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A New Flow Equation for Thixotropic Systems

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Thixotropy is a time-dependent shear-thinning phenomenon. We derived a new thixotropic formula which is based on the generalized viscosity formula of Ree and Eyring, $f = \sum \frac{X_i}{a_i} \sinh^{-1} (\beta_i \cdot \dot{\gamma})$ (Refer to the text concerning the notation.) The following is postulated: (1) thixotropy occurs when small flow units attached to a large flow unit separate from the latter under stress (2) elastic energy(ω) is stored on the large flow unit during the flow process, and (3) the stored energy contributes to decrease the activation energy for flow. A new thixotropic formula was derived by using these postulations, $f = \frac{X_0 \beta_0}{a_0} \dot{\gamma} + \frac{X_1 \beta_1}{a_1} \dot{\gamma} + \frac{X_2}{a_2} \sinh^{-1} [(\beta_0)_2 \exp(-C_2 \dot{\gamma}^2 / RT) \cdot \dot{\gamma}]$ f is the shear stress, and $\dot{\gamma}$ is the rate of shear. In case of concentrated solutions where the Newtonian flow units have little contribution to the viscosity of the system, the above equation becomes, $f = \frac{X_2}{a_2} \sinh^{-1} [(\beta_0)_2 \exp(-C_2 \dot{\gamma}^2 / RT) \cdot \dot{\gamma}]$ In order to confirm these formulas, we applied to TiO₂(anatase and rutile)-water, printing ink and mayonnaise systems. Good agreements between the experiment and theory were observed.

Introduction

Thixotropy is a time-dependent shear-thinning phenomenon.^{1,2} Since 1923, the gel \rightarrow sol transition of Fe₂O₃ aqueous dispersions³ and many interesting observations on thixotropy have been reported. Thixotropic studies started from inelastic systems, then developed remarkably since they were connected with viscoelastic systems like polymer solutions.

Thixotropic phenomena appear in various fields such as paint, polymer and food industries.⁴ Recently, the thixotropy is found in the fields of biochemistry^{5,6} and materials science.^{7,8} In spite of the various observations, thixotropic data are too fragmentary for systematic studies. The interrelation between structure and mechanical properties of thixotropic systems are relatively little known.⁹ Early attempts to analyze thixotropic behavior were centered on qualitative or empirical concepts obtained from hysteresis-loop measurements.¹⁰

Thixotropy is defined here as the phenomenon having the following characteristics,⁴ (1) it accompanies an isothermal decrease of viscosity with increasing shear rate, (2) a structural change is irreversibly brought about by a mechanical disturbance applied to the system, (3) when the mechanical disturbance is removed, the system recovers its original structure, and (4) the flow curves (shear rate vs. shear stress) of the system show a hysteresis loop,¹¹ when the concentration of the system is reasonably high. These statements are similar to Bauer and Collins' definition.³

There are two main streams in the theoretical interpretations of thixotropic phenomena.¹² One is Goodeave's network theory¹³ and the other is the Ree-Eyring's kinetic theory.⁴ In 1955, by developing Eyring's theory of transport phenomena,¹⁴ the generalized viscosity formula known as the Ree-Eyring equation was derived.¹⁵ In 1957, Hahn *et al.* applied the generalized viscosity formula to the thixotropic hysteresis.¹⁶

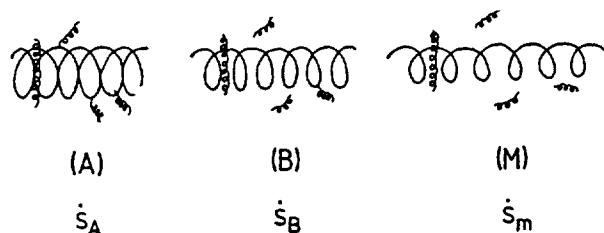


Figure 1. The model of a non-Newtonian unit. (A) The state without stress, (B) the state under stress, (M) the state under higher stress.

Many other investigators developed their own theories with the constitutive equations of inelastic viscous fluids.¹⁷⁻²⁰ Fredrickson²⁰ proposed the inelastic thixotropic model of viscous fluids, which do not exhibit such as viscoelastic phenomena, recoil or stress relaxation. On the other hand, the kinetic theory⁴ has the concept of viscoelasticity which is connected with the strain energy or relaxation time. By developing the kinetic theory further, Park and Ree²¹ proposed an elaborate theory which is successfully applied to bentonite suspensions. In 1971, Utsugi and Ree²² studied the Ostwald curves which is related to thixotropy, and showed that their equation of flow is related with the Einstein equation of flow.²³

In this paper, by introducing the concept of structural change caused by the shear stress into the Ree-Eyring equation of flow, a modified and simple thixotropic equation is derived. This new thixotropic equation is applied to inelastic and viscoelastic systems, then the parameters of the thixotropic equation are investigated.

Theory

1. Model of Thixotropy. We assume that a non-Newtonian unit has a structure as shown by Figure 1A, *i.e.*, it is a tiny spring in which several short springs are attached. The short springs are tightly attached, and they do not detach if no force is applied to the main spring. Figure 1B shows the state when force applied to the main spring; one notices that the latter is elongated and that some short springs are detached. In Figure 1M is shown the state when stronger force is applied to the main spring, as a result, it is more elongated, and more short springs are detached. The short springs represent the flow units 1. As long as the main-spring is under stress field, the detached small springs do not reattach to the main-spring, *i.e.*, the recovery does not occur. The recovery occurs only when the stress is completely removed. The detachment and reattachment is the model of thixotropy.

Hahn, Ree and Eyring⁴ showed that when a molecule is under a stress field which produces strain rate $\dot{\gamma}$, it is deformed and the strain energy $c\dot{\gamma}^2$ (c is constant) is stored in the molecule. In the above mentioned model, the strain energy is proportional to the elongation of the main-springs and to the number of detached small springs.

When no stress is applied to the flow unit (Figure 1A), the activation free-energy for flow ΔG_f^* is very large since the unit accompanies many small springs with it. But, under a stress(flow) field of $\dot{\gamma}_B$, some of small springs are detached from the unit (Figure 1B), the activation free energy becomes $\Delta G_f^* - c\dot{\gamma}_B^2$, *i.e.*, it decrease. When the stress is more increased (Figure 1M), almost all the small springs are removed from the unit, the flow activation-energy decreases to $\Delta G_f^* - c\dot{\gamma}_m^2$ where $\dot{\gamma}_m > \dot{\gamma}_B$.

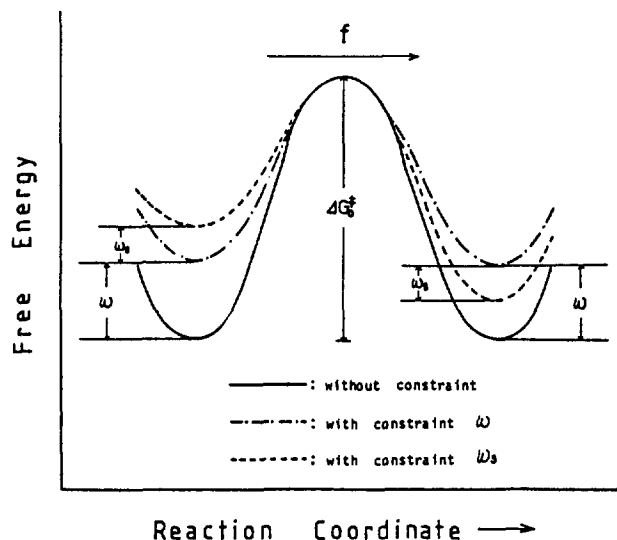


Figure 2. The activation free energy curves for flow. The work ω_s is the constraint causing the flow, and ω is the strain energy stored on the flow unit which helps the detachment of small flow unit, consequently helping the flow.

2. Flow Equation. The activation free-energy diagram for flow of the flow unit is shown in Figure 2, where $\omega = c\dot{\gamma}^2$, $\omega_s = \lambda\lambda_2\lambda_3 f/N/2$, N is Avogadro number, f is the shear stress, and λ , λ_2 , λ_3 are the molecular dimensions introduced by Eyring.¹⁴ From Figure 2, one knows that

$$\Delta G_f^* = \Delta G_b^* - \omega - \omega_s \text{ and } \Delta G_b^* = \Delta G_f^* - \omega + \omega_s$$

where the subscript f and b indicate the direction of jump of the flow unit, *i.e.*, forward and backward, respectively. The rate constants k_f and k_b are represented, respectively,

$$k_f = (kT/h) \cdot \exp[-(\Delta G_f^* - \omega - \omega_s)/RT] \quad (1)$$

$$k_b = (kT/h) \cdot \exp[-(\Delta G_b^* - \omega + \omega_s)/RT] \quad (2)$$

If the net rate forward is represented by $k' (= k_f - k_b)$ the rate of shear $\dot{\gamma}$ is expressed by¹⁴

$$\begin{aligned} \dot{\gamma} &= (\lambda/\lambda_1) \cdot k' \\ &= (\lambda/\lambda_1) \cdot (2kT/h) \cdot \exp[-(\Delta G_f^* - \omega)/RT] \cdot \sinh(\omega_s/RT) \\ &= (\lambda/\lambda_1) \cdot 2k_0 \cdot \exp(\omega/RT) \cdot \sinh(\omega_s/RT) \\ &= 2(\lambda/\lambda_1) \cdot k_0 \cdot \exp(c\dot{\gamma}^2/RT) \cdot \sinh(\lambda\lambda_2\lambda_3 f/2kT) \end{aligned} \quad (3)$$

where k_0 is the rate constant when there is no stress, *i.e.*,

$$k_0 = (kT/h) \cdot \exp(-\Delta G_f^*/RT) \quad (4)$$

Equation (3) is rewritten as,

$$f = (1/\alpha) \sinh^{-1}[\beta_0 \cdot \exp(-c\dot{\gamma}^2/RT) \dot{\gamma}] \quad (5)$$

where

$$\alpha = (\lambda\lambda_2\lambda_3/2kT) \quad (6)$$

and

$$\beta_0 = (2k_0 \lambda/\lambda_1)^{-1} \quad (7)$$

The $1/\alpha$ and β are the physical properties proportional to the shear modulus and relaxation (when there is no stress), respectively. If there are various kinds of flow units in the flow system, we may express f as¹⁵

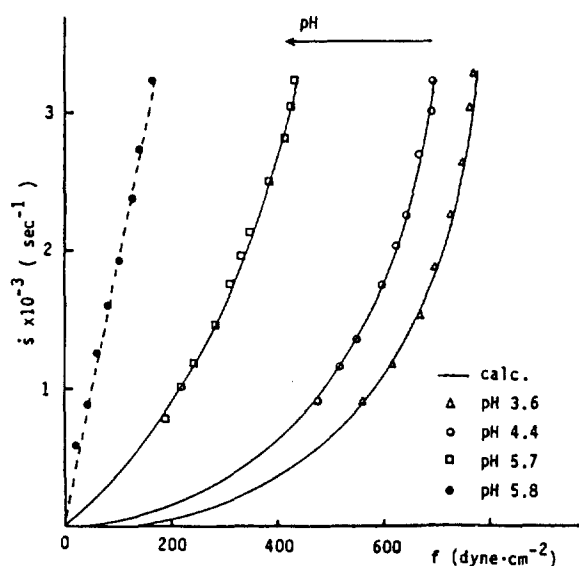


Figure 3. Flow curves of 30wt.% TiO_2 (anatase)-water suspension with various pH at 25°C.

$$f = \sum X_i f_i = \sum \frac{X_i}{\alpha_i} \sinh^{-1} [(\beta_0)_i \cdot \dot{\gamma} \cdot \exp(-c_i \dot{\gamma}^2/RT)] \quad (8)$$

where X_i is the fraction of the area occupied by the i -th kind of flow units. In many cases, Eq.(8) is simplified as

$$f = \frac{X_0 \beta_0}{\alpha_0} \dot{\gamma} + \frac{X_1 \beta_1}{\alpha_1} \dot{\gamma} + \frac{X_2}{\alpha_2} \sinh^{-1} [(\beta_0)_2 \cdot \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}^2/RT)] \quad (9)$$

The subscript 0 and 1 represent the solvent and unit 1 (both being Newtonian), respectively, $c_i = 0$, and $\sinh^{-1} [(\beta_0)_i \dot{\gamma}] = (\beta_0)_i \dot{\gamma}$ where $i = 0$ or 1. When the Newtonian terms in Eq.(9) are negligibly small, it becomes,

$$f = \frac{X_2}{\alpha_2} \sinh^{-1} [(\beta_0)_2 \cdot \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}^2/RT)] \quad (10)$$

Equation (10) is very similar to Bang *et al.*'s equation for dilatancy²⁴ except for the sign in the factor $\exp(-c_2 \dot{\gamma}^2/RT)$ since it becomes $\exp(c_2 \dot{\gamma}^2/RT)$ in Bang *et al.*'s equation.

The flow curves obtained with increasing $\dot{\gamma}$ with time is called the up-curve, Eq.(9) or (10) is applied to the up-curve. The down-curve is the flow curve obtained with the decreasing $\dot{\gamma}$ with time. For the down-curve, the following equation is applied:

$$f = \frac{X_0 \beta_0}{\alpha_0} \dot{\gamma} + \frac{X_1 \beta_1}{\alpha_1} \dot{\gamma} + \frac{X_2}{\alpha_2} \sinh^{-1} [(\beta_0)_2 \cdot \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}_m^2/RT)] \quad (11)$$

where $\dot{\gamma}_m$ is the maximum shear rate (Figure 1M) from which the down-curve starts. The reason is as follows: (1) at the apex, the flow equation is also represented by Eq.(11), and (2) all the parameters in Eq.(11) will not change in the course of the down-curve since no recovery occurs in this process.

By using the above-mentioned model, which is applicable to any case of thixotropy, the results (see the chapter) were obtained, and the related subjects are discussed.

Applications

1. TiO_2 (anatase)-water Suspension. The author's theory is applied to the thixotropic system of TiO_2 (anatase)-water system. Lee *et al.* measured the viscosities of the anatase-

Table 1. Flow Parameters for TiO_2 -Water Suspension, Printing Ink and Mayonnaise Systems

	$X_0 \beta_0 / \alpha_0 + X_1 \beta_1 / \alpha_1$	X_2 / α_2	$(\beta_0)_2$	c_2 / RT
TiO_2(anatase)-water suspension				
pH 3.6		183.0	16.44	4.893×10^{-8}
pH 4.4		181.5	9.547	2.901×10^{-8}
pH 5.7		169.2	2.452	0.650×10^{-8}
TiO_2(rutile)-water suspension				
pH 5.4		62.81	0.745	—
pH 6.3		46.89	1.729	3.547×10^{-9}
pH 7.1		50.14	2.071	5.066×10^{-9}
Printing Ink				
small ($\dot{\gamma}_m = 170 \text{ s}^{-1}$)	2.417	5.928	1.124	2.957×10^{-4}
large ($\dot{\gamma}_m = 1100 \text{ s}^{-1}$)	1.251	7.134	0.536	0.858×10^{-4}
Mayonnaise				
($\dot{\gamma}_m = 1450 \text{ s}^{-1}$) 20°C	1.159	711.9	0.138	3.918×10^{-7}
33°C	1.075	433.7	0.364	4.793×10^{-7}

$X_0 \beta_0 / \alpha_0 + X_1 \beta_1 / \alpha_1$: dyne · sec · cm⁻², X_2 / α_2 : dyne · cm⁻², $(\beta_0)_2$: sec, c_2 / RT : sec².

water suspension by a Couette-type rotational viscometer.²⁵ They reported the dilatancy-thixotropy transition occurs at pH=5.8 which is induced by the electrolytes added to the system. It was also reported that the anatase-water suspension presents a dilatant phenomenon above pH=5.8 and a thixotropy below pH=5.8. The flow curves in Figure 3 are those for the pH effect on the flow properties of TiO_2 (anatase)-water suspension (pH<5.8).

In Figure 3 only the up-curves are presented, because the down-curves are nearly overlapped with the up-curves, *i.e.*, no hysteresis loop. This shows that the recovery to the original structure is very quick. Eq.(10) was applied to the TiO_2 (anatase)-water system, and the parametric values listed in Table 1 were obtained. The theoretical curves were calculated from Eq.(10) by using the parametric values. One notes that the agreement between theory and experiment is very good.

2. TiO_2 (rutile)-water Suspension. The titanium dioxide has three crystal modifications, rutile, anatase and brookite, all of which occur in nature. Their structural difference cause the change of physical properties.

In the case of 30wt.% anatase-water suspension, it has a dilatancy-thixotropy transition at pH=5.8. But for the rutile(TiO_2)-water suspension the dilatancy-thixotropy transition occurs at the two points of pH=5.0 and pH=8.8. Rutile system presents the dilatant phenomena below pH=5.0 and above pH=8.8, and the thixotropy between pH=8.8 and pH=5.0. Figure 4 represents the up-curves of 35wt.% rutile-water suspension at various pH at 25°C. In this case also, no hysteresis loop was observed. The parametric values found by applying Eq.(10) are included in Table 1. As we can see from Figure 4, the calculated thixotropic flow curves and the experiments are also in good agreement.

The TiO_2 suspension is treated as a special case of thixotropy where no hysteresis loop appears. The reason for the disappearance of the hysteresis loop is as follows: the reattachment of the detached units is very quick, *i.e.*, the recovery

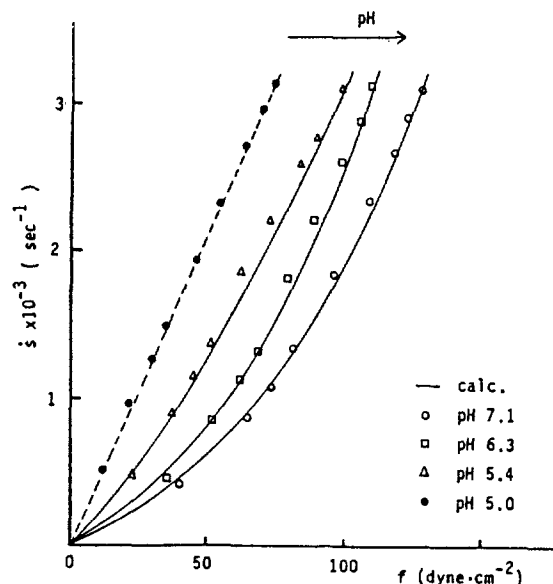


Figure 4. Flow curves of 35wt.% TiO₂(rutile)-water suspension with various pH at 25°C.

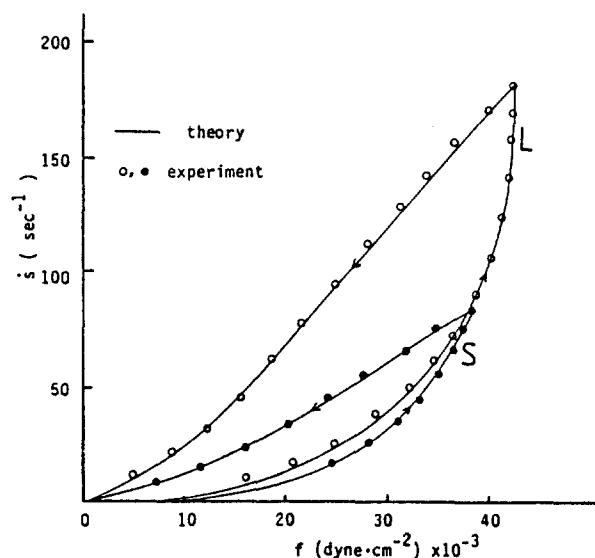


Figure 5. Hysteresis loops of "Second Down Oil Red Printing Ink" at 30°C. Curve L represents a large loop and S indicates a small one.

occurs even in the course of the up-curve process.

3. Printing Ink. Up to now, we only treated the cases without hysteresis loop of the TiO₂-water system. Next, we consider the thixotropic system with hysteresis loops.

Green reported the thixotropic loops of printing ink, which were also analyzed by Hahn *et al.*⁴ The experimental data shown in Figure 5 are those from the reference.²⁶

We applied Eq.(9) and (11) to the up-curves and down-curves in Figure 5, respectively, and obtained the parametric values listed in Table 1. The theoretical curves in Figure 5 are the calculated ones from Eq. (9) and (11) by using the parametric data. The $\dot{\gamma}_m$ values for the large and the small loops are 1100 and 170 sec⁻¹, respectively. We note a good agreement between theory and experiment.

[Note] In the application of Eq.(9) to the up-curve, it is assumed that X_1 is very large, $X_1 + \Delta X_1 \cong X_1$, where ΔX_1 is proportional to the flow units 1 detached from unit 2 in the course

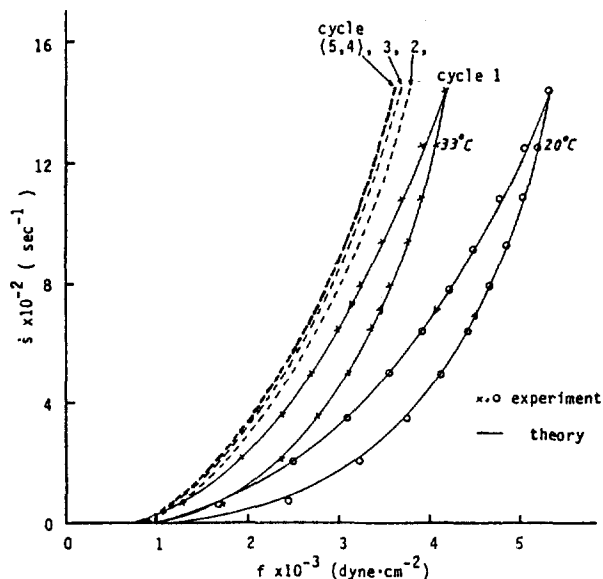


Figure 6. Hysteresis loops of mayonnaise at 20°C and 33°C. The curves 2 to 5 belong to the mayonnaise at 33°C, one notes that the hysteresis loops do not appear.

of the up-curve, and also that α_2 is about constant irrespective of the detachment.

Discussion

1. Hysteresis Loop (Energy Loss). The thixotropic loops in Figure 6 are those for the mayonnaise(Real Ribbon Mayonnaise, Knorr Korea LTD) at 20°C and 33°C. The loops were obtained by using a Couette-type rotational viscometer constructed in this laboratory. By applying Eq.(9) and (11), we obtained the parametric values in Table 1.

The character of the loops is following (1) the hysteresis loop shifts to the lower stress region at higher temperature, (2) the size of the higher temperature loop is smaller than that of the lower temperature loop, and (3) the size of the thixotropic loops decreases with repeated cycling, eventually reaching a line curve. See Figure 6. This is due to the complete detachment of the small units from the unit 2 by the repeated cycling.

The area of the thixotropic loops represent the energy loss during cyclic deformation. The area, built up by the up- and down-curves, is given by the double integral²⁷

$$\text{Area} = \int_0^{\dot{\gamma}_m} \int_{f_d(\dot{\gamma})}^{f_u(\dot{\gamma})} df \cdot d\dot{\gamma} \quad (12)$$

Here, the first integral of $d\dot{\gamma}$ indicates the difference between the up-curve function $f_u(\dot{\gamma})$ [Eq.(9)] and the down-curve function $f_d(\dot{\gamma})$ [Eq.(11)]. Thus, Eq.(12) becomes, as,

$$\text{Area} = \int_0^{\dot{\gamma}_m} [\sinh^{-1} \{ (\beta_0)_2 \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}^2/RT) \} - \sinh^{-1} \{ (\beta_0)_2 \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}_m^2/RT) \}] d\dot{\gamma} \quad (12a)$$

In order to simplify the integration, we use the approximation

$$\sinh^{-1} x \cong \ln(2x) \quad (x \ll 1)$$

i.e., $X = (\beta_0)_2 \dot{\gamma} \cdot \exp(-c_2 \dot{\gamma}^2/RT) \gg 1$ which is experimentally satisfied in practice. Then Eq.(12a) is simplified as follows:

Table 2. Energy Losses($\text{erg} \cdot \text{cm}^{-3} \cdot \text{sec}^{-1}$) in Cyclic Processes of the Mayonnaise System

Temperature (°C)	Energy loss calculated from Eq.(13)	Energy loss measured from the hysteresis loop
20	5.639×10^5	5.955×10^5
33	4.203×10^5	4.591×10^5

$$\text{Area} = \frac{X_2}{\alpha_2} \int_0^{\dot{s}_m} \left(-\frac{c_2 \dot{s}^2}{RT} + \frac{c_2 \dot{s}_m^2}{RT} \right) d\dot{s}$$

$$= 2/3 (X_2/\alpha_2) \cdot (c_2/RT) \cdot \dot{s}_m^2 \quad (13)$$

The area represented the energy loss per unit time and per unit volume ($\text{erg} \cdot \text{cm}^{-3} \cdot \text{sec}^{-1}$). Applying Eq.(13) to the mayonnaise system and by using the parametric values in Table 1, we calculated the area of hysteresis loop, results are shown in Table 2. By using a compensating planimeter, the area was directly measured, and the results are also shown in Table 2. One notes the agreement between the two results is very good.

2. Relaxation Time. In our equation, the parameters are determined by using the approximation $\sinh^{-1} x \cong \ln(2x)$ ($x \gg 1$). This relation is applied to Eq.(10) and one obtains the following equation.

$$f = \frac{X_2}{\alpha_2} \ln[2(\beta_0)_2 \exp(-c_2 \dot{s}^2/RT) \cdot \dot{s}]$$

$$= \frac{X_2}{\alpha_2} [\ln(\beta_0)_2 + \ln(2\dot{s}) - c_2 \dot{s}^2/RT] \quad (14)$$

By apply Eq.(14) to an experimental flow curve of TiO_2 suspensions, the unknown parameters X_2/α_2 , $(\beta_0)_2$, and c_2/RT are obtained. In the cases with hysteresis loops, the parameters are obtained by the following procedures:

(1) by applying Eq.(11) to the down-curve, the parameters $X_0\beta_0/\alpha_0 + X_1\beta_1/\alpha_1$, X_2/α_2 and $(\beta_0)_2 \cdot \exp(-c_2 \dot{s}_m^2/RT) \equiv Z$ are obtained by using the approximation and solving the simultaneous equations; (2) by applying Eq.(9) to the up-curve, the c_2/RT parameter is calculated; and (3) by multiplying $\exp(c_2 \dot{s}_m^2/RT)$ value to Z , we obtain $(\beta_0)_2$.

Eu²⁸ obtained the same form of the Ree-Eyring equation in his paper "shear rate dependence of non-Newtonian viscosity of fluids." He derived this equation from the Boltzmann equation and its dense fluid generalization under some reasonable approximations. In his paper, the relaxation time, τ_e , is unambiguously given in terms of Newtonian viscosity η_0 , temperature T , density n (numbers/volume), molecular diameter d and the reduced mass m_r , i.e.,

$$\tau_e = 2^{1/2} [\eta_0 (2m_r kT)^{1/2}]^{1/2} / nkTd \quad (15)$$

Therefore, if one knows the Newtonian viscosity η_0 and molecular data, one can theoretically calculate the relaxation time τ_e from this relation. Our $(\beta_0)_2$ is the relaxation time for the flow units when there is no constraint. So, it is reasonable to think that $(\beta_0)_2$ is the characteristic property of the system corresponding to τ_e .

In order to compare the τ_e from Eq.(15) with the Ree-Eyring formula $(\beta_0)_2$, molecular diameter d is changed into particle's diameter, m , and n are changed into the mass of a par-

Table 3. Relaxation times $(\beta_0)_2$ of the TiO_2 -Water System from Eq.(10) and Those (τ_e) Calculated from Eu's Theory [Eq.(15)]

TiO_2 Types	pH	$\eta_0^{(N)}$ ($\text{N} \cdot \text{sec}/\text{m}^2$) from Eq.(9)	$(\beta_0)_2 \times 10^3$ (sec)	$\tau_e \times 10^3$ (sec)
Anatase				
$d = 0.3 \mu^a$	3.6	1.04×10^{-2}	16.4	12.2
$m_r = 5.18 \times 10^{-17} \text{kg}^b$	4.4	3.97×10^{-3}	9.55	7.56
$n = 7.72 \times 10^{18}/\text{m}^3^c$	5.7	2.48×10^{-3}	2.45	5.98
Rutile				
$d = 0.2 \mu^a$	5.4	3.84×10^{-4}	0.75	0.74
$m_r = 1.70 \times 10^{-17} \text{kg}^b$	6.3	6.51×10^{-4}	1.73	0.95
$n = 2.82 \times 10^{19}/\text{m}^3^c$	7.1	8.26×10^{-4}	2.07	1.08

^aThe particle size in our system was $\sim \mu$. ^bThe density of the TiO_2 (anatase) = $3.84 \times 10^3 \text{ kg}/\text{m}^3$. The density of the TiO_2 (rutile) = $4.26 \times 10^3 \text{ kg}/\text{m}^3$. From the densities, the m_r values were estimated. ^cThe anatase: 45g in 115 cm^3 of 30wt.% suspension, the rutile: 55g in 115 cm^3 of 35wt.% suspension. From these data, the n values were estimated.

ticle and the number of particles per unit volume, respectively. And the Newtonian viscosity η_0 in Eq.(15) was substituted by the term $\eta^{(N)} = X_0\beta_0/\alpha_0 + X_1\beta_1/\alpha_1$ which is obtained from Eq.(9), since Eu's η_0 is the rare gases viscosity which cannot be used in the comparison. The term $\eta^{(N)}$ in Eq.(9) was neglected compared to the non-Newtonian term in the calculation of the TiO_2 curve. However the size of $\eta^{(N)}$ is calculable, thus the calculated $\eta^{(N)}$ was used in the comparison. The comparison of the relaxation times are shown in Tale 3, where a good agreement between $(\beta_0)_2$ and τ_e is noted.

3. Reconsideration of the Model of Flow Unit 2. Here we consider why the model presented in Figure 1 can express the thixotropic systems. In the TiO_2 -suspension systems, the TiO_2 fine-particles are connected with each other, and make a tiny cluster having some inelasticity. The main spring in Figure 1 corresponds to this TiO_2 -cluster in the suspension, and the micro TiO_2 -fragments correspond to the small springs in Figure 1 acting as flow unit 1.

Printing ink is a system of pigments(organic or inorganic) suspended in vehicles(oils). The pigments behave just like the TiO_2 in the abovementioned suspension. In this case, however, the reattachment of the detached micro-groups to the cluster is not fast, thus hysteresis loop appears.

Mayonnaise is an emulsion system, vegetable oils emulsified by egg yolk. The protein molecule acts as a chain(unit 2) to which oil droplets(unit 1) attach. The oil droplets can be detached completely by repeated cycling. Thus, hysteresis loop becomes smaller with repeated cycling, eventually it disappears.

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Test of a Multi-Reference Many-Body Perturbation Theory for the Description of Electron Correlations in four Valence Electron States of Transition Metal Atoms

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A multi-reference many-body perturbation theory (MRMBPT) method is critically tested in second order by comparing with the corresponding configuration interaction (CI) calculations. Excitation energies of the four-valence-electron states of transition metal atoms and ions are used for the comparison. The agreement between the second order MRMBPT and CI calculations is very reasonable, confirming the reliability of the second order MRMBPT method. The reliability of calculations with the present second order MRMBPT method was only been inferred empirically in the past since most results have been gauged by the agreement with experiment and/or with other MRMBPT calculations based upon different sets of orbitals and configuration spaces. The present MRMBPT method appears to be an efficient ab initio multi-reference method for the calculation of electron correlation effects in atoms and molecules, and it is shown how MRMBPT can be used to estimate core-core and core-valence correlation effects which are often omitted in CI calculations because too many configurations and correlating electrons are involved.

Introduction

Many-body perturbation theory (MBPT) is one of the com-

mon techniques for the study of electron correlation, an effect which is important for the accurate description of the electronic structure of atoms and molecules. The conventional