times10^{-1}$	$11.6 \pm 0.3$	13.8	13.7	13.6	13.4
$1.7\times10^{-1}$	$7.40 \pm 0.23$	8.49	8.41	8.31	8.17
$10^4 \Sigma d_i^2 =$		6.480	6.069	5.555	4.761
$k_{\rm M}^{mr}/{\rm s}^{-1}$		$3.21 \pm$	$4.85 \pm$	$8.07 \pm$	$33.6 \pm$
		$0.34^{d}$	$0.48^{d}$	$0.76^{d}$	$2.9^{d}$
$K_{\rm S}/{\rm M}^{-1}=$		$112\pm18^d$	$115 \pm 18^d$	$116 \pm 17^d$	$115 \pm 16^d$

 $^a$ [NBPT] $_0 = 2.0 \times 10^{-4}$  M, [NaOH] =  $1.0 \times 10^{-3}$  M, T = 35 °C,  $\lambda$  = 300 nm, 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture.  $^b$ Calculated from eqn. (1).  $^c$ Calculated from eqns. (5) and (6) with  $\beta$ = 0.8,  $10^4$  CMC = 3.66 M, and  $k_W^2 = 21.6$  M $^{-1}$ s $^{-1}$ .  $^d$ Error limits are standard deviations.

inconceivable in terms of PIE  $model^2$  and reported data.  $^{12}$ 

A Comparative Look at the Kinetic Parameters,  $k_{\rm M}^{mr}$  and  $K_{\rm S}$ , Derived Using BPP Model (Eqn. 3) and PIE Model (Eqn. 5):

- i. The values of  $k_{\rm M}^{mr}$ , obtained from BPP model, are ~2-fold smaller than those obtained from PIE model.
- ii. The values of  $K_S$ , obtained from BPP model, are ~8- to 9-fold larger than those obtained from PIE model.
- iii. The values of  $K_{\rm S}$ , obtained by spectrophotometric technique at  $2.0 \times 10^{-4}$  and  $5.0 \times 10^{-4}$  M NBPT and [NaOH] = 0, are almost similar to  $K_{\rm S}$  values obtained from BPP model at  $2.0 \times 10^{-4}$  M NBPT as well as  $1.0 \times 10^{-3}$  and  $2.0 \times 10^{-3}$  M NaOH.

### Conclusion

Although the values of least-squares,  $\Sigma d_i^2$ , do not differ significantly in the observed data fit to equations derived based upon BPP and PIE models, the calculated kinetic parameters, especially  $K_S$  from BPP model appear to be more reliable compared to those obtained from PIE model because the values of  $K_S$  from BPP model are, within the limits of experimental uncertainties, similar to the corresponding  $K_S$  values determined spectrophotometrically. However, both BPP and PIE models have their own known intrinsic

**Table 5**. Alkaline hydrolysis  $(2.0 \times 10^{-3} \text{ M NaOH})$  of NBPT at different [CTABr]<sub>T</sub>, calculated from eqn.  $(5)^a$ 

[CTAD <sub>m</sub> ]	$K_{\mathrm{OH}}^{\mathrm{Br}} =$	5	10	20	100
[CTABr] <sub>T</sub> M	$10^3 k_{\rm obs}{}^b$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$	$10^3 k_{\text{calcd}}^c$
141	$s^{-1}$	$s^{-1}$	$s^{-1}$	$s^{-1}$	$\mathrm{s}^{-1}$
$6.0 \times 10^{-4}$	$65.5 \pm 0.8$	68.0	68.2	67.9	67.0
$8.0\times10^{-4}$	$75.9 \pm 1.6$	79.9	80.1	79.8	78.9
$1.0\times10^{-3}$	$105 \pm 2$	89.1	89.3	89.1	88.3
$2.0\times10^{-3}$	$125 \pm 3$	115	115	115	116
$4.0\times10^{-3}$	$130 \pm 3$	130	130	130	131
$5.0\times10^{-3}$	$124 \pm 3$	131	131	131	131
$7.0\times10^{-3}$	$117 \pm 3$	128	128	128	128
$2.0\times10^{-2}$	$97.2 \pm 1.5$	92.3	92.3	92.2	92.0
$3.0\times10^{-2}$	$77.6 \pm 1.0$	73.5	73.5	73.6	73.5
$4.0\times10^{-2}$	$57.1 \pm 0.7$	60.8	60.9	60.9	61.0
$5.0\times10^{-2}$	$56.4 \pm 0.5$	51.8	51.9	51.9	52.0
$7.0\times10^{-2}$	$41.7 \pm 0.5$	39.8	39.9	40.0	40.2
$1.0\times10^{-1}$	$29.8 \pm 0.4$	29.6	29.7	29.7	29.9
$1.7\times10^{-1}$	$20.4 \pm 0.5$	18.5	18.5	18.6	18.7
$10^4 \Sigma d_i^2 =$		6.408	6.278	6.313	6.483
$k_{\rm M}^{mr}/{\rm s}^{-1}$		$3.46 \pm$	$5.21 \pm$	$8.64 \pm$	$35.8 \pm$
		$0.25^{d}$	$0.36^{d}$	$0.61^{d}$	$2.6^{d}$
$K_{\rm S}/{\rm M}^{-1}=$		$79 \pm 9^d$	$77 \pm 9^d$	$73\pm 9^d$	$65 \pm 8^d$

<sup>a</sup>[NBPT]<sub>0</sub> = 2.0 × 10<sup>-4</sup> M, [NaOH] = 2.0 × 10<sup>-3</sup> M, T = 35 °C,  $\lambda$  = 300 nm, 2% v/v CH<sub>3</sub>CN in the aqueous reaction mixture. <sup>b</sup>Calculated from eqn. (1). <sup>c</sup>Calculated from eqns. (5) and (6) with  $\beta$  = 0.8, 10<sup>4</sup> cmc = 3.84 M, and  $k_{\rm W}^2$  = 25.25 M<sup>-1</sup>s<sup>-1</sup>. <sup>d</sup>Error limits are standard deviations.

limitations and therefore present conclusion based upon just present single study cannot be considered as a general one.

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